

Fundamentals of Transport Processes:

Why? What? How

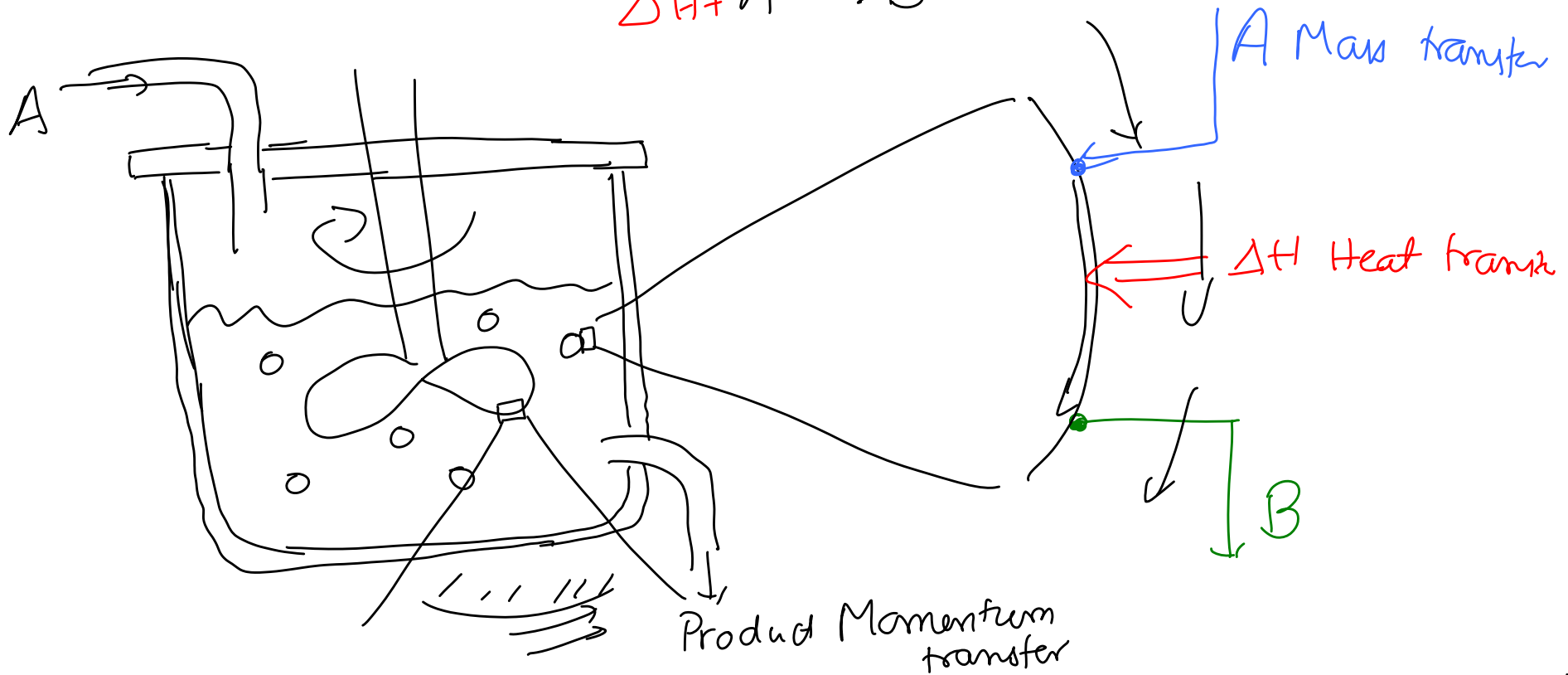
Raw Materials $\xrightarrow[\text{Economical}]{\text{Reliable}}$ Useful products

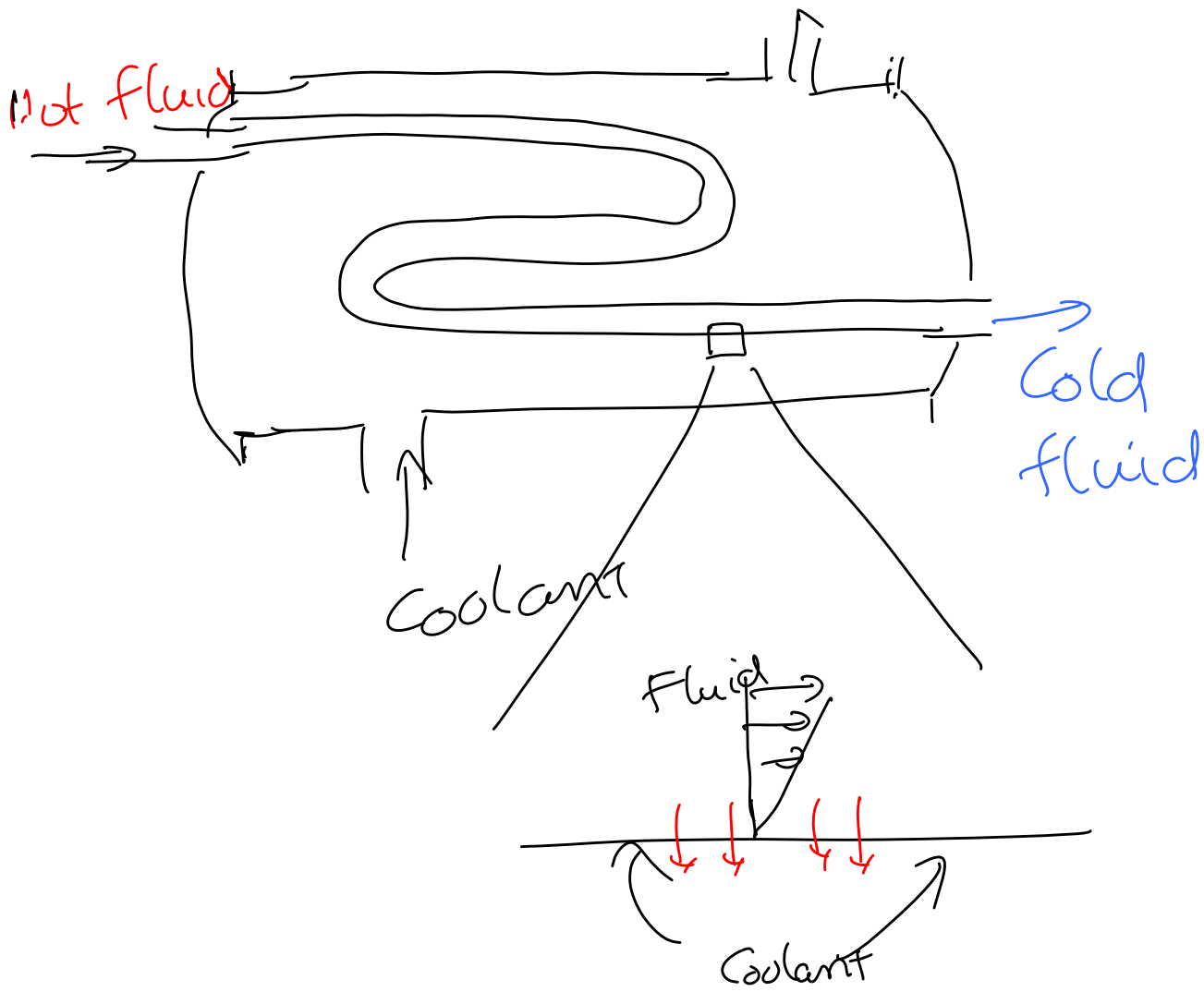
Chemical Reactions

Physical Transformations: Heating, cooling,
melting, evaporation, mixing,
separations, etc.

Fluid systems:

Two-phase continuous stirred tank reactor;

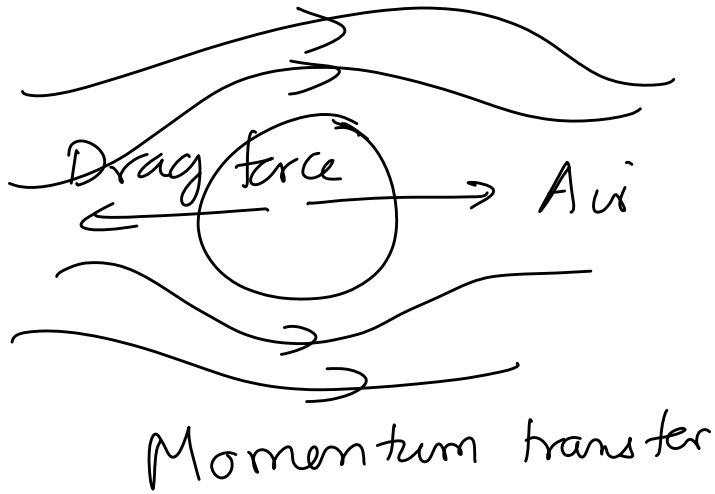




Momentum transfer
 rate / Area = Stress

.
 :

Spray dryer:



What??

Flux = Amount transferred per unit area per unit time

Mass flux j = Mass transferred per unit area per unit time.

Heat flux q = Heat transferred per unit area per unit time

Momentum flux τ = Momentum transferred per unit area per unit time.

= Stress

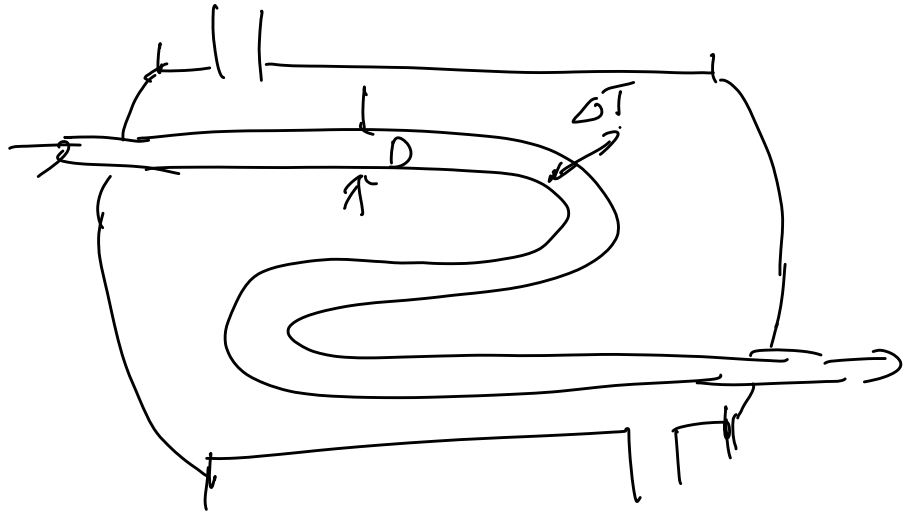
Driving forces

- Mass - Concentration difference
- Heat - Temperature difference
- Momentum - Velocity difference

Unit operations: \Rightarrow Entire equipment

Correlations involving dimensionless variables

Dimensionless heat flux $Nu = \frac{qD}{k\Delta T}$

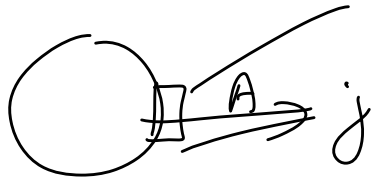


$$Nu = 1.86 Re^{1/3} Pr^{1/3} (L/D)^{1/3} (\mu/\mu_w)^{0.14}$$

for $Re < 20,000$ laminar flow

$$Re = \left(\frac{8UD}{\mu} \right) \quad Pr = \left(\frac{C_p M}{k} \right)$$

$$Nu = 0.023 Re^{0.8} Pr^{1/3} (\mu/\mu_w)^{0.8}$$



$$Sh = \frac{j D}{D_{AB} \Delta C}$$

\bar{j} = Flux

D = diameter

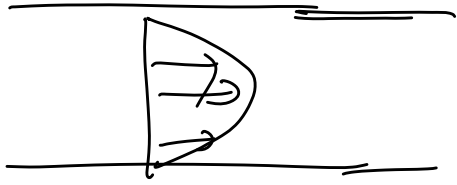
D_{AB} = Diffusion coefficient

ΔC = Average concentration diff.

Sh = function (Re , Sc , dimensionless groups)

$$Sc = \left(\frac{\mu}{\rho D_{AB}} \right)$$

Maximum turn transfer:



$$\text{friction factor } f = \frac{\tau}{(\rho V^2 / 2)}$$

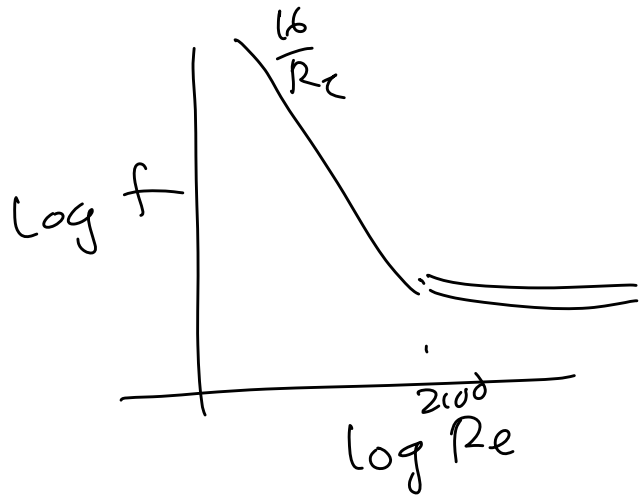
$$f = \text{Function}(Re)$$

Low Reynolds number $Re < 2100$

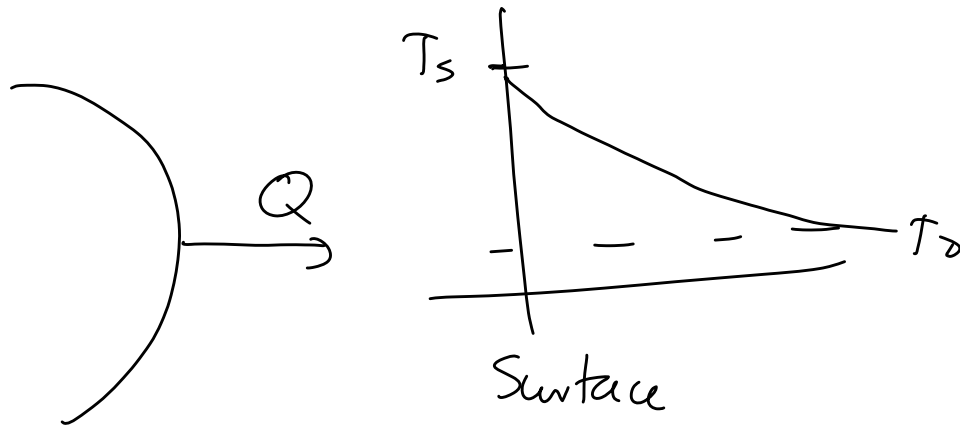
$$f = 16 / Re$$

High Reynolds number $Re > 2100$

$$f = \text{Function}(Re)$$



Relations at the local (microscopic) level



Governing equations - Partial differential equation
Use physical insight to solve these equations in
specific situations - Approximate, analytical

Convection

Transport due to
mean fluid motion

Diffusion

Transport due to the
fluctuating motion of
the molecules

How??

Dimensional Analysis

Height = 1.80 m

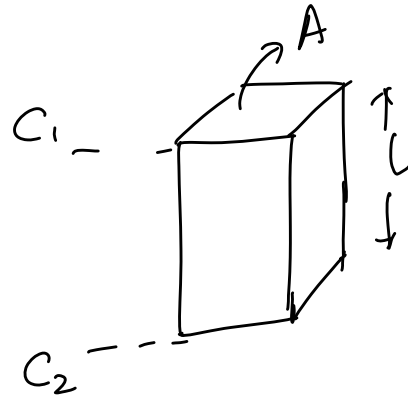
Time of a lecture = 1 hour

Fundamental units:

- Mass (M) (kg, gm, ...)
- Length (L) (m, cm, ...)
- Time (T) (hr, sec, min, ...)
- Temperature (Θ) ($^{\circ}\text{C}$, F, K, ...)
- Ampere (A)
- Candela

Velocity	LT^{-1}
Acceleration	LT^{-2}
Force	MLT^{-2}
Work	ML^2T^{-2}
Energy	ML^2T^{-2}
Power	ML^2T^{-3}
Pressure	$ML^{-1}T^{-2}$
Stress	$ML^{-1}T^{-2}$
Viscosity	$ML^{-1}T^{-1}$
Mass flux	$ML^{-2}T^{-1}$
Diffusion coefficient	L^2T^{-1}

Mass diffusion coefficient
Fick's law



$$j = D \frac{\Delta c}{L}$$

$$ML^{-2}T^{-1} = \frac{[D](ML^{-3})}{L}$$

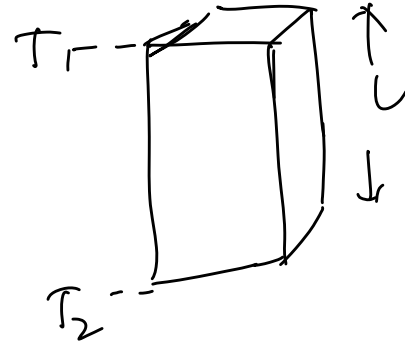
$$[D] = L^2T^{-1}$$

Heat flux q MT^{-3}

Specific Heat C_p $L^2T^{-2}\Theta^{-1}$

Thermal conductivity k $MLT^{-3}\Theta^{-1}$

Fourier's law:



$$q = -k \frac{\Delta T}{L}$$

$$MT^{-3} = \frac{[k]\Theta}{L}$$

$$[k] = MLT^{-3}\Theta^{-1}$$

Buckingham Pi Theorem:

n dimensional quantities, m dimensions, $(n-m)$ dimensionless groups.

Sphere settling in a fluid:

Drag force $F_D(U, R, \mu, \rho, L)$



F_D

$M L T^{-2}$

Quantities = 6

U

$L T^{-1}$

Dimensions = 3

R

L

Dimensionless groups = 3

L

L

Π_1, Π_2, Π_3

μ

$M L^{-1} T^{-1}$

$\Pi_3 = (R/L)$

ρ

$M L^{-3}$

$$\left(\frac{F}{\mu R U}\right) = \text{Function}\left(\frac{S U R}{\mu}, \frac{R}{L}\right)$$

$$F = \mu R U \text{ Function}\left(\frac{S U R}{\mu}\right)$$

Limit $Re \ll 1$,

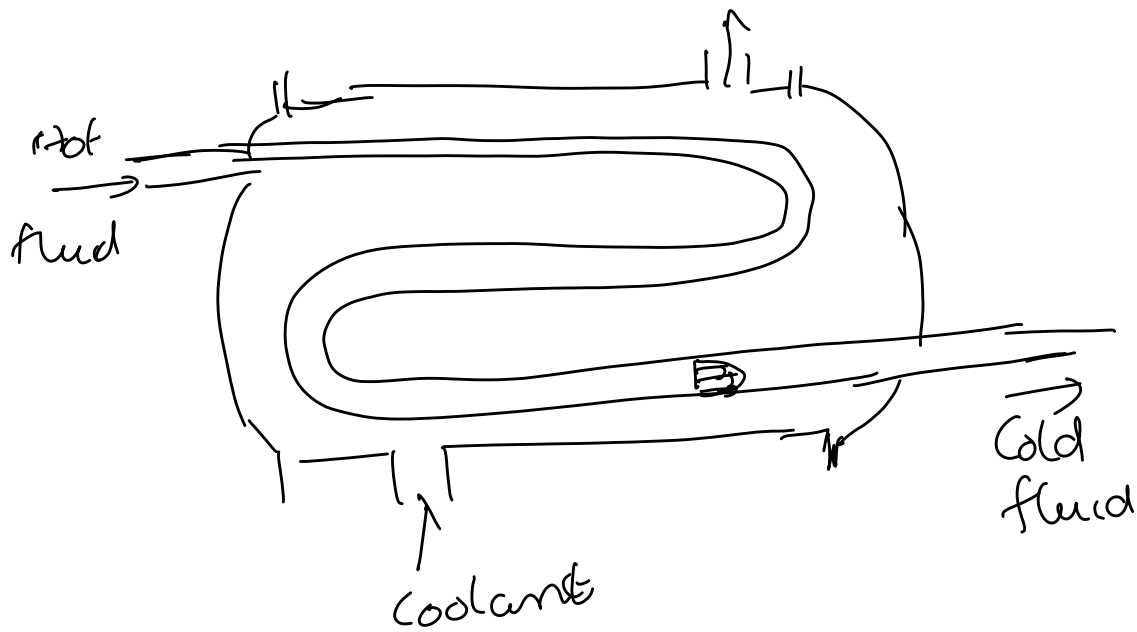
$$F_D = \frac{6\pi}{6\pi} \mu R U \} \text{Stokes law}$$

$$Re \gg 1 \quad \left(\frac{F}{S U^2 R^2}\right) = \text{constant}$$

$$\Pi_1 = \frac{F}{\mu R U}$$

$$\Pi_2 = \left(\frac{S U R}{\mu}\right)$$

$$\Pi_3 = \left(\frac{R}{L}\right)$$



$$q = \frac{\text{Heat transferred}}{\text{Area} \times \text{Time}}$$

$$q = \text{Heat flux} \quad \text{H} \text{L}^{-2} \text{T}^{-1}$$

$$C_p = \text{Specific heat} \quad \text{H} \text{M}^{-1} \text{Θ}^{-1}$$

$$k = \text{Thermal conductivity} \quad \text{H} \text{L}^{-1} \text{T}^{-1} \text{Θ}^{-1}$$

$$\Delta T = \text{Temperature difference} \quad \text{Θ}$$

$$\left(\frac{qD}{k\Delta T} \right) = F \left(\frac{\rho U D}{\mu}, \frac{C_p \mu}{k}, \frac{D}{L} \right)$$

$$\text{Nusselt number} = \left(\frac{qD}{k\Delta T} \right)$$

$$\text{Reynolds number} = \left(\frac{\rho U D}{\mu} \right)$$

$$\text{Prandtl number} = \left(\frac{C_p \mu}{k} \right)$$

$$D = \text{Tube diameter} \quad \text{L}$$

$$\rho = \text{Density of fluid} \quad \text{M} \text{L}^{-3}$$

$$\mu = \text{Viscosity of fluid} \quad \text{M} \text{L}^{-1} \text{T}^{-1}$$

$$U = \text{Fluid velocity} \quad \text{L} \text{T}^{-1}$$

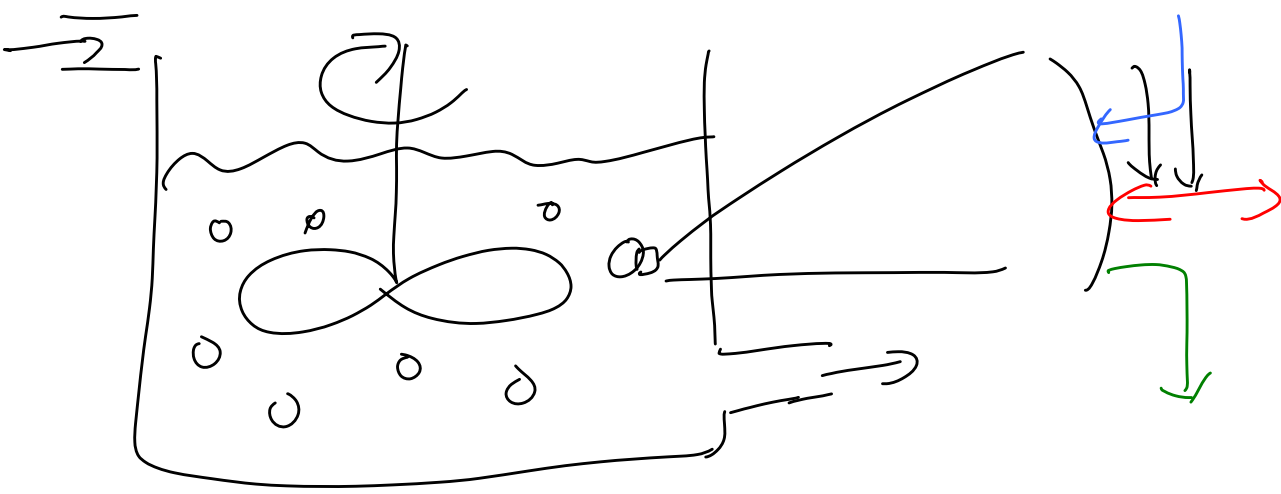
$$L = \text{Length of pipe} \quad \text{L}$$

Laminar flow $Re < 2100$

$$Nu = 1.86 Re^{1/3} Pr^{1/3} (D/L)^{1/3} (\mu/\mu_w)^{0.14}$$

Turbulent flow $Re > 20,000$

$$Nu = 0.023 Re^{0.8} Pr^{1/3} (\mu/\mu_w)^{0.14}$$



$$j = ML^{-2}T^{-1}$$

$$\Delta C = ML^{-3}$$

$$D = L^2T^{-1}$$

$$D = L$$

$$U = LT^{-1}$$

$$\mu = ML^{-1}T^{-1}$$

$$\textcircled{1} Re = \left(\frac{8UD}{\mu} \right)$$

$$\textcircled{2} \frac{jD}{D\Delta C} = \text{Sherwood number}$$

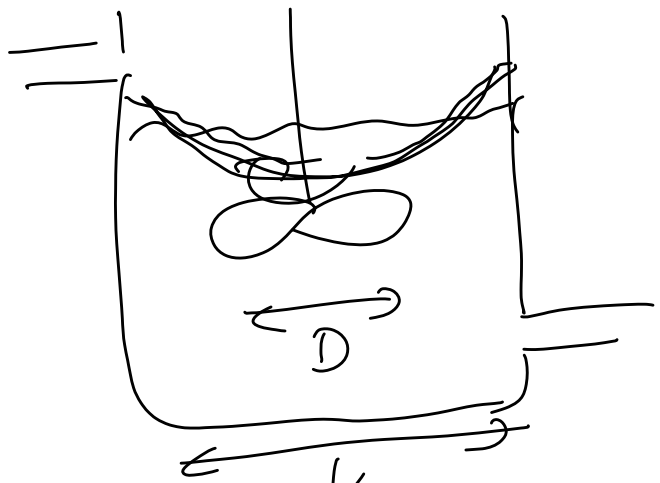
$$\textcircled{3} \frac{\mu}{8D} = \frac{\nu}{D} = \text{Schmidt number}$$

$Sh = 2 + 0.6 Re^{1/2} Sc^{1/3}$ Low Schmidt numbers & Reynolds number

$Sh = 1.24 Re^{1/3} Sc^{1/3}$ High Sc, laminar flow

NTU

Pr



Power $P = ML^2T^{-3}$

$$\Pi_5 = (L/D)$$

$$\Pi_1 = \frac{P}{\rho D^5 f^3} \quad \text{Power number}$$

$$\Pi_2 = \frac{\rho D^2 f}{\mu} = \text{Reynolds number}$$

$$\Pi_3 = \frac{UD}{g} = \text{Froude number}$$

$$\Pi_4 = \frac{\rho D^3 f^2}{\gamma} = \text{Weber number}$$

$$P = ML^2T^{-3}$$

$$f = T^{-1}$$

$$D = L$$

$$\rho = ML^{-3}$$

$$\mu = ML^{-1}T^{-1}$$

$$L = L$$

$$g = LT^{-2}$$

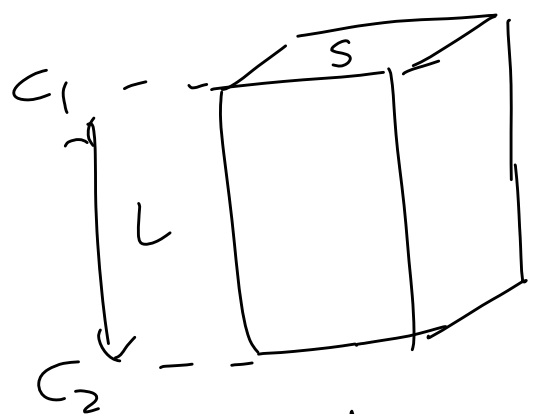
$$\gamma = MT^{-2}$$

$$P_0 = f_n(\text{Re}, \text{Fr}, \text{We}, L/D)$$

Physical meaning of dimensionless numbers:

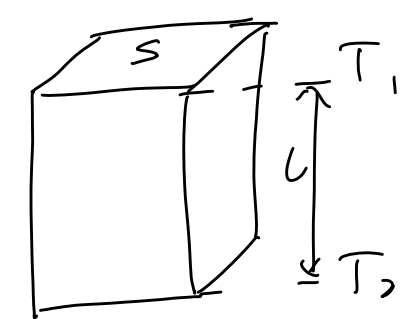
Flux of quantity per unit area per unit time = Diffusion coefficient \times $\frac{\text{Change in density of quantity}}{\text{Unit length}}$

$$D = L^2 T^{-1}$$



$$j = D \frac{\Delta C}{L}$$

Fick's law of diffusion



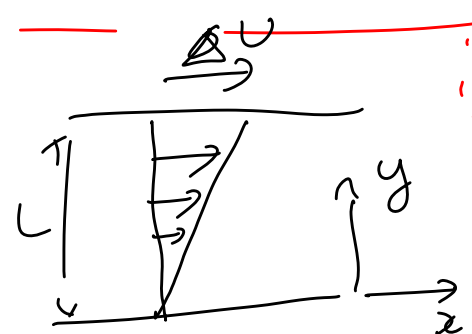
$$q = k \frac{\Delta T}{L}$$

Fourier's Law

$$= \left(\frac{k}{\rho C_p} \right) \frac{\Delta(\rho C_p T)}{L}$$

$$= \alpha \frac{\Delta(\rho C_p T)}{L}$$

α = Thermal diffusivity



$$\tau_{xy} = \frac{\mu \Delta U}{L}$$

$$= \frac{\mu}{\rho} \frac{\Delta(\rho U)}{L}$$

$$= \nu \frac{\Delta(\rho U)}{L}$$

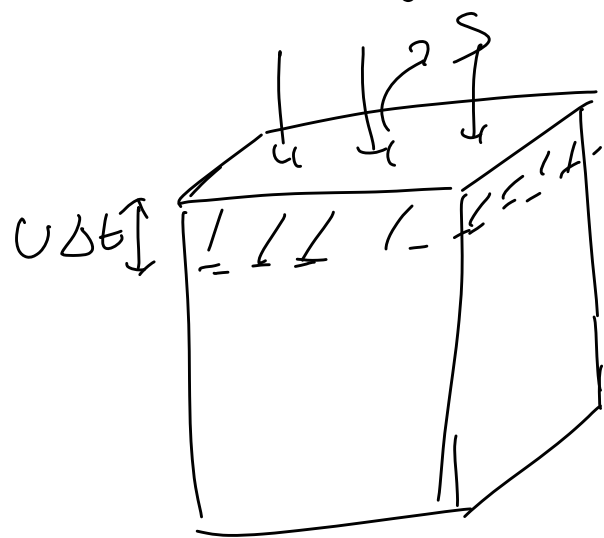
$$\frac{\mu = ML^{-1}T^{-1}}{\rho = ML^{-3}} = L^2 T^{-1}$$

$$\text{MASS DIFFUSIVITY} = D = L^2 T^{-1}$$

$$\text{THERMAL DIFFUSIVITY} = \alpha = \frac{k}{\rho C_p} = L^2 T^{-1}$$

$$\text{MOMENTUM DIFFUSIVITY} = \nu = \frac{\mu}{\rho} = L^2 T^{-1}$$

Convection U



$t, t + \Delta t$

$$\text{Volume } m = S \times U \times \Delta t$$

$$\text{Mass } \bar{m} = C \times S \times U \times \Delta t$$

$$\text{Mass in / unit time} = C \times U \times S$$

$$\text{Flux} = \text{Mass in / unit area / time} = C \times U$$

$$= \text{Density of quantity} \times \text{velocity}$$

Mass transfer:

$$Sc = \left(\frac{\mu}{\rho D} \right) = \left(\frac{\nu}{D} \right) = \frac{\text{Momentum diffusion}}{\text{Mass diffusion}}$$

$$Pr = \left(\frac{c_p \mu}{k} \right) = \left(\frac{\mu}{\rho} \right) \left(\frac{\rho c_p}{k} \right) = \left(\frac{\nu}{\alpha} \right) = \frac{\text{Momentum diffusion}}{\text{Thermal diffusion}}$$

$$Re = \left(\frac{\rho U D}{\mu} \right) = \left(\frac{U D}{\nu} \right) = \frac{\text{Convection}}{\text{Momentum diffusion}}$$

$$Pe = \frac{U D}{D} = Re \times Sc = \frac{\text{Convection}}{\text{Mass diffusion}}$$

$$Pe = \frac{U D}{\alpha} = Re \times Pr = \frac{\text{Convection}}{\text{Thermal diffusion}}$$

Dimensionless numbers involving surface tension

$$\text{Capillary number} = \frac{\mu U}{\gamma} = \frac{\text{Ratio of viscosity}}{\text{Surface tension}}$$

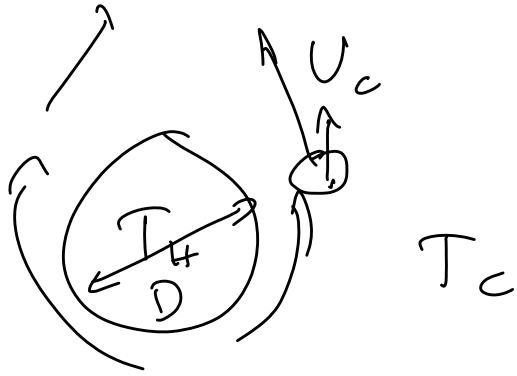
$$\text{Weber number} = \frac{\rho U^2 D}{\gamma} = \frac{\text{Ratio of inertia}}{\text{Surface tension}}$$

Dimensionless groups involving gravity:

$$\begin{aligned} Fr &= \frac{U^2}{gD} \\ &= \frac{\text{Inertia}}{\text{gravity}} \end{aligned}$$

$$\text{Bond number} = \frac{\rho g L^2}{\gamma} = \frac{\text{gravity}}{\text{surface tension}}$$

Natural convection:



$$Gr = \frac{\rho U_c D}{\mu}$$

$$= \left(\frac{\rho D}{\mu} \right) \left(\frac{f D^2}{\mu} \right)$$

$$f = \Delta \rho g$$
$$= \rho \beta \Delta T g$$

$$= \left(\frac{\rho D}{\mu} \right) \left(\frac{D^2}{\mu} \right) (\rho \beta \Delta T g)$$

$$U_c = \left(\frac{f D^2}{\mu} \right)$$

$$= \frac{\rho^2 D^3 \beta g \Delta T}{\mu^2}$$

$$Ra = \frac{U_c D}{\alpha} = \frac{U_c D}{k / (\rho C_p)}$$

$$= \frac{\rho C_p D}{k} \left(\frac{D^2}{\mu} \right) (\rho \beta \Delta T g)$$

$$= \frac{\rho^2 C_p D^3 \beta \Delta T g}{\mu k}$$

Non-dimensional fluxes:

$$Nu = \frac{q_c D}{k \Delta T} \quad Sh = \frac{j D}{D \Delta T}$$

Flow through pipes & channels:

Laminar

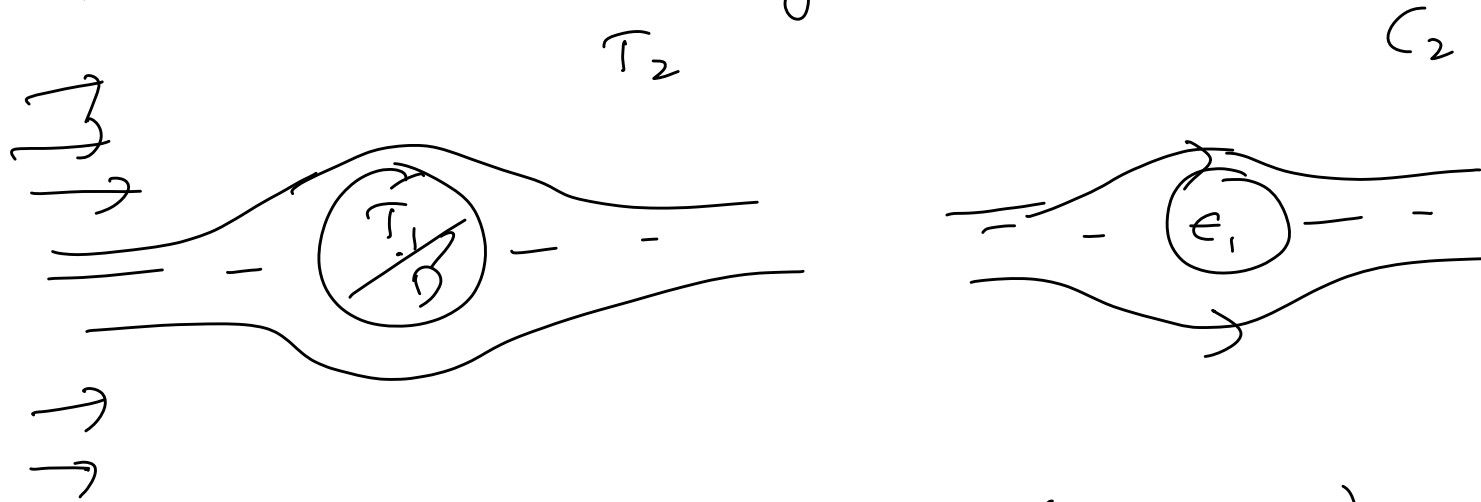
$$Nu = 1.86 Re^{1/3} Pr^{1/3} (D/L)^{1/3} (\mu/\mu_w)^{0.14}$$
$$= 1.86 Pe^{1/3} (D/L)^{1/3} (\mu/\mu_w)^{0.14}$$
$$Sh = 1.86 Re^{1/3} Sc^{1/3} (D/L)^{1/3}$$

Turbulent

Sieder-Tate relation

$$Nu = 0.023 Re^{0.8} Pr^{1/3} (\mu/\mu_w)^{0.14}$$
$$Sh = 0.023 Re^{0.8} Sc^{1/3} (\mu/\mu_w)^{0.14}$$

Flow around objects:



High Peclet number (laminar)

$$Nu = 1.24 \left(Re^{1/3} Pr^{1/3} \right)$$
$$= 1.24 Pe^{1/3}$$

$$Sh = 1.24 \left(Re^{1/3} Sc^{1/3} \right)$$

Natural convection:

$$Nu = 2 + 0.59 (Gr Pr)^{1/4}$$

very low $Gr Pr < 10^4$

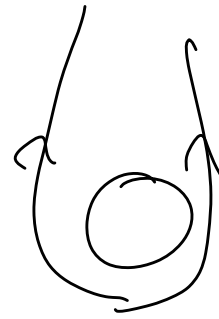
For $Gr Pr$ between 10^4 & 10^9

$$Nu = 0.518 (Gr Pr)^{1/4}$$

Limit $Pr \ll 1$

Limit $Pr \gg 1$

$$Nu \propto Pr^{1/2} Gr^{1/4}$$



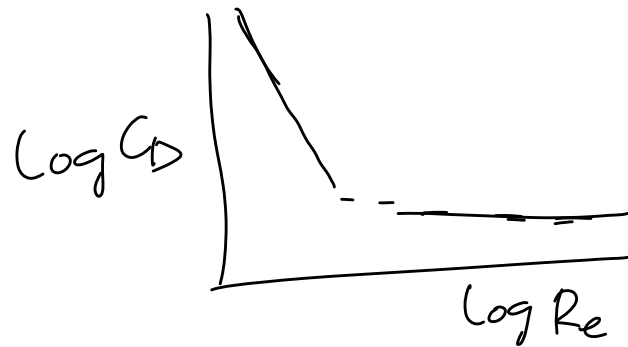
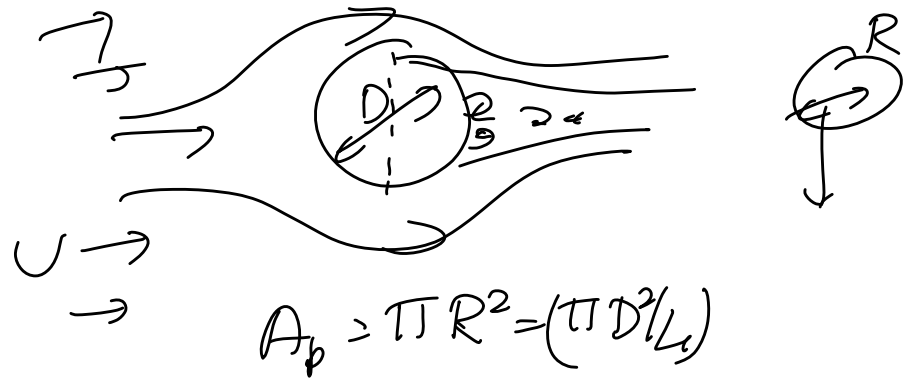
Flow around object

$$C_D = \frac{(F_D/A_p)}{\frac{1}{2}\rho U^2}$$

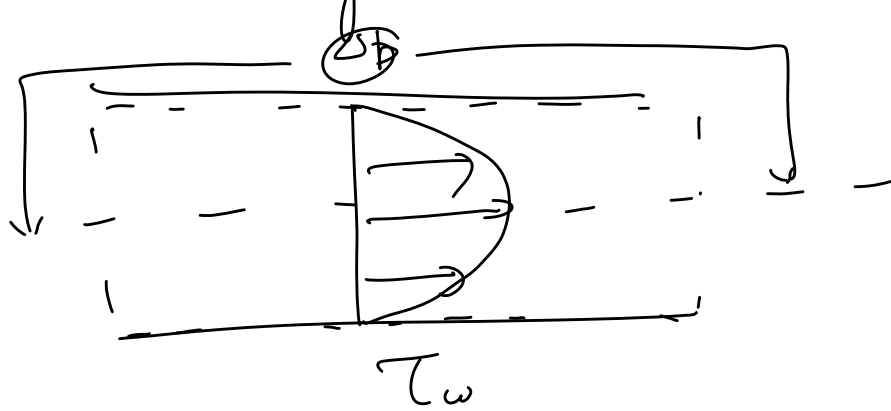
$$F_D = 6\pi\mu R U \text{ Stokes drag law}$$
$$= 3\pi\mu D U$$

$$F_D/A_p = \frac{3\pi\mu D U}{\pi D^2/L_c} = \frac{12\mu U}{D}$$

$$C_D = \frac{12\mu U}{D(\frac{1}{2}\rho U^2)} = \frac{24\mu}{\rho U D} = \frac{24}{Re}$$



Flow through tubes:



$$Re = \frac{\rho U D}{\mu}$$

$Re < 2100 \Rightarrow$ laminar flow

$$f = \frac{\tau_w}{\frac{1}{2} \rho U^2} = \text{Friction factor}$$

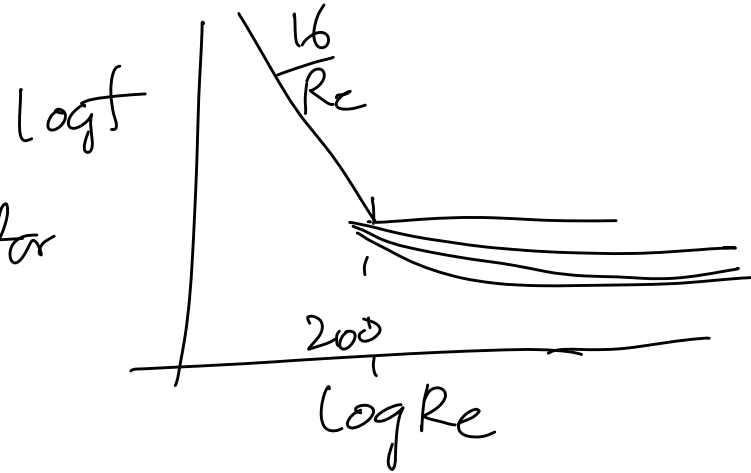
$$(\tau_w 2\pi R L) = \Delta p \pi R^2$$

$$\frac{\Delta p}{L} = \frac{2\tau_w}{R} = \frac{4\tau_w}{D}$$

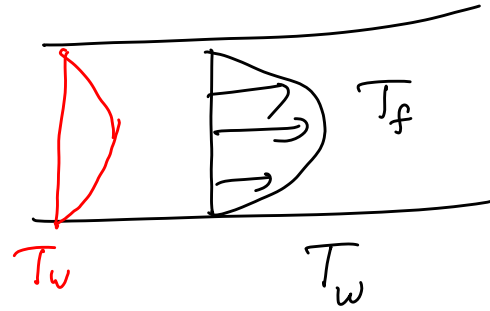
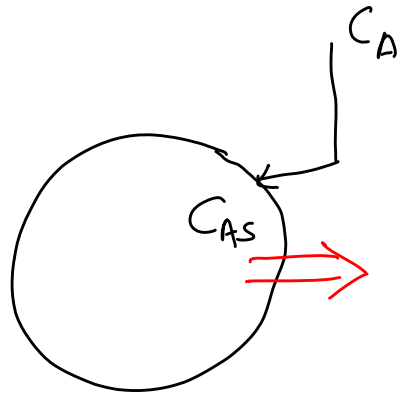
$$f = \left(\frac{\Delta p}{L}\right) \frac{D}{2\rho U^2}$$

$$\tau_w = \frac{c \mu U}{D} \Rightarrow f = c \left(\frac{\mu U}{D}\right) \left(\frac{1}{\frac{1}{2} \rho U^2}\right)$$

$$= 2c \left(\frac{\mu}{\rho U D}\right) = \frac{2c}{Re}$$



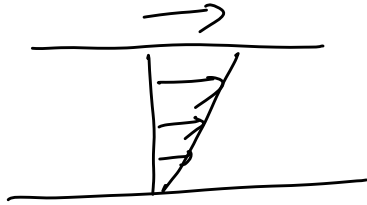
CONTINUUM DESCRIPTION



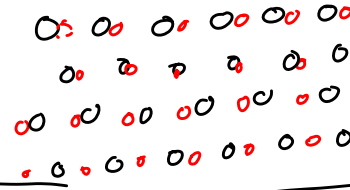
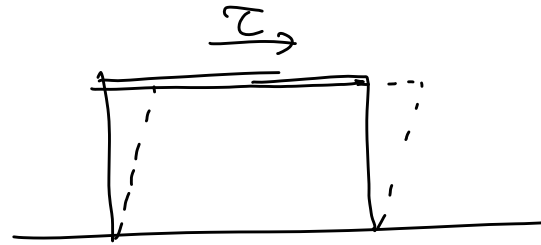
FLUIDS



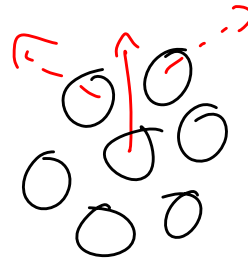
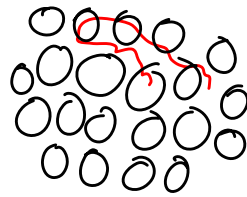
FLUIDS



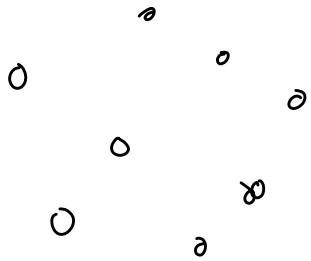
SOLIDS



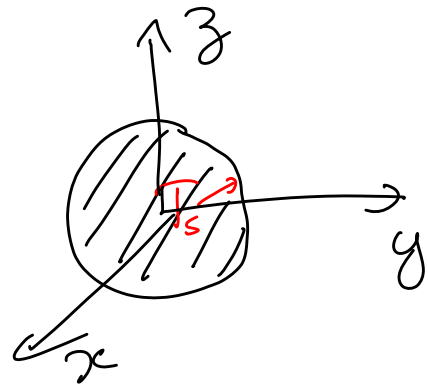
LIQUIDS



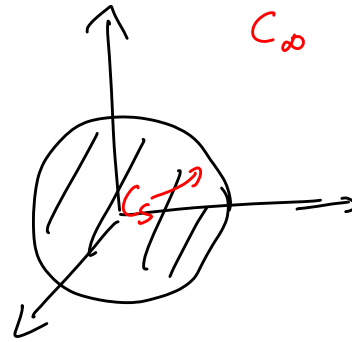
GASES



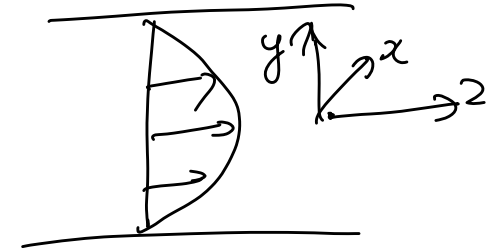
Continuum description:



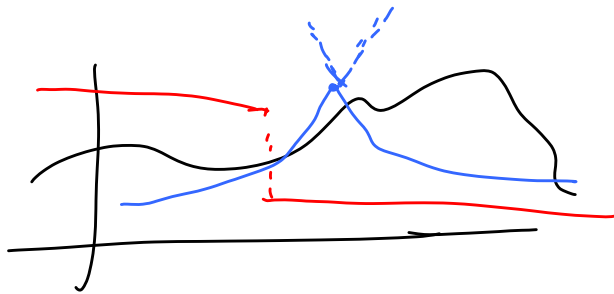
Temperature field
 $T(x, y, z)$

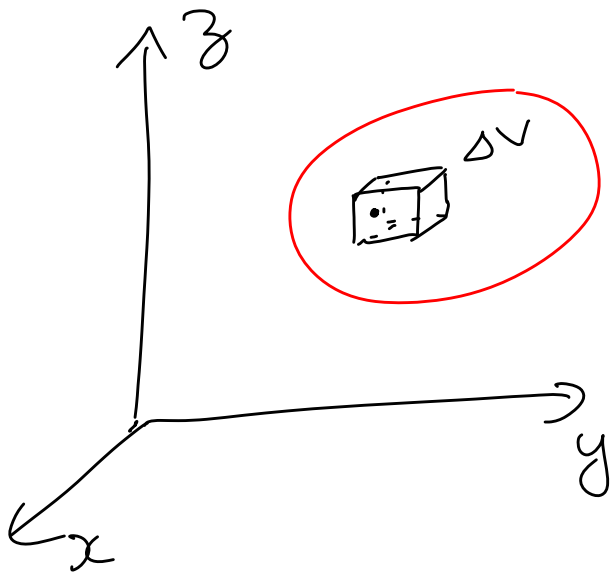


Concentration field
 $C(x, y, z)$



Density field
 $\rho(x, y, z)$
Velocity field
 $u_z(x, y, z)$

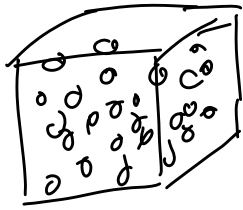




$$\rho(x, y, z)$$

Mass within $\Delta V = m$

$$\text{Density} = \lim_{\Delta V \rightarrow 0} \frac{m}{\Delta V}$$



$$d_{H_2} = 1.38 \text{ \AA}$$

$$d_{O_2} = 3.8 \text{ \AA}$$

Microscopic scale

Liquids $\rightarrow 10^{-9} - 10^{-10} \text{ m}$

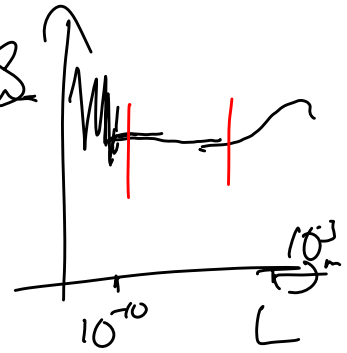
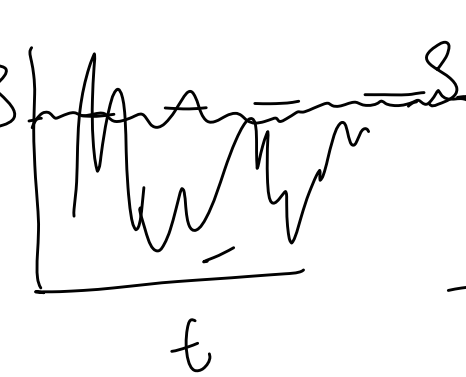
Gases $\rightarrow 10^{-6} \text{ m to } 10^{-8} \text{ m}$

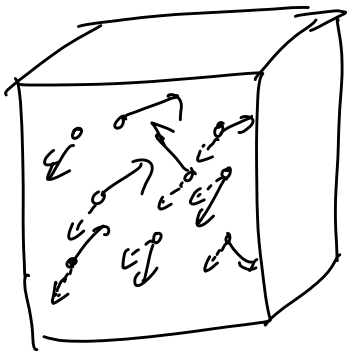
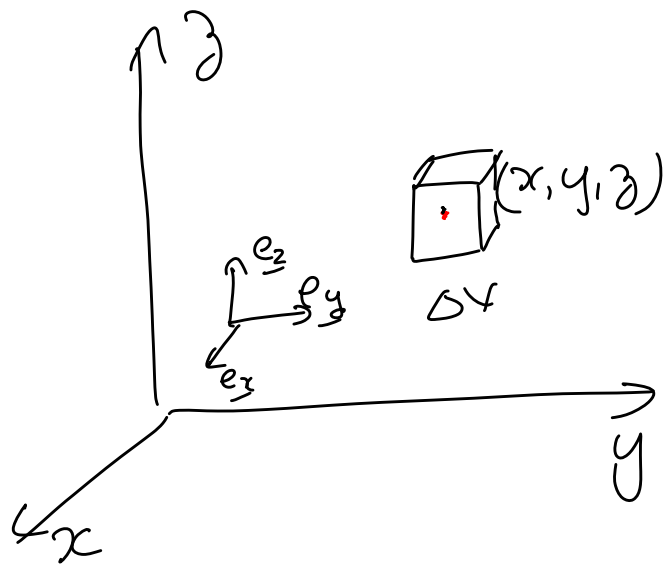
Macroscopic scale

1 mm

10^{-3} m

1 m

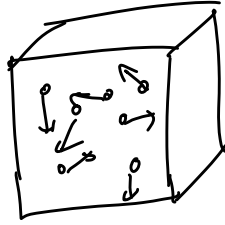
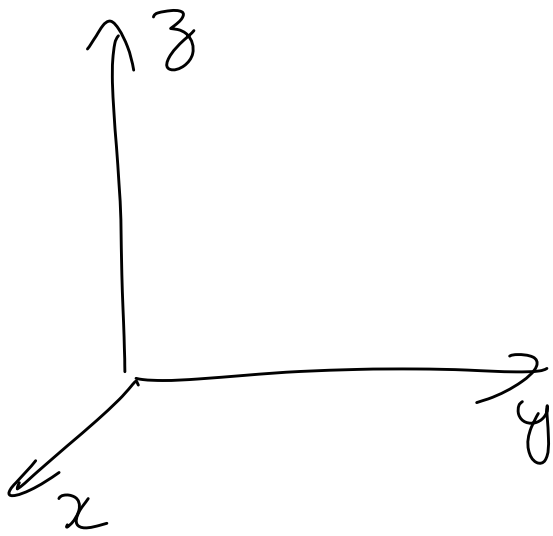




$$\rho(x, y, z) = \lim_{\Delta V \rightarrow 0} \left(\frac{nm}{\Delta V} \right)$$

$$\rho(\underline{u}) = \lim_{\Delta V \rightarrow 0} \frac{\sum_{i=1}^n m \underline{u}_i}{\Delta V}$$

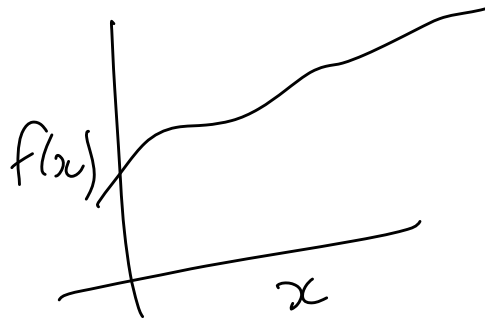
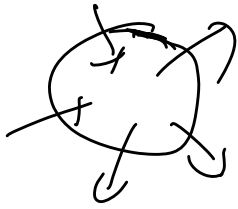
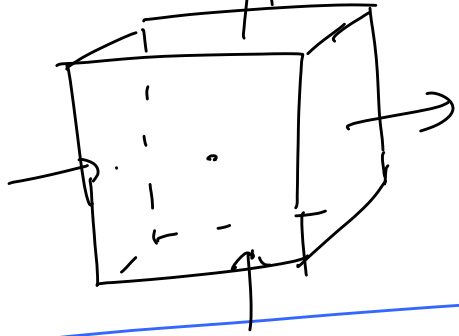
$$\begin{aligned} \underline{u} &= u_x \underline{e}_x + u_y \underline{e}_y + u_z \underline{e}_z \\ &= \underline{e}_x \lim_{\Delta V \rightarrow 0} \frac{\sum m u_{x_i}}{\Delta V} + \underline{e}_y \lim_{\Delta V \rightarrow 0} \frac{\sum m u_{y_i}}{\Delta V} \\ &\quad + \underline{e}_z \lim_{\Delta V \rightarrow 0} \frac{\sum m u_{z_i}}{\Delta V} \end{aligned}$$



Fluctuating energy = $\frac{1}{2} m (\underline{v} - \underline{u})^2$

$$E = \lim_{\Delta V \rightarrow 0} \underbrace{\sum_{i=1}^n \frac{1}{2} m (\underline{v}_i - \underline{u})^2}_{\Delta V} = \frac{3}{2} n k T$$
$$= m n C_v T$$
$$= \rho C_v T$$

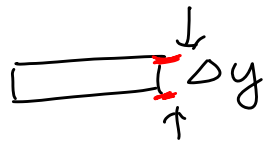
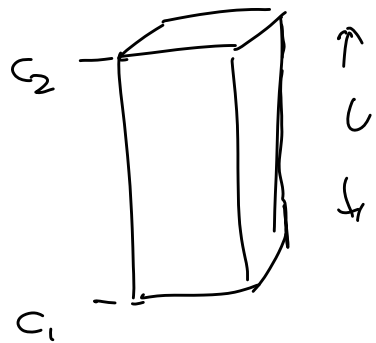
Conservation equations



$$\left(\begin{array}{l} \text{Change in} \\ \text{energy in a} \\ \text{time } \Delta t \end{array} \right) = \left(\begin{array}{l} \text{Energy in} \\ \text{in} \end{array} \right) - \left(\begin{array}{l} \text{Energy out} \\ \text{out} \end{array} \right)$$

$$\left(\begin{array}{l} \text{Rate of} \\ \text{change of} \\ \text{momentum} \end{array} \right) = \left(\begin{array}{l} \text{Momentum} \\ \text{in} \end{array} \right) - \left(\begin{array}{l} \text{Momentum} \\ \text{out} \end{array} \right) + \left(\begin{array}{l} \text{Sum of} \\ \text{all forces} \end{array} \right)$$

Constitutive relations:



$$j = -D \left(\frac{\Delta C}{L} \right)$$

$$j_y = -D \frac{\Delta C}{\Delta y}$$

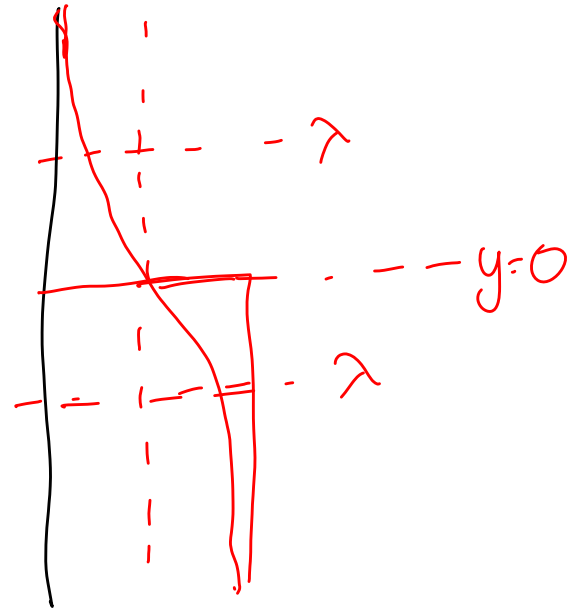
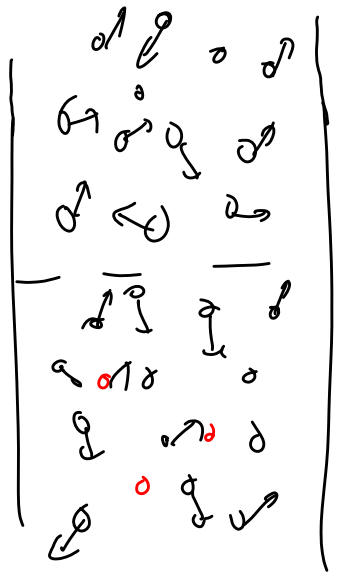
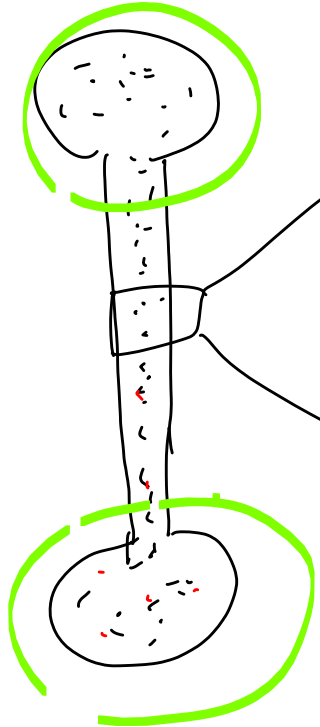
$$j_y = -D \lim_{\Delta y \rightarrow 0} \frac{\partial C}{\partial y} \left| \begin{array}{l} x = \text{const} \\ z = \text{const} \\ t = \text{const} \end{array} \right.$$

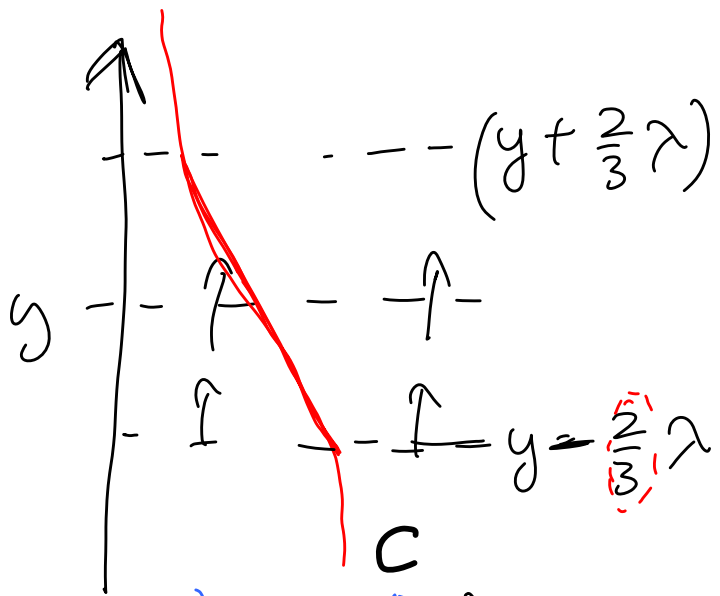
$$j_x = -D \frac{\partial C}{\partial x} ; j_z = -D \frac{\partial C}{\partial z}$$

$$j = e_x j_x + e_y j_y + e_z j_z$$

$$= -D \left[e_x \frac{\partial C}{\partial x} + e_y \frac{\partial C}{\partial y} + e_z \frac{\partial C}{\partial z} \right]$$

DIFFUSION:





$$c(y - \frac{2}{3}\lambda) = c(y) - \frac{2}{3}\lambda \frac{dc}{dy}\bigg|_y + \frac{2}{3}\lambda^2 \frac{d^2c}{2! dy^2}$$

$$c(y + \frac{2}{3}\lambda) = c(y) + \frac{2}{3}\lambda \frac{dc}{dy}\bigg|_y + \dots$$

$$\begin{aligned} \delta y &= \frac{1}{4} v_{rms} \left[c(y) - \frac{2}{3}\lambda \frac{dc}{dy}\bigg|_y - c(y) - \frac{2}{3}\lambda \frac{dc}{dy}\bigg|_y \right] \\ &= -\frac{1}{3} v_{rms} \lambda \frac{dc}{dy}\bigg|_y \end{aligned}$$

$$j_+ = \frac{1}{4} c(y - \frac{2}{3}\lambda) v_{rms}$$

$$j_- = \frac{1}{4} c(y + \frac{2}{3}\lambda) v_{rms}$$

$$\delta j = j_+ - j_- = \frac{1}{4} v_{rms} \left[c(y - \frac{2}{3}\lambda) - c(y + \frac{2}{3}\lambda) \right]$$

$$D \approx \frac{1}{3} v_{rms} \lambda$$

$$\frac{dc}{dy} \sim \frac{c}{L}$$

$$\lambda \frac{dc}{dy} \sim \frac{\lambda c}{L}$$

$$\begin{aligned} &\propto \lambda^2 \frac{d^2c}{dy^2} \\ &\sim \frac{\lambda^2 c}{L^2} \end{aligned}$$

$$v_{\text{rms}} = \sqrt{\frac{3kT}{m}} \quad \frac{1}{2} m \langle v^2 \rangle = \frac{3}{2} kT$$

$$v_{\text{mean}} = \sqrt{\frac{8kT}{\pi m}}$$

Oxygen Mass = $32 \times 10^{-3} \text{ kg}$

$$v_{\text{rms}} = 321 \text{ m/s}$$

$$k = 1.38 \times 10^{-23} \text{ J/K}$$

$$T = 300 \text{ K (room temperature)}$$

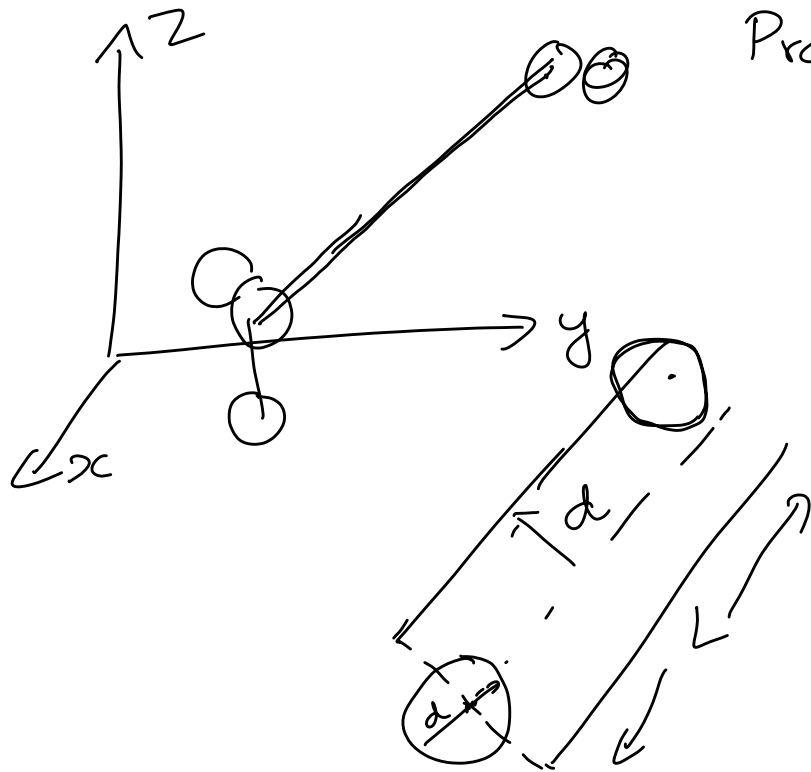
$$kT \approx 4 \times 10^{-21} \text{ J}$$

Hydrogen: Mass = $2 \times 10^{-3} \text{ kg}$
for 6.023×10^{23} molecules

$$m = \frac{2 \times 10^{-3}}{6.023 \times 10^{23}} \text{ kg} = 3.32 \times 10^{-27} \text{ kg}$$

$$v_{\text{rms}} = \sqrt{\frac{3kT}{m}} = 1.29 \times 10^3 \text{ m/s}$$

Mean free path:



$$\text{Volume of cylinder} = (\pi d^2 L)$$

$$\text{Probability of finding a second molecule} \\ = (n \pi d^2 \Delta)$$

$$n \pi d^2 \lambda \sim 1$$

$$\lambda \cong \frac{1}{\pi n d^2} = \frac{1}{\sqrt{2} \pi n d^2}$$

$$\lambda = \frac{1}{\sqrt{2} \pi n d^2}$$

$$n = \left(\frac{p}{kT} \right) = \frac{1 \times 10^5 \text{ N/m}^2}{4 \times 10^{-21} \text{ J}} = 2.5 \times 10^{25} \text{ molecules/m}^3$$

$$D \cong 10^{-5} \text{ m}^2/\text{s}$$

$$\text{H}_2, \text{He} \quad 1.132 \times 10^{-4} \text{ m}^2/\text{s}$$

$$\text{O}_2, \text{H}_2 \cong 1.8 \times 10^{-5} \text{ m}^2/\text{s}$$

$$\lambda = \frac{1}{\sqrt{2} \pi n d^2}$$

Hydrogen $d = 1.38 \text{ \AA} = 1.38 \times 10^{-10} \text{ m}$

$$\lambda = 0.5 \times 10^{-6} \text{ m} \cong 0.5 \mu$$

Oxygen & nitrogen, $d = 3.7 - 3.8 \text{ \AA}$

$$\lambda = 6 \times 10^{-8} \text{ m}$$

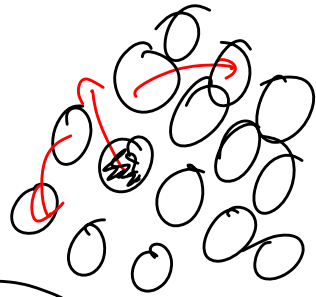
$$D = \frac{1}{3} \underbrace{v_{rms} \lambda}_{\text{Hydrogen}} = \underbrace{6 \times 10^{-4} \text{ m}^2/\text{s}}_{\text{Hydrogen}}$$

$$= \underbrace{2 \times 10^{-5} \text{ m}^2/\text{s}}_{\text{Oxygen, nitrogen}}$$

$$D = \frac{3}{8nd^2} \left(\frac{kT}{\pi m} \right)^{1/2}$$

$$D_{12} = \frac{3}{8n_{12}d_{12}^2} \left(\frac{kT(m_1+m_2)}{\pi m_1 m_2} \right)^{1/2}$$

$$d_{12} = (d_1 + d_2)/2 ; n_{12} = \sqrt{n_1 n_2}$$



$$D = \frac{kT}{3\pi\eta d}$$

Stokes-Einstein relation

Liquids

$$v_{rms} = \left(\frac{3kT}{m} \right)^{1/2}$$

Expect $D_{liquid} \approx \frac{1}{100} D_{gas}$

$$D_{liquid} = 10^{-9} \text{ m}^2/\text{s} \text{ (small molecules)}$$

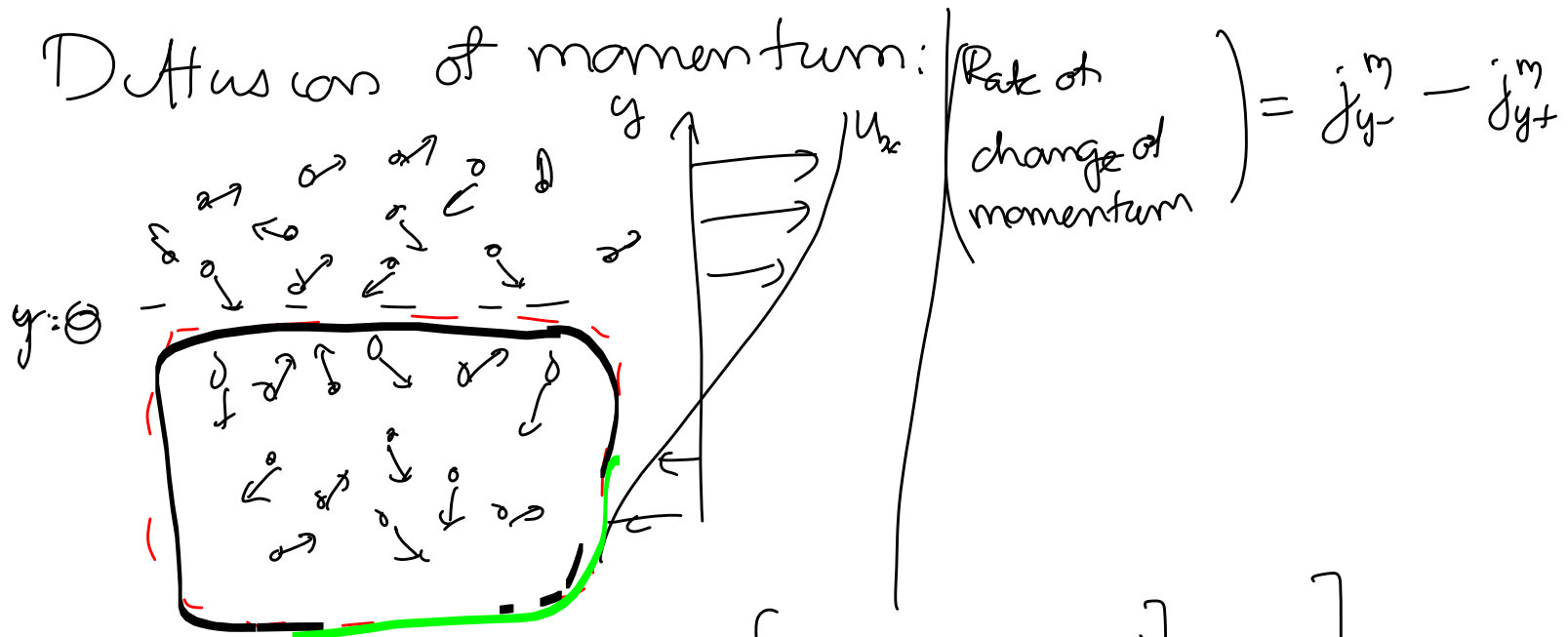
$$= 10^{-11} - 10^{-10} \text{ m}^2/\text{s} \text{ (large molecules)}$$

Gases

$$D = a \lambda \quad v_{\text{rms}} \propto T^{1/2}$$

$$\lambda = \frac{1}{\sqrt{2\pi n} d^2} \quad v_{\text{rms}} = \sqrt{\frac{kT}{m}}$$

Diffusion of momentum:



(Flux of momentum from below to above)

$$j_{y+} = \left[nm u_x \left(y - \frac{2}{3} \lambda \right) \right] v_{rms} a$$

$$j_{y-} = \left[nm u_x \left(y + \frac{2}{3} \lambda \right) \right] v_{rms} a$$

(Net flux of momentum)

$$j_{y-} - j_{y+} = \left(nm u_x \left(y + \frac{2}{3} \lambda \right) - nm u_x \left(y - \frac{2}{3} \lambda \right) \right) v_{rms} a$$

$$= a v_{rms} nm \left[\left(u_x(y) + \frac{2}{3} \lambda \frac{du_x}{dy} \Big|_y \right) - \left(u_x(y) - \frac{2}{3} \lambda \frac{du_x}{dy} \Big|_y \right) \right]$$

$$\tau_{xy} = \frac{4}{3} a v_{rms} nm \lambda \frac{du_x}{dy} \quad \Bigg| \quad \tau_{xy} = \mu \frac{du_x}{dy}$$

$$\mu \equiv v_{rms} nm \lambda$$

$$\mu = A n m v_{rms} \lambda$$

$$\text{Momentum density} = \rho u_x$$

$$\tau_{xy} = \mu \left(\frac{du_x}{dy} \right) = \frac{\mu}{8} \left(\frac{d}{dy} (8u_{1c}) \right)$$

$$\left(\frac{\mu}{8} \right) = \nu = \text{kinematic viscosity}$$

$$\frac{\mu}{8} = \nu = A v_{rms} \lambda$$

$$\mu = A n m v_{rms} \lambda = A n m \sqrt{\frac{3kT}{m}} \left(\frac{1}{\sqrt{2} n d^2} \right)$$

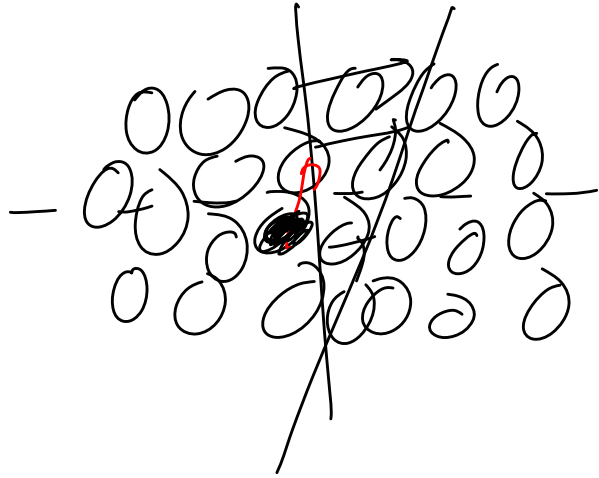
$$= \frac{5}{16 d^2} \left(\frac{m k T}{\pi} \right)^{1/2}$$

$$\nu = \frac{\mu}{n m} = \frac{5}{16 n d^2} \left(\frac{k T}{\pi m} \right)^{1/2}$$

$$D = \frac{3}{8} n d^2 \left(\frac{k T}{\pi m} \right)^{1/2}$$

$$Sc = \frac{D}{\nu} = \frac{5}{6}$$

Momentum transport in liquids:

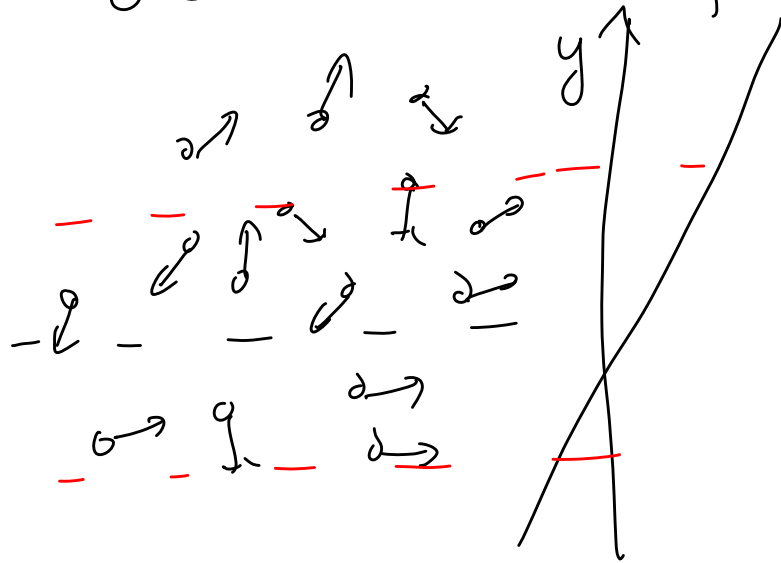


$$\nu_{\text{water}} = 10^{-6} \text{ m}^2/\text{s}$$

$$\nu_{\text{air}} = 1.5 \times 10^{-5} \text{ m}^2/\text{s}$$

$$Sc = \frac{\nu}{D} \approx 10^3$$

Energy diffusion: Gases:



$$j_+ \approx \frac{1}{4} e(y - \frac{2}{3}\lambda) v_{rms}$$

$$j_- \approx \frac{1}{4} e(y + \frac{2}{3}\lambda) v_{rms}$$

Net flux $j = j_+ - j_-$

$$= \frac{1}{4} v_{rms} (e(y - \frac{2}{3}\lambda) - e(y + \frac{2}{3}\lambda))$$

$$= \frac{1}{4} v_{rms} \left[e(y) - \frac{2}{3}\lambda \frac{de}{dy} \Big|_y - e(y) - \frac{2}{3}\lambda \frac{de}{dy} \Big|_y \right]$$

$$= \frac{1}{3} v_{rms} \lambda \left(\frac{de}{dy} \right)$$

$$q = -k \frac{dT}{dy}$$

$$\alpha = \frac{k}{\rho C_p} = \frac{C_v}{C_p} \lambda v_{rms}$$

$$q = -\frac{1}{3} \lambda v_{rms} \frac{d(\rho C_v T)}{dy}$$

$$= -\frac{1}{3} \lambda v_{rms} \rho C_v \frac{dT}{dy}$$

$$k \approx \lambda v_{rms} n m C_v$$

$$\approx \frac{1}{n d^2} \sqrt{\frac{3kT}{m}} n m C_v$$

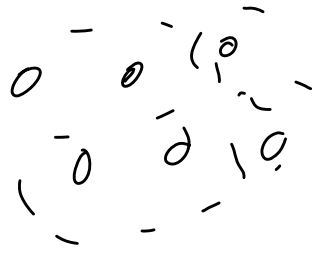
$$k = \frac{75}{64 d^2} \left(\frac{k^3 T}{\pi m} \right)^{3/2} = \frac{5}{2} C_v \mu$$

$$Pr = \frac{C_p \mu}{k} = \frac{2}{5} \frac{C_p}{C_v} = \frac{2}{3}$$

Larger molecules $Pr \rightarrow 1$

Thermal Conduction in liquids:

Liquid metals



$$Pr = \frac{\text{Momentum diffusion}}{\text{Thermal diffusion}}$$

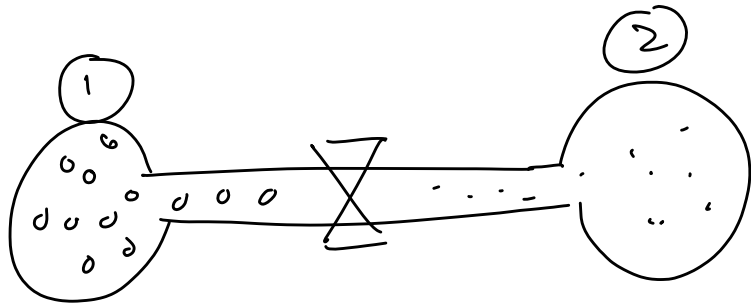
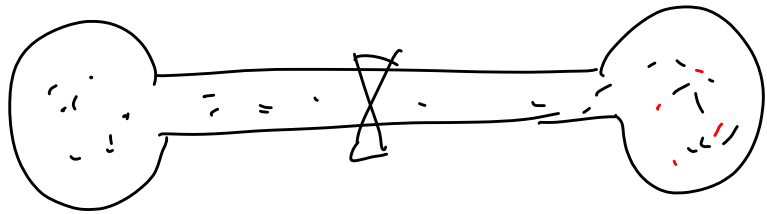
$\ll 1$

Liquid mercury $Pr = 0.015$

Large organic molecules
 $10^2 < Pr < 10^4$

Water $Pr \approx 7$

Multicomponent diffusion:

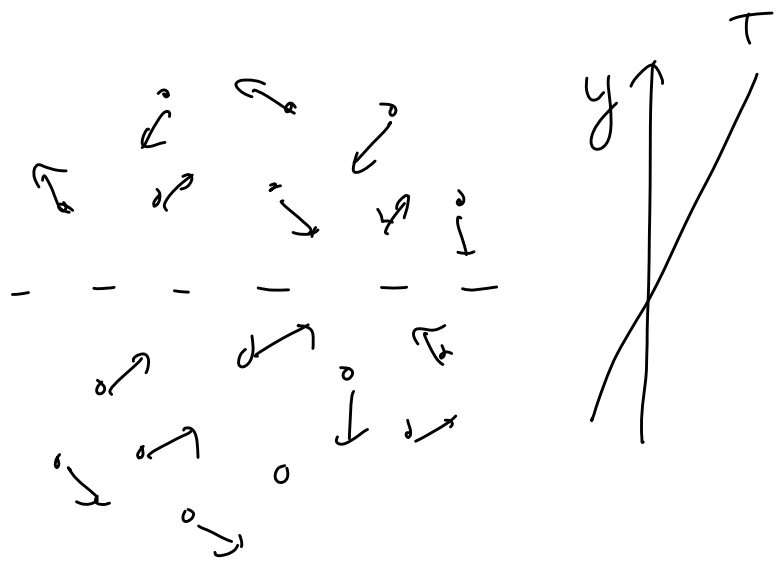


$$n_1 = j_1 + C_1 v_{cm}$$

$$n_2 = j_2 + C_2 v_{cm}$$

$$(n_1 + n_2) = (C_1 + C_2) v_{cm}$$

$$j_1 = -D \frac{\partial C_1}{\partial y}$$



$$j_+ = \frac{1}{4} v_{rms} \left(y - \frac{2}{3} \lambda \right) c \left(y - \frac{2}{3} \lambda \right)$$

$$= \frac{1}{4} v_{rms} \left(y - \frac{2}{3} \lambda \right) c(y)$$

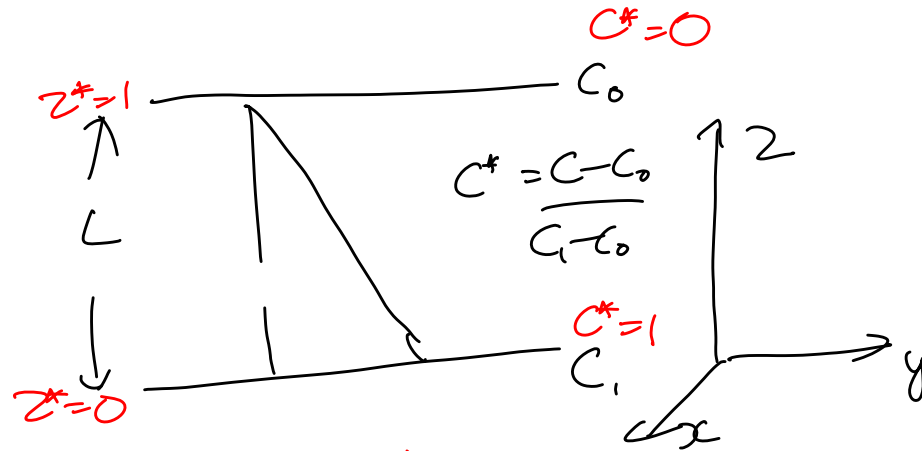
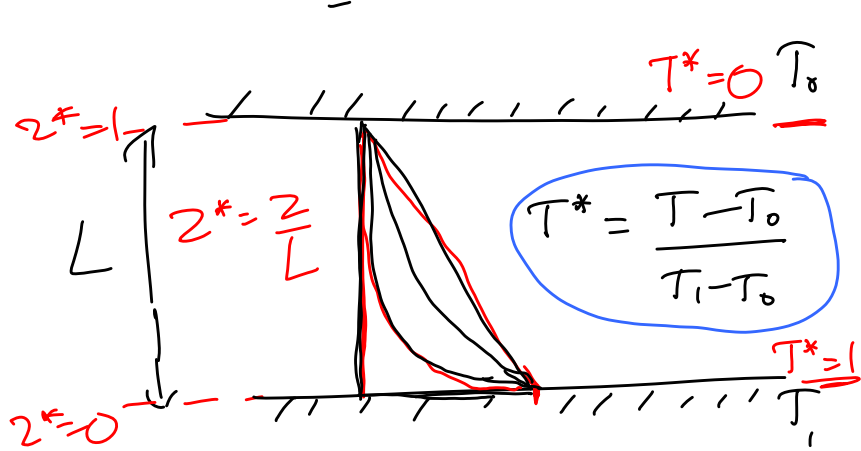
$$j_- = \frac{1}{4} v_{rms} \left(y + \frac{2}{3} \lambda \right) c(y)$$

$$j_+ - j_- = \frac{1}{4} c \left[v_{rms} \left(y - \frac{2}{3} \lambda \right) - v_{rms} \left(y + \frac{2}{3} \lambda \right) \right]$$

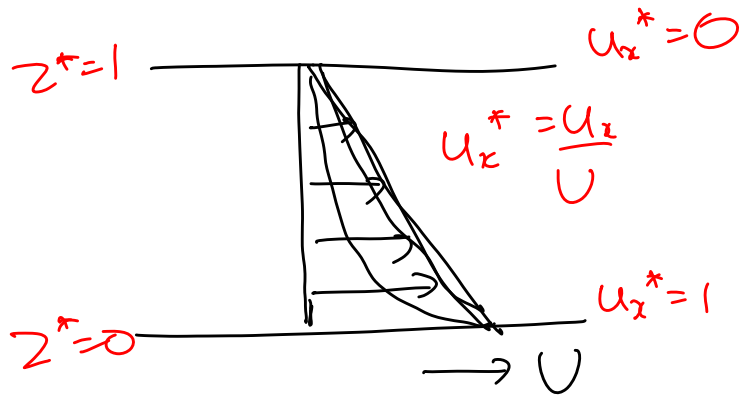
$$= \frac{1}{3} c \frac{dv_{rms}}{dy} = \frac{1}{3} c \frac{d}{dy} \left(\sqrt{\frac{3kT}{m}} \right)$$

$$= \frac{1}{3} c \sqrt{\frac{3kT}{m}} \frac{1}{2T} \frac{dT}{dy}$$

UNIDIRECTIONAL TRANSPORT



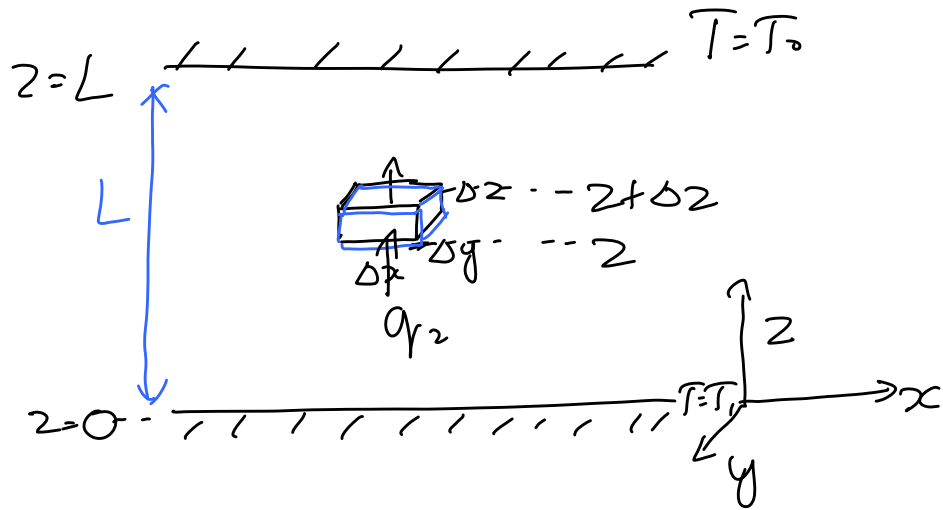
$T^* = C^* = u_x^* = (1 - z^*)$



$\frac{\partial^2 T}{\partial z^2} = 0$

$\frac{\partial^2 T^*}{\partial z^{*2}} = 0$

Shell balance:



$$\text{Energy at time } t = (e \Delta x \Delta y \Delta z) \Big|_t$$

$$\text{Energy at } t + \Delta t = (e \Delta x \Delta y \Delta z) \Big|_{t+\Delta t}$$

Change in energy

$$= [e(x, y, z, t + \Delta t) - e(x, y, z, t)] \Delta x \Delta y \Delta z$$

$$= [\rho C_p T(x, y, z, t + \Delta t) - \rho C_p T(x, y, z, t)] \Delta x \Delta y \Delta z$$

$$\left(\text{Change in energy in time } \Delta t \right) = \left(\text{Energy in} \right) - \left(\text{Energy out} \right) + \left(\text{Source of energy} \right)$$

$$\text{Energy in} = q_z \Big|_z \Delta x \Delta y \Delta t$$

$$\text{Energy out} = q_z \Big|_{z+\Delta z} \Delta x \Delta y \Delta t$$

$$\begin{aligned} \text{Source of energy} &= \int_e \Delta x \Delta y \Delta z \Delta t \\ &= S_e(z, t) \Delta x \Delta y \Delta z \Delta t \end{aligned}$$

$$\left[\rho C_p T(x, y, z, t + \Delta t) - \rho C_p T(x, y, z, t) \right] \Delta x \Delta y \Delta z =$$

$$q_z|_z \Delta x \Delta y \Delta t - q_z|_{z+\Delta z} \Delta x \Delta y \Delta t + S_e \Delta x \Delta y \Delta z \Delta t$$

Divide by $\Delta x \Delta y \Delta z \Delta t$

$$\rho C_p \left[\frac{T(x, y, z, t + \Delta t) - T(x, y, z, t)}{\Delta t} \right] = \frac{q_z|_z - q_z|_{z+\Delta z}}{\Delta z} + S_e$$

$$\rho C_p \left[\frac{T(x, y, z, t + \Delta t) - T(x, y, z, t)}{\Delta t} \right] = - \left(\frac{q_z|_{z+\Delta z} - q_z|_z}{\Delta z} \right) + S_e$$

Take limit $\Delta t \rightarrow 0, \Delta z \rightarrow 0$

$$\rho C_p \frac{\partial T}{\partial t} = - \frac{\partial q_z}{\partial z} + S_e$$

$$\frac{T(z+\Delta z) - T(z)}{\Delta z}$$

$$q_z = -k \left[\frac{T(z+\Delta z) - T(z)}{\Delta z} \right]$$

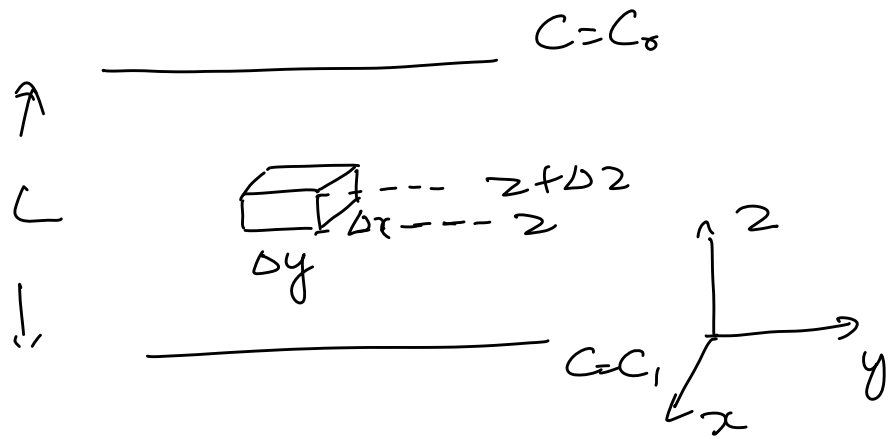
$$= -k \left(\frac{\delta T}{\delta z} \right)$$

$$\begin{aligned} \rho C_p \frac{\partial T}{\partial t} &= - \frac{\partial q_z}{\partial z} = - \frac{\partial}{\partial z} \left(-k \frac{\delta T}{\delta z} \right) \\ &= k \frac{\partial^2 T}{\partial z^2} + S_e \end{aligned}$$

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial z^2} \text{ where } \alpha = \text{thermal diffusivity}$$

$$+ \frac{S_e}{\rho C_p}$$

Concentration diffusion:



$$\left(\begin{array}{l} \text{Change in} \\ \text{mass in} \\ \text{time } \Delta t \end{array} \right) = C(x, y, z, t + \Delta t) \Delta x \Delta y \Delta z - C(x, y, z, t) \Delta x \Delta y \Delta z$$

$$\left(\begin{array}{l} \text{Change in} \\ \text{mass in time} \\ \Delta t \end{array} \right) = \left(\text{Mass in} \right) - \left(\text{Mass out} \right) + \left(\begin{array}{l} \text{Source} \\ \text{of mass} \end{array} \right)$$

$$\text{Mass in} = j_z|_z \Delta x \Delta y \Delta t$$

$$\text{Mass out} = j_z|_{z+\Delta z} \Delta x \Delta y \Delta t$$

$$\text{Source of mass} = S \Delta x \Delta y \Delta z \Delta t$$

$$[C(x, y, z, t + \Delta t) - C(x, y, z, t)] \Delta x \Delta y \Delta z = \underbrace{j_z|_{\underline{z}} \Delta x \Delta y \Delta t - \underbrace{j_z|_{z+\Delta z} \Delta x \Delta y \Delta t}_{z+\Delta z}}_{+ S \Delta x \Delta y \Delta z \Delta t}$$

Divide by $\Delta x \Delta y \Delta z \Delta t$

$$\frac{C(x, y, z, t + \Delta t) - C(x, y, z, t)}{\Delta t} = \frac{j_z|_z - j_z|_{z+\Delta z} + S}{\Delta z}$$

$$= - \left(\frac{j_z(z+\Delta z) - j_z(z)}{\Delta z} \right) + S$$

Limit $\Delta t \rightarrow 0, \Delta z \rightarrow 0$

$$\frac{\partial C}{\partial t} = - \frac{\partial j_z}{\partial z} + S$$

$$j_z = - D \frac{\partial C}{\partial z}$$

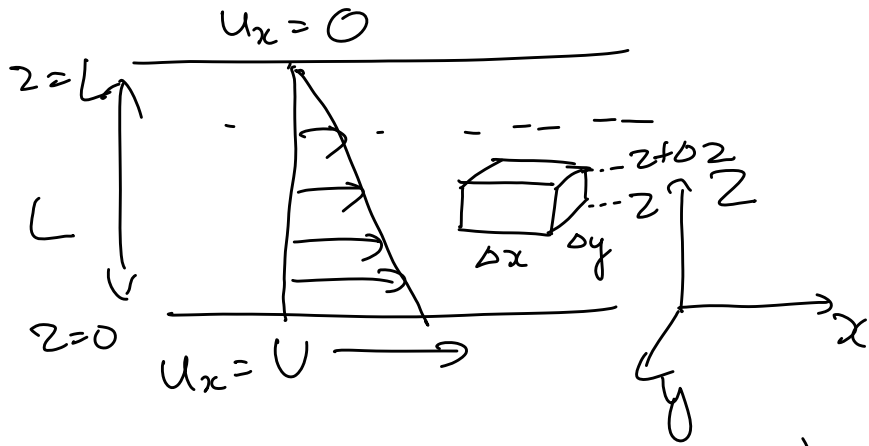
$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial z^2} + S$$

Momentum diffusion: Momentum in the volume $\Delta x \Delta y \Delta z$

$$= \rho u_x(x, y, z) \Delta x \Delta y \Delta z$$

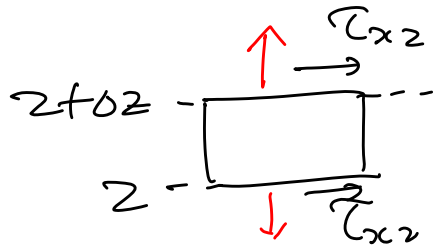
Rate of change of momentum

$$= \frac{[\rho u_x(x, y, z, t + \Delta t) - \rho u_x(x, y, z, t)] \Delta x \Delta y \Delta z}{\Delta t}$$



$$\left(\text{Rate of change of momentum} \right) = \left(\text{Sum of body forces} \right) + \left(\text{Sum of surface forces} \right)$$

Body force = $\rho \Delta x \Delta y \Delta z$
 Gravitational = $\rho g_x \Delta x \Delta y \Delta z$
 $f_x = \rho g_x$



Unit normal =
 Unit vector perpendicular
 to surface

τ_{xz} = Force / Area in the x direction acting at a surface with outward unit normal in z direction

Force on top surface = $\tau_{xz}|_{z+\Delta z} \Delta x \Delta y$

Force on bottom surface = $-\tau_{xz}|_z \Delta x \Delta y$

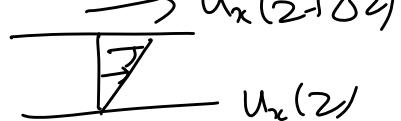
$$\left[\frac{\rho u_x(x, y, z, t + \Delta t) - \rho u_x(x, y, z, t)}{\Delta t} \right] \Delta x \Delta y \Delta z$$

$$= \tau_{xz}|_{z+\Delta z} \Delta x \Delta y - \tau_{xz}|_z \Delta x \Delta y + f_x \Delta x \Delta y \Delta z$$

Divide throughout by $\Delta x \Delta y \Delta z$

$$\frac{\rho u_x(x, y, z, t + \Delta t) - \rho u_x(x, y, z, t)}{\Delta t} = \frac{(\tau_{xz}|_{z+\Delta z} - \tau_{xz}|_z)}{\Delta z} + f_x$$

$$\frac{\partial(\rho u_x)}{\partial t} = \frac{\partial \tau_{xz}}{\partial z} + f_x$$

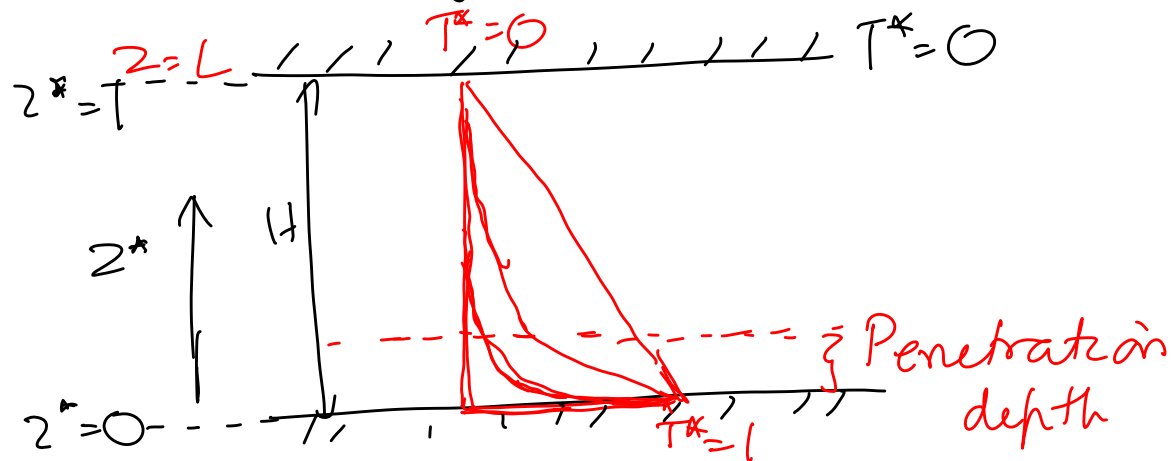
$\rightarrow u_x(z+\Delta z)$

 $u_x(z)$

$$\tau_{xz} = \mu \frac{\Delta u_x}{\Delta z} = \mu \frac{\partial u_x}{\partial z}$$

$$\rho \frac{\partial u_x}{\partial t} = \frac{\partial}{\partial z} \left(\mu \frac{\partial u_x}{\partial z} \right) = \mu \frac{\partial^2 u_x}{\partial z^2} + f_x$$

$$\frac{\partial u_x}{\partial t} = \frac{\mu}{\rho} \frac{\partial^2 u_x}{\partial z^2} = \nu \frac{\partial^2 u_x}{\partial z^2} + \frac{f_x}{\rho}$$

Unsteady diffusion:



For $t < 0$, $T^* = 0$ everywhere

At $t \geq 0$, $T^* = 1$ at $z^* = 0$

$T^* = 0$ as $z \rightarrow \infty$

$$\frac{\partial T^*}{\partial t} = \alpha \frac{\partial^2 T^*}{\partial z^2}$$

(t, z, α) (L, T)

$\xi = \frac{z}{\sqrt{\alpha t}}$ Similarity variable

$$\frac{\partial T^*}{\partial t} = \alpha \frac{\partial^2 T^*}{\partial z^2} \quad \xi = \frac{z}{\sqrt{\alpha t}}$$

$$\frac{\partial T^*}{\partial t} = \frac{\partial \xi}{\partial t} \frac{\partial T^*}{\partial \xi} = \frac{-z}{2\sqrt{\alpha t}^{3/2}} \frac{\partial T^*}{\partial \xi} = -\frac{\xi}{2t} \frac{\partial T^*}{\partial \xi}$$

$$\frac{\partial T^*}{\partial z} = \frac{\partial \xi}{\partial z} \frac{\partial T^*}{\partial \xi} = \frac{1}{\sqrt{\alpha t}} \frac{\partial T^*}{\partial \xi}$$

$$\frac{\partial}{\partial z} \left(\frac{\partial T^*}{\partial z} \right) = \frac{\partial \xi}{\partial z} \frac{\partial}{\partial \xi} \left(\frac{\partial T^*}{\partial \xi} \right) = \frac{1}{\alpha t} \frac{\partial^2 T^*}{\partial \xi^2}$$

$$-\frac{\xi}{2t} \frac{\partial T^*}{\partial \xi} = \frac{\partial^2 T^*}{\partial \xi^2}$$

$$-\frac{\xi}{2} \frac{\partial T^*}{\partial \xi} = \frac{\partial^2 T^*}{\partial \xi^2}$$

Boundary condition

$$z=0, T^*=1 \Rightarrow \xi=0$$

$$z \rightarrow \infty, T^*=0 \Rightarrow \xi \rightarrow \infty$$

$$\text{At } t=0 \text{ for } z > 0, T^*=0 \Rightarrow \xi \rightarrow \infty$$

$$-\frac{c}{2} \frac{\partial T^*}{\partial c} = \frac{\partial^2 T^*}{\partial c^2}$$

$$u = \frac{\partial T^*}{\partial c}$$

$$-\frac{c}{2} u = \frac{\partial u}{\partial c}$$

$$u = C e^{-c^2/4} = \frac{\partial T^*}{\partial c}$$

$$T^* = C \int_0^c d c' e^{-c'^2/4} + D$$

$$T^* = 0 \text{ as } c \rightarrow \infty ; T^* = 1 \text{ at } c = 0$$

$$T^* = \left[1 - \frac{\int_0^c d c' e^{-c'^2/4}}{\int_0^\infty d c' e^{-c'^2/4}} \right]$$

$$T^* = \left[1 - \frac{\int_0^c d c' e^{-c'^2/4}}{\int_0^\infty d c' e^{-c'^2/4}} \right] \sqrt{\pi}$$

$$t \ll (H^2/\alpha)$$

$$\frac{z}{\sqrt{\alpha t}} \sim 1$$

Penetration depth $\sim \sqrt{\alpha t}$

$$\sqrt{\alpha t} \ll H$$

$$t \ll (H^2/\alpha)$$

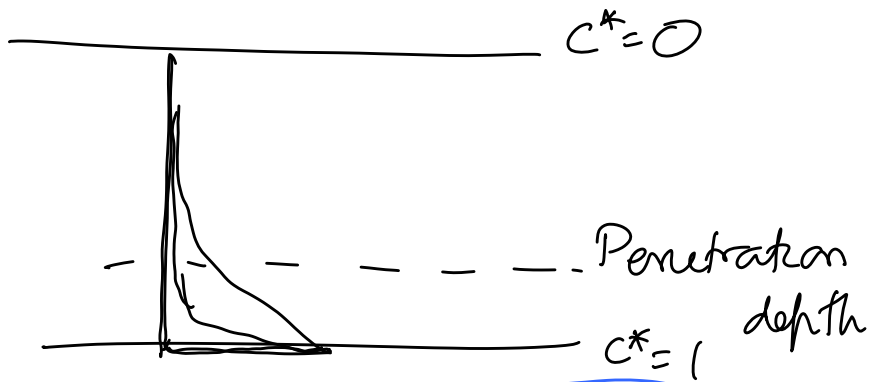
Heat flux

$$q_z = -k \frac{\partial T}{\partial z} = -k (T_1 - T_0) \frac{\partial T^*}{\partial z}$$

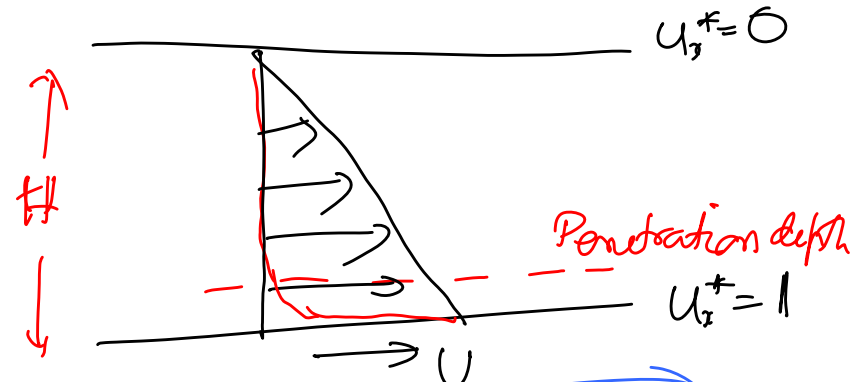
$$= -k (T_1 - T_0) \frac{\partial \zeta}{\partial z} \frac{\partial T^*}{\partial \zeta} = -\frac{k (T_1 - T_0)}{\sqrt{\alpha t}} \frac{\partial T^*}{\partial \zeta}$$

Heat flux at $z=0$ ($\zeta=0$)

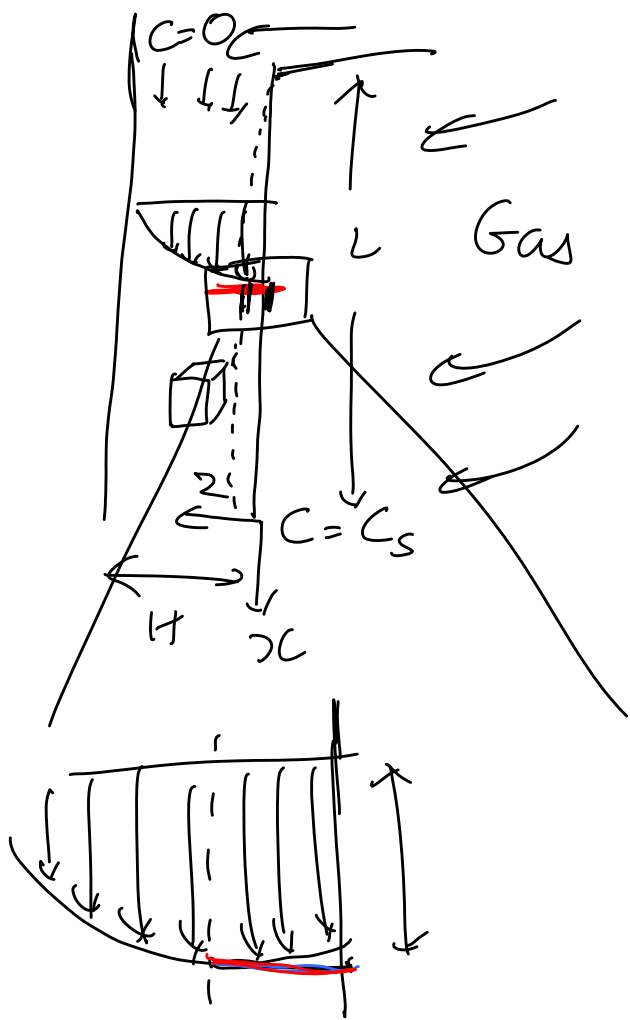
$$\begin{aligned} q_z \Big|_{z=0} &= \frac{-k (T_1 - T_0)}{\sqrt{\alpha t}} \frac{\partial T^*}{\partial \zeta} \Big|_{\zeta=0} \\ &= -\frac{k (T_1 - T_0)}{\sqrt{\alpha t}} \left(\frac{-1}{\int_0^\infty d\zeta' e^{-\zeta'^2/l^2}} \right) \\ &= \frac{k (T_0 - T_1)}{\sqrt{\alpha t} \int_0^\infty d\zeta' e^{-\zeta'^2/l^2}} \end{aligned}$$



$$C^* = \left[1 - \frac{\int_0^{2\sqrt{t/\nu}} d\eta' e^{-\eta'^2/4}}{\int_0^\infty d\eta' e^{-\eta'^2/4}} \right]$$



$$u_x^* = \left[1 - \frac{\int_0^{2\sqrt{t/\nu}} d\eta' e^{-\eta'^2/4}}{\int_0^\infty d\eta' e^{-\eta'^2/4}} \right]$$

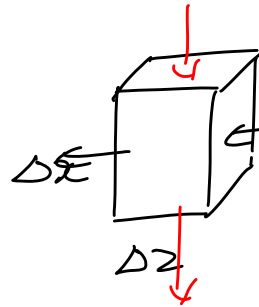


$U = \text{constant}$

① Penetration depth $\ll H$

② Velocity is a constant

③ Diffusion in x -direction is not important.



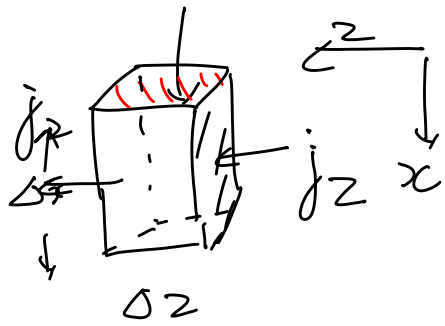
$$C^* = C/C_s$$

Boundary conditions

$$C^* = 1 \text{ at } z = 0$$

$$C^* = 0 \text{ as } z \rightarrow \infty$$

$$C^* = 0 \text{ at } x = 0 \text{ for } z > 0$$



$$(j_z|_z - j_z|_{z+\Delta z}) \Delta x \Delta y \Delta t + ((Uc)|_x - (Uc)|_{x+\Delta x}) \Delta y \Delta z \Delta t = 0$$

$$(\text{Mass in}) - (\text{Mass out}) = 0$$

$$(\text{Mass in due to diffusion at } (x, y, z)) = j_z|_{(x, y, z)} \Delta x \Delta y \Delta t$$

$$(\text{Mass out due to diffusion at } x, y, z+\Delta z) = j_z|_{z+\Delta z} \Delta x \Delta y \Delta t$$

$$(\text{Mass in due to convection at } x, y, z) = (Uc)|_x \Delta y \Delta z \Delta t$$

$$(\text{Mass out due to convection at } x+\Delta x) = (Uc)|_{x+\Delta x} \Delta y \Delta z \Delta t$$

$$\frac{(\bar{j}_z|_z - \bar{j}_z|_{z+\Delta z})}{\Delta z} + \frac{((Uc)|_x - (Uc)|_{x+\Delta x})}{\Delta x} = 0$$

$$-\frac{\partial \bar{j}_z}{\partial z} - \frac{\partial}{\partial x} (Uc) = 0$$

$$\frac{\partial}{\partial x} (Uc) = -\frac{\partial \bar{j}_z}{\partial z}$$

$$U \frac{\partial c}{\partial x} = -\frac{\partial \bar{j}_z}{\partial z}$$

$$\bar{j}_z = -D \frac{\partial c}{\partial z}$$

$$U \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial z^2}$$

$$U \frac{\partial c^*}{\partial x} = D \frac{\partial^2 c^*}{\partial z^2}$$

B.C. $c^* = 1$ at $z = 0$
 $c^* = 0$ as $z \rightarrow \infty$
 $c^* = 0$ at $x = 0$

$$\xi = \frac{z}{\sqrt{Dx/U}}$$

$$C^* = \left[1 - \frac{\int_0^{\sqrt{x D / U}} d\alpha' e^{-\alpha'^2 / 4} }{\int_0^{\infty} d\alpha' e^{-\alpha'^2 / 4}} \right]$$

① Penetration depth $\ll H$

$$\sqrt{\frac{x D}{U}} \ll H \quad \text{Pe}_H \gg 1$$

$$\frac{x D}{U} \ll H^2$$

$$\left(\frac{x}{H} \right) \ll \left(\frac{U H}{D} \right)$$

$$\ll \text{Pe}_H$$

$$\left(\frac{L}{H} \right) \ll \text{Pe}_H$$

② Velocity is nearly constant

$$U(z) = U(z=0) + z \frac{dU}{dz} \Big|_{z=0} + \frac{z^2}{2} \frac{d^2U}{dz^2} \Big|_{z=0} + \dots$$

$$U(z) - U(0) = \frac{z^2}{2} \frac{d^2U}{dz^2} \Big|_{z=0}$$

$$\frac{U(z) - U(0)}{U(0)} = \frac{z^2}{2U} \frac{d^2U}{dz^2} \Big|_{z=0} \ll 1$$

$$\frac{z^2}{2U} \frac{d^2U}{dz^2} \ll 1$$

$$\frac{(\sqrt{Dx})^2}{2U} \left(\frac{U}{H^2} \right) \ll 1$$

$$\frac{Dx}{U} \ll H^2 \Rightarrow \frac{x}{H} \ll \frac{UH}{D} \ll Pe_H$$

Convective flux $\sim U C$

Diffusive flux $\sim D \frac{\partial C}{\partial x} \approx \frac{D C}{x}$

$$\frac{D C}{x} \ll U C$$

$$\frac{U x}{D} \gg 1 \Rightarrow Pe_x \gg 1$$

Flux at interface:

$$j_z|_{z=0} = -D \frac{\partial C}{\partial z} \Big|_{z=0} = -D C_s \frac{\partial C^*}{\partial z} \Big|_{z=0}$$

$$= -D C_s \frac{\partial \xi}{\partial z} \frac{\partial C^*}{\partial \xi} \Big|_{z=0}$$

$$= -D C_s \frac{1}{\sqrt{D x / U}} \frac{\partial C^*}{\partial \xi} \Big|_{\xi=0}$$

$$C^* = \left[1 - \frac{\int_0^{\xi} d\xi' e^{-\xi'^2/4}}{\int_0^{\infty} d\xi' e^{-\xi'^2/4}} \right] \Rightarrow \left[\frac{\partial C^*}{\partial \xi} \Big|_{\xi=0} = \frac{-1}{\int_0^{\infty} d\xi' e^{-\xi'^2/4}} \right]$$

$$j_2 = \frac{-D}{\sqrt{x D / 0}} c_s \left(\frac{-1}{\int_0^{\infty} dq' e^{-q'^2 L}} \right)$$

$$= \frac{D c_s}{\sqrt{x D / 0}} \frac{1}{\int_0^{\infty} dq' e^{-q'^2 L}}$$

$$= \left(\sqrt{\frac{UD}{x}} \right) c_s \frac{1}{\int_0^{\infty} dq' e^{-q'^2 L}}$$

$$\bar{j}_2 = \frac{1}{L} \int_0^L dx j_2(x)$$

$$= \frac{c_s \sqrt{UD}}{\int_0^{\infty} dq' e^{-q'^2 L}} \frac{1}{L} \int_0^L \frac{dx}{x^{1/2}} = \frac{c_s \sqrt{UD}}{\int_0^{\infty} dq' e^{-q'^2 L}} \left[\frac{2}{L^{1/2}} \right]$$

$$= \frac{2 c_s \sqrt{UD}}{L^{1/2} \int_0^{\infty} dq' e^{-q'^2 L}}$$

$$Nu = \frac{\overline{j_z}}{(DC_s/L)}$$

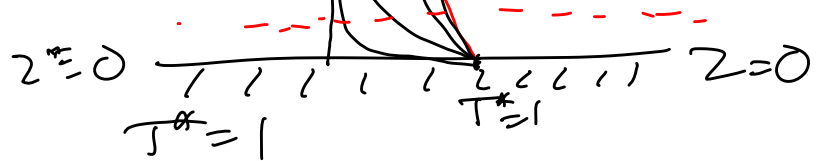
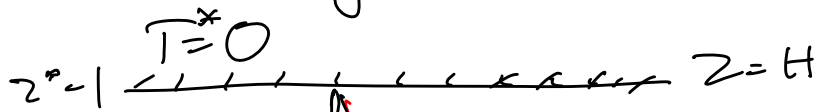
$$= \frac{2}{\int_0^\infty d\zeta' e^{-\zeta'^2/L}} \left(\frac{UL}{D} \right)^{1/2}$$

$$Sh = \frac{2}{\int_0^\infty d\zeta' e^{-\zeta'^2/L}} \quad Pe_L^{1/2} = \frac{2}{\int_0^\infty d\zeta' e^{-\zeta'^2/L}} (Re Sc)^{1/2}$$

1.12

$$Nu = \frac{2}{\int_0^\infty d\zeta' e^{-\zeta'^2/L}} (Re Pr)^{1/2}$$

Unsteady diffusion in a finite channel



$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial z^2}$$

$$T^* = \frac{T - T_0}{T_1 - T_0} \quad z^* = (z/H)$$

$$t^* = \left(\frac{t \alpha}{H^2} \right)$$

$$\frac{\partial T^*}{\partial t} = \frac{\alpha}{H^2} \frac{\partial^2 T^*}{\partial z^{*2}}$$

$$\frac{\partial T^*}{\partial t^*} = \frac{\partial^2 T^*}{\partial z^{*2}}$$

At $z^* = 0, T^* = 1$

At $z^* = 1, T^* = 0$

At $t = 0, T^* = 0 \quad z^* > 0$

$$\frac{\partial T^*}{\partial t^*} = \frac{\partial^2 T^*}{\partial z^{*2}}$$

In the limit $t^* \rightarrow \infty,$

$$\frac{\partial^2 T^*}{\partial z^{*2}} = 0 \Rightarrow T_s^* = (1 - z^*)$$

$$T^* = T_s^* + T_t^*$$

$$\frac{\partial^2 T_s^*}{\partial z^{*2}} = 0$$

$$T_s^* = 1 \text{ at } z^* = 0$$

$$T_s^* = 0 \text{ at } z^* = 1$$

$$\frac{\partial (T_s^* + T_e^*)}{\partial t} = \frac{\partial^2 (T_s^* + T_e^*)}{\partial z^{*2}}$$

$$T_s^* + T_e^* = 1 \text{ at } z^* = 0$$

$$T_s^* + T_e^* = 0 \text{ at } z^* = 1$$

$$\frac{\partial T_e^*}{\partial t} = \frac{\partial^2 T_e^*}{\partial z^{*2}}$$

$$T_e^* = 0 \text{ at } z^* = 0$$

$$T_e^* = 0 \text{ at } z^* = 1$$

At $t^* = 0$, $T^* = 0$ at all $z^* > 0$

$T_e^* + T_s^* = 0$ at all $z^* > 0$

Initial condition $T_e^* = -T_s^*$ at $t^* = 0$ for all z^*

$$T_e^* = -(1 - z^*)$$

'Homogeneous boundary conditions'

Separation of variables:

$$T_t^*(z^*, t^*) = Z(z^*) \Theta(t^*)$$

$$\frac{\partial}{\partial t^*} (Z \Theta) = \frac{\partial^2}{\partial z^{*2}} (Z \Theta)$$

$$Z \frac{d\Theta}{dt^*} = \Theta \frac{d^2 Z}{dz^{*2}}$$

Divide by $Z \Theta$

$$\frac{1}{\Theta} \frac{d\Theta}{dt} = \frac{1}{Z} \frac{d^2 Z}{dz^{*2}}$$

$$\frac{1}{Z} \frac{d^2 Z}{dz^{*2}} = \alpha$$

$$\frac{d^2 Z}{dz^{*2}} = \alpha Z$$

$$Z = A e^{\sqrt{\alpha} z^*} + B e^{-\sqrt{\alpha} z^*}$$

$$\frac{1}{Z} \frac{d^2 Z}{dz^{*2}} = -\beta^2$$

$$\frac{d^2 Z}{dz^{*2}} = -\beta^2 Z$$

$$Z = A \sin(\beta z^*) + B \cos(\beta z^*)$$

$$\text{BC } Z=0 \text{ at } z^*=0$$

$$Z=0 \text{ at } z^*=1$$

$$A + B = 0$$

$$A e^{\sqrt{\lambda} z^*} + B e^{-\sqrt{\lambda} z^*} = 0$$

$$A = 0 \text{ \& } B = 0$$

$$\text{BC } Z=0 \text{ at } z^*=0$$

$$Z=0 \text{ at } z^*=1$$

$$B = 0$$

$$A \sin(\beta z^*) = 0$$

$$\beta_n = n\pi$$

where n is integer

$$Z = A \sin(\beta_n z^*) = A \sin(n\pi z^*)$$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t^*} = -\beta^2 = -(n\pi)^2$$

$$\frac{\partial \Theta}{\partial t^*} = -(n\pi)^2 \Theta$$

$$\Theta = e^{-(n\pi)^2 t^*}$$

$$T_t^* = \sum_{n=0}^{\infty} A_n \sin(n\pi z^*) e^{-(n\pi)^2 t^*}$$

'Orthogonality conditions'

$$\int_0^1 dz^* \sin(n\pi z^*) \sin(m\pi z^*) = \frac{1}{2} \text{ if } m=n$$
$$= 0 \text{ if } m \neq n$$
$$= \frac{\delta_{mn}}{2}$$

Initial conditions:

$$T_t^* = -(1-z^*) \text{ at } t^* = 0$$

$$= -T_s$$

$$\text{At } t^* = 0; T_t^* = \sum_{n=0}^{\infty} A_n \sin(n\pi z^*) = -(1-z^*)$$

$$\sum_{n=0}^{\infty} A_n \int dz^* \sin(n\pi z^*) \sin(m\pi z^*) = - \int dz^* (1-z^*) \sin(m\pi z^*)$$

$$\sum_{n=0}^{\infty} A_n \frac{1}{2} \delta_{mn} = - \int dz^* (1-z^*) \sin(m\pi z^*)$$

$$\frac{1}{2} A_m = - \int dz^* (1-z^*) \sin(m\pi z^*)$$

$$A_m = -2 \int dz^* (1-z^*) \sin(m\pi z^*)$$

$$= -\frac{2}{m\pi} \text{ for odd } m$$

$$= 0 \text{ for even } m$$

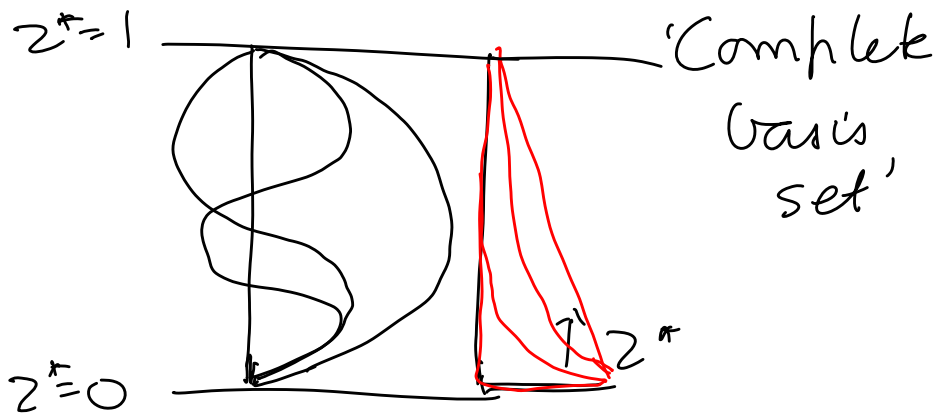
$$T_t^* = - \sum_{n=1,3,5,\dots}^{\infty} \frac{2}{n\pi} \sin(n\pi z^*) e^{-n^2\pi^2 t^*}$$

$$T^* = (1 - z^*) - \sum_{n=1,3,5,\dots}^{\infty} \left(\frac{2}{n\pi} \right) \sin(n\pi z^*) e^{-n^2\pi^2 t^*}$$

$$S_n = \sin(n\pi z^*) \quad S_m = \sin(m\pi z^*)$$

$$\langle S_n, S_m \rangle = \int_0^1 dz^* S_n(z^*) S_m(z^*)$$

$$= \frac{\delta_{mn}}{2}$$



$$T_b^* = \sum A_n S_n e^{-(n\pi)^2 t^*}$$

At time $t^* = 0$, $T_b^* = -(1 - z^*)$

$$\sum_{n=0}^{\infty} A_n S_n = -(1 - z^*)$$

$$\left\langle \sum_{n=0}^{\infty} A_n S_n, S_m \right\rangle = -\langle (1 - z^*), S_m \rangle$$

$$\sum_{n=0}^{\infty} A_n \langle S_n, S_m \rangle = -\langle (1 - z^*), S_m \rangle$$

$$\sum_{n=0}^{\infty} A_n \frac{\delta_{mn}}{2} = -\langle (1 - z^*), S_m \rangle$$

$$\frac{A_m}{2} = -\langle (1 - z^*), S_m \rangle$$

$$B_n = n\pi \leftarrow \text{Eigenvalues}$$

$$T^*_{\text{approx}} \equiv \sum_{n=1,3,\dots}^b \frac{2}{n\pi} \sin(n\pi z^*) e^{-n^2\pi^2 t^*}$$

$$\text{Error} = T^*_t - T^*_{\text{approx}}$$

$$= \sum_{b+1}^{\infty} \frac{2}{n\pi} \sin(n\pi z^*) e^{-n^2\pi^2 t^*}$$

$$\leq \sum_{b+1}^{\infty} \frac{2}{n\pi} e^{-n^2\pi^2 t^*}$$

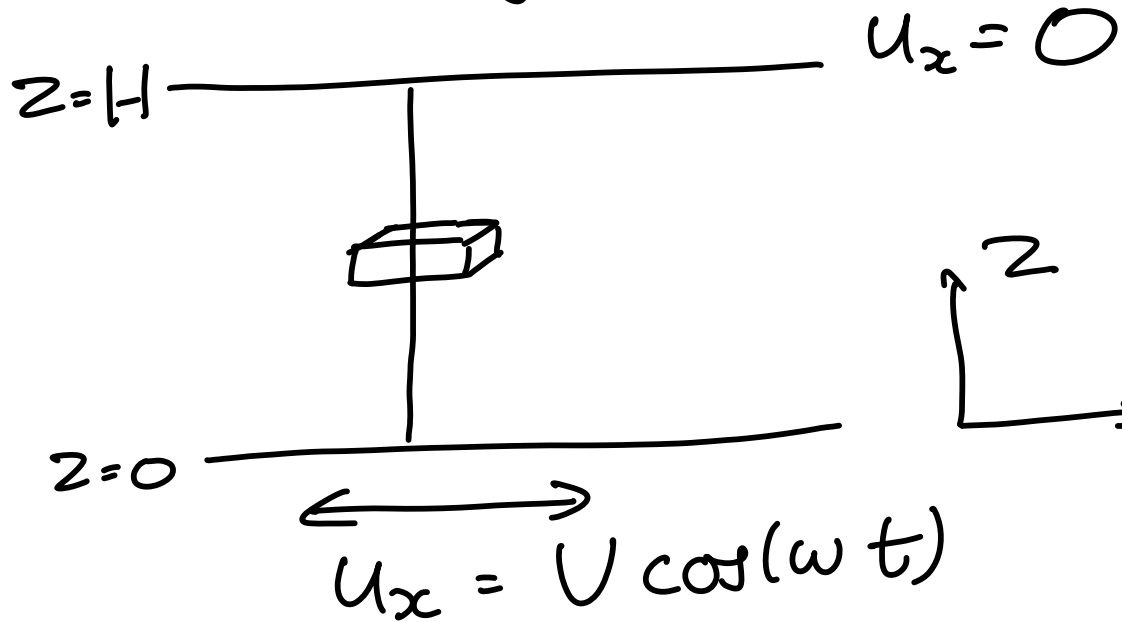
$$\leq \int_{b+1}^{\infty} dn \left(\frac{2}{n\pi} \right) e^{-n^2\pi^2 t^*}$$

Define $n^* = (n^2\pi^2 t^*)^{1/2} \Rightarrow n = n^*/\pi t^{*1/2}$

$$\text{Error} \leq \int_{b^*}^{\infty} dn^* \left(\frac{2}{n^*} \right) e^{-n^{*2}}$$

where $b^* = b\pi t^{*1/2}$

Oscillatory flow:



$$z^* = (z/H)$$

$$u_x^* = (u_x/U)$$

$$t^* = \omega t$$

$$U\omega \frac{\partial u_x^*}{\partial t^*} = \frac{\nu U}{H^2} \frac{\partial^2 u_x^*}{\partial z^{*2}}$$

$$\left(\frac{\omega H^2}{\nu} \right) \frac{\partial u_x^*}{\partial t^*} = \frac{\partial^2 u_x^*}{\partial z^{*2}}$$

Re ω

$$\frac{\partial u_x}{\partial t} = \nu \frac{\partial^2 u_x}{\partial z^2}$$

At $z=H$, $u_x=0$

$z=0$, $u_x = U \cos(\omega t)$

$$\operatorname{Re}_w \frac{\partial u_x^*}{\partial t^*} = \frac{\partial^2 u_x^*}{\partial z^{*2}} \quad | \quad u_x^* = \operatorname{Re}(u_x^+)$$

$$\text{At } z^* = 1 \quad u_x^* = 0$$

$$z^* = 0 \quad u_x^* = \cos t^*$$

$$\operatorname{Re}_w \frac{\partial u_x^+}{\partial t^*} = \frac{\partial^2 u_x^+}{\partial z^{*2}}$$

$$\text{At } z^* = 1, \quad u_x^+ = 0$$

$$z^* = 0, \quad u_x^+ = e^{it^*}$$

$$\operatorname{Re}_w \frac{\partial u_x^+}{\partial t^*} = \frac{\partial^2 u_x^+}{\partial z^{*2}}$$

$$\text{At } z^* = 1, \quad u_x^+ = 0$$

$$z^* = 0, \quad u_x^+ = e^{it^*}$$

$$u_x^+(z^*, t^*) = e^{it^*} \tilde{u}_x(z^*)$$

$$\operatorname{Re}_w \tilde{u}_x(z) i e^{it^*} = \frac{\partial^2 \tilde{u}_x}{\partial z^{*2}} e^{it^*}$$

$$\partial^2 \tilde{u}_x = i \operatorname{Re} \omega \tilde{u}_x$$

$$\partial z^{*2}$$

$$\text{At } z^* = 1, u_x^+ = 0 \Rightarrow \tilde{u}_x = 0$$

$$\text{At } z^* = 0, u_x^+ = e^{it^*} \Rightarrow \tilde{u}_x = 1$$

$$u_x^+ = \tilde{u}_x(z) e^{it^*}; \quad u_x^* = \operatorname{Real}(u_x^+)$$

$$\tilde{u}_x = A_1 e^{\sqrt{i \operatorname{Re} \omega} z^*} + A_2 e^{-\sqrt{i \operatorname{Re} \omega} z^*}$$

$$\tilde{u}_x = \left[\frac{e^{\sqrt{i \operatorname{Re} \omega} z^*} - e^{\sqrt{i \operatorname{Re} \omega} (2-z^*)}}{1 - e^{2\sqrt{i \operatorname{Re} \omega}}} \right]$$

$$u_x^+ = \left[\frac{e^{\sqrt{i \operatorname{Re} \omega} z^*} - e^{\sqrt{i \operatorname{Re} \omega} (2-z^*)}}{1 - e^{2\sqrt{i \operatorname{Re} \omega}}} \right] e^{it^*}$$

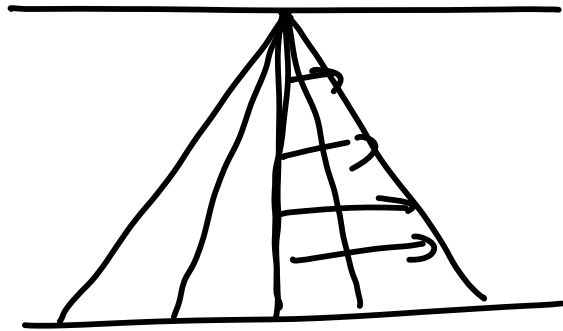
$$u_x^* = \operatorname{Real}(u_x^+)$$

Limit $Re\omega \ll 1$

$$\tilde{u}_x = (1 - z^*) \quad u_x^+ = (1 - z^*) e^{it^*}$$

$$u_x^* = (1 - z^*) \cos(t^*)$$

$$Re\omega = \left(\frac{\omega H^2}{\nu} \right) = \left(\frac{t_1^2 / \nu}{1/\omega} \right)$$



$$\text{Re } \omega \gg 1$$

$$\tilde{u}_x(z^*) = e^{-\sqrt{i \text{Re } \omega} z^*}$$

$$u_x^+(z^*) = e^{-\sqrt{i \text{Re } \omega} z^*} e^{it^*}$$

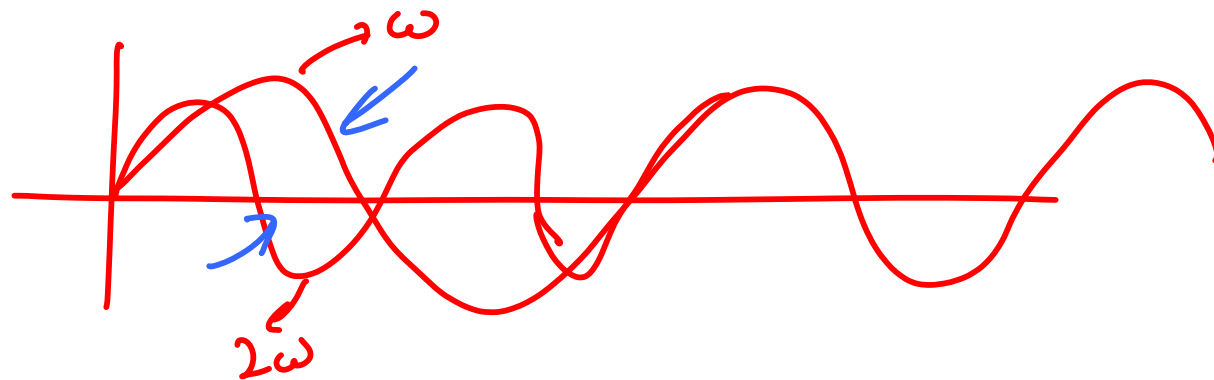
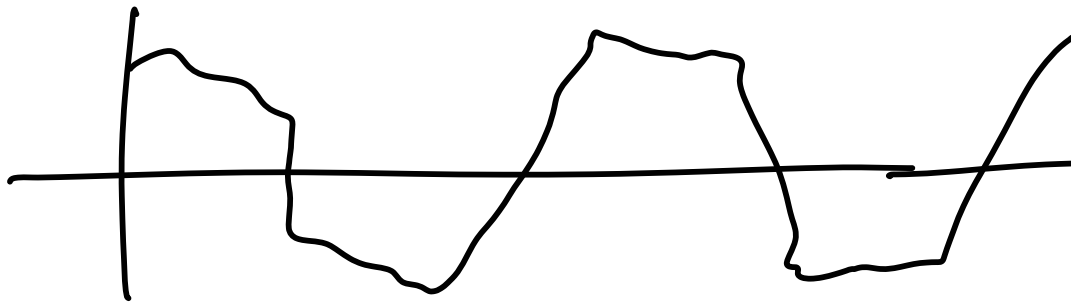
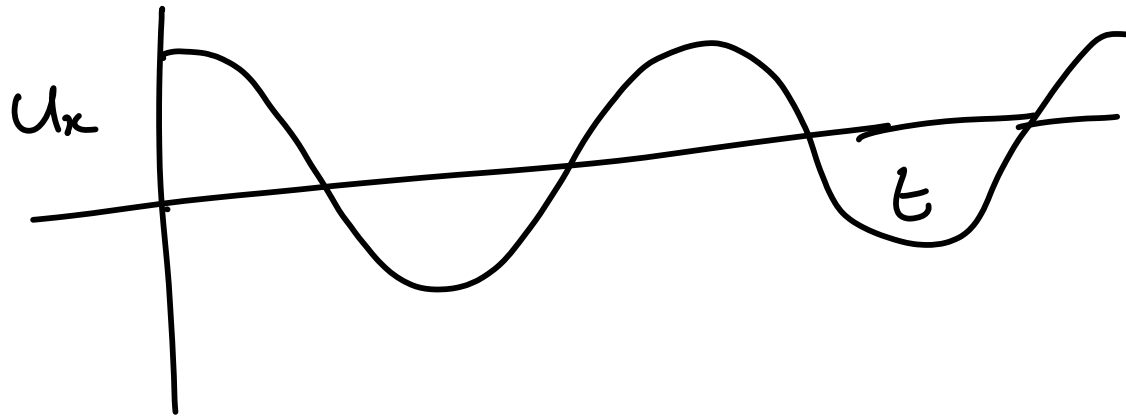
$$u_x^*(z^*) = e^{-\left(\sqrt{\frac{\text{Re } \omega}{2}} z^*\right)} \left[\cos\left(\sqrt{\frac{\text{Re } \omega}{2}} z^*\right) \cos t^* - \sin\left(\sqrt{\frac{\text{Re } \omega}{2}} z^*\right) \sin t^* \right]$$

$$\sqrt{\text{Re } \omega} z^* = \sqrt{\frac{\omega H^2}{\nu}} \left(\frac{z}{H}\right) = \left[\frac{z}{\sqrt{\nu/\omega}}\right]$$

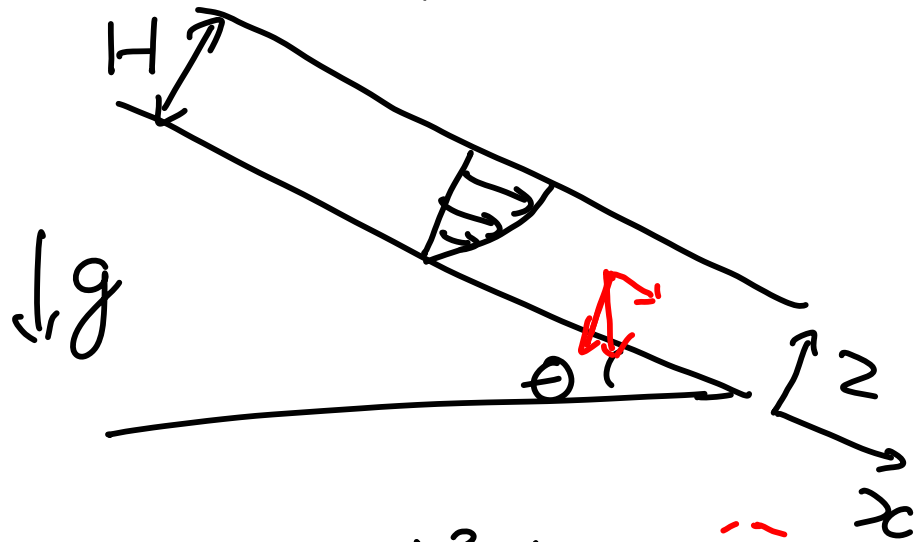
$$\text{Penetration depth} = (\nu/\omega)^{1/2}$$

$$\text{Re } \omega = \frac{\omega H^2}{\nu} = \left[\frac{H}{(\nu/\omega)^{1/2}}\right]^2$$

Oscillatory flows:



Sources / Sinks within the fluid:



$$f_x = (g \sin \theta) \rho$$

$$\frac{\partial u_x}{\partial t} = \nu \frac{\partial^2 u_x}{\partial z^2} + g \sin \theta$$

$$z^* = (z/H)$$

$$\frac{1}{g \sin \theta} \frac{\partial u_x}{\partial t} = \frac{\nu}{H^2 g \sin \theta} \frac{\partial^2 u_x}{\partial z^{*2}} + 1$$

$$u_x^* = \left(\frac{u_x \nu}{H^2 g \sin \theta} \right)$$

$$\frac{\partial u_x}{\partial t} = \nu \frac{\partial^2 u_x}{\partial z^2} + \frac{f_x}{\rho}$$

$$\text{At } z = 0, u_x = 0$$

$$\text{At } z = H; \tau_{xz} = 0$$

$$\mu \frac{\partial u_x}{\partial z} = 0$$

$$\frac{\partial u_x}{\partial z} = 0$$

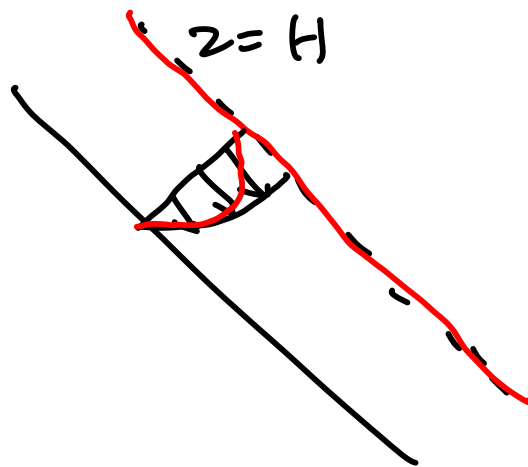
$$\frac{\partial u_x^*}{\partial t^*} = \frac{\partial^2 u_x^*}{\partial z^{*2}} + 1$$

where $z^* = (z/H)$, $u_x^* = \left(\frac{u_x N}{H^2 g \sin \theta} \right)$, $t^* = \left(\frac{t N}{H^2} \right)$

Boundary conditions

$$u_x^* = 0 \text{ at } z^* = 0$$

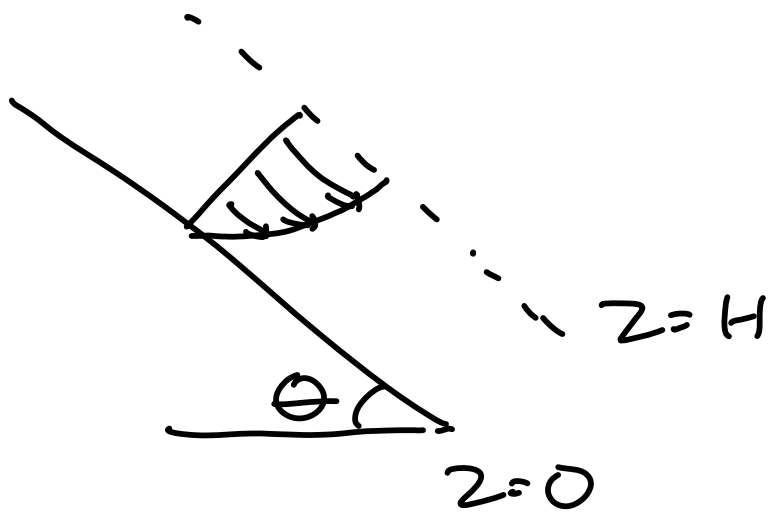
$$\frac{du_x^*}{dz^*} = 0 \text{ at } z^* = 1$$



Steady solution:

$$\frac{\partial^2 u_x^*}{\partial z^{*2}} + 1 = 0 \quad ; \quad u_x^* = z^* - \frac{z^{*2}}{2}$$

$$u_x = \frac{u_x^* (H^2 g \sin \theta)}{N} = \frac{g \sin \theta}{N} \left(zH - \frac{z^2}{2} \right)$$



$$\frac{\partial U_x^*}{\partial t^*} = \frac{\partial^2 U_x^*}{\partial z^{*2}} + 1$$

B.C. $U_x^* = 0$ at $z^* = 0$
 $\frac{dU_x^*}{dz} = 0$ at $z^* = 1$

Initial condition
 At $t^* = 0$, $U_x^* = 0$ for all z^*

$$U_x^* = U_{xs}^* + U_{xt}^*$$

$$\frac{\partial^2 U_{xs}^*}{\partial z^{*2}} + 1 = 0$$

$$U_{xs}^* = z^* - \frac{z^{*2}}{2}$$

$$\frac{\partial U_{xt}^*}{\partial t^*} = \frac{\partial^2 U_{xt}^*}{\partial z^{*2}}$$

BC $U_{xt}^* = 0$ at $z^* = 0$

$$\frac{dU_{xt}^*}{dz^*} = 0$$
 at $z^* = 1$

IC $U_{xt}^* = -U_{xs}^*$ at $t^* = 0$

$$\frac{\partial U_{xt}^*}{\partial t^*} = \frac{\partial^2 U_{xt}^*}{\partial z^{*2}}$$

$$\text{BC: } U_{xt}^* = 0 \text{ at } z^* = 0$$

$$\frac{dU_{xt}^*}{dz^*} = 0 \text{ at } z^* = 1$$

$$\text{IC: } U_{xt}^* = -U_{xs}^* \\ = -(z^* - z^{*2}/2) \\ \text{at } t^* = 0$$

$$u_{xt}^* = \Theta(t) Z(z^*)$$

$$Z(z^*) \frac{\partial \Theta}{\partial t} = \Theta \frac{\partial^2 Z}{\partial z^{*2}}$$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t} = \frac{1}{Z} \frac{\partial^2 Z}{\partial z^{*2}}$$

$$\frac{1}{Z} \frac{\partial^2 Z}{\partial z^{*2}} = -\beta_n^2$$

$$Z = A \sin(\beta_n z^*) + B \cos(\beta_n z^*)$$

$$\text{At } z^* = 0, Z = 0 \Rightarrow B = 0$$

$$\text{At } z^* = 1, \frac{dZ}{dz^*} = 0$$

$$\beta_n = (\pi/2), (3\pi/2), (5\pi/2), \dots$$

$$= \frac{(2n+1)\pi}{2}$$

$$Z = A \sin\left(\frac{(2n+1)\pi z^*}{2}\right)$$

$$\frac{1}{\Theta} \frac{d\Theta}{dt^*} = -\beta_n^2 = -\left(\frac{(2n+1)\pi}{2}\right)^2$$

$$\Theta = e^{-\left(\frac{(2n+1)\pi}{2}\right)^2 t^*}$$

$$U_{xt}^* = \sum_{n=0}^{\infty} A_n \sin\left(\frac{(2n+1)\pi z^*}{2}\right) e^{-\left(\frac{(2n+1)\pi}{2}\right)^2 t^*}$$

$$S_n = \sin\left(\frac{(2n+1)\pi z^*}{2}\right)$$

$$\langle S_n, S_m \rangle = \int_0^1 dz^* S_n S_m = \frac{\delta_{mn}}{2}$$

$$\text{At } t^* = 0$$

$$u_{xt}^* = \sum A_n \sin\left(\frac{(2n+1)\pi z^*}{2}\right)$$

$$= \sum A_n S_n = -(z^* - z^{*2}/2)$$

$$\sum A_n \langle S_n, S_m \rangle = -\langle (z^* - z^{*2}/2), S_m \rangle$$

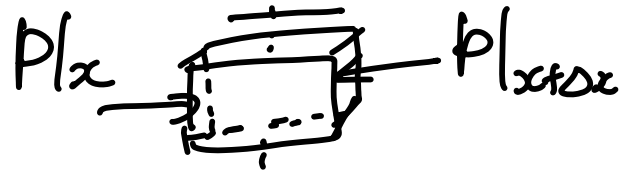
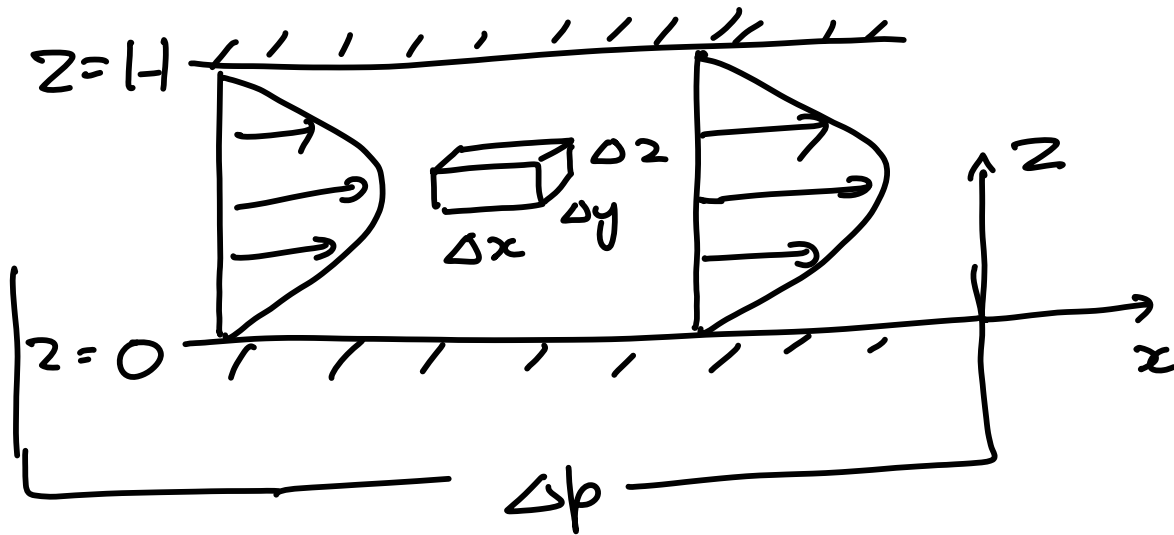
$$\sum A_n \frac{\delta_{mn}}{2} = -\int dz^* (z^* - z^{*2}/2) \sin\left(\frac{(2m+1)\pi z^*}{2}\right)$$

$$\frac{A_m}{2} = \frac{1}{\pi^3 \left(\frac{2m+1}{2}\right)^3}$$

$$A_m = \frac{-2}{\pi^3 \left(\frac{2m+1}{2}\right)^3}$$

$$u_{xt}^* = \sum_{n=0}^{\infty} -\frac{2}{\pi^3 \left(\frac{2n+1}{2}\right)^3} \sin\left(\frac{(2n+1)\pi z^*}{2}\right) e^{-\left(\frac{(2n+1)\pi}{2}\right)^2 t^*}$$

Pressure driven flow in a channel:



$$\tau_{xz} = \mu \frac{du_x}{dz}$$

= Force in x direction
at surface with
normal in z direction

$$\left(\text{Rate of change of momentum} \right) = \left(\text{Sum of forces} \right)$$

$$\frac{\rho u_x(x, y, z, t + \Delta t) - u_x(x, y, z, t) \Delta x \Delta y \Delta z}{\Delta t} =$$

$$\begin{aligned} & (\tau_{xz}|_{z+\Delta z}) \Delta x \Delta y - \tau_{xz}|_z \Delta x \Delta y \\ & + (p|x \Delta y \Delta z) - p|x+\Delta x (\Delta y \Delta z) \end{aligned}$$

Divide by $\Delta x \Delta y \Delta z$

$$\frac{\rho(u_x|_{t+\Delta t} - u_x|_t)}{\Delta t} = \frac{\rho|_x - \rho|_{x+\Delta x}}{\Delta x} + \frac{\tau_{xz}|_{z+\Delta z} - \tau_{xz}|_z}{\Delta z}$$

$$\rho \frac{\partial u_x}{\partial t} = - \frac{\partial p}{\partial x} + \frac{\partial \tau_{xz}}{\partial z}$$

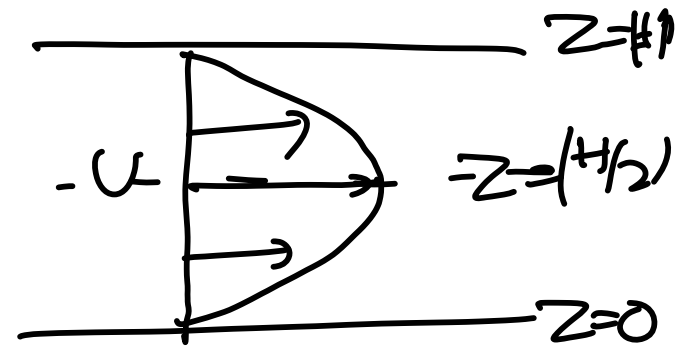
$$\tau_{xz} = \mu \frac{\partial u_x}{\partial z}$$

$$\rho \frac{\partial u_x}{\partial t} = - \frac{\partial p}{\partial x} + \mu \frac{\partial^2 u_x}{\partial z^2}$$

$$\frac{\partial u_x}{\partial t} = - \frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \frac{\partial^2 u_x}{\partial z^2}$$

At steady state,

$$-\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \frac{\partial^2 u_x}{\partial z^2} = 0$$



B.C:

$$u_x^* = 0 \text{ at } z = 0$$

$$u_x^* = 0 \text{ at } z = H$$

$$z^* = (z/H)$$

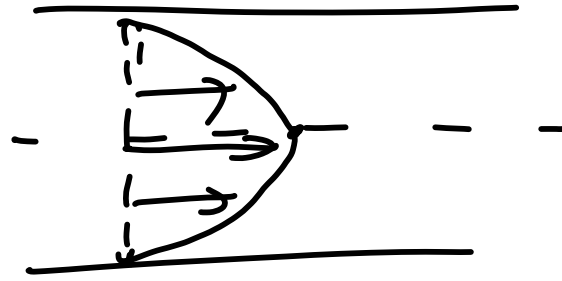
$$-\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\nu}{H^2} \frac{\partial^2 u_x}{\partial z^{*2}} = 0$$

$$-1 + \left(\frac{\mu}{H^2}\right) \left(\frac{\partial p}{\partial x}\right)^{-1} \frac{\partial^2 u_x}{\partial z^{*2}} = 0$$

$$u_x^* = \left(\frac{\mu u_x}{H^2}\right) \left(\frac{\partial p}{\partial x}\right)^{-1}$$

$$u_x \sim \left(\frac{\partial p}{\partial x}\right) \left(\frac{H^2}{\mu}\right)$$

$$\frac{d^2 u_x^*}{dz^{*2}} - 1 = 0$$



B.C.

$$u_x^* = 0 \text{ at } z^* = 0$$

$$u_x^* = 0 \text{ at } z^* = 1$$

$$u_x^* = \frac{z^{*2}}{2} + C_1 z^* + C_2$$

$$u_x^* = \left(\frac{z^{*2}}{2} - \frac{z^*}{2} \right)$$

$$u_x = \left(\frac{dp}{dx} \right) \left(\frac{H^2}{\mu} \right) \left(\frac{z^{*2}}{2} - \frac{z^*}{2} \right)$$

$$= \frac{-1}{2\mu} \left(\frac{dp}{dx} \right) z (z-H)$$

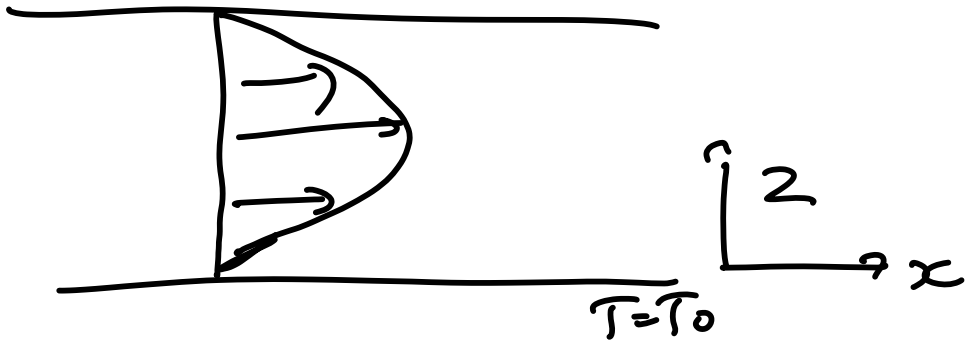
'Plane Poiseuille flow'

Maximum velocity at $z = H/2$

$$U_x = -\frac{1}{2\mu} \left(\frac{dp}{dx} \right) \frac{H^2}{4} = U$$

$$U_x = 4U \left(\frac{z}{H} - \left(\frac{z}{H} \right)^2 \right)$$

Viscous heating in the channel
 $T = T_0$



$$S_e = \tau_{xy} \frac{du_x}{dy}$$

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial z^2} + \frac{S_e}{\rho C_p} \quad \left| \begin{array}{l} z^* = (z/H) \\ T^* = \left(\frac{T - T_0}{T_0} \right) \end{array} \right.$$

$$T = T_0 \text{ at } z = 0$$

$$= T_0 \text{ at } z = H$$

Steady state $\frac{\partial T}{\partial t} = 0$

$$k \frac{\partial^2 T}{\partial z^2} + S_e = 0$$

$$S_e = \tau_{xz} \left(\frac{du_x}{dz} \right) = \mu \left(\frac{du_x}{dz} \right)^2$$

$$u_x = 4U \left(\frac{z}{H} - \left(\frac{z}{H} \right)^2 \right)$$

$$\Rightarrow \frac{du_x}{dz} = \frac{4U}{H} \left[1 - \frac{2z}{H} \right]$$

$$S_e = \frac{16U^2}{H^2} \left[1 - \frac{2z}{H} \right]^2 = \frac{16U^2}{H^2} (1 - 2z^*)^2$$

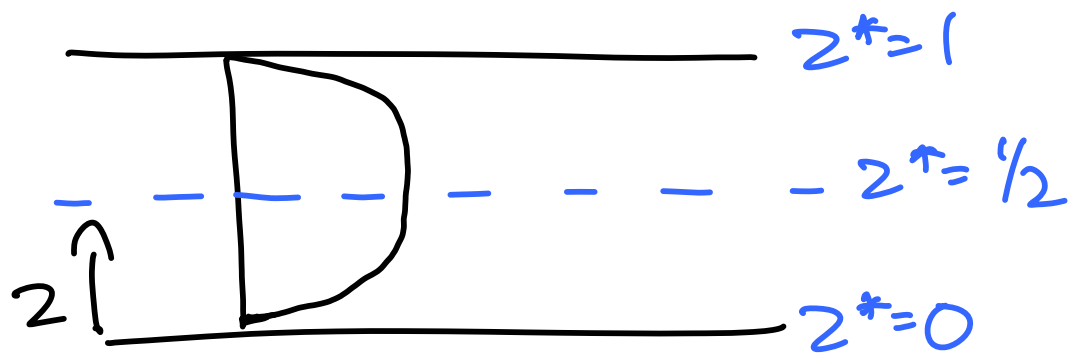
$$k \frac{\partial^2 T}{\partial z^2} + \frac{16U^2}{H^2} (1 - 2z^*)^2 = 0$$

$$\frac{kT_0}{H^2} \frac{d^2 T^*}{dz^{*2}} + \frac{16\mu U^2}{H^2} (1 - 2z^*)^2 = 0$$

$$\frac{d^2 T^*}{dz^{*2}} + 16 Br (1 - 2z^*)^2 = 0$$

$$Br = \left(\frac{\mu U^2}{kT_0} \right)$$

$$T^* = Br \left(\frac{8z^*(1-2z^*)(1-2z^*+2z^{*2})}{3} \right)$$



$$q_z = -k \frac{dT}{dz} = -\frac{kT_0}{H} \frac{dT^*}{dz^*}$$

$$= -\frac{8kT_0}{3H} (1-2z^*)^3 Br$$

$$= -\frac{8\mu U^2}{3H} (1-2z^*)^3$$

$$q_z = \frac{8\mu U^2}{3H} \ll \text{Flux due to temperature difference}$$

$$q_2 = \frac{k \Delta T}{\Delta z} \quad \frac{\mu U^2}{3H} \ll \frac{k \Delta T}{hw}$$

$$\Delta T \gg \left(\frac{\mu U^2 hw}{Hk} \right)$$

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial z^2} + S$$

$$S = -kC \quad \left(\begin{array}{l} \text{if } C \text{ is concentration} \\ \text{of a reactant} \end{array} \right)$$

$$= +kC \quad \left(\begin{array}{l} \text{if } C \text{ is the concentration} \\ \text{of a product} \end{array} \right)$$

$$\text{Steady state} \quad D \frac{\partial^2 C}{\partial z^2} - kC = 0$$

$$\frac{\partial^2 C}{\partial z^2} - \frac{k}{D} C = 0$$

$$C^* = (C/C_0); \quad z^* = z \left(\frac{k}{D} \right)^{1/2}$$

Penetration
depth

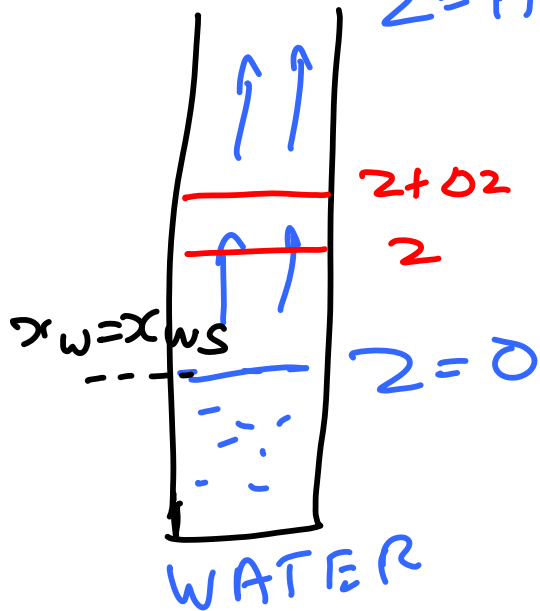
$$\frac{\partial^2 C^*}{\partial z^{*2}} - C^* = 0$$

Multicomponent diffusion:

Dry air $x_w=0$ $z=H$

$$j_w = -\bar{D} \frac{d\bar{c}_w}{dz} + x_w (j_w + j_{air})$$

$$= -D C \frac{dx_w}{dz} + x_w (j_w + j_{air})$$



Total mean flow
 $= (j_w + j_{air})$

$$(1-x_w) j_w = -D C \frac{dx_w}{dz}$$

$$j_w = \frac{-D C}{1-x_w} \frac{dx_w}{dz}$$

At steady state, $j_w|_{z+\delta z} - j_w|_z = 0$

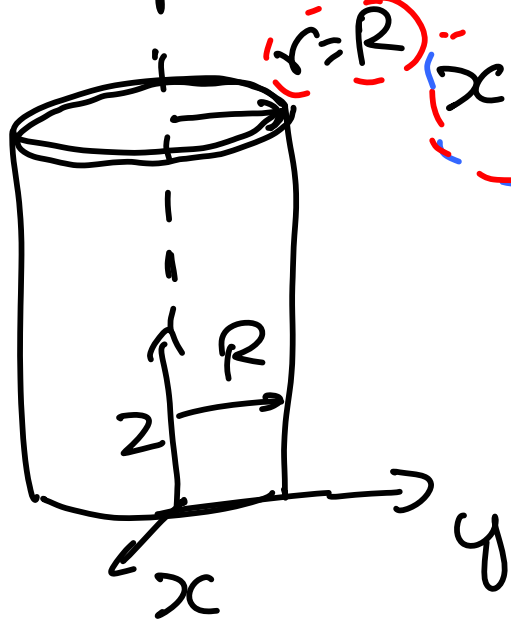
$$\frac{d f_w}{d z} = 0$$

$$\frac{d}{d z} \left(\frac{1}{1-x_w} \frac{d x_w}{d z} \right) = 0$$

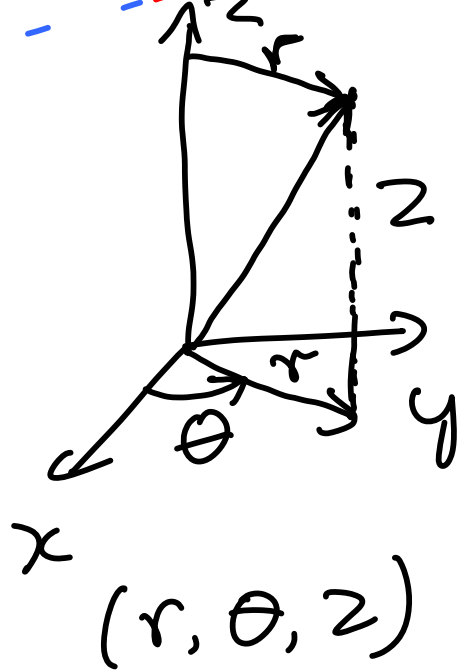
$$-\log(1-x_w) = A_1 z + A_2$$

$$\frac{(1-x_w)}{(1-x_{ws})} = \left(\frac{1}{1-x_{ws}} \right)^{z/H}$$

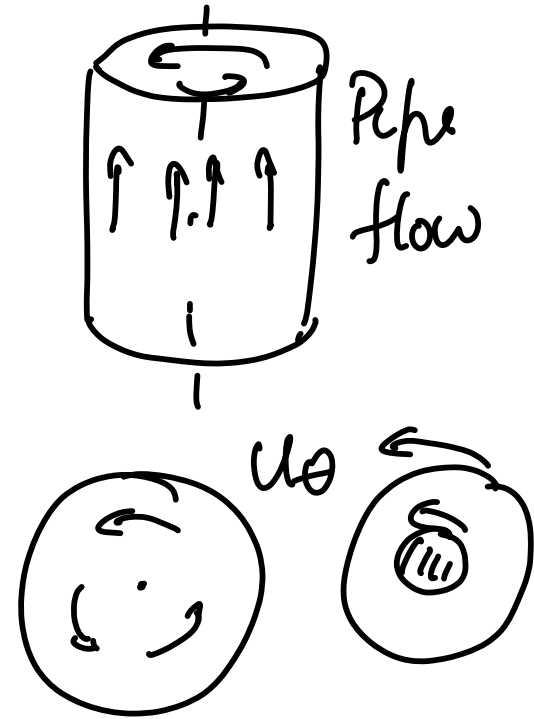
Transport in cylindrical coordinates:



$$r=R$$
$$x^2 + y^2 = R^2$$



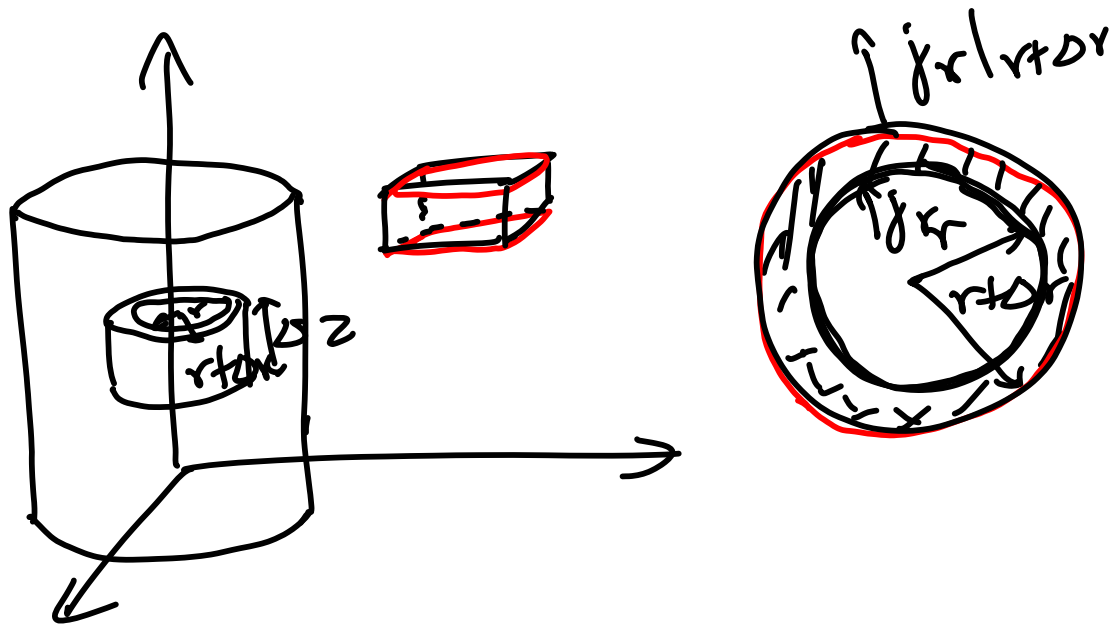
$$(r, \theta, z)$$



$$r = \sqrt{x^2 + y^2}$$

$$z = z$$

$$\tan \theta = (y/x)$$



Mass balance:

$$\left(\text{Accumulation of mass in time } \Delta t \right) = \left(\text{Input of mass} \right) - \left(\text{Output of mass} \right) + \text{Sources}$$

$$\left(\text{Accumulation of mass in time } \Delta t \right) = \left[c(r, z, t + \Delta t) - c(r, z, t) \right] 2\pi r \Delta r \Delta z$$

$$\left(\text{Input of mass} \right)_{\text{at } r} = \left(j_r 2\pi r \Delta z \right) \Big|_r \Delta t$$

$$\left(\text{Output of mass at } r+\Delta r \right) = \left(j_r 2\pi r \Delta z \right) \Big|_{r+\Delta r} \Delta t$$

$$\left(\text{Source of mass} \right) = S (2\pi r \Delta r \Delta z) \Delta t$$

$$\begin{aligned} & [c(r, z, t+\Delta t) - c(r, z, t)] 2\pi r \Delta r \Delta z \\ &= \left(j_r 2\pi r \Delta z \right) \Big|_r \Delta t - \left(j_r 2\pi r \Delta z \right) \Big|_{r+\Delta r} \Delta t \\ &+ S (2\pi r \Delta r \Delta z \Delta t) \end{aligned}$$

Divide by $2\pi r \Delta r \Delta z \Delta t$

$$\frac{C(r, z, t + \Delta t) - C(r, z, t)}{\Delta t} =$$

$$\frac{1}{r} \frac{1}{\Delta r} \left[(r j_r)|_r - (r j_r)|_{r+\Delta r} \right] + S$$

$$\frac{\partial C}{\partial t} = -\frac{1}{r} \frac{\partial}{\partial r} (r j_r) + S$$

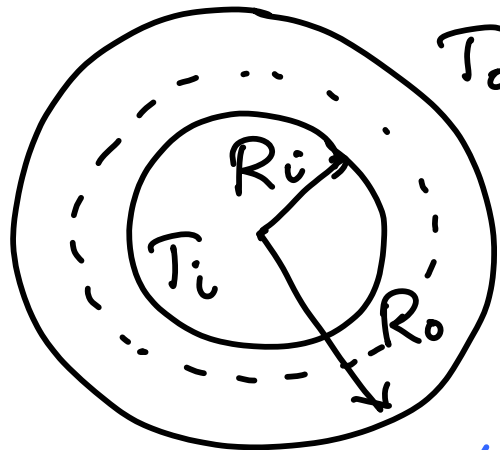
$$j_r = -D \frac{\partial C}{\partial r}$$

$$\frac{\partial C}{\partial t} = D \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial C}{\partial r} \right) \right) + S$$

$$\frac{\partial T}{\partial t} = \alpha \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) \right) + \frac{S_e}{\rho C_p}$$

$$\frac{\partial u_\theta}{\partial t} = \nu \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_\theta}{\partial r} \right) \right) + \frac{f_\theta}{\rho} - \frac{\nu u_\theta}{r^2}$$

Steady diffusion:



$$\alpha \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) \right) = 0$$

$$r^* = (r / R_i)$$

$$T^* = \left(\frac{T - T_i}{T_o - T_i} \right)$$

At $r^* = 1$; $T^* = 0$

At $r^* = (R_o / R_i)$; $T^* = 1$

$$\frac{1}{r^*} \frac{d}{dr^*} \left(r^* \frac{\partial T^*}{\partial r^*} \right) = 0$$

$$r^* \frac{\partial T^*}{\partial r^*} = C_1$$

$$\frac{\partial T^*}{\partial r^*} = \frac{C_1}{r^*} \Rightarrow T^* = C_1 \log(r^*) + C_2$$

$$T^* = \frac{\log(r^*)}{\log(R_0/R_i)}$$

$$\frac{T - T_i}{T_0 - T_i} = \frac{\log(r/R_i)}{\log(R_0/R_i)}$$

$$q_r = -k \frac{\partial T}{\partial r} = -\frac{k(T_0 - T_i)}{R_i} \frac{\partial T^*}{\partial r^*}$$

$$= \frac{-k(T_o - T_i)}{R_i r \log(R_o/R_i)} = \frac{-k(T_o - T_i)}{r \log(R_o/R_i)}$$

$$Q = (2\pi r L) \left[\frac{-k(T_o - T_i)}{r \log(R_o/R_i)} \right]$$

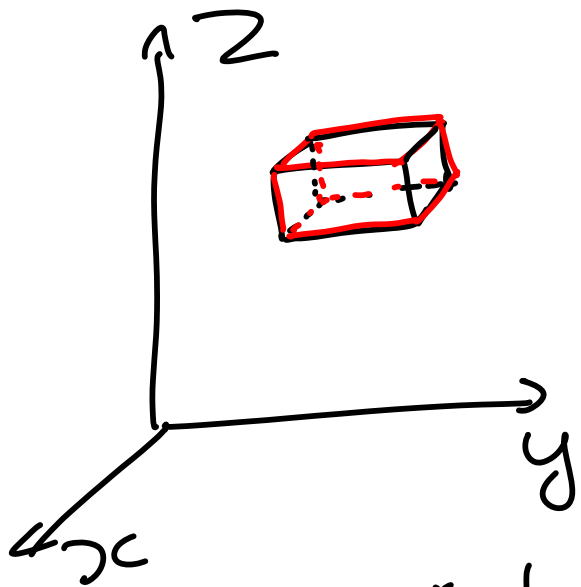
$$= \frac{-k(T_o - T_i)(2\pi L)}{\log(R_o/R_i)}$$

$$Q = \frac{-k(T_o - T_i) A_L}{(R_o - R_i)}$$

$$A_L = \frac{(2\pi L)(R_o - R_i)}{\log(R_o/R_i)} \quad \left| \quad r_L = \frac{R_o - R_i}{\log(R_o/R_i)} \right.$$

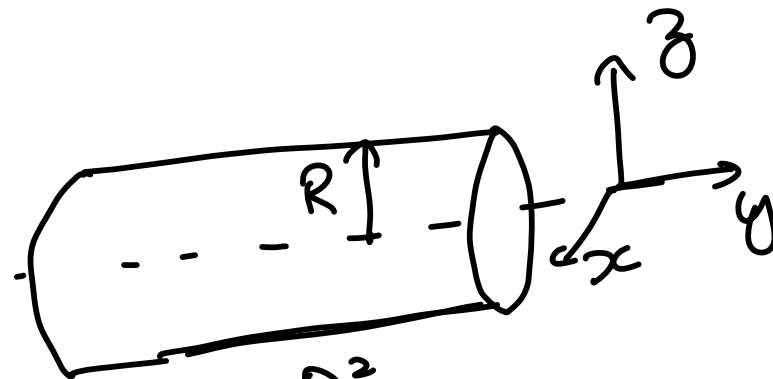
Cylindrical co-ordinate system:

Curvilinear co-ordinate systems

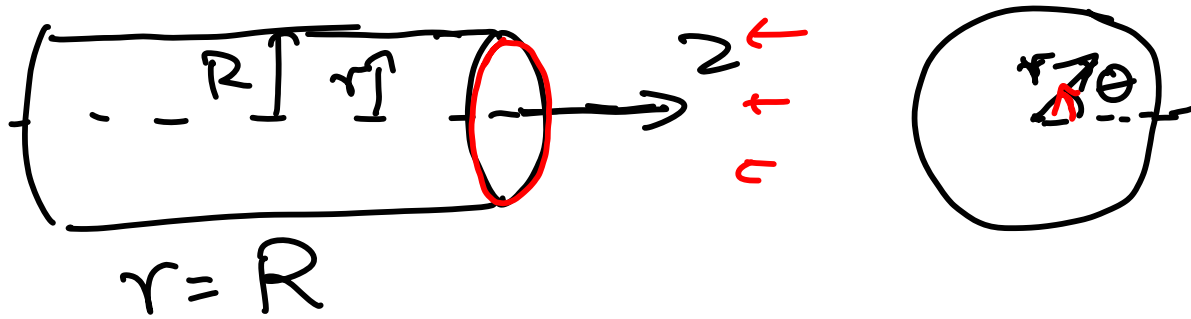


$$T^* = 0 \text{ at } z^* = 1$$
$$T^* = 1 \text{ at } z^* = 0$$

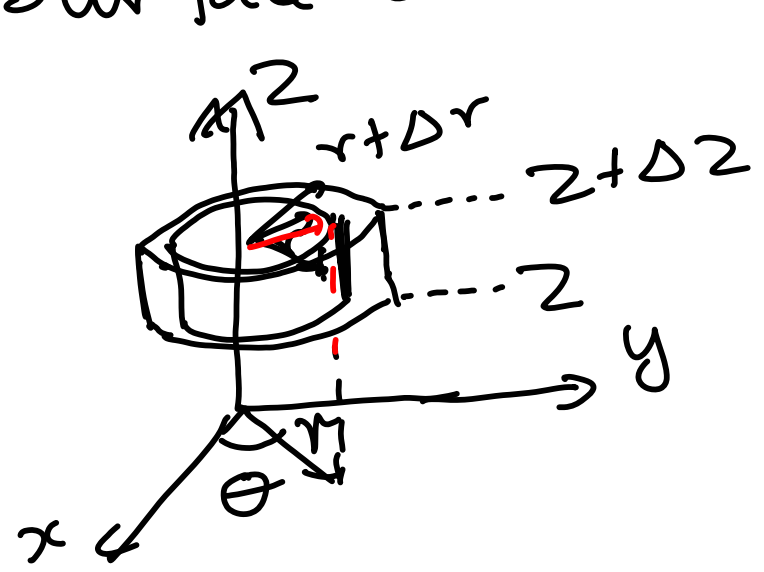
$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial z^2}$$



$$x^2 + z^2 = R^2$$
$$T^* = 1 \text{ at } x^2 + y^2 = R^2$$



Surface of constant r



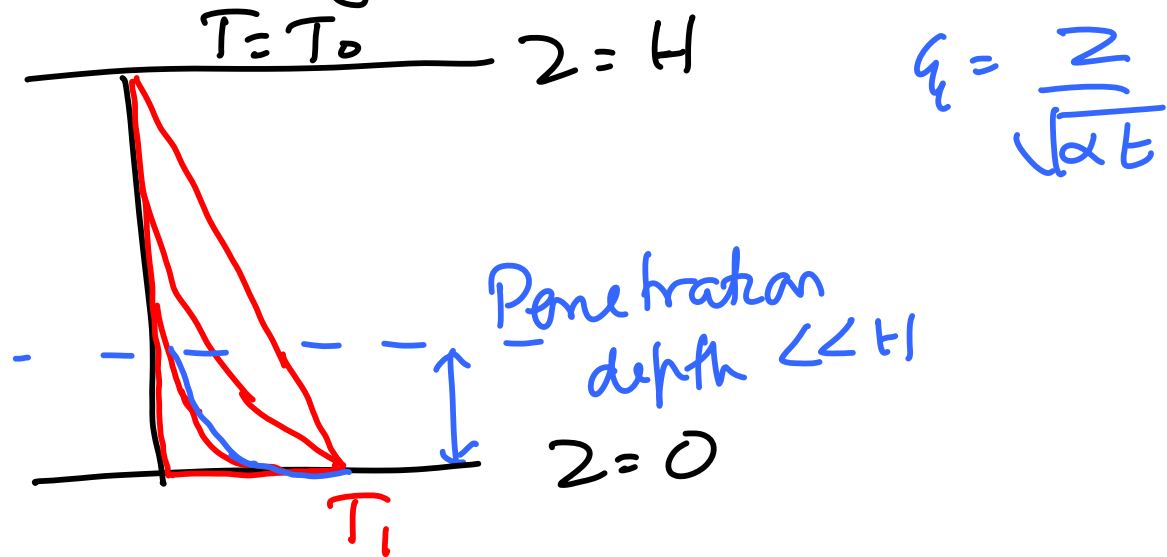
$$x = r \cos \theta$$

$$y = r \sin \theta$$

$$r = \sqrt{x^2 + y^2}$$

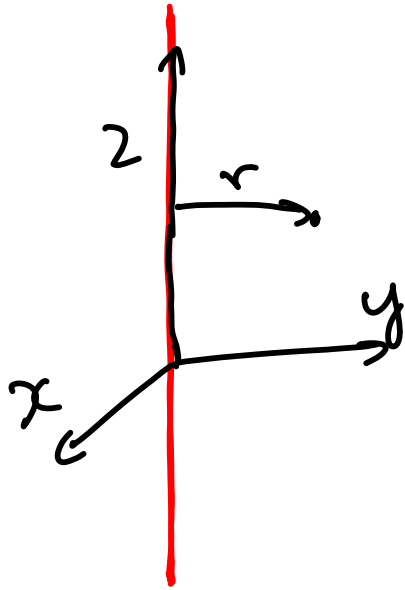
$$\tan \theta = \left(\frac{y}{x} \right)$$

Unsteady diffusion in cylindrical co-ordinates:



At $t = 0$, $T = T_1$ at $z = 0$
 $T = T_0$ for $z > 0$

$T = T_0$ as $z \rightarrow \infty$
 $T = T_1$ at $z = 0$



$$T = T_0$$

$$\text{as } r \rightarrow \infty$$

At $t = 0$, $T = T_0$ everywhere

B.C. $T = T_0$ as $r \rightarrow \infty$

~~$$q_r = -k \frac{\partial T}{\partial r}$$~~

At $r \rightarrow 0$

$$q_r (2\pi r L) = Q$$

$$\frac{\partial T}{\partial t} = \alpha \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) \right)$$

$$T^* = \left(\frac{T - T_0}{t_0} \right)$$

$$\frac{\partial T^*}{\partial t} = \alpha \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T^*}{\partial r} \right) \right)$$

Boundary conditions

$T^* = 0$ as $r \rightarrow \infty$ for all t

$(q_r \cdot 2\pi r L) = Q$ as $r \rightarrow 0$

Initial condition

$T^* = 0$ at $t = 0$ for $r > 0$

$$\frac{\partial T^*}{\partial t} = \alpha \left[\frac{\partial^2 T^*}{\partial r^2} + \frac{1}{r} \frac{\partial T^*}{\partial r} \right]$$

$$\xi_4 = \frac{r}{\sqrt{\alpha t}}$$

$$\frac{\partial T^*}{\partial t} = \left(\frac{\partial \xi_4}{\partial t} \right) \left(\frac{\partial T}{\partial \xi_4} \right)$$

$$= \frac{-r}{2\sqrt{\alpha t}^3} \left(\frac{\partial T}{\partial \xi_4} \right)$$

$$= -\frac{\xi_4}{2t} \frac{\partial T}{\partial \xi_4}$$

$$\frac{\partial T^*}{\partial r} = \left(\frac{\partial \xi_4}{\partial r} \right) \left(\frac{\partial T}{\partial \xi_4} \right)$$

$$= \frac{1}{\sqrt{\alpha t}} \left(\frac{\partial T}{\partial \xi_4} \right)$$

$$\frac{\partial^2 T^*}{\partial r^2} = \frac{1}{\alpha t} \left(\frac{\partial^2 T}{\partial \xi_4^2} \right)$$

$$\frac{1}{r} \frac{\partial T^*}{\partial r} = \frac{1}{r} \frac{1}{\sqrt{\alpha t}} \frac{\partial T^*}{\partial \xi_4}$$

$$= \frac{1}{\alpha t} \left(\frac{1}{\xi_4} \frac{\partial T^*}{\partial \xi_4} \right)$$

$$-\frac{\xi_4}{2t} \frac{\partial T^*}{\partial \xi_4} = \frac{\alpha}{\alpha t} \left(\frac{\partial^2 T^*}{\partial \xi_4^2} + \frac{1}{\xi_4} \frac{\partial T^*}{\partial \xi_4} \right)$$

$$\left(\frac{\partial^2 T^*}{\partial \zeta^2} \right) + \left(\frac{1}{\zeta} + \frac{\zeta}{2} \right) \left(\frac{\partial T}{\partial \zeta} \right) = 0 \quad \frac{\partial^2 T^*}{\partial \zeta^2} + \frac{\zeta}{2} \frac{\partial T}{\partial \zeta} = 0$$

Boundary conditions:

$$T^* = 0 \text{ as } r \rightarrow \infty \text{ or } \zeta \rightarrow \infty$$

$$2\pi r L q_r = Q \text{ as } r \rightarrow 0$$

Initial condition

$$T^* = 0 \text{ at } t = 0 \text{ or } \zeta \rightarrow \infty$$

$$\frac{\partial T^*}{\partial \zeta} = \frac{C}{\zeta} e^{-\zeta^2/4}$$

$$T^* = \int_{\infty}^{\zeta} \frac{C}{\zeta'} e^{-\zeta'^2/4} d\zeta'$$

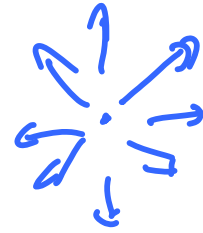
$$\begin{aligned}
 q_r &= -k \frac{\partial T}{\partial r} \\
 &= -k \frac{\partial \psi}{\partial r} \frac{\partial T}{\partial \psi} \\
 &= -k \frac{1}{\sqrt{\alpha t}} \frac{C}{\psi} e^{-\psi^2/4} \\
 &= -\frac{k}{r} C e^{-\psi^2/4}
 \end{aligned}$$

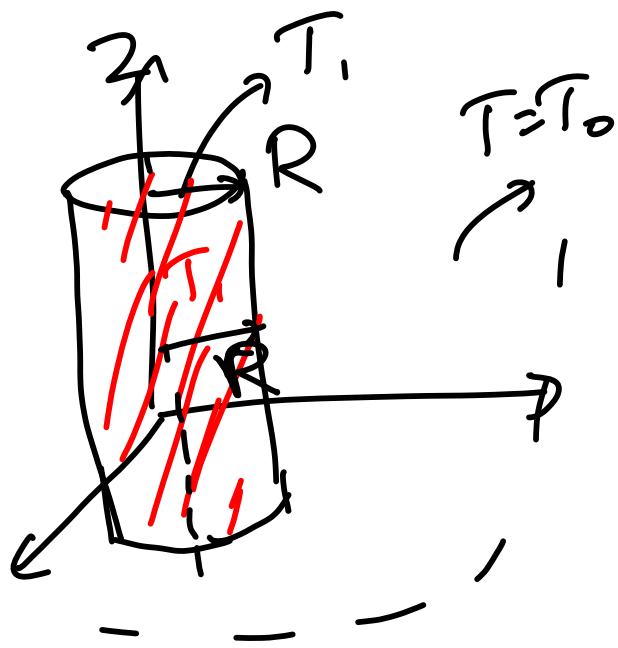
$$Q = 2\pi r L q_r = -k C (2\pi L) e^{-\psi^2/4}$$

for $r \rightarrow 0$ or $\psi \rightarrow 0$

$$C = \frac{-Q}{2\pi k L} \frac{r}{\sqrt{\alpha t}}$$

$$T^* = -\frac{Q}{2\pi k L} \int_{\infty}^{\psi} d\psi' \frac{1}{\psi'} e^{-\psi'^2/4}$$





Boundary conditions:

$$T = T_0 \text{ at } r = R$$

$$\frac{\partial T}{\partial r} = 0 \text{ at } r = 0 \text{ 'Symmetry'}$$

Initial condition

$$T = T_1 \text{ for all } r < R \text{ at } t = 0$$

$$r^* = (r/R)$$

$$t^* = \frac{t}{(R^2/\alpha)}$$

$$T^* = \left(\frac{T - T_0}{T_1 - T_0} \right)$$

$$\frac{\partial T}{\partial t} = \alpha \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right)$$

$$\frac{\partial T^*}{\partial t^*} = \frac{\alpha}{R^2} \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial T^*}{\partial r^*} \right)$$

$$\frac{\partial T^*}{\partial t^*} = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial T^*}{\partial r^*} \right)$$

Boundary conditions

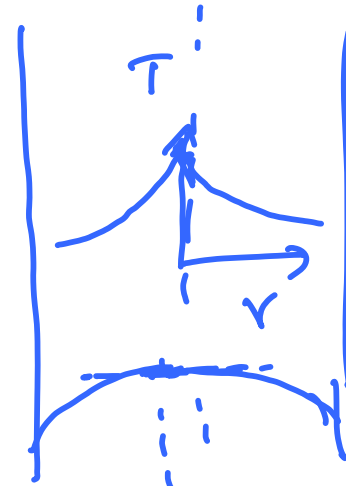
$$T = T_0 \text{ at } r = R \Rightarrow T^* = 0 \text{ at } r^* = 1$$

$$\frac{\partial T}{\partial r} = 0 \text{ at } r = 0 \Rightarrow \frac{\partial T^*}{\partial r^*} = 0 \text{ at } r^* = 0$$

Initial condition:

$$T = T_i \text{ at } t = 0 \text{ for } r < R$$

$$T^* = 1 \text{ at } t^* = 0 \text{ for } r^* < 1$$



$$\frac{\partial T^*}{\partial r^*} = 0$$



$$T^* = R(r^*) \Theta(t^*)$$

$$\frac{\partial}{\partial t^*} (R \Theta) = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial}{\partial r^*} (R \Theta) \right)$$

$$R \frac{\partial \Theta}{\partial t^*} = \Theta \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial R}{\partial r^*} \right)$$

Divide by $R \Theta$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t} = \frac{1}{R} \left(\frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial R}{\partial r^*} \right) \right)$$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t} = -\beta^2$$

$$\frac{1}{R} \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial R}{\partial r^*} \right) = \beta^2$$

$$\frac{d^2 R}{dr^{*2}} + \frac{1}{r^*} \frac{\partial R}{\partial r^*} + \beta^2 R = 0$$

$$r^{*2} \frac{d^2 R}{dr^{*2}} + r^* \frac{\partial R}{\partial r^*} + \beta^2 r^{*2} R = 0$$

$$(r^+ = \beta r^{*})$$

$$r^{+2} \frac{d^2 R}{dr^{+2}} + r^+ \left(\frac{\partial R}{\partial r^+} \right) + r^{+2} R = 0$$

'Bessel eqn.'

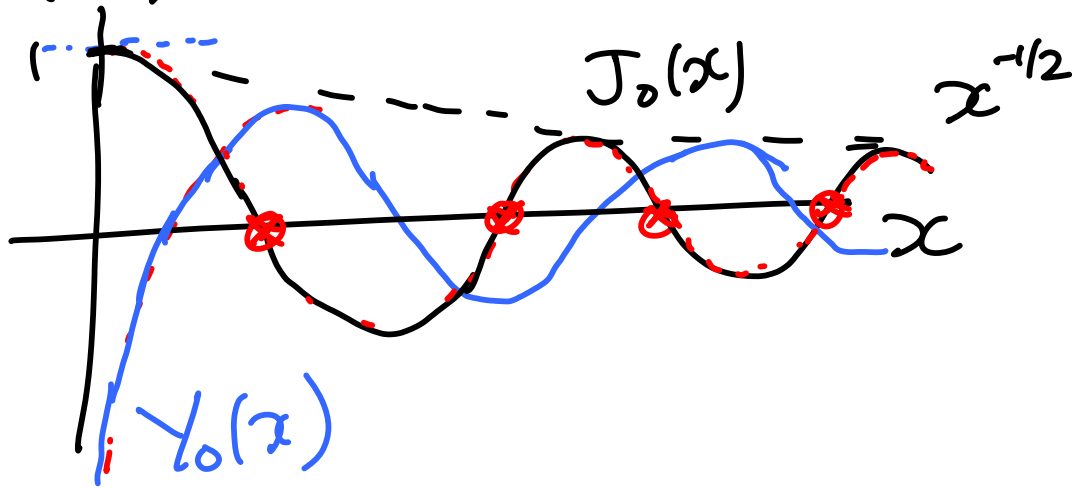
Bessel functions:

$$x^2 \frac{d^2 y}{dx^2} + x \frac{dy}{dx} + (x^2 - n^2)y = 0$$

$$y = A_1 \underline{J}_n(x) + A_2 \underline{Y}_n(x)$$

$$\frac{d^2 y}{dx^2} + y = 0 \Rightarrow y = A \sin x + B \cos x$$

$$R(r^*) = C_1 J_0(r^*) + C_2 Y_0(r^*)$$



$C_2 = 0$ to satisfy BC
at $r^* = 0$

$$R(r^*) = C_1 J_0(r^*)$$

$$R(r^*) = C_1 J_0(\beta r^*)$$

B.C $T^* = 0$ at $r^* = 1 \Rightarrow R(r^*) = 0$
at $r^* = 1$

$$R(r^*) = C_1 J_0(\beta r^*) \Rightarrow C_1 J_0(\beta) = 0$$

Discrete set of β at which
 $J_0(\beta) = 0$

$$\beta_1 = 2.40483 \quad R = C_1 J_0(\beta_n r^*)$$

$$\beta_2 = 5.52008$$

$$\beta_3 = 8.65373$$

$$\beta_4 = 11.79150$$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t^*} = -\beta_n^2$$

$$\Theta = e^{-\beta_n^2 t^*}$$

$$T^* = R \Theta = \sum_{n=1}^{\infty} C_n J_0(\beta_n r^*) e^{-\beta_n^2 t^*}$$

$$\text{At } t^* = 0, T^* = 1$$

$$\sum_{n=1}^{\infty} C_n J_0(\beta_n r^*) = 1$$

$$\int_0^1 r^* dr^* J_0(\beta_n r^*) J_0(\beta_m r^*)$$

$$= 0 \text{ for } n \neq m$$

$$= \frac{1}{2} (J_1(\beta_n))^2 \text{ for } n = m$$

$$\langle S_n, S_m \rangle = \int_0^1 dz^* \sin(n\pi z^*) \sin(m\pi z^*)$$

$$= \frac{1}{2} \delta_{nm}$$

$$\langle J_n, J_m \rangle = \int_0^1 r^* dr^* J_0(\beta_n r^*) J_0(\beta_m r^*)$$

$$= \frac{1}{2} (J_1(\beta_n))^2 \delta_{mn}$$

$$\sum_{n=1}^{\infty} C_n J_0(\beta_n r^*) = 1$$

$$\sum_{n=1}^{\infty} C_n \int_0^1 r^* dr^* J_0(\beta_n r^*) J_0(\beta_m r^*) = \int_0^1 J_0(\beta_m r^*) r^* dr^*$$

$$\sum_{n=1}^{\infty} C_n \delta_{mn} (J_1(\beta_n))^2 = \frac{J_1(\beta_m)}{\beta_m}$$

$$C_m = \frac{2}{\beta_m J_1(\beta_m)}$$

$$T^* = \sum C_n J_n \left(e^{-\beta_n^2 t^*} \right)$$

$$\text{At } t^* = 0, T^* = 1$$

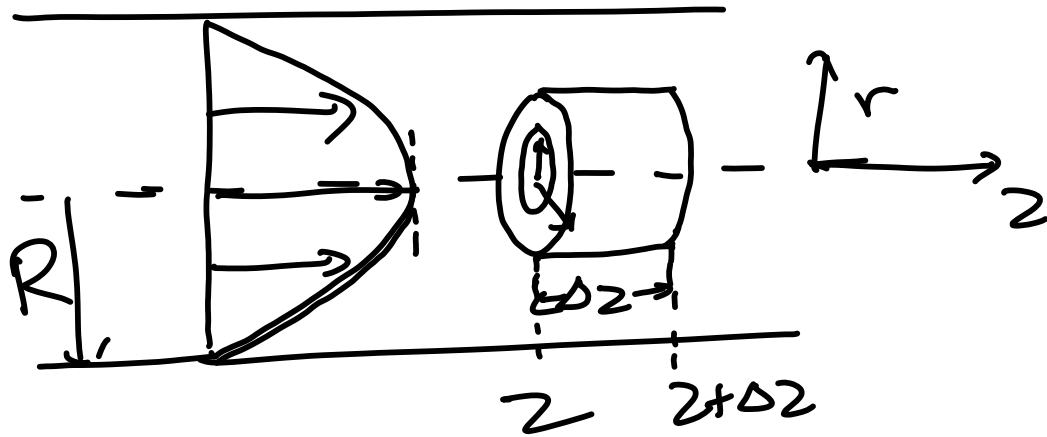
$$\sum_{n=1}^{\infty} C_n J_n = 1$$

$$\sum_{n=1}^{\infty} C_n \langle J_n, J_m \rangle = \langle 1, J_m \rangle$$

$$\sum_{n=1}^{\infty} C_n \frac{1}{2} \left(J_0(\beta_n) \right)^2 \delta_{mn} = \langle 1, J_m \rangle$$

$$C_m \left[\frac{1}{2} J_0(\beta_m) \right]^2 = \int r^* dr^* J_0(\beta_m r^*)$$

Flow in a pipe:

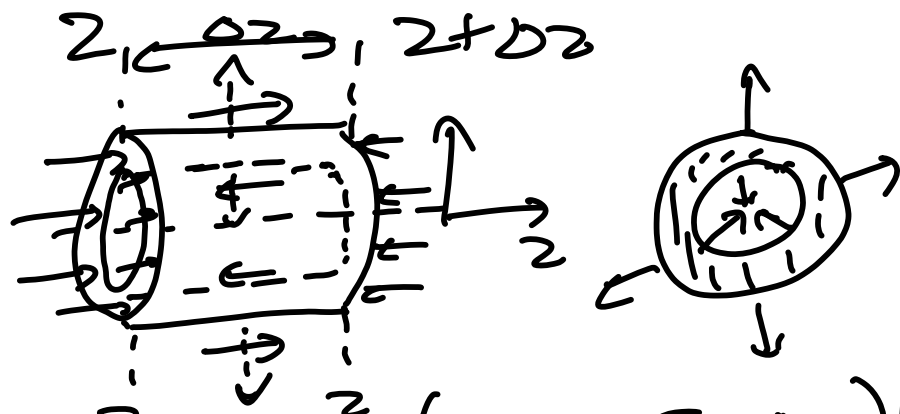


$$\text{At } r=R \quad u_2=0$$

$$\text{At } r=0 \quad \frac{\partial u_2}{\partial r}=0$$

$$\left(\text{Rate of change of momentum} \right) = \left(\text{Sum of applied forces} \right)$$

$$\frac{\int \rho u_2(r, z, t + \Delta t) - \int \rho u_2(r, z, t)}{\Delta t} (2\pi r \Delta r \Delta z)$$



$$\text{Shear forces} = (\tau_{zr} 2\pi r \Delta z)|_{r+\Delta r} - (\tau_{zr} 2\pi r \Delta z)|_r$$

τ_{zr} = Force in z direction
at surface with unit
normal in r-direction

$$\text{Pressure forces} = (p 2\pi r \Delta r)|_z - (p 2\pi r \Delta r)|_{z+\Delta z}$$

$$\frac{[\rho u_z(r, z, t + \Delta t) - \rho u_z(r, z, t)] 2\pi r \Delta r \Delta z}{\Delta t}$$

$$= (\tau_{zr} 2\pi r \Delta z)|_{r+\Delta r} - (\tau_{zr} 2\pi r \Delta z)|_r$$

$$+ (p 2\pi r \Delta r)|_z - (p 2\pi r \Delta r)|_{z+\Delta z}$$

Divide by $2\pi r \Delta r \Delta z$

$$\frac{\rho u_2(r, z, t + \Delta t) - \rho u_2(r, z, t)}{\Delta t} =$$

$$\frac{1}{r} \frac{1}{\Delta r} \left[(\tau_{zr} r) \Big|_{r+\Delta r} - (\tau_{zr} r) \Big|_r \right] + \frac{(\rho |z - \rho |z + \Delta z)}{\Delta z}$$

$$\rho \frac{\partial u_2}{\partial t} = \frac{1}{r} \frac{\partial}{\partial r} (r \tau_{zr}) - \frac{\partial p}{\partial z}$$

$$\tau_{zr} = \mu \left(\frac{\partial u_2}{\partial r} \right)$$

$$\rho \frac{\partial u_2}{\partial t} = \mu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_2}{\partial r} \right) - \frac{\partial p}{\partial z}$$

$$\frac{\partial u_2}{\partial t} = \nu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_2}{\partial r} \right) - \frac{1}{\rho} \frac{\partial p}{\partial z}$$

Steady state $\frac{\partial u_2}{\partial t} = 0$

$$\mu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_2}{\partial r} \right) = \left(\frac{\partial p}{\partial z} \right)$$

$$\frac{\partial}{\partial r} \left(r \frac{\partial u_2}{\partial r} \right) = \frac{1}{\mu} \left(\frac{\partial p}{\partial z} \right) r$$

$$r \frac{\partial u_2}{\partial r} = \frac{1}{\mu} \frac{\partial p}{\partial z} \frac{r^2}{2} + C_1$$

$$\frac{\partial u_2}{\partial r} = \frac{1}{\mu} \frac{\partial p}{\partial z} \frac{r}{2} + \frac{C_1}{r}$$

$$u_2 = \frac{1}{4\mu} \frac{\partial p}{\partial z} r^2 + C_1 \log r + C_2$$

Boundary conditions

$$u_z = 0 \text{ at } r = R$$

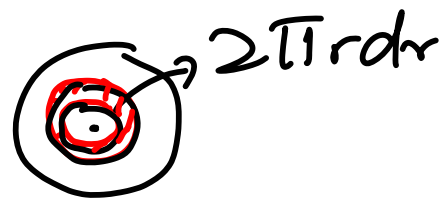
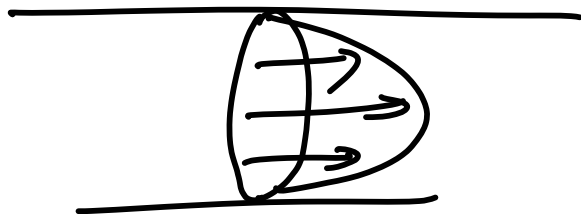
$$\frac{\partial u_z}{\partial r} = 0 \text{ at } r = 0$$

$$u_z = -\frac{1}{4\mu} \left(\frac{\partial p}{\partial z} \right) (R^2 - r^2)$$

'Hagen-Poiseuille flow'

$$u_z = -\frac{R^2}{4\mu} \left(\frac{\partial p}{\partial z} \right) \left[1 - \left(\frac{r}{R} \right)^2 \right]$$

$$Q = \int_0^R u_z r dr 2\pi$$



$$Q = - \left(\frac{\pi R^4}{8\mu} \frac{\partial p}{\partial x} \right)$$

$$\bar{u}_z = \frac{Q}{\pi R^2} = - \frac{\pi R^2}{8\mu} \frac{\partial p}{\partial x}$$

$$= \left(\frac{u_{z \max}}{2} \right)$$

$$u_z(r) = u_{z \max} \left(1 - \left(\frac{r}{R} \right)^2 \right)$$

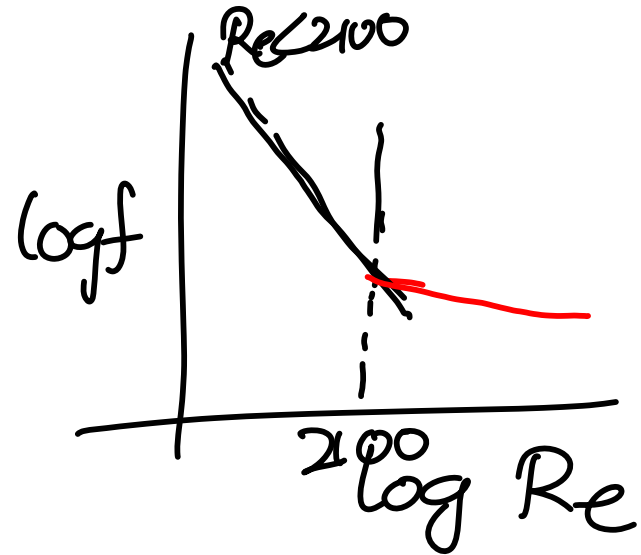
$$\tau_{zr} = \mu \frac{\partial u_z}{\partial r} = - \frac{2u_{z \max} r \mu}{R^2}$$

Wall shear stress

$$\tau_{zr} \Big|_{r=R} = - \frac{2u_{z \max} \mu}{R}$$

$$f = \frac{\tau_{2r}}{\frac{1}{2} \rho \bar{u}^2} = \frac{-2 u_{2 \max} \mu}{R (\frac{1}{2} \rho \bar{u}^2)}$$

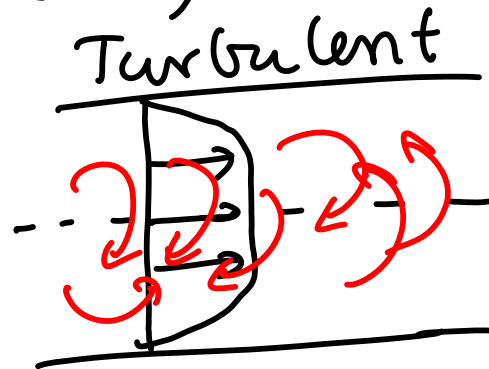
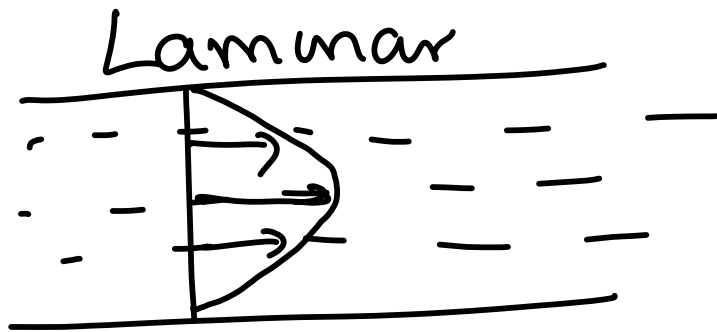
$$= \frac{4 \bar{u} \mu}{R (\frac{1}{2} \rho \bar{u}^2)} = \frac{8 \mu}{\rho \bar{u} R}$$



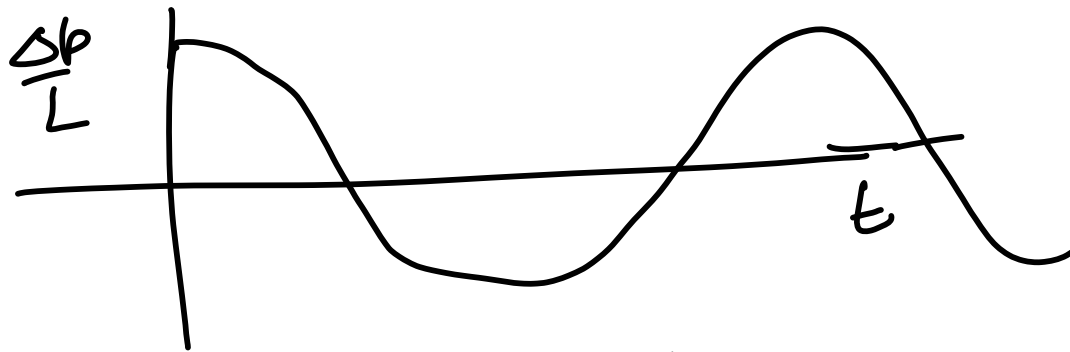
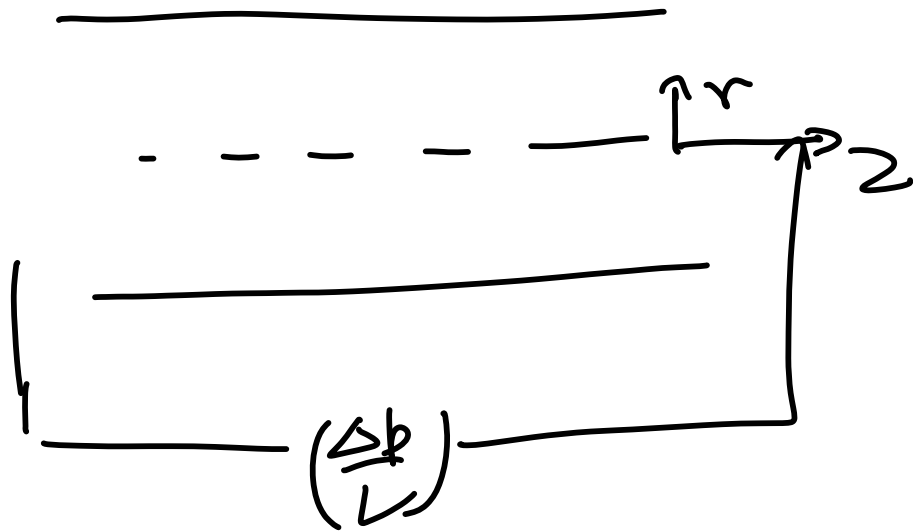
$$f = \frac{16 \mu}{\rho \bar{u} D} = \frac{16}{Re}$$

$$\log f = \log(16) - \log Re$$

$$Re = \left(\frac{\rho \bar{u} D}{\mu} \right) = \left(\frac{\rho u_{2 \max} R}{\mu} \right)$$



Oscillatory flow in a pipe:



$$\frac{\Delta p}{L} = K \cos(\omega t)$$

$$\rho \frac{\partial u_2}{\partial t} = \mu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_2}{\partial r} \right) - \frac{\partial \bar{p}}{\partial z}$$

$$\rho \frac{\partial u_2}{\partial t} = \mu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_2}{\partial r} \right) + K \cos(\omega t)$$

Boundary conditions:

$$u_2 = 0 \text{ at } r = R$$

$$\frac{\partial u_2}{\partial r} = 0 \text{ at } r = 0$$

$$r^* = (r/R) \quad t^* = \omega t$$

$$\rho \omega \frac{\partial u_2}{\partial t^*} = \frac{\mu}{R^2} \left(\frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2}{\partial r^*} \right) \right) - K \cos(t^*)$$

$$\frac{\rho \omega}{k} \frac{\partial u_2}{\partial t^*} = \frac{\mu}{k R^2} \left(\frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2}{\partial r^*} \right) \right) - \cos t^*$$

$$u_2^* = \left(\frac{\mu u_2}{k R^2} \right)$$

$$Re_\omega = \left(\frac{\rho \omega R^2}{\mu} \right)$$

$$\left(\frac{\rho \omega R^2}{\mu} \right) \frac{\partial u_2^*}{\partial t^*} = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2^*}{\partial r^*} \right) - \cos t^*$$

$$Re_\omega \frac{\partial u_2^*}{\partial t^*} = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2^*}{\partial r^*} \right) - \cos t^*$$

$$\text{At } r^* = 0, \quad \frac{\partial u_2^*}{\partial r^*} = 0$$

$$\text{At } r^* = 1, \quad u_2^* = 0$$

$$\cos(t^*) = \text{Real}(e^{it^*})$$

$$\text{Re}_w \frac{\partial u_2^+}{\partial t^*} = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2^+}{\partial r^*} \right) - e^{it^*}$$

$$u_2^* = \text{Real}(u_2^+)$$

$$\frac{\partial u_2^+}{\partial r^*} = 0 \text{ at } r^* = 0$$

$$u_2^+ = 0 \text{ at } r^* = 1$$

$$u_2^+ = \tilde{u}_2(r^*) e^{it^*}$$

$$\text{Re}_w \tilde{u}_2(r^*) i e^{it^*} = e^{it^*} \left(\frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2}{\partial r^*} \right) \right) - e^{it^*}$$

$$i \text{Re}_w \tilde{u}_2(r^*) = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2}{\partial r^*} \right) - 1$$

$$\frac{\partial^2 \tilde{u}_2}{\partial r^{*2}} + \frac{1}{r^*} \frac{\partial \tilde{u}_2}{\partial r^*} - i \text{Re}_\omega \tilde{u}_2(r^*) = 1$$

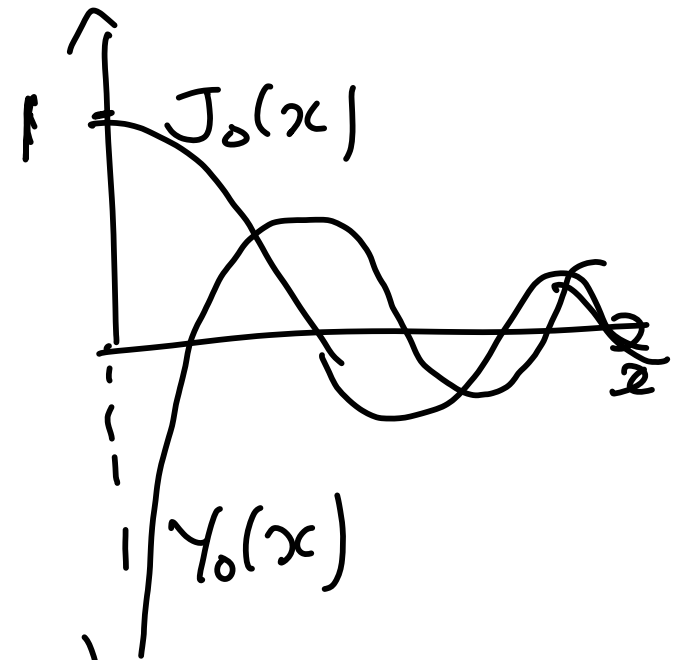
$$\frac{\partial^2 \tilde{u}_{2g}}{\partial r^{*2}} + \frac{1}{r^*} \frac{\partial \tilde{u}_{2g}}{\partial r^*} - i \text{Re}_\omega \tilde{u}_{2g} = 0$$

$$r^{*2} \frac{\partial^2 \tilde{u}_{2g}}{\partial r^{*2}} + r^* \frac{\partial \tilde{u}_{2g}}{\partial r^*} - i \text{Re}_\omega r^{*2} \tilde{u}_{2g} = 0$$

$$x^2 \frac{d^2 y}{dx^2} + x \frac{dy}{dx} + (x^2 - n^2) y = 0$$

$$x = \left(\sqrt{-i \text{Re}_\omega} r^* \right)$$

$$\tilde{u}_{2g} = C_1 J_0 \left(\sqrt{-i \text{Re}_\omega} r^* \right) + C_2 Y_0 \left(\sqrt{-i \text{Re}_\omega} r^* \right)$$



$$-iRe_\omega \tilde{U}_{2p} = 1; \tilde{U}_{2p} = \frac{1}{iRe_\omega} = \frac{-i}{Re_\omega}$$

$$\tilde{U}_2 = \frac{i}{Re_\omega} + C_1 J_0(\sqrt{-iRe_\omega} r^*)$$

Boundary condition

$$\tilde{U}_2 = 0 \text{ at } r^* = 1$$

$$\tilde{U}_2 = \frac{i}{Re_\omega} \left(1 - \frac{J_0(\sqrt{-iRe_\omega} r^*)}{J_0(\sqrt{-iRe_\omega})} \right)$$

$$U_2^+ = \frac{i}{Re_\omega} \left(1 - \frac{J_0(\sqrt{-iRe_\omega} r^*)}{J_0(\sqrt{-iRe_\omega})} \right) e^{it^*}$$

$$U_2^* = \text{Real}(U_2^+)$$

Low Reynolds number

$$Re_\omega \ll 1$$

$$\frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2^*}{\partial r^*} \right) \cos t^* = 0$$

$$u_2^* = -\frac{1}{4} (1 - r^{*2}) \cos t^*$$

$$u_2 = u_2^* \left(\frac{k}{\mu R^2} \right) = -\frac{k}{4\mu} (R^2 - r^2) \cos(\omega t)$$

$$Re_\omega = \left(\frac{8\omega R^2}{\mu} \right) = \left(\frac{\omega}{\nu/R^2} \right) \sim \left(\frac{t_{diff}}{t_{period}} \right)$$

$$\omega \sim \frac{2\pi}{t_{period}}$$

Limite $Re_\omega \ll 1$ $Re_\omega \rightarrow 0$

$$\tilde{u}_2 = \tilde{u}_2^{(0)} + Re_\omega \tilde{u}_2^{(1)} + Re_\omega^2 \tilde{u}_2^{(2)} + \dots$$

$$Re_\omega i \tilde{u}_2 = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2}{\partial r^*} \right) - 1$$

$$Re_\omega i \left[\tilde{u}_2^{(0)} + Re_\omega \tilde{u}_2^{(1)} + Re_\omega^2 \tilde{u}_2^{(2)} \right] = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial}{\partial r^*} \left(\tilde{u}_2^{(0)} + Re_\omega \tilde{u}_2^{(1)} + Re_\omega^2 \tilde{u}_2^{(2)} \right) \right) - 1$$

$$0 + Re_\omega i \tilde{u}_2^{(0)} = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2^{(0)}}{\partial r^*} \right) - 1 \quad O(1)$$

$$+ Re_\omega \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2^{(1)}}{\partial r^*} \right) \quad O(Re_\omega)$$

$$+ Re_\omega^2 i U_2^{(1)}$$

$$+ Re_\omega^2 \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial U_2^{(2)}}{\partial r^*} \right) \quad O(Re_\omega^2)$$

$$Re_\omega \ll 1 \Rightarrow Re_\omega^2 \ll Re_\omega$$

$$0 = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2^{(0)}}{\partial r^*} \right) - 1$$

$$i \tilde{u}_2^{(0)} = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2^{(1)}}{\partial r^*} \right)$$

$$i \tilde{u}_2^{(1)} = \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial \tilde{u}_2^{(2)}}{\partial r^*} \right)$$

$$\tilde{u}_2^{(0)} = 0; \quad \tilde{u}_2^{(1)} = 0; \quad \tilde{u}_2^{(2)} = 0 \quad \text{at } r^* = 1$$

$$\frac{\partial \tilde{u}_2^{(0)}}{\partial r^*} = 0; \quad \frac{\partial \tilde{u}_2^{(1)}}{\partial r^*} = 0; \quad \frac{\partial \tilde{u}_2^{(2)}}{\partial r^*} = 0 \quad \text{at } r^* = 1$$

$$\tilde{u}_2^{(0)} + Re_\omega \tilde{u}_2^{(1)} + Re_\omega^2 \tilde{u}_2^{(2)} = 0$$

$$\text{at } r^* = 1$$

$$\frac{d}{dr^*} \left(\tilde{u}_2^{(0)} + Re_\omega \tilde{u}_2^{(1)} + Re_\omega^2 \tilde{u}_2^{(2)} \right) = 0$$

$$\text{at } r^* = 0$$

$$\tilde{u}_2^{(0)} = \frac{-1}{4} (1 - r^{*2})$$

$$\tilde{u}_2^{(1)} = \frac{i (3 - 4r^{*2} + r^{*4})}{64}$$

$$\tilde{u}_2^{(2)} = \frac{(19 - 27r^{*2} + 9r^{*4} - r^{*6})}{2304}$$

$$u_2^* = \frac{-(1 - r^{*2}) \cos(t^*)}{4} - \frac{\text{Re}_\omega \sin(t^*) (3 - 4r^{*2} + r^{*4})}{64} + \frac{\text{Re}_\omega^2 (19 - 27r^{*2} + 9r^{*4} - r^{*6}) \cos(t^*)}{2304}$$

+ $O(\text{Re}_\omega^3)$ Regular perturbation expansion

$$\rho \frac{\partial u_2}{\partial t} = \mu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_2}{\partial r} \right) - k \cos(\omega t) \quad Re_\omega \gg 1$$

$$r^* = (r/R) ; t^* = \omega t$$

$$\rho \omega \frac{\partial u_2}{\partial t^*} = \frac{\mu}{R^2} \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2}{\partial r^*} \right) - k \cos(t^*)$$

$$\frac{\rho \omega}{k} \frac{\partial u_2}{\partial t^*} = \frac{\mu}{R^2 k} \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2}{\partial r^*} \right) - \cos(t^*)$$

$$u_2^* = \left(\frac{u_2 \rho \omega}{k} \right)$$

$$\frac{\partial u_2^*}{\partial t^*} = \left(\frac{\mu}{\rho \omega R^2} \right) \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2^*}{\partial r^*} \right) - \cos(t^*)$$

$$\frac{\partial u_2^*}{\partial t^*} = \frac{1}{Re_\omega} \frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2^*}{\partial r^*} \right) - \cos(t^*)$$

Limit $Re_\omega \gg 1$

$$\frac{\partial u_2^*}{\partial t^*} = -\cos(t^*) \Rightarrow u_2^* = -\sin(t^*)$$

Boundary conditions:

$$\frac{\partial u_2^*}{\partial r^*} = 0 \text{ at } r^* = 0$$

$$u_2^* = 0 \text{ at } r^* = 1$$

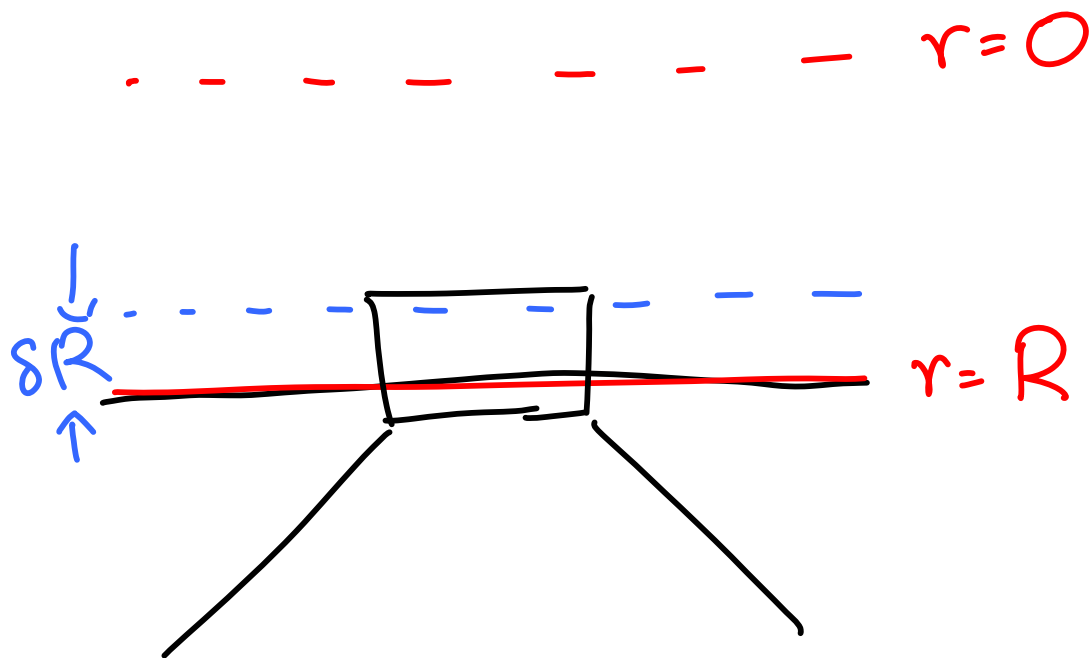
$$Re_\omega \gg 1$$

$$\left(\frac{\omega R^2}{\nu} \right) \gg 1$$

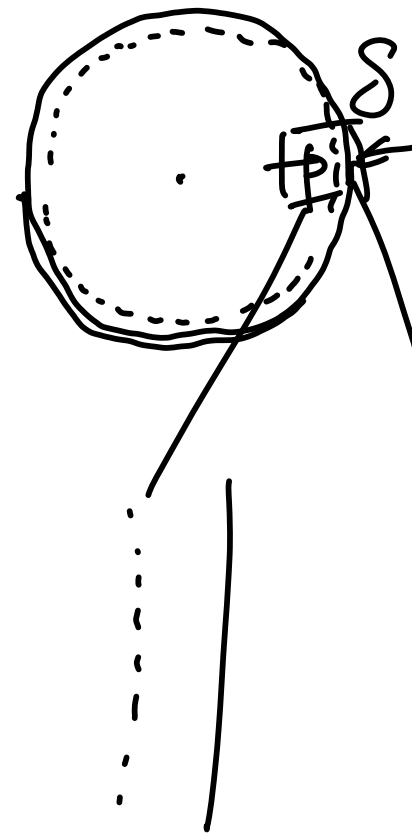
$$\frac{R^2}{\nu} \gg \omega^{-1}$$

$$\text{Distance} = \left(\frac{\nu}{\omega} \right)^{1/2} = \delta R$$

$$\delta = \left(\frac{\nu}{R^2 \omega} \right)^{1/2} = Re_\omega^{-1/2}$$



'Boundary layer'



y 'Inner co-ordinate'

$$y = \frac{(R-r)}{\delta R} = \frac{1}{\delta} (1-r^*)$$

$$r^* = (1 - \delta y)$$

$$\frac{\partial u_2^*}{\partial t^*} = \frac{1}{Re_\omega} \left(\frac{1}{r^*} \frac{\partial}{\partial r^*} \left(r^* \frac{\partial u_2^*}{\partial r^*} \right) \right) - \cos(t^*)$$

$$\frac{\partial u_2^*}{\partial t^*} = \frac{1}{Re_\omega} \left(\frac{1}{(-\delta y)} \frac{1}{\delta} \frac{\partial}{\partial y} \left((1-\delta y) \frac{1}{\delta} \frac{\partial u_2^*}{\partial y} \right) \right) - \cos t^*$$

$$\frac{\partial u_2^*}{\partial t^*} = \frac{1}{Re_\omega \delta^2} \frac{\partial^2 u_2^*}{\partial y^2} - \cos t^*$$

$$\delta \sim Re_\omega^{-1/2} \quad \delta = c Re_\omega^{-1/2}$$

$$\frac{\partial u_2^*}{\partial t^*} = \frac{1}{c^2} \frac{\partial^2 u_2^*}{\partial y^2} - \cos t^*$$

$$u_2^* = \text{Real} [\tilde{u}_2 e^{it^*}]$$

$$i \tilde{u}_2 = \frac{1}{c^2} \frac{d^2 \tilde{u}_2}{dy^2} - 1$$

$$\tilde{u}_{2p} = -\frac{1}{i} = i$$

$$\tilde{u}_{2g} = C_1 e^{\pm \sqrt{i} cy} + C_2 e^{\sqrt{i} cy}$$

Boundary conditions.

$$\frac{\partial \tilde{u}_2}{\partial r^*} = 0 \quad \text{at} \quad r^* = 0 \Rightarrow y = \left(\frac{1}{8}\right)$$

as $y \rightarrow \infty$

$$\tilde{u}_2 = 0 \quad \text{at} \quad r^* = 1 \Rightarrow y = 0$$

$$r^* = (1 - \delta y)$$

$$\tilde{u}_2 = i(1 - e^{-\sqrt{i}cy})$$

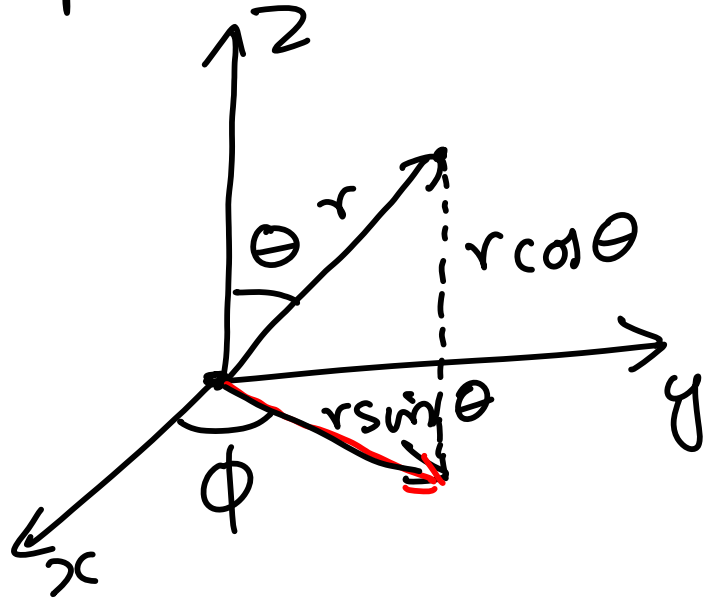
$$\begin{aligned} \tilde{u}_2 &= i \left[1 - e^{-\left(\sqrt{i} \frac{c(1-r^*)}{\delta}\right)} \right] \\ &= i \left[1 - e^{-\left(\frac{\sqrt{i} \tau (1-r^*)}{c Re_{\omega}^{-1/2}}\right)} \right] \\ &= i \left[1 - e^{-\left(\sqrt{i} Re_{\omega} (1-r^*)\right)} \right] \end{aligned}$$

$$u_2^* = \text{Real} \left[\tilde{u}_2 e^{i t^*} \right]$$

$$\begin{aligned} &= -\sin t^* \left[1 - \exp\left[-\frac{Re_{\omega}^{1/2}(1-r^*)}{\sqrt{2}}\right] \right] \cos\left(\frac{-Re_{\omega}^{1/2}(1-r^*)}{\sqrt{2}}\right) \\ &\quad + \cos t^* \sin\left(\frac{-Re_{\omega}^{1/2}(1-r^*)}{\sqrt{2}}\right) \exp\left[-\frac{Re_{\omega}^{1/2}(1-r^*)}{\sqrt{2}}\right] \end{aligned}$$

'Singular perturbation expansion'

Spherical co-ordinate system:



$$x^2 + y^2 + z^2 = R^2$$

$$r = \sqrt{x^2 + y^2 + z^2}$$

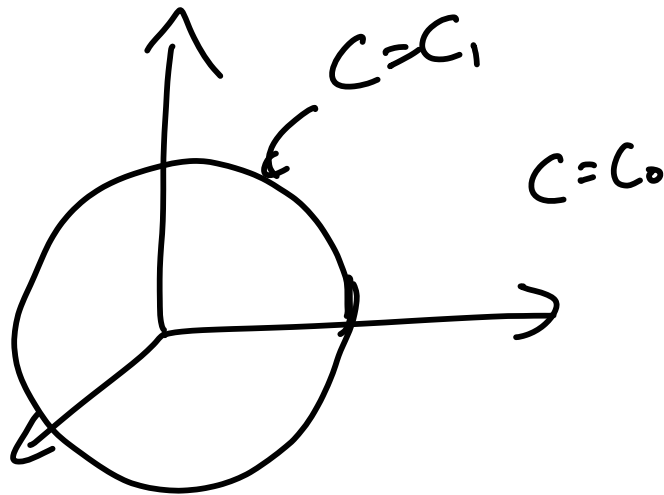
Azimuthal angle θ

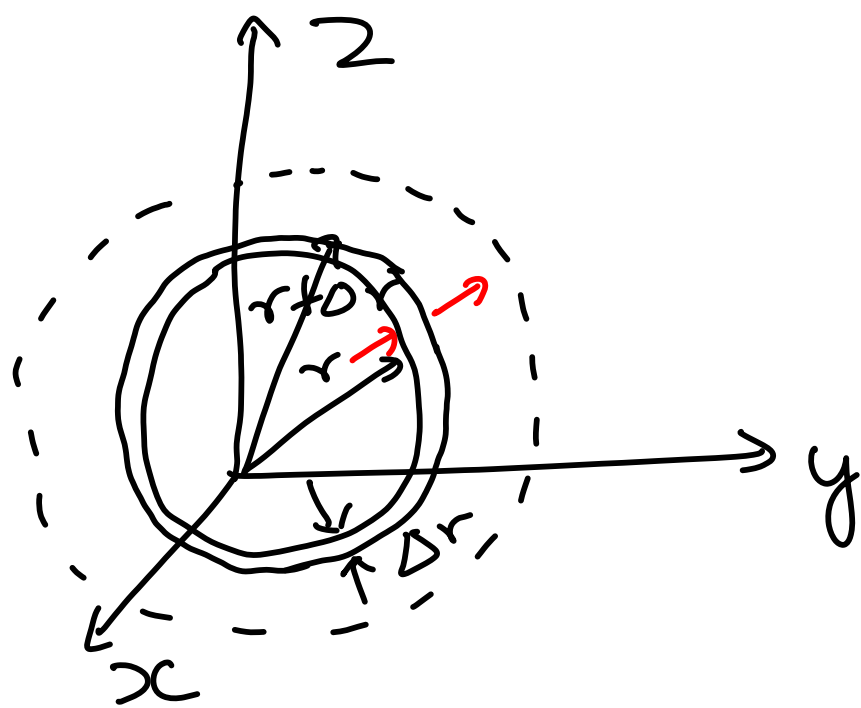
$$z = r \cos \theta$$

$$x = r \sin \theta \cos \phi$$

$$y = r \sin \theta \sin \phi$$

Meridional angle ϕ





$$\left(\begin{array}{c} \text{Change in} \\ \text{mass} \\ \text{in time } \Delta t \end{array} \right) = \left(\begin{array}{c} \text{Mass} \\ \text{in} \end{array} \right) - \left(\begin{array}{c} \text{Mass} \\ \text{out} \end{array} \right) + \left(\begin{array}{c} \text{Sources} \end{array} \right)$$

$$\left(c(r, t + \Delta t) - c(r, t) \right) \times 4\pi r^2 \Delta r$$

$$(\text{Mass in}) = (j_r 4\pi r^2)|_r \Delta t$$

$$(\text{Mass out}) = (j_r 4\pi r^2)|_{r+\Delta r} \Delta t$$

$$(\text{Source}) = S (4\pi r^2 \Delta r) \Delta t$$

$$(c(r, t+\Delta t) - c(r, t)) (4\pi r^2 \Delta r) = \Delta t (j_r (4\pi r^2)|_r - j_r (4\pi r^2)|_{r+\Delta r}) + S (4\pi r^2 \Delta r \Delta t)$$

$$\frac{c(r, t+\Delta t) - c(r, t)}{\Delta t} = \frac{1}{r^2 \Delta r} \left[(j_r r^2)|_r - (j_r r^2)|_{r+\Delta r} \right] + S$$

Limit $\Delta r \rightarrow 0$ & $\Delta t \rightarrow 0$

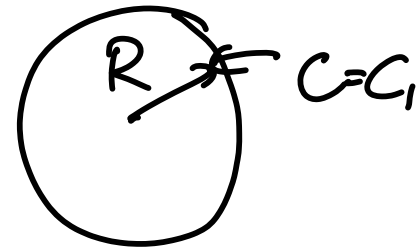
$$\frac{\partial c}{\partial t} = -\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 j_r) + S$$

$$j_r = -D \frac{\partial C}{\partial r}$$

$$\frac{\partial C}{\partial t} = \frac{D}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial C}{\partial r} \right) + S$$

$$C = C_0$$

$$\frac{\partial T}{\partial t} = \alpha \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) + \frac{S_e}{\rho C_p}$$



Steady state, no sources:

$$\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial C}{\partial r} \right) = 0$$

Boundary conditions:

$$C = C_1 \quad \text{at} \quad r = R$$

$$C = C_0 \quad \text{as} \quad r \rightarrow \infty$$

$$C^* = \frac{C - C_0}{C_1 - C_0} \quad r^* = \left(\frac{r}{R} \right)$$

$$\frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial C^*}{\partial r^*} \right) = 0$$

$$C^* = 1 \quad \text{at} \quad r^* = 1 \quad A = 1$$

$$C^* = 0 \quad \text{as} \quad r^* \rightarrow \infty \quad B = 0$$

$$C^* = \frac{A}{r^*} + B$$

$$C^* = \frac{1}{r^*}$$

$$C - C_0 = \left(\frac{(C_1 - C_0) R}{r} \right)$$

$$T - T_0 = \frac{(T_1 - T_0) R}{r}$$

$$j_r = -D \left(\frac{\partial C}{\partial r} \right)$$

$$= -D \left[\frac{-(C_1 - C_0) R}{r^2} \right]$$

$$= \frac{D(C_1 - C_0) R}{r^2}$$

$$q_r = \frac{k(T_1 - T_0) R}{r^2}$$

$$J = 4\pi r^2 j_r$$

$$= 4\pi D R (C_1 - C_0)$$

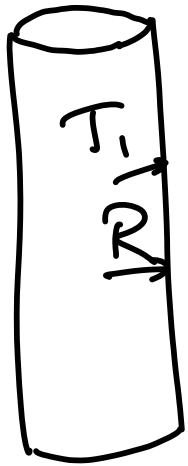
$$(C - C_0) = \frac{J}{4\pi D r}$$

$$Q = 4\pi k R (T_1 - T_0)$$

$$T_1 - T_0 = \frac{Q}{4\pi k r}$$

Limit $R \rightarrow 0$ 'point particle limit'

$$\frac{1}{r} \frac{d}{dr} \left(r \frac{\partial T}{\partial r} \right) = 0$$



$$T = T_i \text{ at } r = R$$

$$T = T_0 \text{ as } r \rightarrow \infty$$

T_0

$$T^* = \left(\frac{T - T_0}{T_i - T_0} \right) \text{ \& } r^* = \left(\frac{r}{R} \right)$$

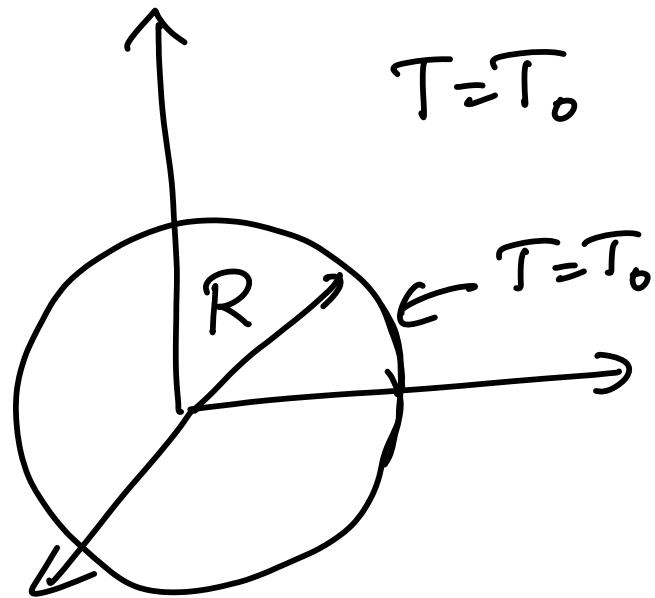
$$\frac{1}{r^*} \frac{d}{dr^*} \left(r^* \frac{\partial T^*}{\partial r^*} \right) = 0$$

$$T^* = 1 \text{ at } r^* = 1$$

$$T^* = 0 \text{ as } r^* \rightarrow \infty$$

$$T^* = A \log(r^*) + B$$

Unsteady diffusion in spherical co-ordinates.



Boundary condition:

$$T=T_0 \text{ at } r=R$$

Initial condition

$$T=T_1 \text{ at } t=0 \text{ for } r < R$$

$$\frac{\partial T}{\partial t} = \alpha \left(\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) \right)$$

$$T^* = \left(\frac{T - T_0}{T_1 - T_0} \right) \quad r^* = \left(\frac{r}{R} \right) \quad t^* = \left(\frac{t \alpha}{R^2} \right)$$

$$\frac{\partial T^*}{\partial t^*} = \frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial T^*}{\partial r^*} \right)$$

$$\text{At } r^* = 1, T^* = 0 \quad \text{BC 1}$$

$$\text{At } t^* = 0, T^* = 1 \quad \text{for } r^* < 1 \quad \text{IC}$$

$$\text{At } r^* = 0, \frac{\partial T^*}{\partial r^*} = 0 \quad \text{BC 2}$$

$$T^* = F(r^*) \Theta(t^*)$$

$$F(r^*) \frac{\partial \Theta}{\partial t^*} = \Theta(t^*) \frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial F}{\partial r^*} \right)$$

Divide by $F(r^*) \Theta(t^*)$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t^*} = \frac{1}{F(r^*)} \frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial F}{\partial r^*} \right)$$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t} = -\beta^2$$

$$\frac{1}{F(r^*)} \frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial F}{\partial r^*} \right) = -\beta^2$$

$$\frac{\partial^2 F}{\partial r^{*2}} + \frac{2}{r^*} \frac{\partial F}{\partial r^*} + \beta^2 F = 0$$

$$r^{*2} \frac{\partial^2 F}{\partial r^{*2}} + 2r^* \frac{\partial F}{\partial r^*} + \beta^2 r^{*2} F = 0$$

$$r^+ = \beta r^*$$

$$r^{+2} \frac{\partial^2 F}{\partial r^{+2}} + 2r^+ \frac{\partial F}{\partial r^+} + r^{+2} F = 0$$

$$F = \frac{A' \sin(r^+)}{r^+} + \frac{B' \cos(r^+)}{r^+}$$

$$= \frac{A \sin(\beta r^*)}{r^*} + \frac{B \cos(\beta r^*)}{r^*}$$

$B = 0$
for $\frac{\partial T^*}{\partial r^*} = 0$
at $r^* = 0$

$$F = \frac{A \sin(\beta r^*)}{r^*}$$

$$T^* = 0 \text{ at } r^* = 1$$

Only if $\beta_n = (n\pi)$

$$F = \frac{A \sin(n\pi r^*)}{r^*}$$

$$\textcircled{+} \quad \perp \frac{\partial \textcircled{+}}{\partial t^*} = -\beta_n^2 = -n^2 \pi^2$$

$$\textcircled{+} = e^{-n^2 \pi^2 t^*}$$

$$T^* = \sum_{n=1}^{\infty} A_n \frac{\sin(n\pi r^*)}{r^*} e^{-n^2 \pi^2 t^*}$$

$$\psi_n = \frac{\sin(n\pi r^*)}{r^*}$$

$$\langle \psi_n, \psi_m \rangle = \int r^{*2} dr^* \left(\frac{\sin(n\pi r^*)}{r^*} \right) \left(\frac{\sin(m\pi r^*)}{r^*} \right)$$

$$= \frac{1}{2} \delta_{mn}$$

Initial condition:

At $t^* = 0$, $T^* = 1$ for all $r^* < 1$

$$T^* = \sum_{n=1}^{\infty} A_n \left(\frac{\sin(n\pi r^*)}{r^*} \right) e^{-n^2 \pi^2 t^*}$$

At $t^* = 0$,

$$T^* = \sum_{n=1}^{\infty} A_n \left(\frac{\sin(n\pi r^*)}{r^*} \right) = 1$$

Multiply by $\left(\frac{\sin(m\pi r^*)}{r^*} \right) r^{*2} dr^*$
 & integrate from 0 to 1

$$\sum_{n=1}^{\infty} A_n \int_0^1 r^{*2} dr^* \left(\frac{\sin(n\pi r^*)}{r^*} \right) \left(\frac{\sin(m\pi r^*)}{r^*} \right) = \int_0^1 r^{*2} dr^* \left(1 \times \frac{\sin(m\pi r^*)}{r^*} \right)$$

$$\sum_{n=1}^{\infty} A_n \left(\frac{\delta_{mn}}{2} \right) = \int_0^1 r^{*2} dr^* \sin(m\pi r^*)$$

$$\frac{A_m}{2} = \left(\frac{1}{m\pi} \right)^2 \Rightarrow A_m = \frac{2}{(m\pi)^2}$$

Bessel equation $\frac{1}{r} \frac{\partial}{\partial r} (r \frac{\partial T}{\partial r})$

$$x^2 \frac{d^2 y}{dx^2} + x \frac{dy}{dx} + (x^2 - n^2) y = 0$$

$$y = C_1 J_n(x) + C_2 Y_n(x)$$

$$\langle \psi_n, \psi_m \rangle = \int x dx (\psi_n(x) \psi_m(x))$$

$\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \frac{\partial T}{\partial r})$

$$x^2 \frac{d^2 y}{dx^2} + 2x \frac{dy}{dx} + (x^2 - n(n+1)) y = 0$$

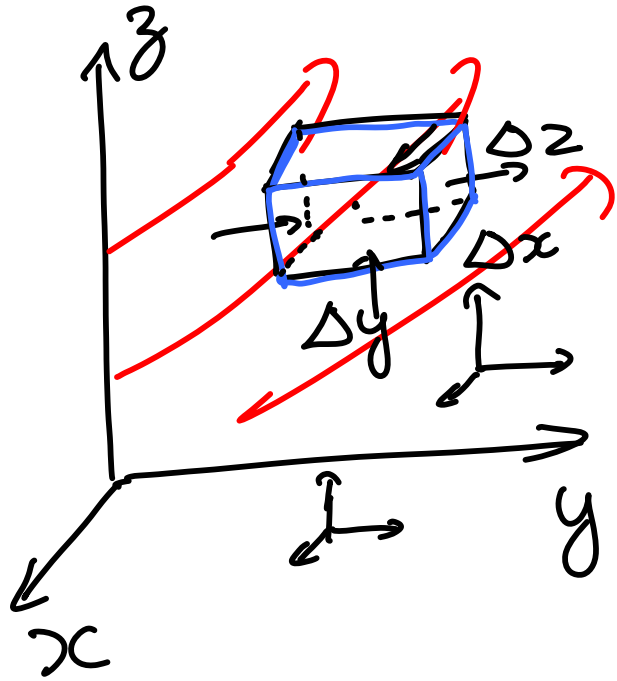
$$y = C_1 j_n(x) + C_2 y_n(x)$$

$$\langle \psi_n, \psi_m \rangle = \int x^2 dx \psi_n(x) \psi_m(x)$$

$$j_0(x) = \frac{\sin x}{x} \quad \& \quad y_0(x) = \left(\frac{\cos x}{x} \right)$$

Conservation Equations for Mass and Energy:

Cartesian co-ordinate system:



Accumulation of mass
in time Δt

$$= (c(x, y, z, t + \Delta t) - c(x, y, z, t)) \Delta x \Delta y \Delta z$$

$$\left(\text{Accumulation of mass in time } \Delta t \right) = \left(\text{Mass in} \right) - \left(\text{Mass out} \right) + \left(\text{Production in volume} \right)$$

$$\text{Accumulation of mass} = (C(x, y, z, t + \Delta t) - C(x, y, z, t)) \Delta x \Delta y \Delta z$$

$$\text{Mass in at } \left(z - \frac{\Delta z}{2}\right) = \dot{j}_z \Big|_{z - \frac{\Delta z}{2}} \Delta x \Delta y \Delta t$$

$$\text{Mass in at } \left(y - \frac{\Delta y}{2}\right) = \dot{j}_y \Big|_{y - \frac{\Delta y}{2}} \Delta x \Delta z \Delta t$$

$$\text{Mass in at } \left(x - \frac{\Delta x}{2}\right) = \dot{j}_x \Big|_{x - \frac{\Delta x}{2}} \Delta y \Delta z \Delta t$$

$$\text{Mass out at } \left(z + \frac{\Delta z}{2}\right) = \dot{j}_z \Big|_{z + \frac{\Delta z}{2}} \Delta x \Delta y \Delta t$$

$$\text{Mass out at } \left(y + \frac{\Delta y}{2}\right) = \dot{j}_y \Big|_{y + \frac{\Delta y}{2}} \Delta x \Delta z \Delta t$$

$$\text{Mass out at } \left(x + \frac{\Delta x}{2}\right) = \dot{j}_x \Big|_{x + \frac{\Delta x}{2}} \Delta y \Delta z \Delta t$$

Convection:

$$\text{Mass in at } \left(z - \frac{\Delta z}{2}\right) = C u_z \Big|_{z - \frac{\Delta z}{2}} \Delta x \Delta y \Delta t$$

$$\text{Mass in at } \left(y - \frac{\Delta y}{2}\right) = C u_y \Big|_{y - \frac{\Delta y}{2}} \Delta x \Delta z \Delta t$$

$$\text{Mass in at } \left(x - \frac{\Delta x}{2}\right) = C u_x \Big|_{x - \frac{\Delta x}{2}} \Delta y \Delta z \Delta t$$

$$\text{Mass out at } \left(z + \frac{\Delta z}{2}\right) = C u_z \Big|_{z + \frac{\Delta z}{2}} \Delta x \Delta y \Delta t$$

$$\text{Mass out at } \left(y + \frac{\Delta y}{2}\right) = C u_y \Big|_{y + \frac{\Delta y}{2}} \Delta x \Delta z \Delta t$$

$$\text{Mass out at } \left(x + \frac{\Delta x}{2}\right) = C u_x \Big|_{x + \frac{\Delta x}{2}} \Delta y \Delta z \Delta t$$

$$\text{Production of mass} = S (\Delta x \Delta y \Delta z) \Delta t$$

$$(C(x, y, z, t + \Delta t) - C(x, y, z, t)) \Delta x \Delta y \Delta z =$$

$$\left((C u_x) \Big|_{x-\frac{\Delta x}{2}} - (C u_x) \Big|_{x+\frac{\Delta x}{2}} \right) \Delta y \Delta z \Delta t$$

$$+ (C u_y) \Big|_{y-\frac{\Delta y}{2}} - (C u_y) \Big|_{y+\frac{\Delta y}{2}} \Delta x \Delta z \Delta t$$

$$+ (C u_z) \Big|_{z-\frac{\Delta z}{2}} - (C u_z) \Big|_{z+\frac{\Delta z}{2}} \Delta x \Delta y \Delta t$$

$$+ (j_x \Big|_{x-\frac{\Delta x}{2}} - j_x \Big|_{x+\frac{\Delta x}{2}}) \Delta y \Delta z \Delta t$$

$$+ (j_y \Big|_{y-\frac{\Delta y}{2}} - j_y \Big|_{y+\frac{\Delta y}{2}}) \Delta x \Delta z \Delta t$$

$$+ (j_z \Big|_{z-\frac{\Delta z}{2}} - j_z \Big|_{z+\frac{\Delta z}{2}}) \Delta x \Delta y \Delta t$$

$$+ S \Delta x \Delta y \Delta z \Delta t$$

Divide by $\Delta x \Delta y \Delta z \Delta t$

$$\begin{aligned}
 \frac{C|_{t+\Delta t} - C|_t}{\Delta t} = & \frac{(Cu_x|_{x-\frac{\Delta x}{2}} - Cu_x|_{x+\frac{\Delta x}{2}})}{\Delta x} + \frac{(j_x|_{x-\frac{\Delta x}{2}} - j_x|_{x+\frac{\Delta x}{2}})}{\Delta x} \\
 & + \frac{(Cu_y|_{y-\frac{\Delta y}{2}} - Cu_y|_{y+\frac{\Delta y}{2}})}{\Delta y} + \frac{(j_y|_{y-\frac{\Delta y}{2}} - j_y|_{y+\frac{\Delta y}{2}})}{\Delta y} \\
 & + \frac{(Cu_z|_{z-\frac{\Delta z}{2}} - Cu_z|_{z+\frac{\Delta z}{2}})}{\Delta z} + \frac{(j_z|_{z-\frac{\Delta z}{2}} - j_z|_{z+\frac{\Delta z}{2}})}{\Delta z}
 \end{aligned}$$

$$\begin{aligned}
 \frac{\partial C}{\partial t} = & - \frac{\partial}{\partial x} (Cu_x) - \frac{\partial j_x}{\partial x} \\
 & - \frac{\partial}{\partial y} (Cu_y) - \frac{\partial j_y}{\partial y} \\
 & - \frac{\partial}{\partial z} (Cu_z) - \frac{\partial j_z}{\partial z}
 \end{aligned}$$

$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x} (c u_x) + \frac{\partial}{\partial y} (c u_y) + \frac{\partial}{\partial z} (c u_z) = -\frac{\partial j_x}{\partial x} - \frac{\partial j_y}{\partial y} - \frac{\partial j_z}{\partial z} + S$$

$$\underline{u} = u_x \underline{e}_x + u_y \underline{e}_y + u_z \underline{e}_z$$

$$\underline{j} = j_x \underline{e}_x + j_y \underline{e}_y + j_z \underline{e}_z$$

$$\nabla = \left(\underline{e}_x \frac{\partial}{\partial x} + \underline{e}_y \frac{\partial}{\partial y} + \underline{e}_z \frac{\partial}{\partial z} \right)$$

$$\nabla \cdot \underline{j} = \left(\underline{e}_x \frac{\partial}{\partial x} + \underline{e}_y \frac{\partial}{\partial y} + \underline{e}_z \frac{\partial}{\partial z} \right) (j_x \underline{e}_x + j_y \underline{e}_y + j_z \underline{e}_z)$$

$$= \frac{\partial j_x}{\partial x} + \frac{\partial j_y}{\partial y} + \frac{\partial j_z}{\partial z}$$

$$\nabla \cdot (c \underline{u}) = \frac{\partial}{\partial x} (c u_x) + \frac{\partial}{\partial y} (c u_y) + \frac{\partial}{\partial z} (c u_z)$$

$$\frac{\partial C}{\partial t} + \nabla \cdot (c \underline{u}) = -\nabla \cdot \underline{j} + S$$

$\nabla \cdot \underline{j}$ = Divergenz (\underline{j})

$$j_x = -D \frac{\partial C}{\partial x} \quad j_y = -D \frac{\partial C}{\partial y} \quad j_z = -D \frac{\partial C}{\partial z}$$

$$\underline{j} = j_x \underline{e}_x + j_y \underline{e}_y + j_z \underline{e}_z$$

$$= -D \left[\underline{e}_x \frac{\partial C}{\partial x} + \underline{e}_y \frac{\partial C}{\partial y} + \underline{e}_z \frac{\partial C}{\partial z} \right]$$

$$= -D \nabla C$$

$$\frac{\partial C}{\partial t} + \nabla \cdot (\underline{u} C) = -\nabla \cdot (-D \nabla C)$$

$$= D \nabla^2 C$$

$$\nabla^2 = \nabla \cdot \nabla = \left(\underline{e}_x \frac{\partial}{\partial x} + \underline{e}_y \frac{\partial}{\partial y} + \underline{e}_z \frac{\partial}{\partial z} \right) \cdot \left(\underline{e}_x \frac{\partial}{\partial x} + \underline{e}_y \frac{\partial}{\partial y} + \underline{e}_z \frac{\partial}{\partial z} \right)$$

$$= \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2}$$

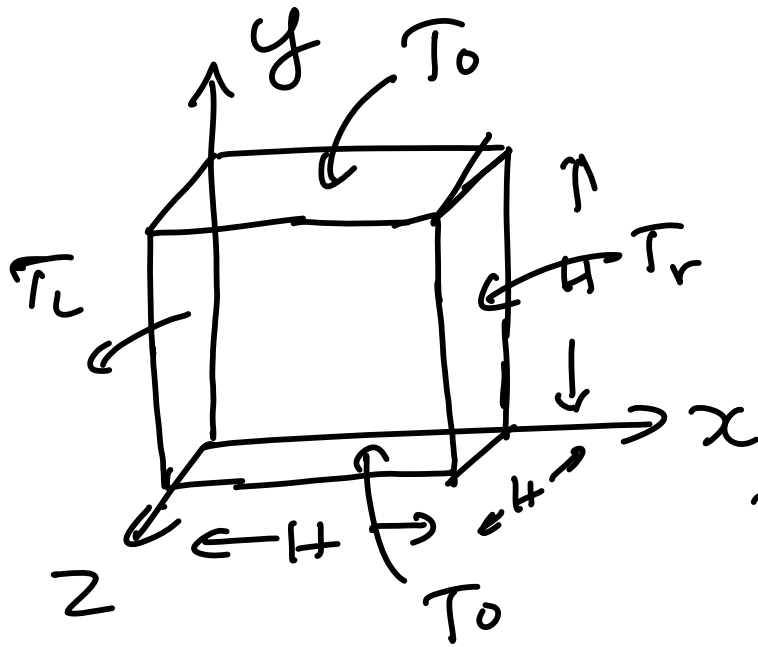
$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x} (u_x C) + \frac{\partial}{\partial y} (u_y C) + \frac{\partial}{\partial z} (u_z C) = D \left(\frac{\partial^2 C}{\partial x^2} + \frac{\partial^2 C}{\partial y^2} + \frac{\partial^2 C}{\partial z^2} \right) + S$$

$$\frac{\partial c}{\partial t} + \nabla \cdot (\underline{y}c) = D \nabla^2 c + S \quad \begin{array}{l} q = -k \nabla T \\ j = -D \nabla c \end{array}$$

$$\rho C_p \left(\frac{\partial T}{\partial t} + \nabla \cdot (\underline{y}T) \right) = k \nabla^2 T + S_e$$

$$\left(\frac{\partial T}{\partial t} + \nabla \cdot (\underline{y}T) \right) = \alpha \nabla^2 T + \frac{S_e}{\rho C_p}$$

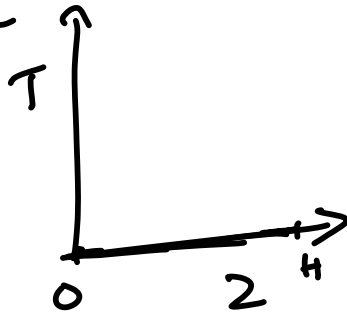
Conduction in a cube:



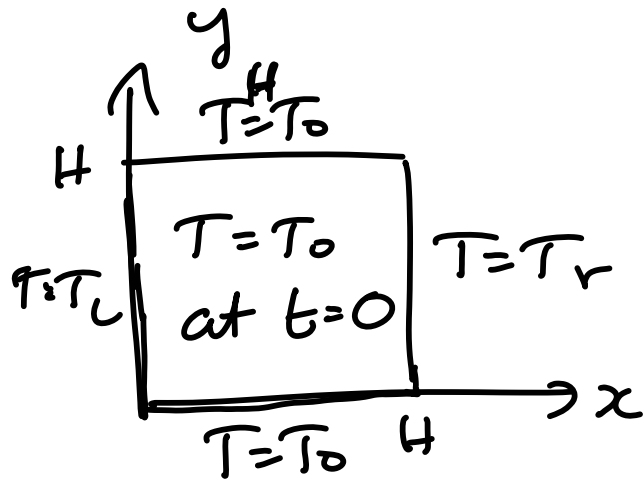
Front & back-insulated

$$\Rightarrow k \frac{\partial T}{\partial z} = 0$$

At $t=0$, $T=T_0$ everywhere



$$\frac{\partial T}{\partial t} = \alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right)$$



$$x^* = (x/H), \quad y^* = (y/H)$$

$$T^* = \left(\frac{T - T_0}{T_0} \right)$$

$$t^* = \left(\frac{t \alpha}{H^2} \right)$$

$$\frac{\partial T^*}{\partial t^*} = \frac{\partial^2 T^*}{\partial x^{*2}} + \frac{\partial^2 T^*}{\partial y^{*2}}$$

B.C. $T^* = 0$ at $y^* = 0$

$$T^* = 0 \quad \text{at } y^* = 1$$

$$T^* = \left(\frac{T_L - T_0}{T_0} \right) = T_L^* \quad \text{at } x^* = 0$$

$$= \left(\frac{T_R - T_0}{T_0} \right) = T_R^* \quad \text{at } x^* = 1$$

I.C. $T^* = 0$ for all $0 < x^* < 1$ & $0 < y^* < 1$ at $t^* = 0$

$$T^* = T_b^* + T_s^*$$

$$\frac{\partial^2 T_b^*}{\partial x^{*2}} + \frac{\partial^2 T_s^*}{\partial y^{*2}} = 0$$

At $y^* = 0$ & $y^* = 1$, $T_s^* = 0$

At $x^* = 0$, $T_s^* = T_c^*$

$x^* = 1$, $T_s^* = T_c^*$

$$T_s^* = X(x^*) Y(y^*)$$

$$Y(y^*) \frac{\partial^2 X}{\partial x^{*2}} + X(x^*) \frac{\partial^2 Y}{\partial y^{*2}} = 0$$

Divide by XY

$$\frac{1}{X} \frac{\partial^2 X}{\partial x^{*2}} + \frac{1}{Y} \frac{\partial^2 Y}{\partial y^{*2}} = 0$$

$$\frac{1}{X} \frac{\partial^2 X}{\partial x^{*2}} = \beta_n^2 \quad \frac{1}{Y} \frac{\partial^2 Y}{\partial y^{*2}} = -\beta_n^2$$

$$Y = A \sin(\beta_n y^*) + B \cos(\beta_n y^*)$$

$$\text{// At } y^* = 0, Y = 0 \Rightarrow B = 0$$

$$\text{// At } y^* = 1, Y = 0 \Rightarrow \beta_n = n\pi$$

$$Y_n = \sin(n\pi y^*)$$

$$X = C e^{+n\pi x^*} + D e^{-n\pi x^*}$$

$$T_s^* = \sum_{n=1}^{\infty} (C_n e^{n\pi x^*} + D_n e^{-n\pi x^*}) \sin(n\pi y^*)$$

Boundary conditions in x-direction

$$\text{At } x^* = 0, T_s^* = T_c^*$$

$$\sum_{n=1}^{\infty} (C_n + D_n) \sin(n\pi y^*) = T_c^*$$

$$\text{At } x^* = L, T_s^* = T_r^*$$

$$\sum_{n=0}^{\infty} (C_n e^{n\pi} + D_n e^{-n\pi}) \sin(n\pi y^*) = T_r^*$$

Multiply both sides by $\sin(m\pi y^*)$ & integrate.

$$\sum_{n=1}^{\infty} (C_n + D_n) \left(\frac{\delta_{mn}}{2}\right) = \int_0^1 dy^* T_c^* \sin(m\pi y^*)$$

$$\sum_{n=1}^{\infty} (C_n e^{n\pi} + D_n e^{-n\pi}) \left(\frac{\delta_{mn}}{2}\right) = \int_0^1 dy^* T_r^* \sin(m\pi y^*)$$

$$\frac{1}{2} (C_m + D_m) = \frac{2}{m\pi} T_c^*$$

$$\frac{1}{2} (C_m e^{m\pi} + D_m e^{-m\pi}) = \frac{2}{m\pi} T_r^*$$

$$C_m = \frac{4}{m\pi} \left(\frac{T_i^* - e^{-m\pi} T_c^*}{1 - e^{-m\pi}} \right)$$

$$D_m = \frac{4}{m\pi} \left(\frac{T_c^* - e^{-m\pi} T_r^*}{1 - e^{-m\pi}} \right)$$

$$T_s^* = \sum_{n=1}^{\infty} (C_n e^{n\pi x^*} + D_n e^{-n\pi x^*}) \sin(m\pi y^*)$$

Transient temperature profile:

$$T_t^* = T^* - T_s^*$$

$$\frac{\partial T^*}{\partial t} = \frac{\partial^2 T^*}{\partial x^{*2}} + \frac{\partial^2 T^*}{\partial y^{*2}}$$

$$0 = \frac{\partial^2 T_s^*}{\partial x^{*2}} + \frac{\partial^2 T_s^*}{\partial y^{*2}}$$

$$\frac{\partial T_t^*}{\partial t} = \frac{\partial^2 T_t^*}{\partial x^{*2}} + \frac{\partial^2 T_t^*}{\partial y^{*2}}$$

Boundary conditions:

$$\text{At } y^* = 0, \quad T^* = 0, \quad T_s^* = 0 \Rightarrow T_t^* = 0$$

$$y^* = 1 \quad T^* = 0, \quad T_s^* = 0 \Rightarrow T_t^* = 0$$

$$x^* = 0 \quad T^* = T_L^*, \quad T_s^* = T_L^* \Rightarrow T_t^* = 0$$

$$x^* = 1 \quad T^* = T_R^*, \quad T_s^* = T_R^* \Rightarrow T_t^* = 0$$

$$\text{At } t^* = 0, \quad T^* = 0; \quad T_s^* = T_s^* \Rightarrow T_t^* = -T_s^* !$$

Separation of variables $T_t^* = X(x^*)Y(y^*)\Theta(t^*)$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t^*} = \frac{1}{X} \frac{\partial^2 X}{\partial x^{*2}} + \frac{1}{Y} \frac{\partial^2 Y}{\partial y^{*2}}$$

$$X_n = \sin(n\pi x^*)$$

$$Y_m = \sin(m\pi y^*)$$

$$\frac{1}{\Theta} \frac{\partial \Theta}{\partial t} = -(n^2 + m^2)\pi^2$$

$$\textcircled{T} = A e^{-(n^2+m^2)\pi^2 t^*}$$

$$T_t^* = \textcircled{T} \times y$$

$$= \sum_{n=1}^{\infty} \sum_{m=1}^{\infty} A_{nm} e^{-(n^2+m^2)\pi^2 t^*} \sin(n\pi x^*) \sin(m\pi y^*)$$

Initial condition:

$$\text{At } t^* = 0, T_t^* = -T_s^*$$

$$\sum_{n=1}^{\infty} \sum_{m=1}^{\infty} A_{nm} \sin(n\pi x^*) \sin(m\pi y^*) = -T_s^*(x^*, y^*)$$

Multiply by $\sin(p\pi x^*) \sin(q\pi y^*)$ & integrate over

$$0 < x^* < 1 \quad \& \quad 0 < y^* < 1$$

$$\sum_{n=1}^{\infty} \sum_{m=1}^{\infty} A_{nm} \left(\frac{\delta_{np}}{2}\right) \left(\frac{\delta_{mq}}{2}\right) = - \int_0^1 dx^* \int_0^1 dy^* T_s^*(x^*, y^*) \frac{\sin(p\pi x^*)}{\sin(q\pi y^*)}$$

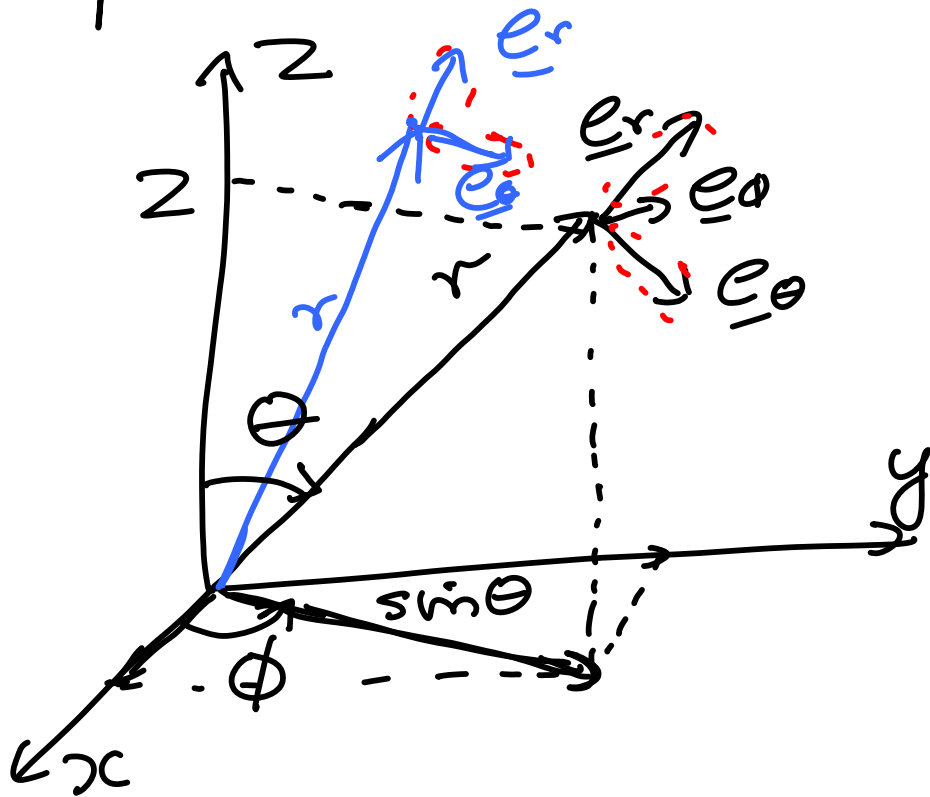
$$\frac{A_{pq}}{4} = - \int_0^1 dx^* \int_0^1 dy^* T_s^*(x^*, y^*) \sin(p\pi x^*) \sin(q\pi y^*)$$

$$\int dx^* \int dy^* \sin(p\pi x^*) \sin(q\pi y^*) \sum_{n=1}^{\infty} (C_n e^{n\pi x^*} + D_n e^{-n\pi x^*}) \sin(n\pi y^*)$$

$$= \int dx^* \sin(p\pi x^*) (C_n e^{n\pi x^*} + D_n e^{-n\pi x^*}) \left(\frac{\delta_{nq}}{2} \right)$$

$$A_{pq} = - \int dx^* \sin(p\pi x^*) \frac{(C_q e^{q\pi x^*} + D_q e^{-q\pi x^*})}{2}$$

Spherical co-ordinate system:



$$0 \leq \theta \leq \pi$$

$$0 \leq \phi \leq 2\pi$$

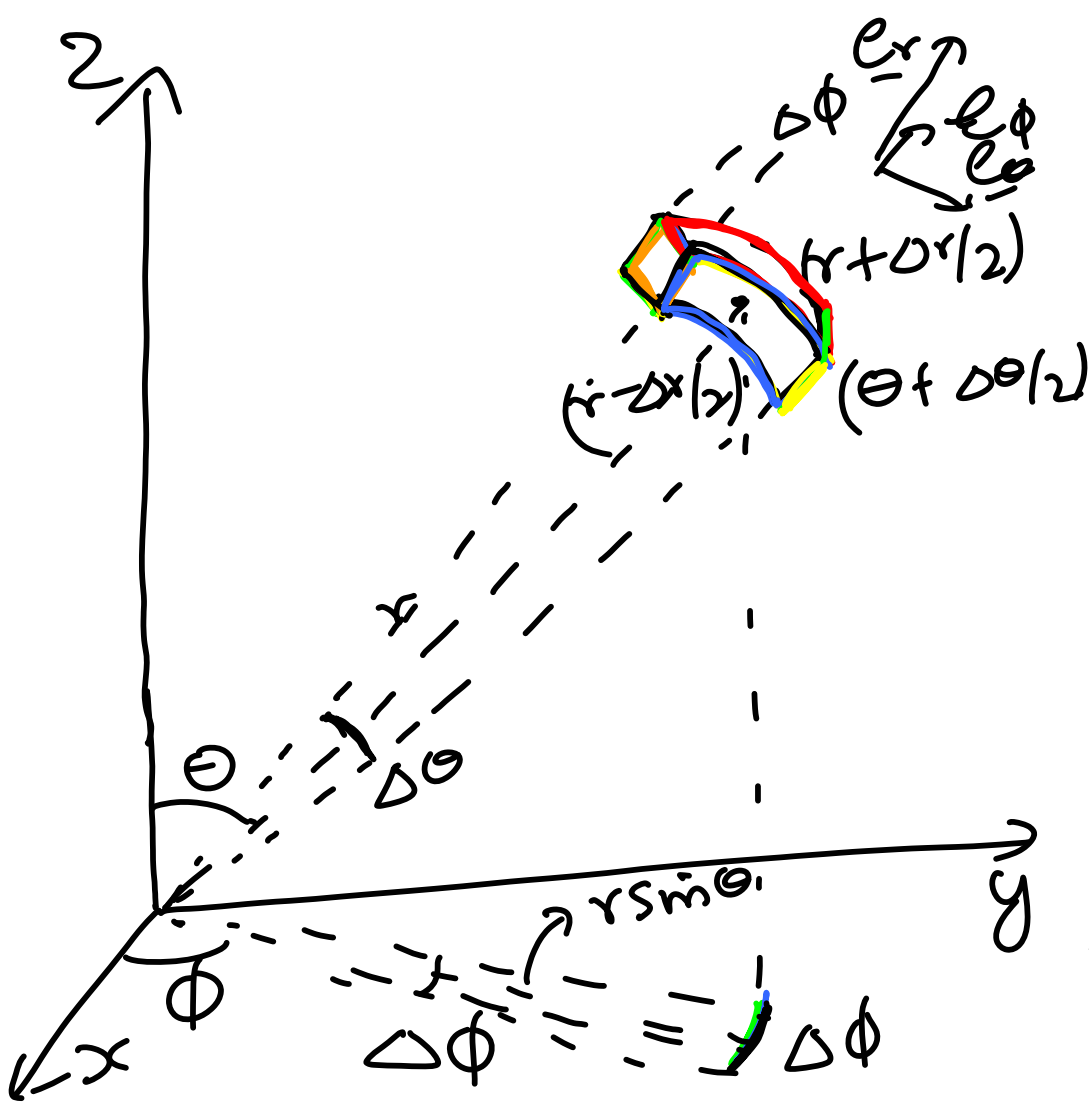
$$r = \sqrt{x^2 + y^2 + z^2}$$

$$\cos \theta = \frac{z}{r} = \frac{z}{\sqrt{x^2 + y^2 + z^2}}$$

$$\sin \theta = \frac{\sqrt{x^2 + y^2}}{r}$$

$$x = r \sin \theta \cos \phi$$

$$y = r \sin \theta \sin \phi$$



Centered at (r, θ, ϕ)

Surface areas:

Surface at $(r + \Delta r/2)$
 $= (r \Delta \theta)(r \sin \theta \Delta \phi) \Big|_{r+\Delta r/2}$

Surface at $(r - \Delta r/2)$
 $= (r \Delta \theta)(r \sin \theta \Delta \phi) \Big|_{r-\Delta r/2}$

Surface at $(\phi + \Delta \phi/2)$
 $= (\Delta r) r \Delta \theta$

Surface at $(\phi - \Delta \phi/2)$
 $= (\Delta r) (r \Delta \theta)$

Surface at $(\theta - \Delta \theta/2)$
 $= (\Delta r) (r \sin \theta \Delta \phi) \Big|_{\theta-\Delta \theta/2}$

Surface at $(\theta + \Delta \theta/2)$
 $= (\Delta r) (r \sin \theta \Delta \phi) \Big|_{\theta+\Delta \theta/2}$

$$\left(\text{Change in mass in time } \Delta t \right) = (\text{Mass in}) - (\text{Mass out}) + (\text{Sources})$$

$$\begin{aligned} \left(\text{Change in mass in } \Delta t \right) &= (C(r, \theta, \phi, t + \Delta t) - C(r, \theta, \phi, t)) \\ &\quad \times (\Delta r) (r \Delta \theta) (r \sin \theta \Delta \phi) \\ &= C(r, \theta, \phi, t + \Delta t) - C(r, \theta, \phi, t) r^2 \Delta r \sin \theta \Delta \theta \Delta \phi \end{aligned}$$

$$\left(\text{Mass in at } r - \Delta r/2 \right) = j_r (r \Delta \theta) (r \sin \theta \Delta \phi) \Delta t \Big|_{r - \Delta r/2}$$

$$\left(\text{Mass out at } r + \Delta r/2 \right) = j_r (r \Delta \theta) (r \sin \theta \Delta \phi) \Delta t \Big|_{r + \Delta r/2}$$

$$\left(\text{Mass in at } \theta - \frac{\Delta \theta}{2} \right) = j_\theta (\Delta r) (r \sin \theta \Delta \phi) \Big|_{\theta - \frac{\Delta \theta}{2}}^{\Delta t}$$

$$\left(\text{Mass in out} \right)_{\theta + \Delta\theta/2} = j_{\theta} (\Delta r) (r \sin \theta \Delta \phi) \Big|_{\theta + \Delta\theta/2}^{\Delta t}$$

$$\left(\text{Mass in at} \right)_{\phi - \Delta\phi/2} = j_{\phi} (\Delta r) (r \Delta \theta) \Big|_{\phi - \Delta\phi/2}^{\Delta t}$$

$$\left(\text{Mass out at} \right)_{\phi + \Delta\phi/2} = j_{\phi} (\Delta r) (r \Delta \theta) \Big|_{\phi + \Delta\phi/2}^{\Delta t}$$

$$\left(\text{Source} \right) = \int (\Delta r) (r \Delta \theta) (r \sin \theta \Delta \phi) \Delta t$$

$$\begin{aligned} & (c(r, \theta, \phi, t + \Delta t) - c(r, \theta, \phi, t)) (\Delta r) (r \Delta \theta) (r \sin \theta \Delta \phi) \\ &= j_r (\overline{r \Delta \theta}) (\overline{r \sin \theta \Delta \phi}) \Big|_{r - \Delta r/2} - j_r (\overline{r \Delta \theta}) (\overline{r \sin \theta \Delta \phi}) \Big|_{r + \Delta r/2} \\ &+ j_{\theta} (\overline{\Delta r}) (\overline{r \sin \theta \Delta \phi}) \Big|_{\theta - \Delta \theta/2} - j_{\theta} (\overline{\Delta r}) (\overline{r \sin \theta \Delta \phi}) \Big|_{\theta + \Delta \theta/2} \\ &+ j_{\phi} (\overline{\Delta r}) (\overline{r \Delta \theta}) \Big|_{\phi - \Delta \phi/2} - j_{\phi} (\overline{\Delta r}) (\overline{r \Delta \theta}) \Big|_{\phi + \Delta \phi/2} \end{aligned}$$

$$\begin{aligned}
& + (C_{u_r})(r\Delta\theta)(r\sin\theta\Delta\phi) \Big|_{r-\Delta r/2} - (C_{u_r})(r\Delta\theta)(r\sin\theta\Delta\phi) \Big|_{r+\Delta r/2} \\
& + (C_{u_\theta})(\Delta r)(r\sin\theta\Delta\phi) \Big|_{\theta-\Delta\theta/2} - (C_{u_\theta})(\Delta r)(r\sin\theta\Delta\phi) \Big|_{\theta+\Delta\theta/2} \\
& + (C_{u_\phi})(\Delta r)(r\Delta\theta) \Big|_{\phi-\Delta\phi/2} - (C_{u_\phi})(\Delta r)(r\Delta\theta) \Big|_{\phi+\Delta\phi/2} \\
& + S \Delta r r \Delta\theta r \sin\theta \Delta\phi \Delta t
\end{aligned}$$

Divide by $(\Delta r)(r\Delta\theta)(r\sin\theta\Delta\phi)(\Delta t)$

$$\begin{aligned}
\frac{C(r, \theta, \phi, t + \Delta t) - C(r, \theta, \phi, t)}{\Delta t} &= \frac{1}{r^2 \Delta r} \left(j_r r^2 \Big|_{r-\Delta r/2} - j_r r^2 \Big|_{r+\Delta r/2} \right) \\
&+ \frac{1}{r \sin\theta \Delta\theta} \left[j_\theta \sin\theta \Big|_{\theta-\Delta\theta/2} - j_\theta \sin\theta \Big|_{\theta+\Delta\theta/2} \right] \\
&+ \frac{1}{r \sin\theta \Delta\phi} \left[j_\phi \Big|_{\phi-\Delta\phi/2} - j_\phi \Big|_{\phi+\Delta\phi/2} \right] \\
&+ \frac{1}{r^2 \Delta r} \left[C_{u_r} r^2 \Big|_{r-\Delta r/2} - C_{u_r} r^2 \Big|_{r+\Delta r/2} \right]
\end{aligned}$$

$$+ \frac{1}{r \sin \theta \Delta \theta} (c u_{\theta} \sin \theta |_{\theta - \frac{\Delta \theta}{2}} - c u_{\theta} \sin \theta |_{\theta + \frac{\Delta \theta}{2}})$$

$$+ \frac{1}{r \sin \theta \Delta \phi} (c u_{\phi} |_{\phi - \frac{\Delta \phi}{2}} - c u_{\phi} |_{\phi + \frac{\Delta \phi}{2}})$$

+ S

$$\frac{\partial C}{\partial t} = -\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 j_r) - \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta j_{\theta}) - \frac{1}{r \sin \theta} \frac{\partial j_{\phi}}{\partial \phi}$$

$$- \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 c u_r) - \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta c u_{\theta}) - \frac{1}{r \sin \theta} \frac{\partial (c u_{\phi})}{\partial \phi}$$

+ S

$$\frac{\partial C}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 c u_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta c u_{\theta}) + \frac{1}{r \sin \theta} \frac{\partial (c u_{\phi})}{\partial \phi}$$

$$= -\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 j_r) - \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta j_{\theta}) + \frac{1}{r \sin \theta} \frac{\partial j_{\phi}}{\partial \phi} + S$$

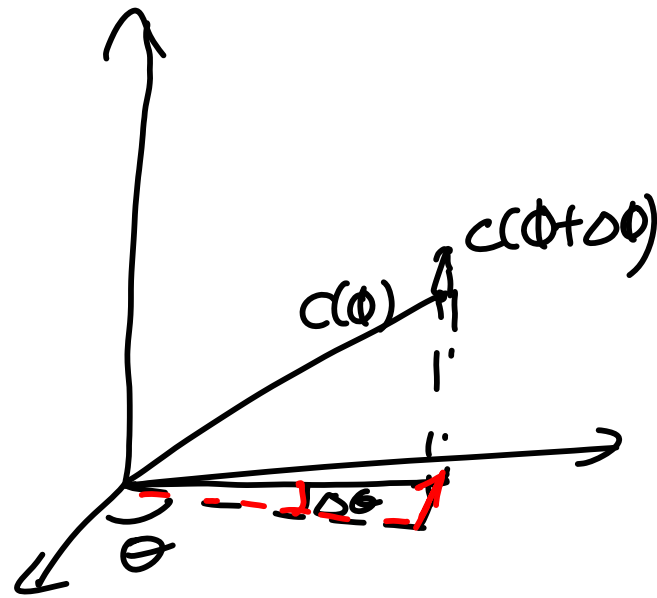
$$j_r = -D \frac{\Delta C}{\Delta r} = -D \frac{dC}{dr}$$

$$j_\theta = -D \left(\frac{C(\theta + \Delta\theta) - C(\theta)}{r \Delta\theta} \right)$$

$$= -D \frac{dC}{r d\theta}$$

$$j_\phi = -D \left(\frac{C(\phi + \Delta\phi) - C(\phi)}{r \sin\theta \Delta\phi} \right)$$

$$= -D \frac{dC}{r \sin\theta d\phi}$$



$$\frac{\partial C}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 C u_r) + \frac{1}{r \sin\theta} \frac{\partial}{\partial \theta} (\sin\theta C u_\theta) + \frac{1}{r \sin\theta} \frac{\partial (C u_\phi)}{\partial \phi}$$

$$= -\frac{1}{r^2} \frac{\partial}{\partial t} (r^2 j_r) - \frac{1}{r \sin\theta} \frac{\partial}{\partial \theta} (\sin\theta j_\theta) - \frac{1}{r \sin\theta} \frac{\partial j_\phi}{\partial \phi} + S$$

$$\frac{\partial c}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 c u_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta c u_\theta) + \frac{1}{r \sin \theta} \frac{\partial (c u_\phi)}{\partial \phi}$$

$$= D \left[\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial c}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial c}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 c}{\partial \phi^2} \right] + S$$

$$\frac{\partial c}{\partial t} + \nabla \cdot (u c) = D \nabla^2 c + S$$

$$\frac{\partial c}{\partial t} + \nabla \cdot (u c) = -\nabla \cdot j + S$$

$$j = -D \nabla c$$

$$\nabla c = \underline{e}_r \frac{\partial c}{\partial r} + \frac{\underline{e}_\theta}{r} \frac{\partial c}{\partial \theta} + \frac{\underline{e}_\phi}{r \sin \theta} \frac{\partial c}{\partial \phi}$$

$$j = j_r \underline{e}_r + j_\theta \underline{e}_\theta + j_\phi \underline{e}_\phi$$

$$\nabla \cdot (c \underline{u}) = \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 c u_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta c u_\theta) + \frac{1}{r \sin \theta} \frac{\partial (c u_\phi)}{\partial \phi}$$

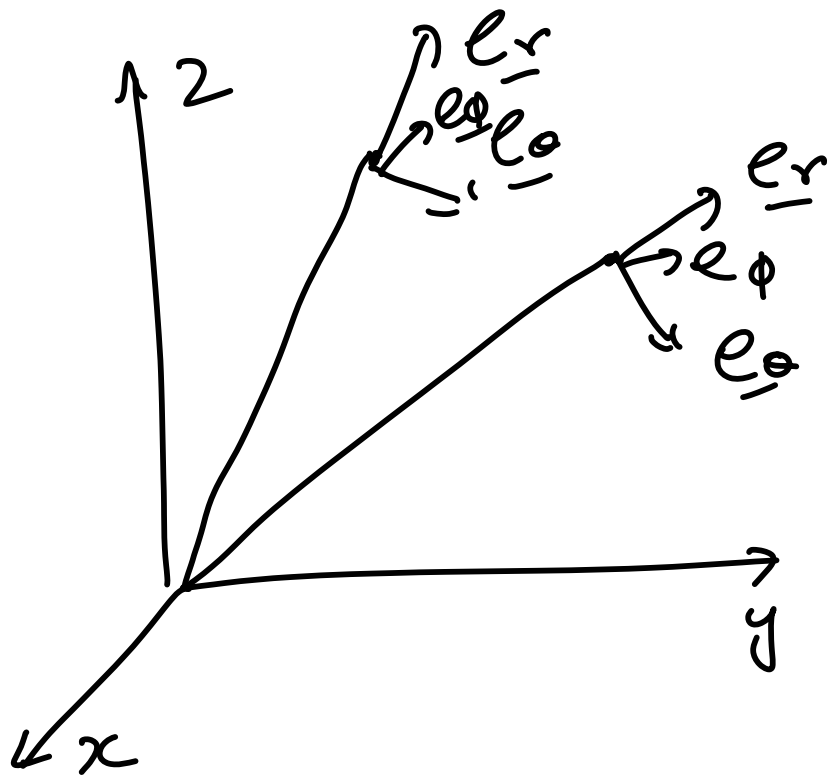
$$\nabla^2 c = \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial c}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial c}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 c}{\partial \phi^2}$$

$$\nabla = \underline{e}_r \frac{\partial}{\partial r} + \frac{\underline{e}_\theta}{r} \frac{\partial}{\partial \theta} + \frac{\underline{e}_\phi}{r \sin \theta} \frac{\partial}{\partial \phi}$$

$$\nabla \cdot \underline{A} = \left(\underline{e}_r \frac{\partial}{\partial r} + \frac{\underline{e}_\theta}{r} \frac{\partial}{\partial \theta} + \frac{\underline{e}_\phi}{r \sin \theta} \frac{\partial}{\partial \phi} \right) \cdot (A_r \underline{e}_r + A_\theta \underline{e}_\theta + A_\phi \underline{e}_\phi)$$

$$= \left(\underline{e}_x \frac{\partial}{\partial x} + \underline{e}_y \frac{\partial}{\partial y} + \underline{e}_z \frac{\partial}{\partial z} \right) \cdot (A_x \underline{e}_x + A_y \underline{e}_y + A_z \underline{e}_z)$$

$$= \frac{\partial A_x}{\partial x} + \frac{\partial A_y}{\partial y} + \frac{\partial A_z}{\partial z}$$



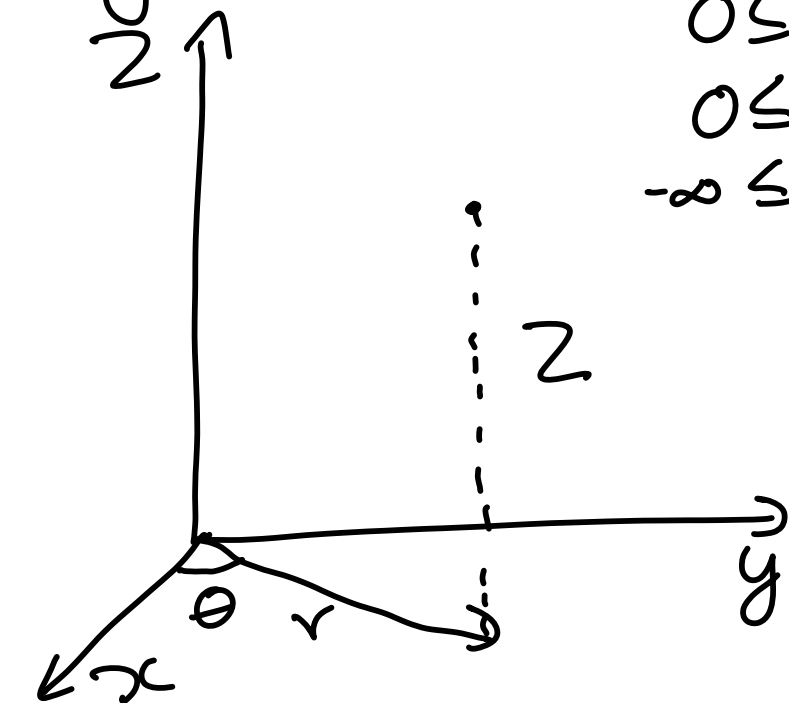
$$\nabla \cdot \underline{A} = \left(\underline{e}_r \frac{\partial}{\partial r} + \underline{e}_\theta \frac{\partial}{\partial \theta} + \underline{e}_\phi \frac{\partial}{\partial \phi} \right) \cdot (\underline{A}_r \underline{e}_r + \underline{A}_\theta \underline{e}_\theta + \underline{A}_\phi \underline{e}_\phi)$$

$$\begin{aligned} \nabla^2 &= \nabla \cdot \nabla \\ &= \left(\underline{e}_r \frac{\partial}{\partial r} + \frac{\underline{e}_\theta}{r} \frac{\partial}{\partial \theta} + \frac{\underline{e}_\phi}{r \sin \theta} \frac{\partial}{\partial \phi} \right) \cdot \left(\underline{e}_r \frac{\partial}{\partial r} + \frac{\underline{e}_\theta}{r} \frac{\partial}{\partial \theta} + \frac{\underline{e}_\phi}{r \sin \theta} \frac{\partial}{\partial \phi} \right) \\ &= \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial}{\partial r} \right) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2}{\partial \phi^2} \end{aligned}$$

$$\frac{\partial T}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 T u_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta T u_\theta) + \frac{1}{r \sin \theta} \frac{\partial (T u_\phi)}{\partial \phi}$$

$$= \alpha \left[\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} \right] + \frac{S_e}{\rho C_p}$$

Cylindrical co-ordinate system:



$$0 \leq \theta \leq 2\pi \quad (r, \theta, z)$$

$$0 \leq r < \infty$$

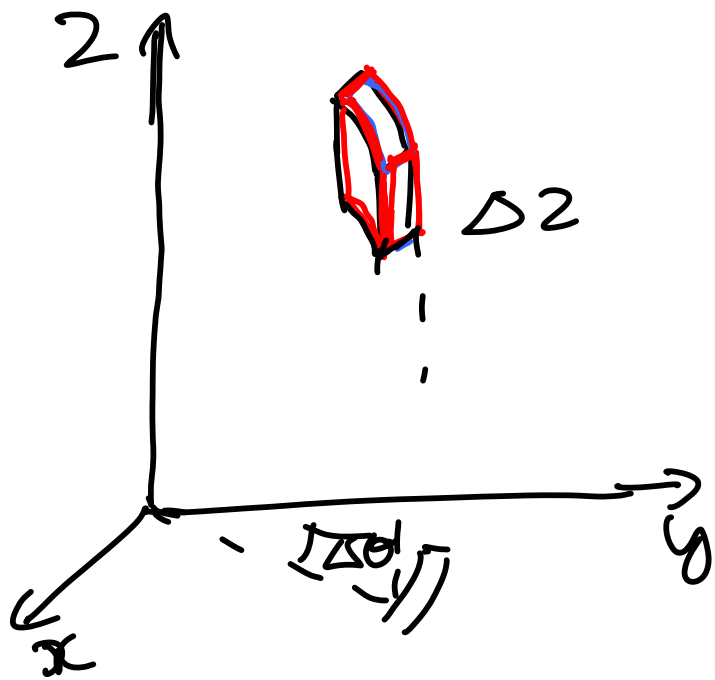
$$-\infty \leq z \leq \infty \quad r = \sqrt{x^2 + y^2}$$

$$z = z$$

$$\cos \theta = \frac{x}{\sqrt{x^2 + y^2}}$$

$$\sin \theta = \frac{y}{\sqrt{x^2 + y^2}}$$

$$\tan \theta = (y/x)$$



$$\frac{\partial C}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (r c u_r) + \frac{1}{r} \frac{\partial}{\partial \theta} (c u_\theta) + \frac{\partial}{\partial z} (c u_z)$$

$$= -\frac{1}{r} \frac{\partial}{\partial r} (r j_r) - \frac{1}{r} \frac{\partial}{\partial \theta} (j_\theta) - \frac{\partial}{\partial z} (j_z) + S$$

$$\vec{A} = -D \left[\underline{e}_r \frac{\partial C}{\partial r} + \frac{\underline{e}_\theta}{r} \frac{\partial C}{\partial \theta} + \underline{e}_z \frac{\partial C}{\partial z} \right]$$

$$\Delta = \underline{e}_r \frac{\partial^2}{\partial r^2} + \frac{\underline{e}_\theta}{r} \frac{\partial^2}{\partial \theta^2} + \underline{e}_z \frac{\partial^2}{\partial z^2}$$

$$\nabla \cdot \mathbf{j} = \frac{1}{r} \frac{\partial}{\partial r} (r j_r) + \frac{1}{r} \frac{\partial j_\theta}{\partial \theta} + \frac{\partial j_z}{\partial z}$$

$$\frac{\partial C}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (r C u_r) + \frac{1}{r} \frac{\partial (C u_\theta)}{\partial \theta} + \frac{\partial (C u_z)}{\partial z}$$

$$= D \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial C}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 C}{\partial \theta^2} + \frac{\partial^2 C}{\partial z^2} \right]$$

$$\mathbf{j} = -D \left[\underline{e}_r \frac{\partial C}{\partial r} + \frac{\underline{e}_\theta}{r} \frac{\partial C}{\partial \theta} + \underline{e}_z \frac{\partial C}{\partial z} \right]$$

$$\frac{\partial C}{\partial t} + \underline{u} \cdot \nabla C = D \nabla^2 C + S$$

$$\nabla^2 = \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \right) \right) + \frac{1}{r^2} \frac{\partial^2}{\partial \theta^2} + \frac{\partial^2}{\partial z^2}$$

$$\frac{\partial c}{\partial t} + \nabla \cdot (\underline{u} c) = D \nabla^2 c + S \quad \text{'Convection-diffusion eqn'}$$

$$Pe \ll 1 \quad D \nabla^2 c + S = 0$$

$$Pe \gg 1 \quad \frac{\partial c}{\partial t} + \nabla \cdot (\underline{u} c) = 0$$

$$\frac{\partial c}{\partial t} + \nabla \cdot (\underline{u} c) = D \nabla^2 c + S$$

$$c^* = (c/c_0) \quad \underline{u}^* = (\underline{u}/U) ; r^* = (r/L) \quad t^* = \left(\frac{tU}{L}\right)$$

$$\frac{\partial c^*}{\partial t^*} + \frac{U}{L} \nabla^* \cdot (\underline{u}^* c^*) = \frac{D}{L^2} \nabla^{*2} c^* + S$$

$$\nabla^* = \frac{1}{L} \nabla \quad \nabla^* = \left(\underline{e}_x \frac{\partial}{\partial x^*} + \underline{e}_y \frac{\partial}{\partial y^*} + \underline{e}_z \frac{\partial}{\partial z^*} \right)$$

$$\text{Pe} \left(\frac{\partial c^*}{\partial t^*} + \nabla^* \cdot (u^* c) \right) = \nabla^{*2} c^* + \left(\frac{SL^2}{D} \right)$$

$$S^* = \left(SL^2/D \right)$$

$$\text{Pe} = \left(\frac{UL}{D} \right)$$

$$D \nabla^2 c + S = 0$$

Diffusion equation.

Diffusion equation:

$$\nabla^2 C = 0 \quad \nabla^2 T = 0$$

$$\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial C}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial C}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 C}{\partial \phi^2} = 0$$

$$C(r, \theta, \phi) = R(r) \Theta(\theta) \Phi(\phi)$$

$$\frac{1}{R} \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial R}{\partial r} \right) + \frac{1}{\Theta} \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial \Theta}{\partial \theta} \right) + \frac{1}{\Phi} \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 \Phi}{\partial \phi^2} = 0$$

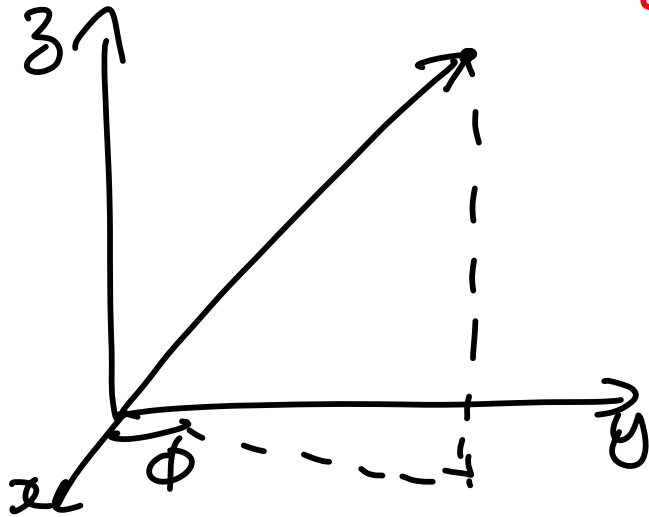
$$r^2 \sin^2 \theta \left[\frac{1}{R} \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial R}{\partial r} \right) + \frac{1}{\Theta} \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial \Theta}{\partial \theta} \right) \right] + \frac{\partial^2 \Phi}{\partial \phi^2} = 0$$

$$\frac{1}{r^2} \frac{\partial^2 \Phi}{\partial \phi^2} = -m^2 \quad \text{If } C = +m^2, \Phi = Ae^{m\phi} + Be^{-m\phi}$$

$$\text{If } C = -m^2, \Phi = A \sin(m\phi) + B \cos(m\phi)$$

$$\Phi(\phi + 2\pi) = \Phi(\phi)$$

$$m = \text{Integer}$$



$$r^2 \sin \theta \left[\frac{1}{R} \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial R}{\partial r} \right) + \frac{1}{\sin^2 \theta} \frac{1}{r^2} \frac{\partial}{\partial \theta} \left(\sin^2 \theta \frac{\partial \Phi}{\partial \theta} \right) \right] - m^2 = 0$$

$$\left[\frac{1}{R} \frac{\partial}{\partial r} \left(r^2 \frac{\partial R}{\partial r} \right) + \left[\frac{1}{\sin^2 \theta} \frac{\partial}{\partial \theta} \left(\sin^2 \theta \frac{\partial \Phi}{\partial \theta} \right) - \frac{m^2}{\sin^2 \theta} \right] \right] = 0$$

$$\frac{1}{R} \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial R}{\partial r} \right) - \frac{m^2}{\sin^2 \theta} = C$$

Case where $m=0$

$$\frac{1}{\Theta} \frac{1}{\sin \theta} \frac{d}{d\theta} \left(\sin \theta \frac{d\Theta}{d\theta} \right) = C$$

$$\frac{d^2 \Theta}{d\theta^2} + \frac{\cos \theta}{\sin \theta} \frac{d\Theta}{d\theta} - C\Theta = 0$$

$$\cos \theta = x$$

$$\frac{d}{dx} = -\frac{1}{\sin \theta} \frac{d}{d\theta}$$

$$\frac{1}{\Theta} \frac{d}{dx} \left((1-x^2) \frac{d\Theta}{dx} \right) = C$$

$$(1-x^2) \frac{d^2 \Theta}{dx^2} - 2x \frac{d\Theta}{dx} - C\Theta = 0$$

Legendre equation:

Has convergent solutions only for $C = n(n+1)$ and n is an integer.

$$(1-x^2) \frac{d^2 \Theta}{dx^2} - 2x \frac{d\Theta}{dx} + p(p+1)\Theta = 0$$

$$\Theta = \sum_{n=0}^{\infty} C_n x^n \quad x = \cos \theta$$

$$\frac{d\Theta}{dx} = \sum_{n=0}^{\infty} n C_n x^{n-1}$$

$$\frac{d^2 \Theta}{dx^2} = \sum_{n=0}^{\infty} n(n-1) C_n x^{n-2}$$

$$\left(\sum_{n=0}^{\infty} C_n n(n-1) x^{n-2} \right) - \left(\sum_{n=0}^{\infty} C_n n(n-1) x^n \right) - 2 \sum_{n=0}^{\infty} C_n n x^n + p(p+1) \sum_{n=0}^{\infty} C_n x^n = 0$$

$$\sum_{n=2}^{\infty} \left[C_{n+2} n(n+1) x^n \right] - \sum_{n=0}^{\infty} C_n n(n+1) x^n + p(p+1) \sum_{n=0}^{\infty} C_n x^n = 0$$

$$C_{n+2} n(n+1) + p(p+1) C_n = 0$$

$$C_{n+2} = \frac{[n(n+1) - b(b+1)]C_n}{(n+2)(n+1)} //$$

In the limit $n \gg 1$; $C_{n+2} \approx C_n$

$$n(n+1) - b(b+1) = 0$$

$$C = -b(b+1)$$

$$\Theta = P_n(\cos \theta)$$

where $P_n =$ Legendre polynomial.

$$(1-x^2) \frac{\partial^2 \Theta}{\partial x^2} - 2x \frac{\partial \Theta}{\partial x} + n(n+1)\Theta = 0$$

$$P_0(\cos \theta) = 1$$

$$P_1(\cos \theta) = \cos \theta$$

$$P_2(\cos \theta) = \frac{1}{2}(3\cos^2 \theta - 1)$$

$$\int_0^\pi \sin \theta d\theta P_n(\cos \theta) P_m(\cos \theta) = \frac{2n}{2n+1} \delta_{nm}$$

$$(1-x^2) \frac{d^2 \Theta}{dx^2} - 2x \frac{d\Theta}{dx} - \frac{m^2}{1-x^2} = -n(n+1)$$

$$\Theta = P_n^m(\cos \theta) \int \sin \theta d\theta P_n^m(\cos \theta) P_p^m(\cos \theta) = \left(\frac{2n}{2n+1} \right) \left(\frac{(n+m)!}{(n-m)!} \right) \delta_{np}$$

$$|m| \leq n$$

$$\Theta \Phi = \sum_{n=0}^{\infty} \sum_{m=-n}^n Y_n^m(\theta, \phi)$$

$$Y_n^m(\theta, \phi) = P_n^m(\cos \theta) \begin{pmatrix} \sin(m\phi) \\ \cos(m\phi) \end{pmatrix}$$

$$\int_0^{2\pi} d\phi \int_0^\pi \sin \theta d\theta Y_n^m(\theta, \phi) Y_p^q(\theta, \phi) = \frac{2n}{2n+1} \left(\frac{(n+m)!}{(n-m)!} \right) \delta_{np} \delta_{mq}$$

$$\frac{1}{R} \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial R}{\partial r} \right) - \frac{n(n+1)}{r^2} = 0$$

$$r^2 \frac{\partial^2 R}{\partial r^2} + 2r \frac{\partial R}{\partial r} - n(n+1)R = 0$$

$$R = r^\alpha$$

$$\alpha(\alpha-1) + 2\alpha - n(n+1) = 0$$

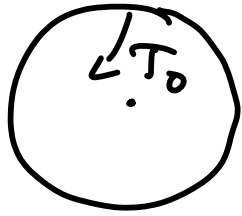
$$\alpha = n, -(n+1)$$

$$R = A_n r^n + B_n r^{-(n+1)}$$

$$\Theta = P_n^m(\cos \theta); \quad \Phi = \begin{pmatrix} \cos m\phi \\ \sin m\phi \end{pmatrix}$$

$$\Theta \Phi = Y_n^m(\theta, \phi)$$

$$C = \sum_{n=0}^{\infty} \sum_{m=-n}^{+n} \left(A_n r^n + \frac{B_n}{r^{n+1}} \right) Y_n^m(\theta, \phi)$$

T_∞ 

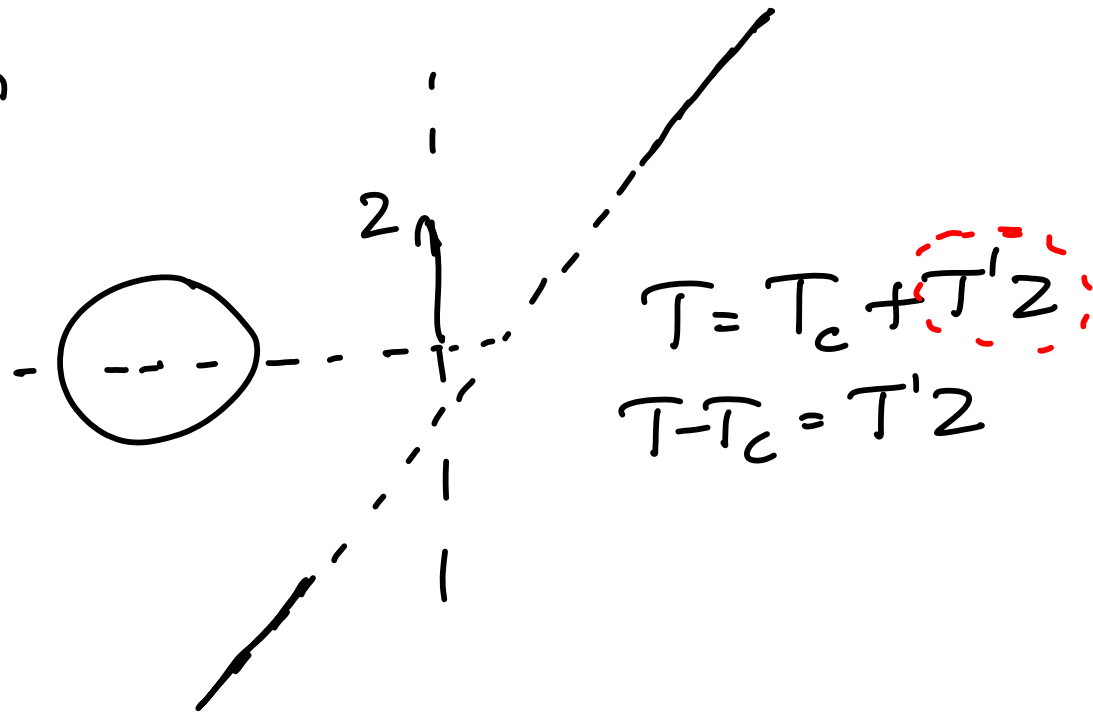
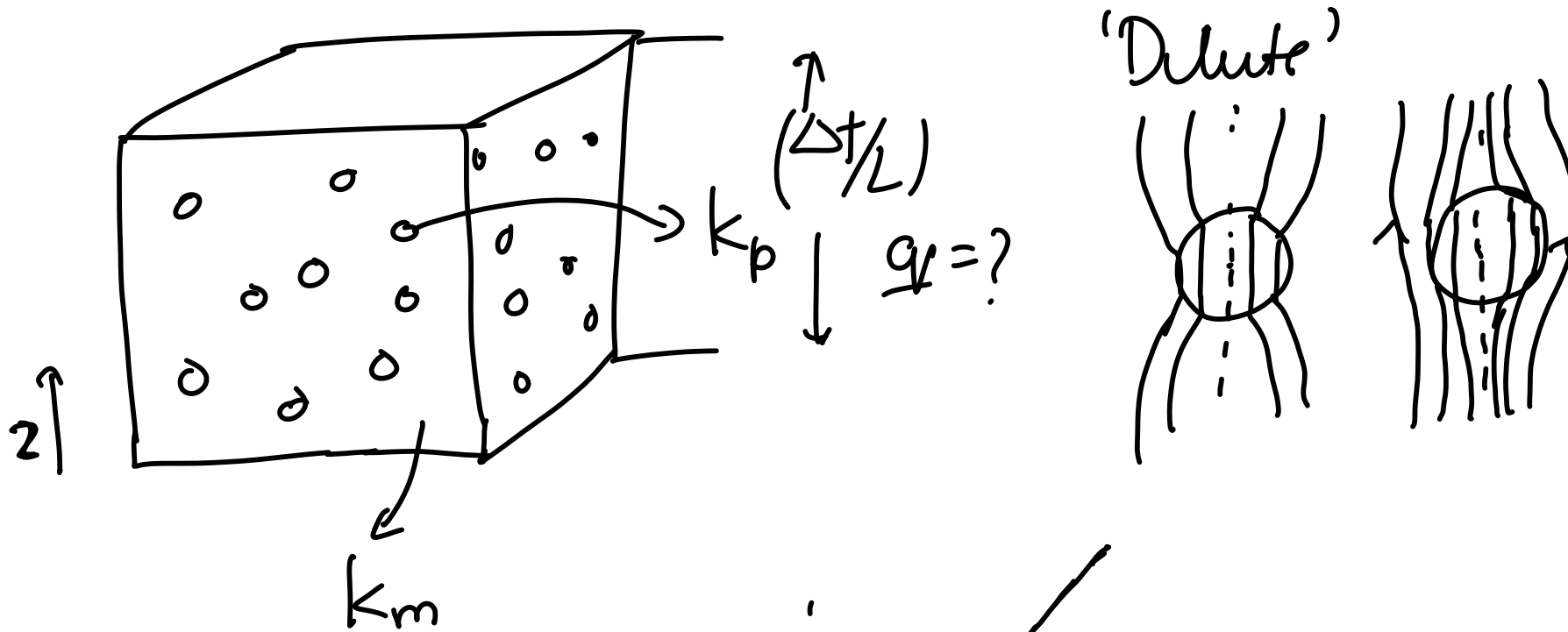
$$T = T_\infty + \frac{(T_0 - T_\infty)R}{r}$$

$$n=0 \ \& \ m=0$$

$$T = A_0 + \frac{B_0}{r}$$

$$T = T_\infty + \frac{Q}{4\pi k r}$$

Effective conductivity of a composite:



$$\langle q_2 \rangle = -k_{eff} \left\langle \frac{dT}{dz} \right\rangle = -k_{eff} T'$$

$$\langle q_2 \rangle = \frac{1}{V} \int dV q_2$$

$$= \frac{1}{V} \left[\int_{\text{particles}} dV q_2 + \int_{\text{matrix}} dV q_2 \right]$$

For particles, $q_2 = -k_p \frac{\partial T}{\partial z}$

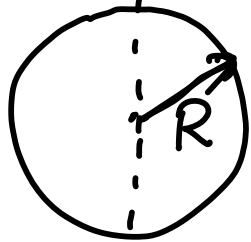
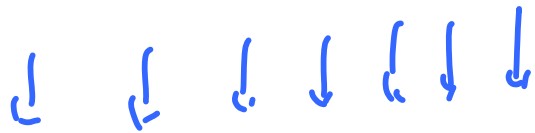
For matrix $q_2 = -k_m \frac{\partial T}{\partial z}$

$$\langle q_2 \rangle = \frac{1}{V_{\text{particle}}} \int dV \left(-k_p \frac{\partial T}{\partial z} \right) + \frac{1}{V_{\text{matrix}}} \int dV \left(-k_m \frac{\partial T}{\partial z} \right)$$

$$= \frac{1}{V} \int_{\text{total volume}} dV \left(-k_m \frac{dT}{dz} \right) + \frac{1}{V_{\text{particle}}} \int dV \left(-(k_p - k_m) \frac{dT}{dz} \right)$$

$$= \left(-k_m \left\langle \frac{dT}{dz} \right\rangle \right) + \frac{1}{V_{\text{particle}}} \int dV \left(-(k_p - k_m) \frac{dT}{dz} \right)$$

$$= -k_m T' + \frac{N}{V_{\text{particle}}} \int dV \left(-(k_p - k_m) \frac{dT}{dz} \right)$$



T_2

$$T = T_c + T'z$$

$$\nabla^2 T_p = 0$$

$$\nabla^2 T_m = 0$$

At $r = R$,

$$T_p = T_m$$

$$-q_r|_h = -q_r|_m$$

$$\text{As } r \rightarrow \infty, T = T'z$$



$$T_p = \sum_{n=0}^{\infty} \left(A_{pn} r^n + \frac{B_{pn}}{r^{n+1}} \right) P_n(\cos\theta) \quad T'_2 = T' r P'_1(\cos\theta)$$

$$T_m = \sum_{n=0}^{\infty} \left(A_{mn} r^n + \frac{B_{mn}}{r^{n+1}} \right) P_n(\cos\theta)$$

$$\text{At } r=R, \quad T_p = T_m$$

$$\sum_{n=0}^{\infty} \left(A_{pn} R^n + \frac{B_{pn}}{R^n} \right) P_n(\cos\theta) = \sum_{n=0}^{\infty} \left(A_{mn} R^n + \frac{B_{mn}}{R^n} \right) P_n(\cos\theta)$$

$$A_{pn} R^n + \frac{B_{pn}}{R^n} = A_{mn} R^n + \frac{B_{mn}}{R^n}$$

$$q_r = -k_p \frac{\partial T_p}{\partial r} \Big|_{r=R} = -k_m \frac{\partial T_m}{\partial r} \Big|_{r=R}$$

$$k_p \left[A_{pn} (n R^{n-1}) - \frac{B_{pn} (n+1)}{R^{n+2}} \right] = k_m \left[A_{mn} n R^{n-1} - \frac{B_{mn} (n+1)}{R^{n+2}} \right]$$

$$\text{At } r=0, \frac{\partial T_p}{\partial r} = 0 \Rightarrow B_{pn} = 0 \text{ for all } n$$

$$\text{As } r \rightarrow \infty, T = T' z = T' r \cos \theta = T' r P_1(\cos \theta)$$

$$\sum_{n=0}^{\infty} \left(A_{mn} r^n + \frac{B_{mn}}{r^{n+1}} \right) P_n(\cos \theta) = T' r \cos \theta$$

$$= T' r P_1(\cos \theta)$$

$$= T' r \delta_{m1}$$

$$\Rightarrow A_{m1} = T' \text{ \& } A_{mn} = 0 \text{ for } n \neq 1$$

For $n=1$,

$$A_{p1} R = A_{m1} R + \frac{B_{m1}}{R^2}$$

Matrix

$$T = T' r P_1^0(\cos\theta)$$

$$+ \frac{B_{m1}}{r^2} P_1^0(\cos\theta)$$

$$k_p A_{p1} = k_m A_{m1} - \frac{2 B_{m1}}{R^3}$$

For $n > 1$

$$A_{pn} R^n = \frac{B_{mn}}{R^{n+1}}$$

$$k_p A_{pn} n(R^{n-1}) = - \frac{k_m B_{mn} (n+1)}{R^{n+2}}$$

$$A_{pn} = 0 \quad \& \quad B_{mn} = 0 \quad \text{for } n > 1$$



$$A_{b1} = \frac{3T'}{(2 + k_p/k_m)} \quad B_{m1} = \frac{(1 - k_p/k_m) R^3 T'}{(2 + k_p/k_m)}$$

$$T_b = \frac{3T' R r P_1(\cos\theta)}{2 + k_R} = \frac{3T' R z}{2 + k_R}$$

$$T_m = T' r P_1(\cos\theta) + \frac{(1 - k_R) R^3 T' P_1(\cos\theta)}{2 + k_R}$$

where $k_R = (k_p/k_m)$

$$\begin{aligned} \langle q_{z2} \rangle &= -k_m T' + \frac{N}{V} \int dV (-(k_p - k_m)) \frac{\partial T}{\partial z} \\ &= \left[-k_m T' + \frac{N}{V} \int dV [-(k_p - k_m)] \left(\frac{3T' R}{2 + k_R} \right) \right] \end{aligned}$$

$$= - \left[k_m T' + \frac{N V_0}{V} (k_0 - k_m) \left(\frac{3T'}{2 + k_R} \right) \right]$$

$$= - \left[k_m + \phi_V \frac{(k_0 - k_m) 3}{2 + k_R} \right] T'$$

$$k_{\text{eff}} = k_m \left[1 + \phi_V \frac{3(k_R - 1)}{2 + k_R} \right]$$

where $k_R = (k_p / k_m)$

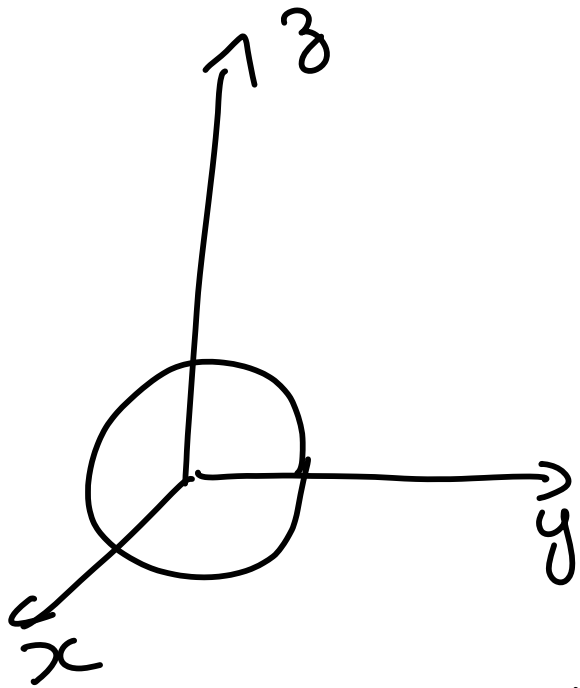
$$\text{Forcing term} = T' z = T' r \cos \theta$$

$$= T' r Y_{10}(\theta, \phi)$$

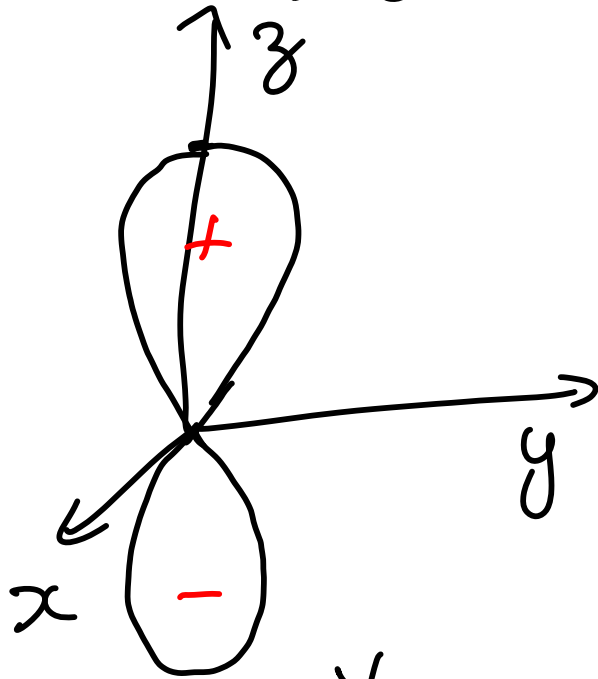
$$Y_{10} = P_1^0(\cos \theta)$$

$$\text{Symmetry} - Y_{10}(\theta, \phi)$$

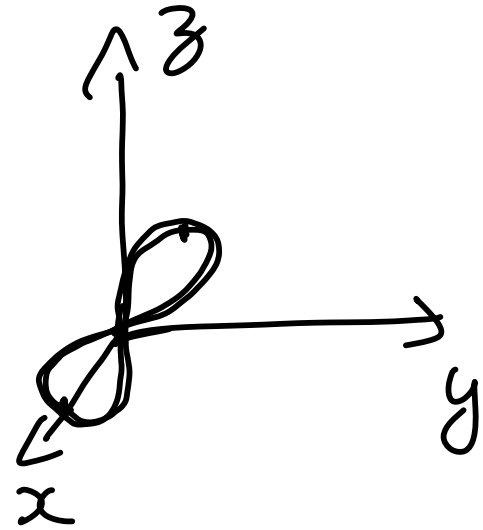
$$Y_{00} = 1$$



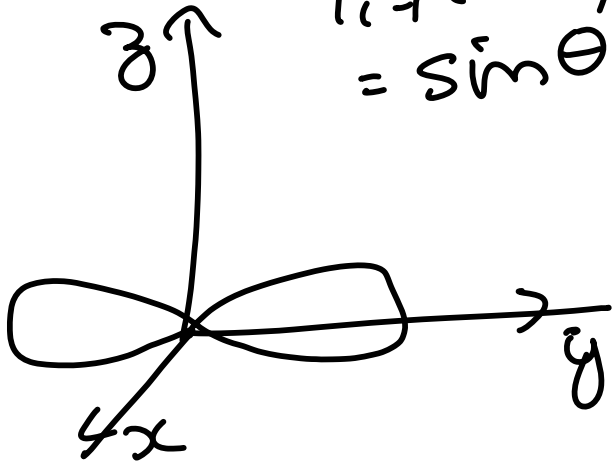
$$Y_{10} = P_1^0(\cos\theta) = \cos\theta$$



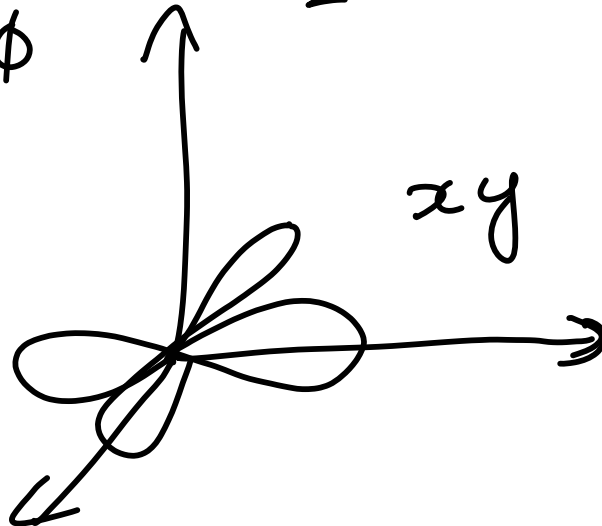
$$Y_{11} = P_1^1(\cos\theta)\cos\phi = \sin\theta\cos\phi$$

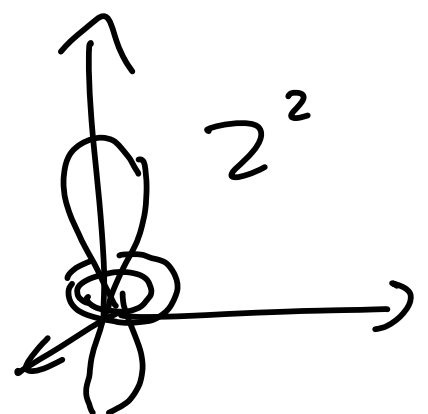
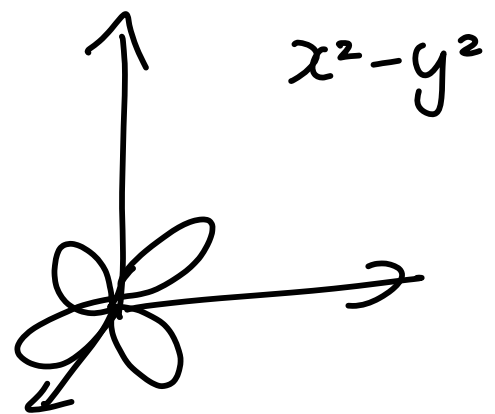
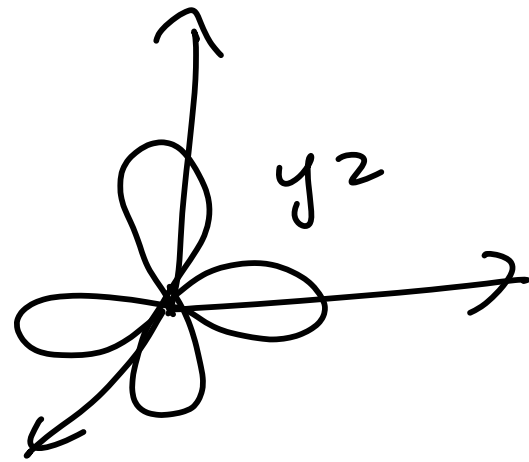
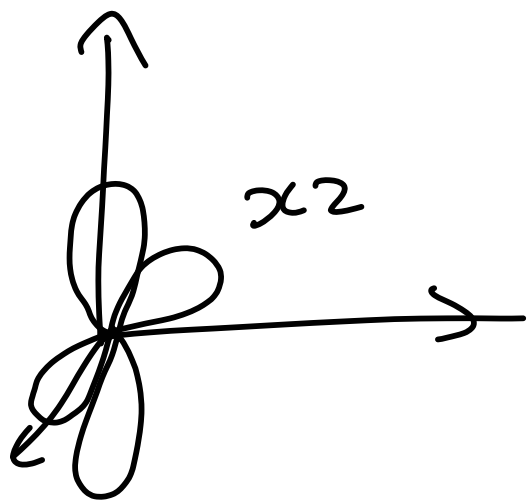


$$Y_{1,-1}(\theta, \phi) = \sin\theta\sin\phi$$



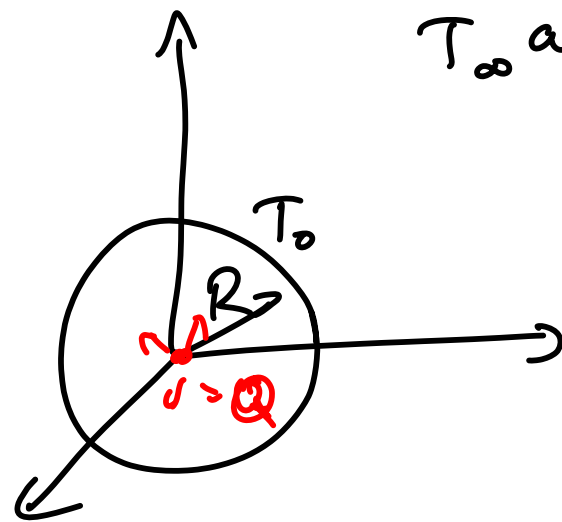
$$Y_2$$





$$\left[-\frac{\hbar^2}{2m} \nabla^2 + V(r) \right] \psi = E \psi$$

Source, dipole, . . .



T_∞ as $r \rightarrow \infty$

$$T - T_\infty = \frac{(T_0 - T_\infty)R}{r}$$

$$q_r = -k \frac{\partial T}{\partial r} = \frac{k(T_0 - T_\infty)R}{r^2}$$

$$Q = 4\pi r^2 q_r = k(T_0 - T_\infty)(4\pi R)$$

$$T - T_\infty = \frac{Q}{4\pi k r}$$

'Point source' $R \rightarrow 0$

$$k \nabla^2 T + S_e = 0$$

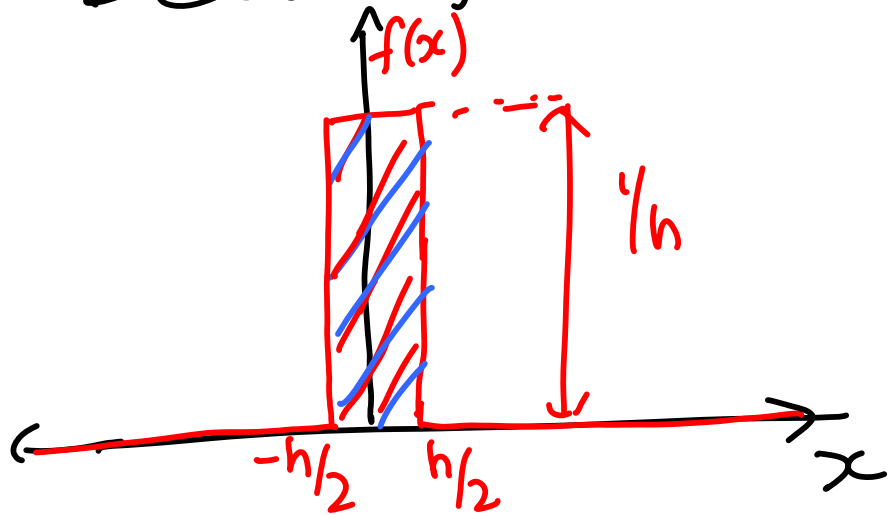
Delta functions:

$$\nabla^2 T + Q \delta(x) = 0$$

$$Q \delta(x) = 0 \text{ for } x \neq 0$$

$$\int dV Q \delta(x) = Q$$

Delta function:



Area = 1

$$\int_{-h/2}^{h/2} dx f(x) = 1$$

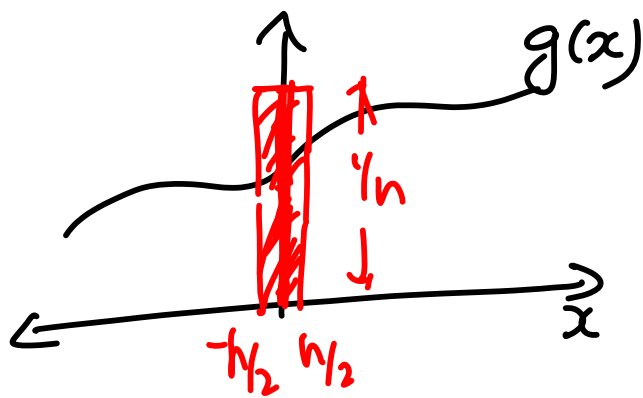
$$\int_{-\infty}^{\infty} dx f(x) = 1$$

$$\delta(x) = \lim_{h \rightarrow 0} (f(x))$$

$$\delta(x) = 0 \text{ for } x \neq 0$$

$$\int_{-\infty}^{\infty} dx \delta(x) = 1$$

$$\int_{-\infty}^{\infty} dx \delta(x) g(x) = g(0)$$



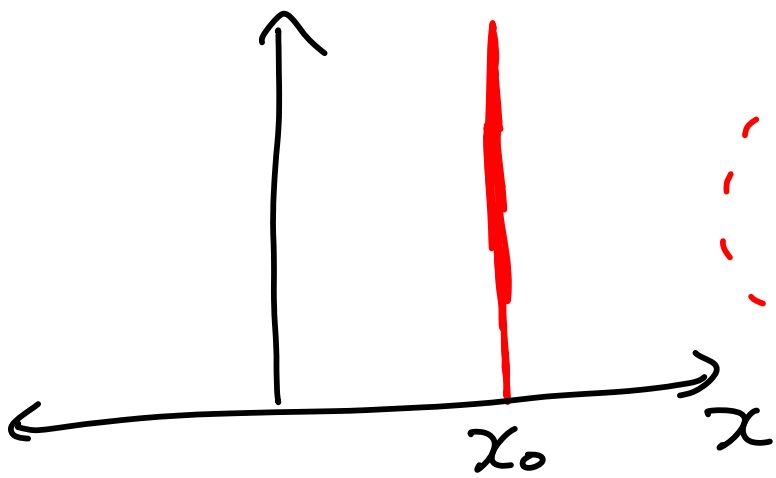
$$\int_{-\infty}^{\infty} dx f(x) g(x) = \int_{-\infty}^{\infty} dx \left(\frac{1}{h}\right) g(x)$$

$$= \int_{-\infty}^{\infty} dx \left(\frac{1}{h}\right) \left[g(0) + x \left. \frac{dg}{dx} \right|_{x=0} + \frac{x^2}{2} \left. \frac{d^2g}{dx^2} \right|_{x=0} + \dots \right]$$

$$= \int_{-\infty}^{\infty} dx \frac{1}{h} (g(0)) + \frac{1}{h} \left. \frac{dg}{dx} \right|_{x=0} \int_{-\infty}^{\infty} dx x$$

$$+ \frac{1}{h} \left. \frac{d^2g}{dx^2} \right|_{x=0} \int_{-\infty}^{\infty} dx x^2$$

$$= g(0)$$



$\delta(x-x_0) \neq 0$ only for $x=x_0$

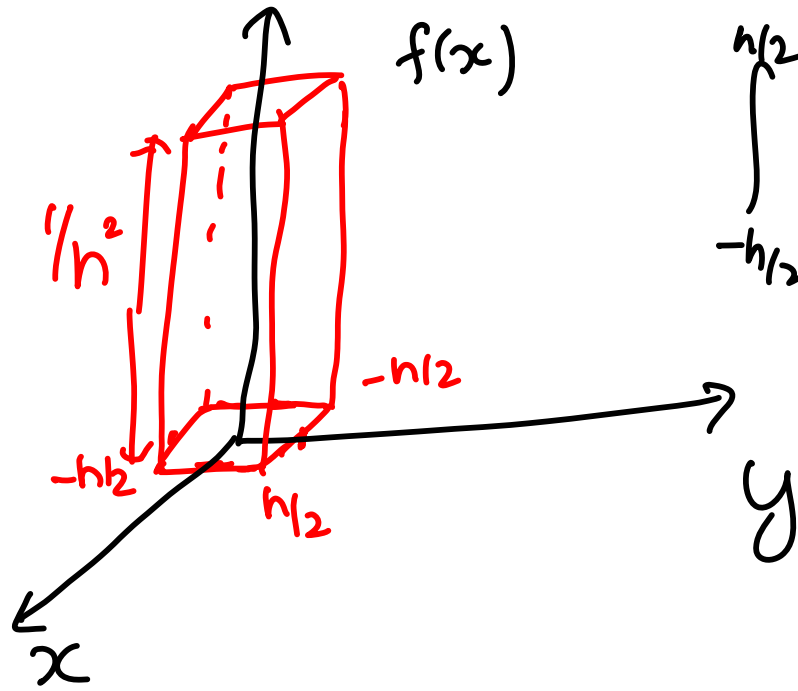
$$\int_{-\infty}^{\infty} dx \delta(x-x_0) = 1$$

$$\int_{-\infty}^{\infty} dx \delta(x-x_0) g(x) = g(x_0)$$

Function $f(x,y) = 1/h^2$ for $-h/2 < x < h/2$
 & $-h/2 < y < h/2$

= 0 otherwise

$$\delta(x,y) = \lim_{h \rightarrow 0} f(x,y)$$



$$\int_{-h/2}^{h/2} \int_{-h/2}^{h/2} dx dy f(x,y) = 1$$

$$\int_{-\infty}^{\infty} dx \int_{-\infty}^{\infty} dy f(x,y) = 1$$

limit $f(x,y) = \delta(x,y)$
 $h \rightarrow 0$

Two-dimensional delta function:

$$\int_{-\infty}^{\infty} dx \int_{-\infty}^{\infty} dy \delta(x,y) = 1$$

$\delta(x, y) = 0$ for $x \neq 0$ or $y \neq 0$
 $\neq 0$ only for $x = 0$ & $y = 0$

$$\int_{-\infty}^{\infty} dx \int_{-\infty}^{\infty} dy \delta(x, y) g(x, y) = g(0, 0)$$

$\int_{-\infty}^{\infty} \int_{-\infty}^{\infty} \delta(x - x_0, y - y_0) g(x, y) = g(x_0, y_0)$

Three dimensional delta function:

$$f(x, y, z) = \frac{1}{h^3} \text{ for } -h/2 < x < h/2$$

$\& \quad -h/2 < y < h/2$
 $\& \quad -h/2 < z < h/2$

$= 0$ otherwise

$$\delta(x, y, z) = \lim_{h \rightarrow 0} f(x, y, z)$$

$$\int_{-\infty}^{\infty} dx \int_{-\infty}^{\infty} dy \int_{-\infty}^{\infty} dz \delta(x, y, z) = 1$$

$$\delta(x, y, z) = 0 \text{ for } x \neq 0 \text{ or } y \neq 0 \text{ or } z \neq 0$$

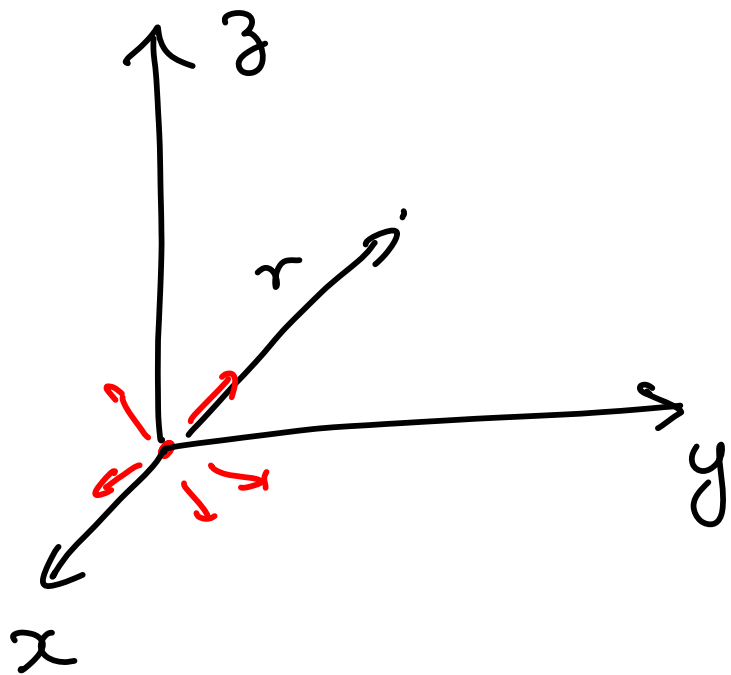
$$\int_{-\infty}^{\infty} dx \int_{-\infty}^{\infty} dy \int_{-\infty}^{\infty} dz \delta(x, y, z) g(x, y, z) = g(0, 0, 0)$$

$$\delta(\underline{x}) = \delta(x, y, z)$$

$$\int dV \delta(\underline{x}) = 1$$

$$\delta(\underline{x}) = 0 \text{ for } \underline{x} \neq 0$$

$$\int dV \delta(\underline{x}) g(\underline{x}) = g(0)$$



Heat/unit time = Q

$$T = \frac{Q}{4\pi k r}$$

$$k \nabla^2 T + Q \delta(\mathbf{x}) = 0$$

For $(\mathbf{x} \neq 0)$,

$$k \nabla^2 T = 0$$

$$k \left(\frac{1}{r^2} \frac{d}{dr} \left(r^2 \frac{dT}{dr} \right) \right) = 0$$

$$T = \frac{A}{r}$$

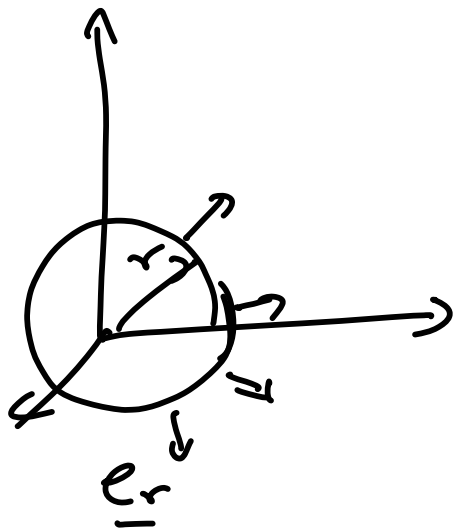
$$k \nabla^2 T = -Q \delta(\mathbf{x})$$

$$\int dV k \nabla^2 T = - \int dV Q \delta(\underline{x})$$

$$= - Q \int dV \delta(\underline{x}) = -Q$$

$$\int dV k \nabla^2 T = \int dV \nabla \cdot (k \nabla T)$$

$$= \int dS \underline{n} \cdot (k \nabla T)$$



$$k \nabla T = k \underline{e}_r \frac{\partial T}{\partial r}$$

$$= -k \underline{e}_r \frac{A}{r^2}$$

$$\underline{n} \cdot k \nabla T = \frac{-kA}{r^2}$$

$$\int dS \underline{n} \cdot k \nabla T = 4\pi r^2 \left(\frac{-kA}{r^2} \right) = -4\pi kA$$

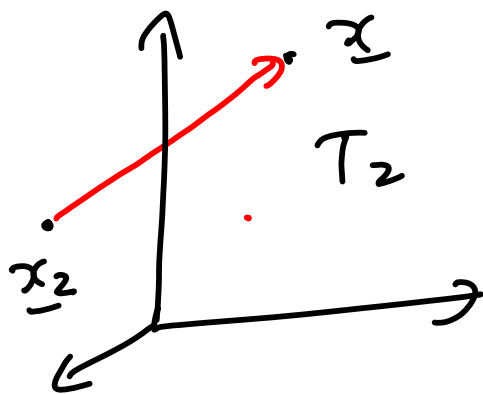
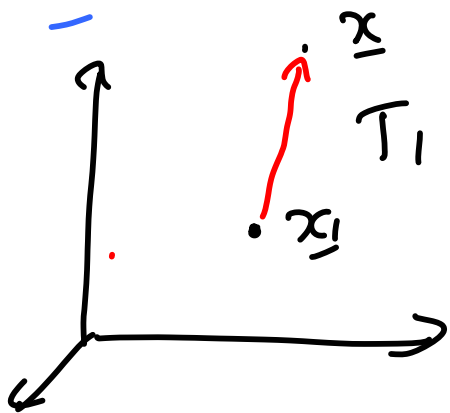
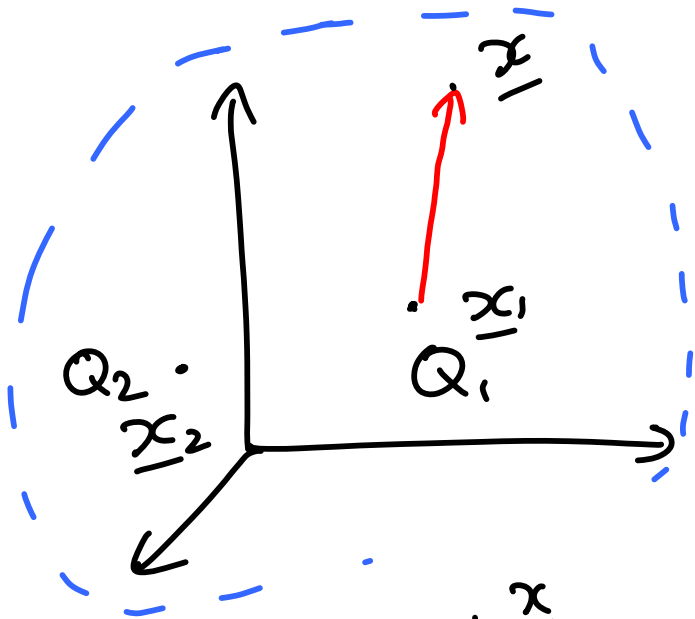
$$-4\pi kA = -Q \Rightarrow A = \frac{Q}{4\pi k}$$

$$k \nabla^2 T + Q \delta(\underline{x}) = 0 \quad (k \nabla^2 T + S_e = 0)$$

$$T = \frac{Q}{4\pi k r}$$

$$T(\underline{x}) = \frac{Q_1}{4\pi k |\underline{x} - \underline{x}_1|} + \frac{Q_2}{4\pi k |\underline{x} - \underline{x}_2|}$$

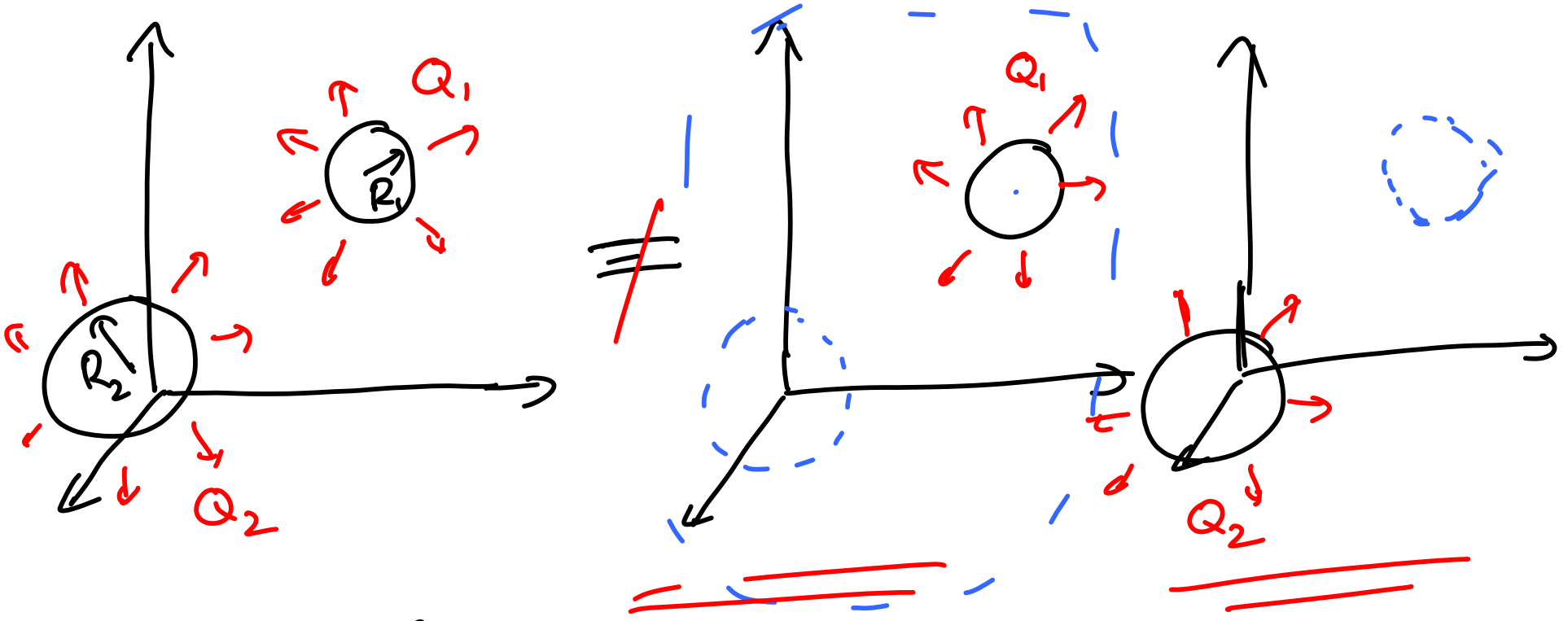
$$|\underline{x} - \underline{x}_i| = \left((x-x_i)^2 + (y-y_i)^2 + (z-z_i)^2 \right)^{1/2}$$



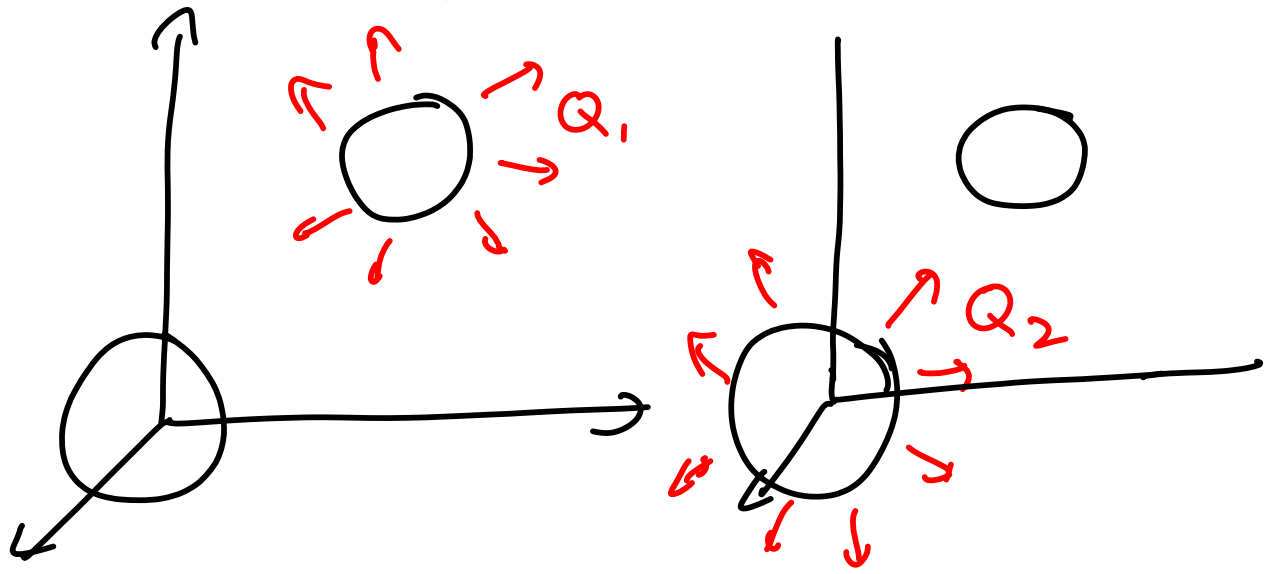
$$T_1 = \frac{Q_1}{4\pi k |\underline{x} - \underline{x}_1|}$$

$$T_2 = \frac{Q_2}{4\pi k |\underline{x} - \underline{x}_2|}$$

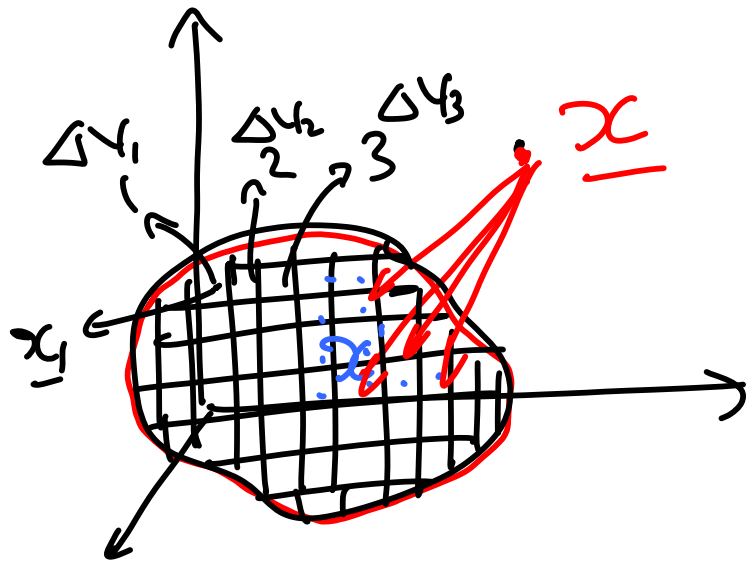
Linear superposition.



=



...



Heat generated = q (unit volume / time)

Heat generated / time in each volume
 $= q_1(\underline{x}_1) \Delta V_1, q_2(\underline{x}_2) \Delta V_2, \dots$

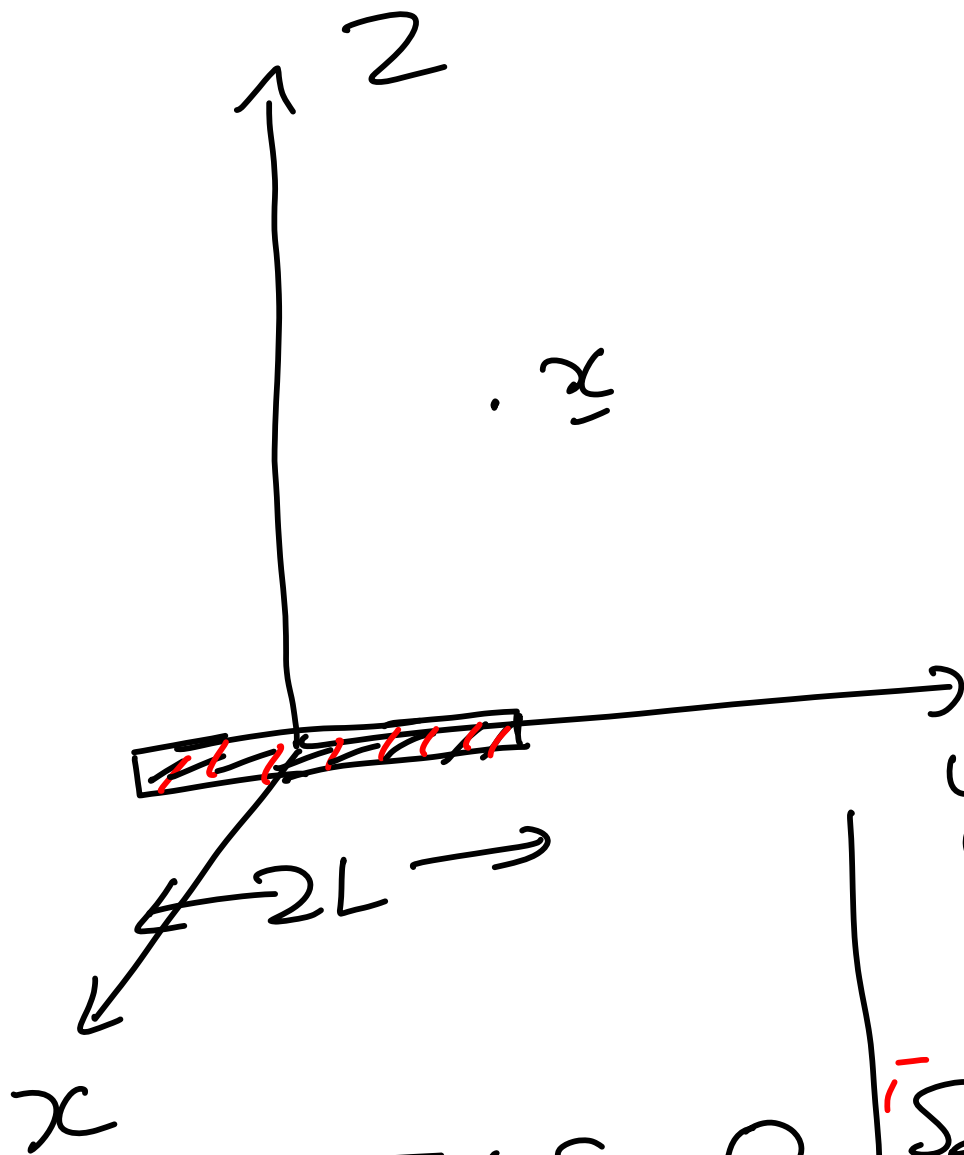
$$T(\underline{x}) \text{ due to source at } \underline{x}_1 = \frac{q_1(\underline{x}_1) \Delta V_1}{4\pi k |\underline{x} - \underline{x}_1|}$$

$$T(\underline{x}) \text{ due to source at } \underline{x}_2 = \frac{q_2(\underline{x}_2) \Delta V_2}{4\pi k |\underline{x} - \underline{x}_2|}$$

$$T(\underline{x}) = \sum_{i=1}^N \frac{q(\underline{x}_i) \Delta V_i}{|\underline{x} - \underline{x}_i|}$$

limit $\Delta V_i \rightarrow 0$

$$T(\underline{x}) = \int \frac{dV' q(\underline{x}')}{|\underline{x} - \underline{x}'|}$$



$$\nabla^2 T + S_e = 0$$

$$-L \leq y \leq L$$

(unit length / time)

$$S_e(\underline{x}) = Q$$

$S_e(\underline{x}) \neq 0$ only for $x=0$
& $z=0$

$= 0$ otherwise

$$\int dx \int dz S_e(\underline{x}) = Q$$

$$S_e(\underline{x}) = Q \delta(x) \delta(z)$$

for $-L \leq y \leq L$

$$k \nabla^2 T + Q \delta(x) \delta(z) = 0$$

$$T(\underline{x}) = \frac{1}{4\pi k} \int dV' \frac{\delta(x') \delta(z') Q}{|\underline{x} - \underline{x}'|}$$

$$= \frac{1}{4\pi k} \int dx' \int dy' \int dz' \frac{Q \delta(x') \delta(z')}{\sqrt{(x-x')^2 + (y-y')^2 + (z-z')^2}}$$

$$\int dx \delta(x) g(x) = g(0)$$

$$T(\underline{x}) = \frac{1}{4\pi k} \int dy' \int dz' \frac{Q \delta(z')}{\sqrt{x^2 + (y-y')^2 + z^2}}$$

$$= \frac{1}{4\pi k} \int dy' \frac{Q}{\sqrt{x^2 + (y-y')^2 + z^2}}$$

$$T(x, z) = \frac{Q}{4\pi k} \int_{-L}^L dy' \frac{1}{\sqrt{x^2 + (y - y')^2 + z^2}}$$

$$T(x, z) = \frac{Q}{4\pi k} \log \left[\frac{L + y + \sqrt{r^2 + (L + y)^2}}{-L + y + \sqrt{r^2 + (y - L)^2}} \right]$$

where $r^2 = (x^2 + z^2)$

Along the x - z plane, $y = 0$,

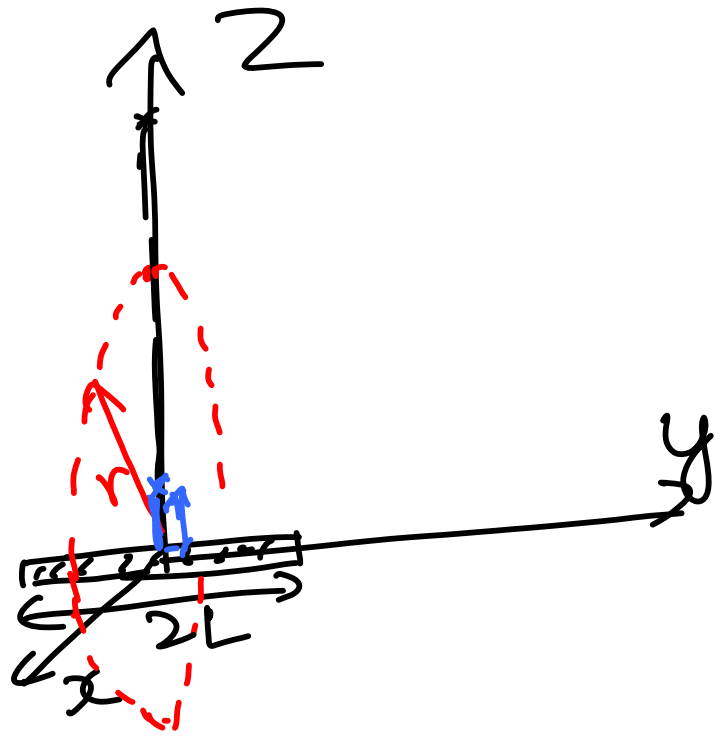
$$T = \frac{Q}{4\pi k} \log \left[\frac{L + \sqrt{r^2 + L^2}}{-L + \sqrt{r^2 + L^2}} \right]$$

$$\textcircled{1} \quad r \gg L$$

Expansion in small (L/r)

$$T = \frac{Q}{4\pi k} \log \left[\frac{(L/r) + \sqrt{1 + (L/r)^2}}{(-L/r) + \sqrt{1 + (L/r)^2}} \right]$$

$$= \frac{2QL}{4\pi k r}$$



$$\textcircled{2} \quad r \ll L$$

Expansion in small (r/L)

$$T = \frac{Q}{4\pi k} \log \left(\frac{1 + \sqrt{(r/L)^2 + 1}}{-1 + \sqrt{(r/L)^2 + 1}} \right) \quad \parallel \parallel$$

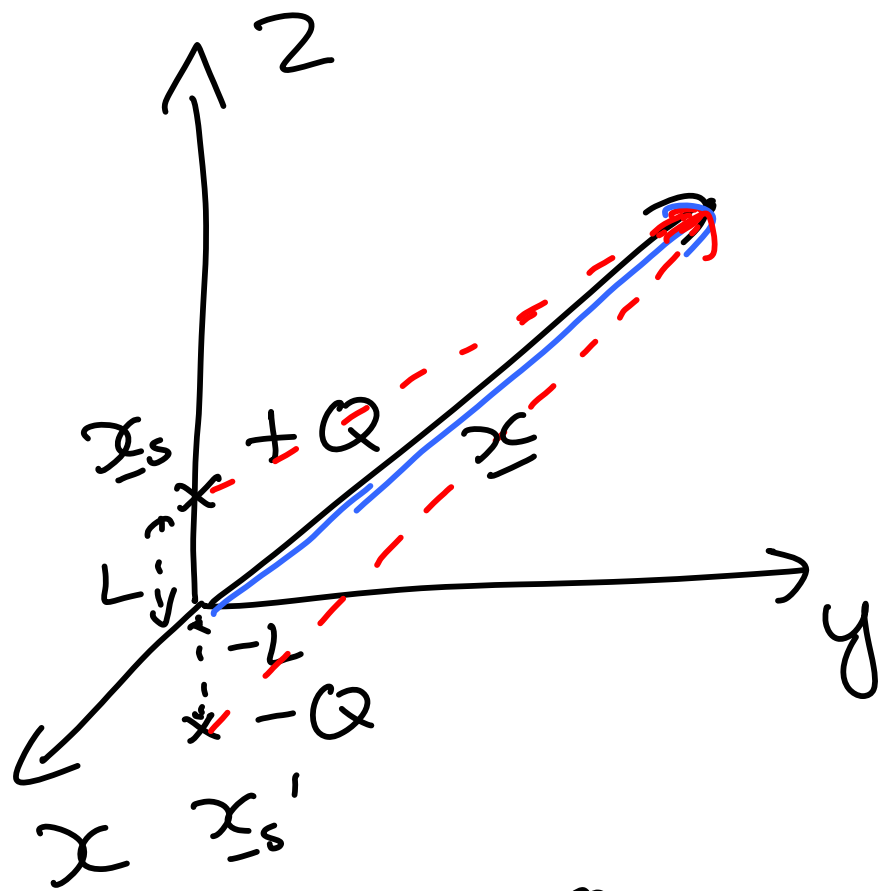
$$T(x) = \frac{Q}{4\pi k} \log\left(\frac{4L^2}{r^2}\right)$$

$$= \left(\frac{Q}{2\pi k}\right) (\log(2L) - \log(r))$$

$$\nabla^2 T = 0 \Rightarrow \frac{1}{r} \frac{d}{dr} \left(r \frac{\partial T}{\partial r} \right) = 0$$

$$T = C_1 \log r + C_2$$

$$= -\frac{Q}{2\pi k} \log r + C_2$$



Source $+Q$ at $(0, 0, L)$

Sink $-Q$ at $(0, 0, -L)$

$$T(\underline{x}) = \frac{Q}{4\pi k |\underline{x} - \underline{x}_s|} - \frac{Q}{4\pi k |\underline{x} - \underline{x}_s'|}$$

$$= \frac{Q}{4\pi k} \left[\frac{1}{\sqrt{x^2 + y^2 + (z-L)^2}} - \frac{1}{\sqrt{x^2 + y^2 + (z+L)^2}} \right]$$

Expand in (L/r) :

$$\begin{aligned} T(x) &= \frac{Q}{4\pi k} \left[\frac{1}{\sqrt{x^2 + y^2 + z^2 - 2Lz + L^2}} - \frac{1}{\sqrt{x^2 + y^2 + z^2 + 2Lz + L^2}} \right] \\ &= \frac{Q}{4\pi k} \left[\frac{1}{\sqrt{r^2 - 2Lz + L^2}} - \frac{1}{\sqrt{r^2 + 2Lz + L^2}} \right] \\ &= \frac{Q}{4\pi k r} \left[\frac{1}{\left(1 - \frac{2Lz}{r^2} + \frac{L^2}{r^2}\right)^{1/2}} - \frac{1}{\left(1 + \frac{2Lz}{r^2} - \frac{L^2}{r^2}\right)^{1/2}} \right] \\ &= \frac{Q}{4\pi k r} \left[\left(1 + \frac{1}{2} \left(\frac{2Lz}{r^2}\right) + \dots\right) - \left(1 - \frac{1}{2} \left(\frac{2Lz}{r^2}\right) + \dots\right) \right] \end{aligned}$$

$$= \left(\frac{Q}{4\pi k r} \right) \left(\frac{2Lz}{r^2} \right)$$

$$= \frac{(2QL)}{4\pi k} \left(\frac{z}{r^3} \right)$$

$$z = r \cos \theta$$

$$= \frac{(2QL)}{4\pi k} \left(\frac{\cos \theta}{r^2} \right)$$

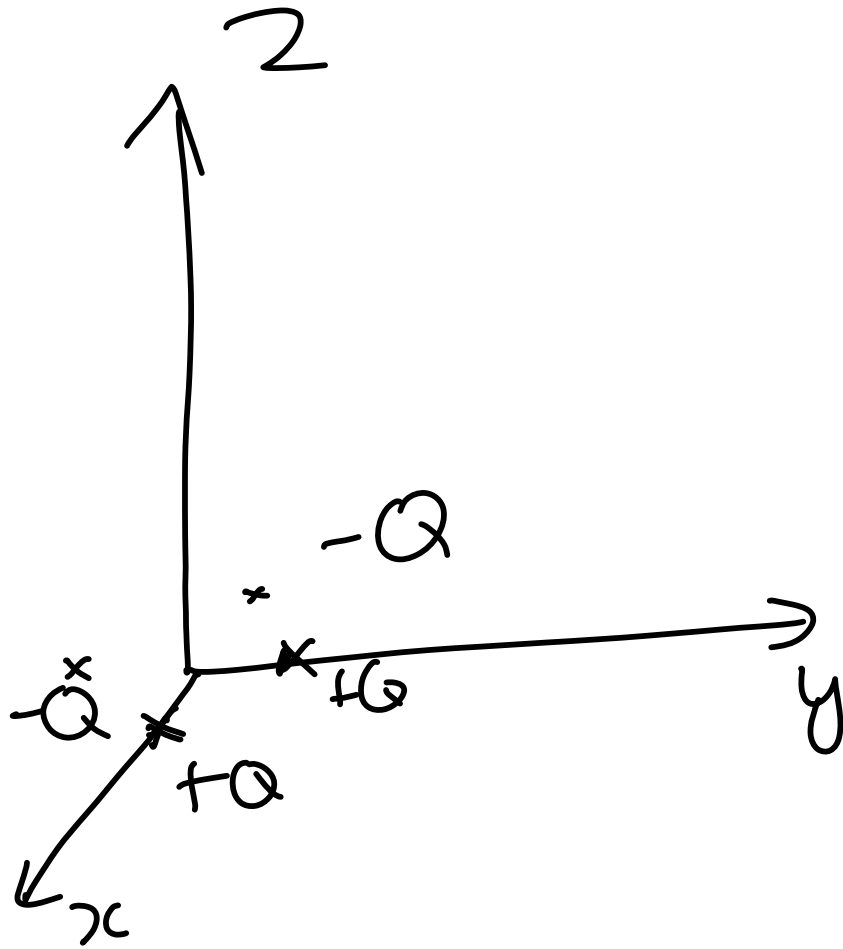
$$= \left(\frac{2QL}{4\pi k} \right) \frac{P_1^0(\cos \theta)}{r^2}$$

Spherical harmonic
 $n=1$ & $m=0$

$$T = \sum_{n=0}^{\infty} \sum_{m=-n}^n \left(A_{nm} r^n + \frac{B_{nm}}{r^{n+1}} \right) P_n^m(\cos \theta) \begin{pmatrix} \cos \\ \sin \end{pmatrix} (m\phi)$$

'Dipole'

$2QL$ = Dipole moment



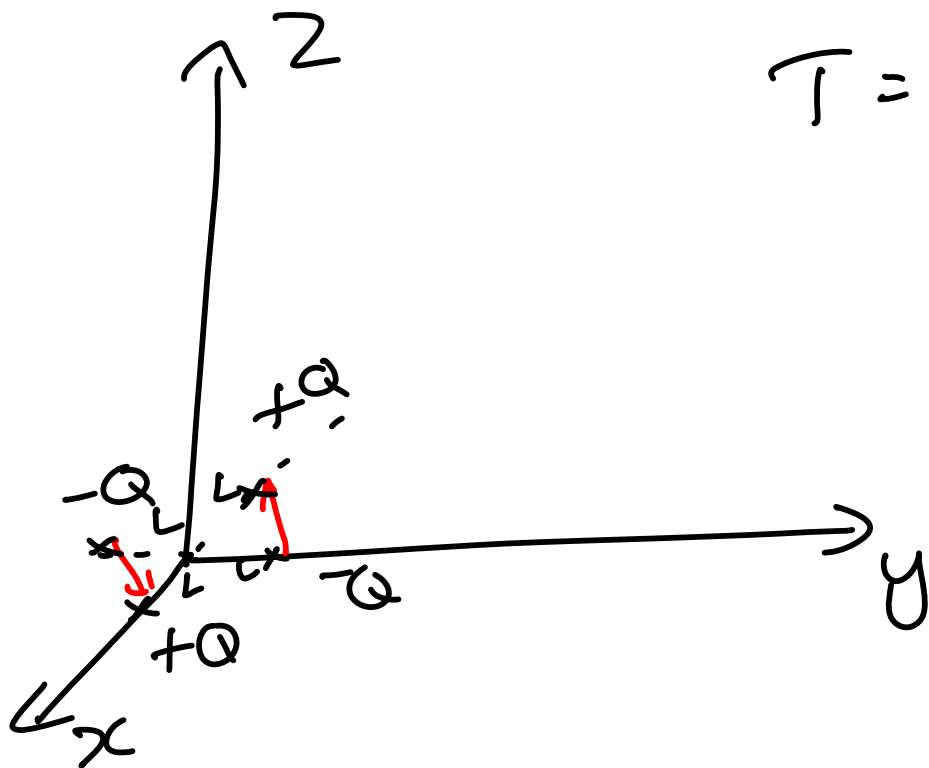
$$T = \frac{2QL}{4\pi k} \frac{\sin\theta \cos\phi}{r^2}$$
$$= \frac{2QL}{4\pi k} \frac{P_1(\cos\theta) \cos\phi}{r^2}$$

$$T = \frac{2QL}{4\pi k} \frac{\sin\theta \sin\phi}{r^2}$$

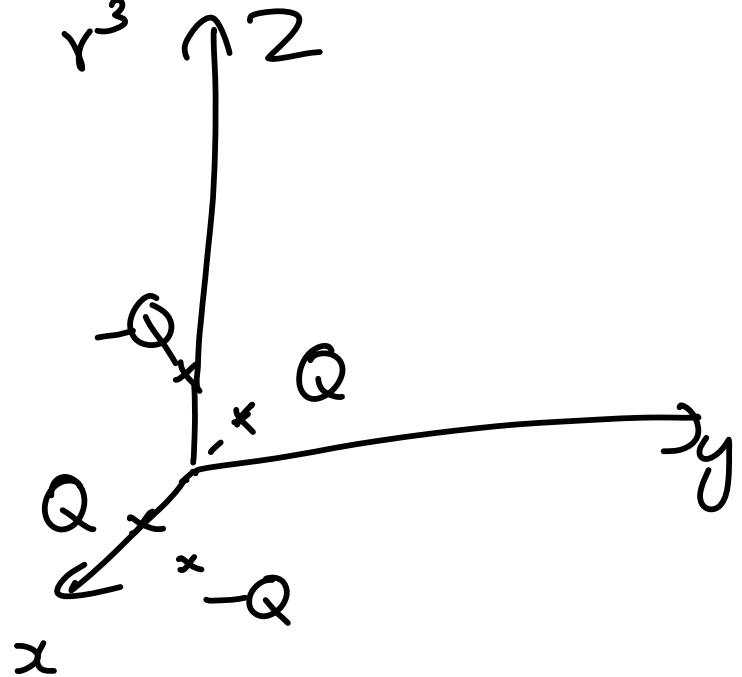
Quadrupole $n=2$

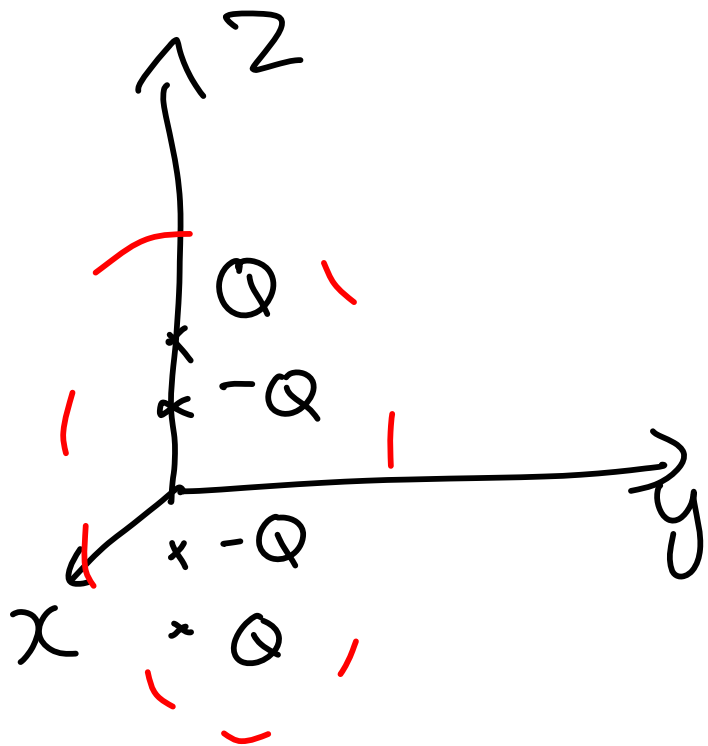
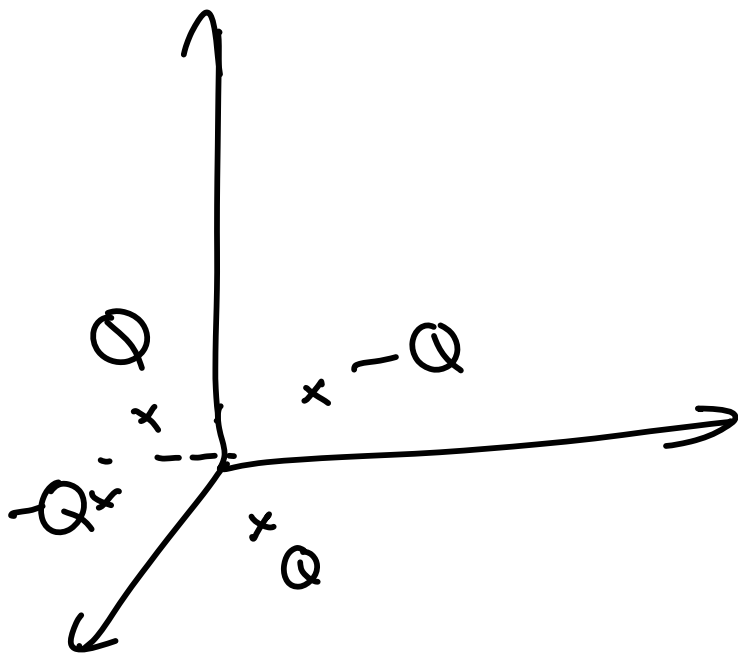
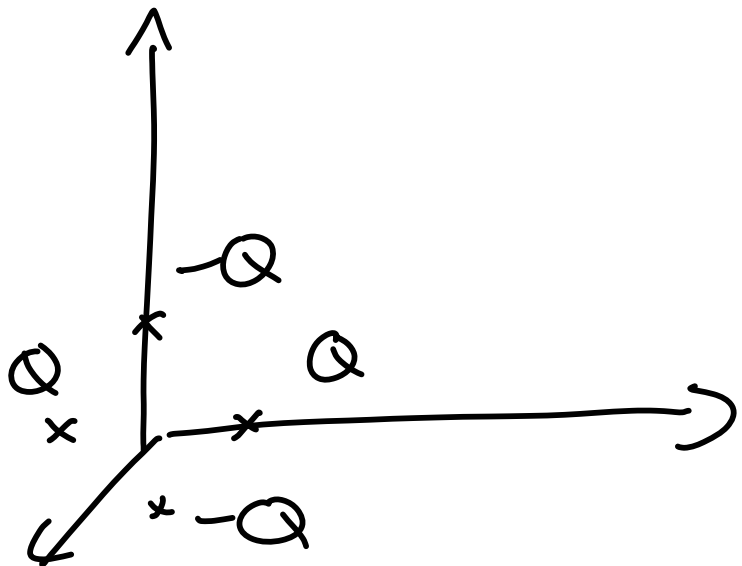
Two sources, two sinks of equal strength Q

Arranged so that net source is zero & net dipole is zero.



$$T = \frac{1}{r^3} P_2^m(\cos\theta) \sin(m\phi)$$



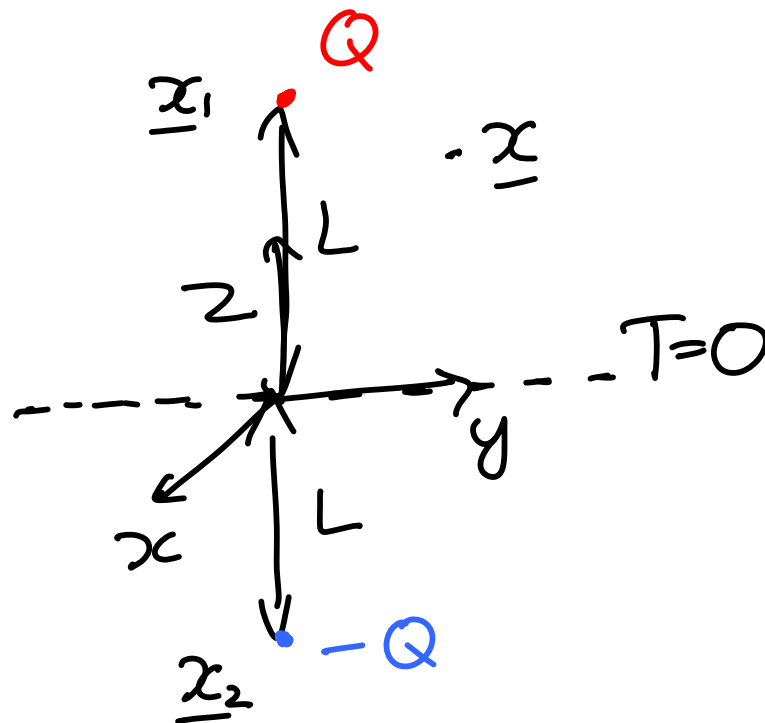
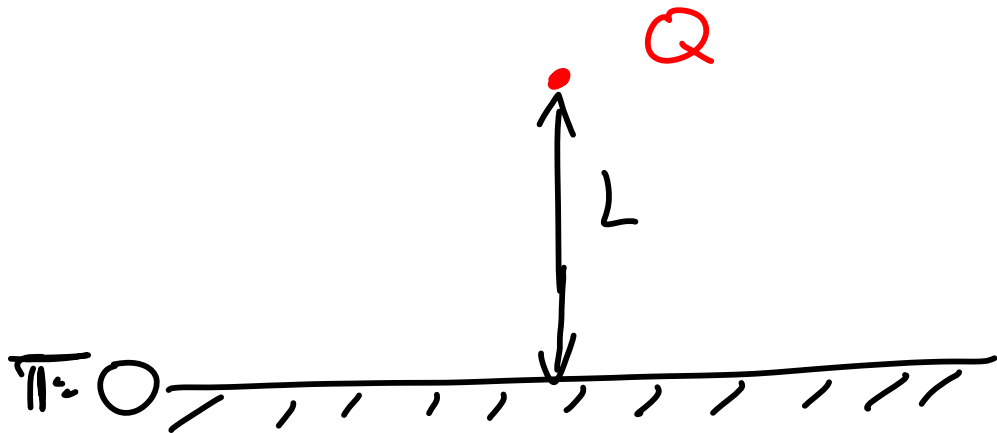
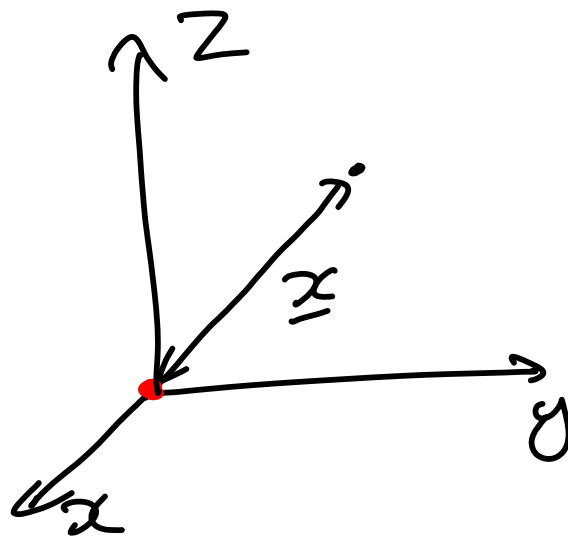


Green's function:

$$k \nabla^2 G(\underline{x}) = \delta(\underline{x})$$

$$G(\underline{x}) = \frac{1}{4\pi k |\underline{x}|}$$

$$= \frac{1}{4\pi k r}$$

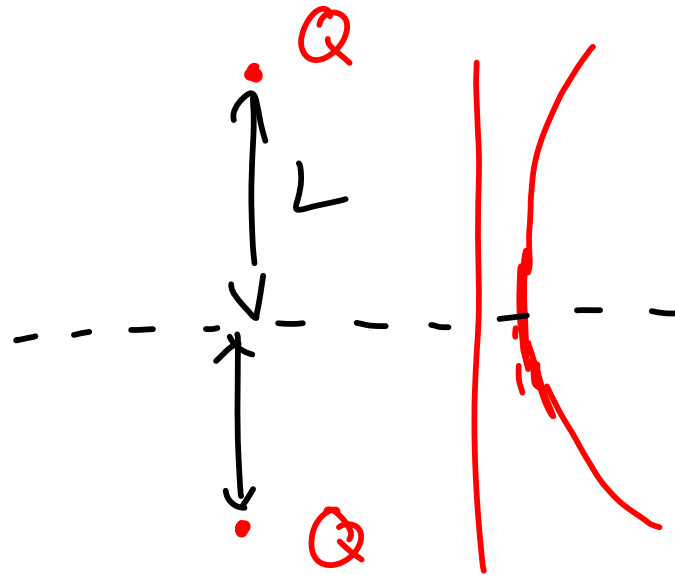
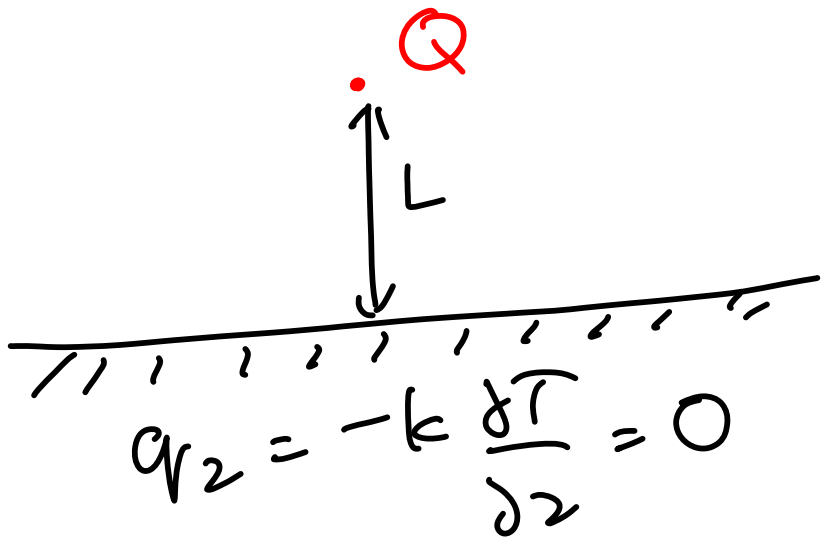


Source Q at $(x, y, z) = (0, 0, L)$

Sink $-Q$ at $(x, y, z) = (0, 0, -L)$

$$T(x) = \frac{Q}{4\pi k |z - z_1|} - \frac{Q}{4\pi k |z - z_2|}$$

$$= \frac{Q}{4\pi k \sqrt{x^2 + y^2 + (z - L)^2}} - \frac{Q}{4\pi k \sqrt{x^2 + y^2 + (z + L)^2}}$$



$$T = \frac{Q}{4\pi k |\underline{x} - \underline{x}_1|} + \frac{Q}{4\pi k |\underline{x} - \underline{x}_2|}$$

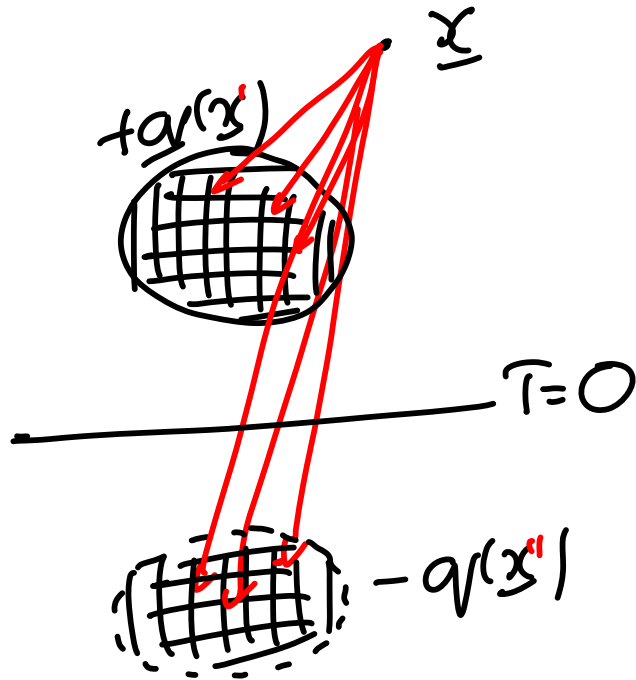
$$= \frac{Q}{4\pi k (x^2 + y^2 + (z-L)^2)^{1/2}} + \frac{Q}{4\pi k (x^2 + y^2 + (z+L)^2)^{1/2}}$$

Distributed source:

$$T(\underline{x}) = \frac{1}{4\pi k} \int dV' \frac{q(\underline{x}')}{|\underline{x} - \underline{x}'|}$$

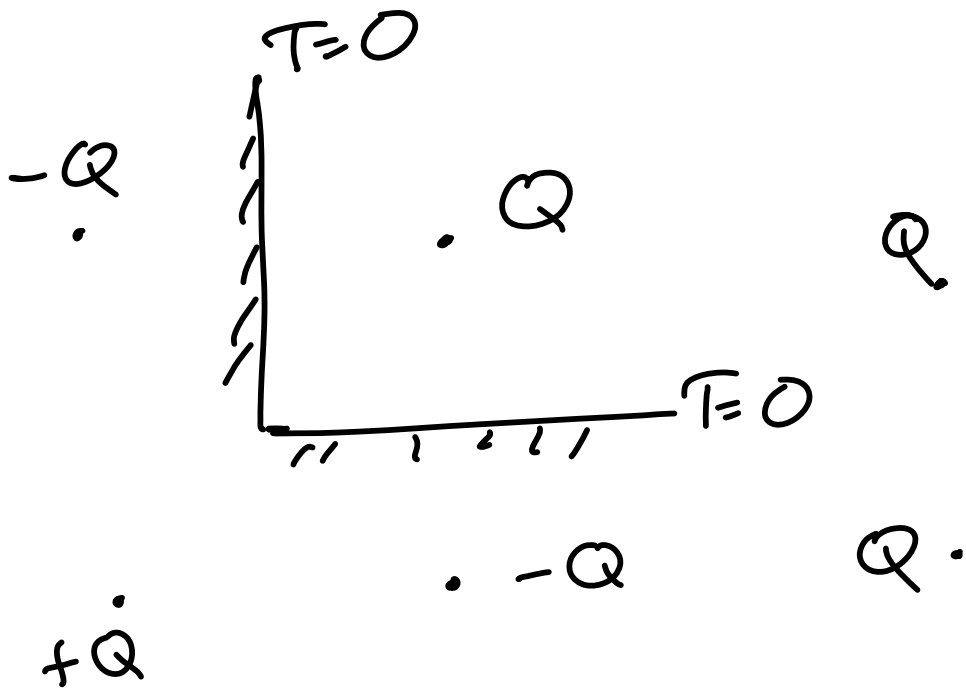
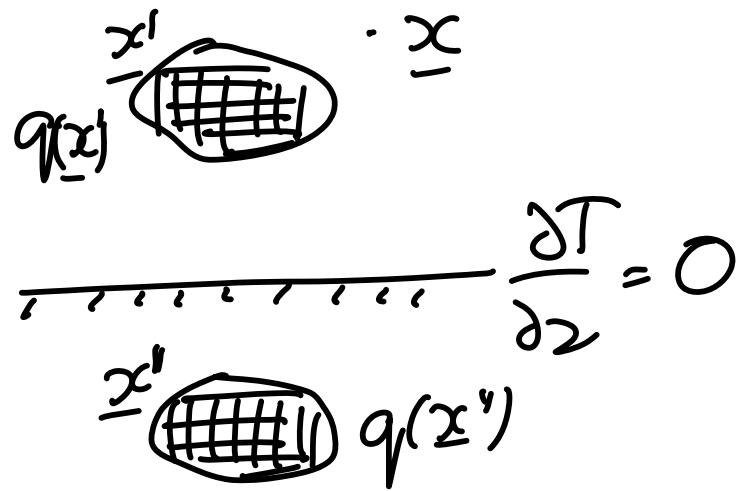
$$- \frac{1}{4\pi k} \int dV'' \frac{q(\underline{x}'')}{|\underline{x} - \underline{x}''|}$$

$$G(\underline{x}) = \frac{1}{4\pi k |\underline{x} - \underline{x}'|} - \frac{1}{4\pi k |\underline{x} - \underline{x}''|}$$

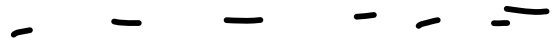


$$T(\underline{x}) = \frac{1}{4\pi k} \int dV' \frac{q(\underline{x}')}{|\underline{x} - \underline{x}'|}$$

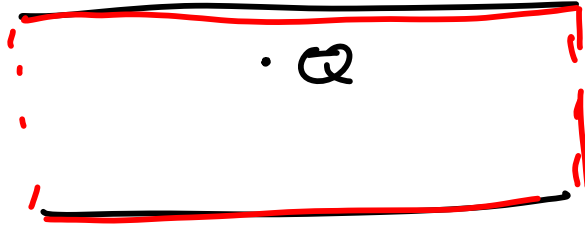
$$+ \frac{1}{4\pi k} \int dV'' \frac{q(\underline{x}'')}{|\underline{x} - \underline{x}''|}$$



• Q



• Q



• Q

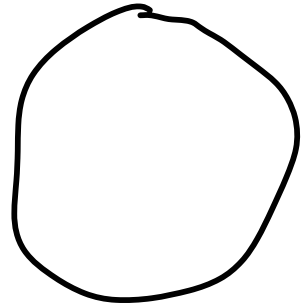


• Q



$$k \nabla^2 T = -q_f(\underline{x})$$

Subject to boundary conditions:



$$k \nabla^2 G = -\delta(\underline{x})$$

$$\nabla' = \underline{e}_x \frac{\partial}{\partial x'} + \underline{e}_y \frac{\partial}{\partial y'} + \underline{e}_z \frac{\partial}{\partial z'}$$

$$G(\underline{x}) = \frac{1}{4\pi k |\underline{x}|}$$

$$\int dV' \nabla' \cdot \left(T(\underline{x}') \nabla' (G(\underline{x} - \underline{x}')) - G(\underline{x} - \underline{x}') \nabla' T(\underline{x}') \right)$$

$$= \int dV' \left(T(\underline{x}') \nabla'^2 G(\underline{x} - \underline{x}') - G(\underline{x} - \underline{x}') \nabla'^2 T(\underline{x} - \underline{x}') \right)$$

$$= \int dV' T(\underline{x}') \left(\frac{1}{k} \delta(\underline{x} - \underline{x}') \right) - G(\underline{x} - \underline{x}') \frac{1}{k} q_f(\underline{x}')$$

$$= \frac{1}{k} T(\underline{x}) - \frac{1}{k} \int dV' G(\underline{x} - \underline{x}') q_f(\underline{x}')$$

$$\int dV' \nabla' \cdot (\mathbf{T}(\underline{x}') \nabla' G(\underline{x} - \underline{x}') - G(\underline{x} - \underline{x}') \nabla' \mathbf{T}(\underline{x}'))$$

$$= \int dS \mathbf{n}' \cdot (\mathbf{T}(\underline{x}') \nabla' G(\underline{x} - \underline{x}') - G(\underline{x} - \underline{x}') \nabla' \mathbf{T}(\underline{x}'))$$

$$\mathbf{T}(\underline{x}) = \int dV G(\underline{x} - \underline{x}') q(\underline{x}') + \int dS \mathbf{n}' \cdot (\mathbf{T}(\underline{x}') \nabla' (G(\underline{x} - \underline{x}')) - G(\underline{x} - \underline{x}') \nabla' \mathbf{T}(\underline{x}'))$$

'Boundary integral technique'

$$\frac{\partial c}{\partial t} + \nabla \cdot (\underline{u} c) = D \nabla^2 c + S$$

$$\underline{u}^* = \underline{u} / U \quad ; \quad \underline{x}^* = (\underline{x} / L) \quad t^* = (t D / L^2)$$

$$Pe \left(\frac{\partial c^*}{\partial t^*} + \nabla^* \cdot (\underline{u}^* c^*) \right) = \nabla^{*2} c^* + \frac{S}{(D/L^2)}$$

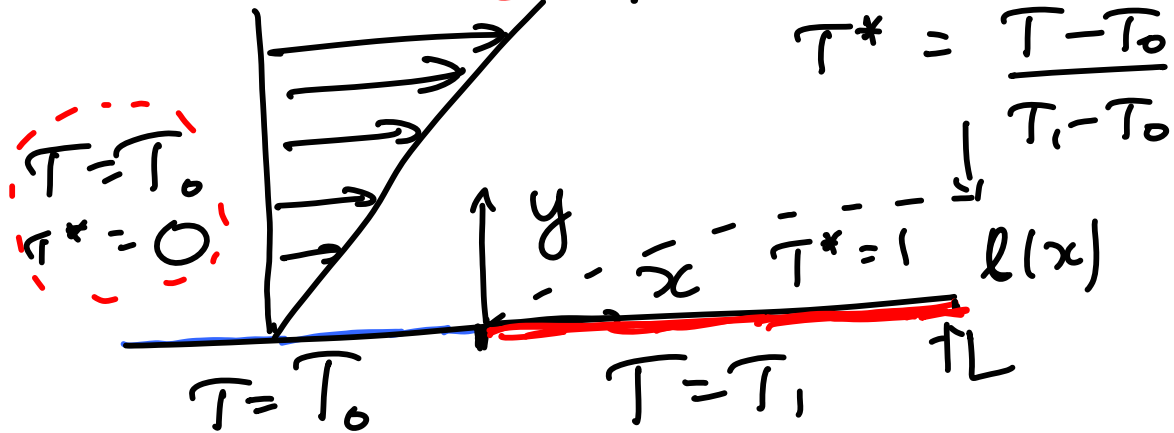
$$Pe = \left(\frac{UL}{D} \right)$$

$$\text{So far, } Pe \ll 1 \Rightarrow D \nabla^2 c + S = 0$$

$$Pe \gg 1 \quad \frac{\partial c}{\partial t} + \nabla \cdot (\underline{u} c) = 0$$

Flow past a flat plate:

$u_x = \dot{\gamma} y$ where $\dot{\gamma} = \text{Strain rate}$



$$\nabla \cdot (uT) = \alpha \nabla^2 T$$

Limit $Pe \gg 1$

$$Pe = \left(\frac{\dot{\gamma} L^2}{\alpha} \right)$$

u_x is independent of x

$$u_y = 0$$

$$u_x \frac{\partial T}{\partial x} = \alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$

$$\gamma y \frac{\partial T}{\partial x} = \alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$

Scale $x^* = (x/L)$, $y^* = (y/L)$

$$\left(\frac{\gamma L^2}{\alpha} \right) y^* \frac{\partial T}{\partial x^*} = \left(\frac{\partial^2 T}{\partial x^{*2}} + \frac{\partial^2 T}{\partial y^{*2}} \right)$$

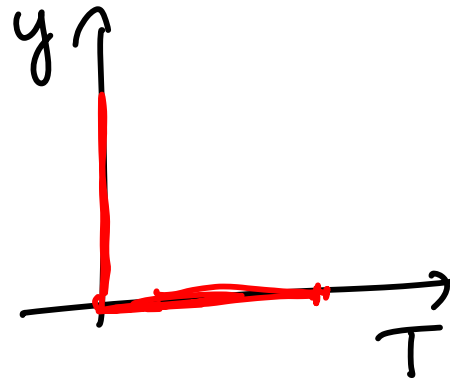
$$Pe y^* \frac{\partial T^*}{\partial x^*} = \frac{\partial^2 T^*}{\partial x^{*2}} + \frac{\partial^2 T^*}{\partial y^{*2}} \quad Pe \gg 1$$

Boundary conditions:

$$T^* = 1 \text{ at } y^* = 0 \text{ for } x^* > 0$$

$$T^* = 0 \text{ as } y^* \rightarrow \infty \text{ for } x^* = 0$$

$$T^* = 0 \text{ at } x^* = 0 \text{ for } y^* > 0$$



Naive approach:
Neglect diffusion

$$\frac{\partial T^*}{\partial x^*} = 0$$

Only solution $T^* = 0$ everywhere

$$y^* \frac{\partial T^*}{\partial x^*} = \frac{1}{Pe} \left(\frac{\partial^2 T^*}{\partial x^{*2}} + \frac{\partial^2 T^*}{\partial y^{*2}} \right)$$

$$x^* = (x/L) \quad y^* = (y/l) \quad T^* = \left(\frac{T - T_0}{T_1 - T_0} \right)$$

$$\rho y \frac{\partial T}{\partial x} = \alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$

$$\frac{\rho l y^*}{L} \frac{\partial T^*}{\partial x^*} = \alpha \left(\frac{1}{L^2} \frac{\partial^2 T^*}{\partial x^{*2}} + \frac{1}{l^2} \frac{\partial^2 T^*}{\partial y^{*2}} \right)$$

$$y^* \frac{\partial T^*}{\partial x^*} = \frac{\alpha L}{l \dot{\gamma}} \left(\frac{1}{l^2} \frac{\partial^2 T^*}{\partial y^{*2}} + \frac{1}{L^2} \frac{\partial^2 T^*}{\partial x^{*2}} \right)$$

$$= \frac{\alpha L}{l^3 \dot{\gamma}} \left(\frac{\partial^2 T^*}{\partial y^{*2}} + \frac{l^2}{L^2} \frac{\partial^2 T^*}{\partial x^{*2}} \right)$$

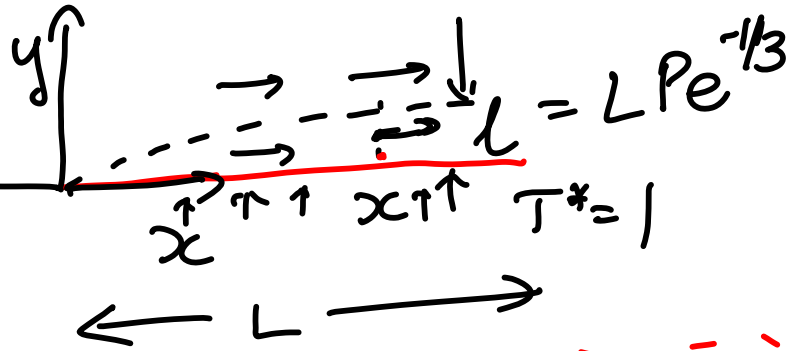
$$y^* \frac{\partial T^*}{\partial x^*} = \left(\frac{\alpha L}{l^3 \dot{\gamma}} \right) \left(\frac{\partial^2 T^*}{\partial y^{*2}} \right) \quad \text{Pe} = \left(\frac{\dot{\gamma} L^2}{\alpha} \right)$$

$$\frac{l^3 \dot{\gamma}}{\alpha L} = 1 \quad \Rightarrow \quad \left(\frac{l}{L} \right)^3 = \left(\frac{\alpha}{\dot{\gamma} L^2} \right) = \text{Pe}^{-1}$$

$$\frac{l}{L} = \text{Pe}^{-1/3}$$

$$\dot{\gamma} y \frac{\partial T^*}{\partial x} = \alpha \frac{\partial^2 T^*}{\partial y^2}$$

$$T^* = 0$$



$$\frac{l}{L} = Pe_L^{-1/3}$$

$$\frac{l(x)}{x} = Pe_x^{-1/3} = \left(\frac{\alpha}{\dot{\gamma} x^2} \right)^{1/3}$$

$$\eta = y/l(x) = y / \left(\frac{\alpha x}{\dot{\gamma}} \right)^{1/3}$$

$$l(x) = \left(\frac{\alpha x}{\dot{\gamma}} \right)^{1/3}$$

$$\eta = y / \left(\frac{\alpha x}{\dot{\gamma}} \right)^{1/3}$$

$$\ddot{y} \frac{\partial T^*}{\partial x} = \alpha \frac{\partial^2 T^*}{\partial y^2}$$

$$\frac{\partial T}{\partial y} = \frac{\partial T}{\partial \eta} \frac{\partial \eta}{\partial y} = \frac{1}{(\alpha x / \dot{y})^{1/3}} \frac{\partial T}{\partial \eta}$$

$$\frac{\partial^2 T}{\partial y^2} = \frac{1}{(\alpha x / \dot{y})^{2/3}} \frac{\partial^2 T}{\partial \eta^2}$$

$$\frac{\partial T}{\partial x} = \frac{\partial T}{\partial \eta} \frac{\partial \eta}{\partial x} = \frac{-y}{3x (\alpha x / \dot{y})^{1/3}} \frac{\partial T}{\partial \eta}$$

$$\ddot{y} \left(\frac{-y}{3x (\alpha x / \dot{y})^{1/3}} \right) \frac{\partial T}{\partial \eta} = \frac{\alpha}{(\alpha x / \dot{y})^{2/3}} \frac{\partial^2 T}{\partial \eta^2}$$

$$y = \eta \left(\frac{\alpha x}{\dot{y}} \right)^{1/3}$$

$$\frac{-\dot{\gamma} \eta^2 \left(\frac{\alpha x}{\dot{\gamma}}\right)^{2/3}}{3\alpha (\alpha x / \dot{\gamma})^{1/3}} \frac{\partial T}{\partial \eta} = \frac{\alpha}{(\alpha x / \dot{\gamma})^{2/3}} \frac{\partial T}{\partial \eta^2}$$

$$-\eta^2 \frac{\partial T}{\partial \eta} = \frac{\partial^2 T}{\partial \eta^2}$$

$$\eta = \left(\frac{\alpha x}{\dot{\gamma}}\right)^{1/3}$$

At $y=0$, $T^*=1 \Rightarrow \eta=0$

As $y \rightarrow \infty$, $T^*=0 \Rightarrow \eta \rightarrow \infty$

At $x=0$ for $y > 0$, $T^*=0 \Rightarrow \eta \rightarrow \infty$

$$-\eta^2 \frac{\partial T^*}{\partial \eta} = \frac{\partial^2 T^*}{\partial \eta^2}$$

$$\frac{\partial T^*}{\partial \eta} = C_1 \exp(-\eta^3/3)$$

$$T^* = C_1 \int_0^\eta d\eta' \exp(-\eta'^3/3) + C_2$$

$$T^* = 0 \text{ as } \eta \rightarrow \infty \text{ \& } T^* = 1 \text{ at } \eta = 0$$

$$T^* = \left[1 - \frac{\int_0^\eta d\eta' e^{(-\eta'^3/3)}}{\int_0^\infty d\eta' e^{-\eta'^3/3}} \right]$$

$$\text{where } \eta = y / (\alpha x / \dot{\gamma})^{1/3}$$

Heat flux

$$q_y = -k \left. \frac{\partial T}{\partial y} \right|_{y=0} = \frac{-k}{(\alpha x / \dot{\gamma})^{1/3}} \left. \frac{\partial T}{\partial \eta} \right|_{\eta=0}$$

$$= \frac{-k}{(\alpha x / \delta)^{1/3}} \left[-\frac{1}{\int_0^\infty d\eta' e^{-\eta'^{3/3}} \right] (T_1 - T_0)$$

$$q_y = \frac{k (T_1 - T_0)}{(\alpha x / \delta)^{1/3}} \frac{3^{2/3}}{\Gamma(1/3)} \int_0^\infty d\eta' e^{-\eta'^{3/3}} = \frac{\Gamma(1/3)}{3^{2/3}}$$

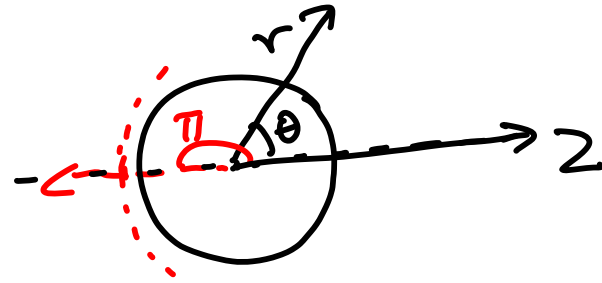
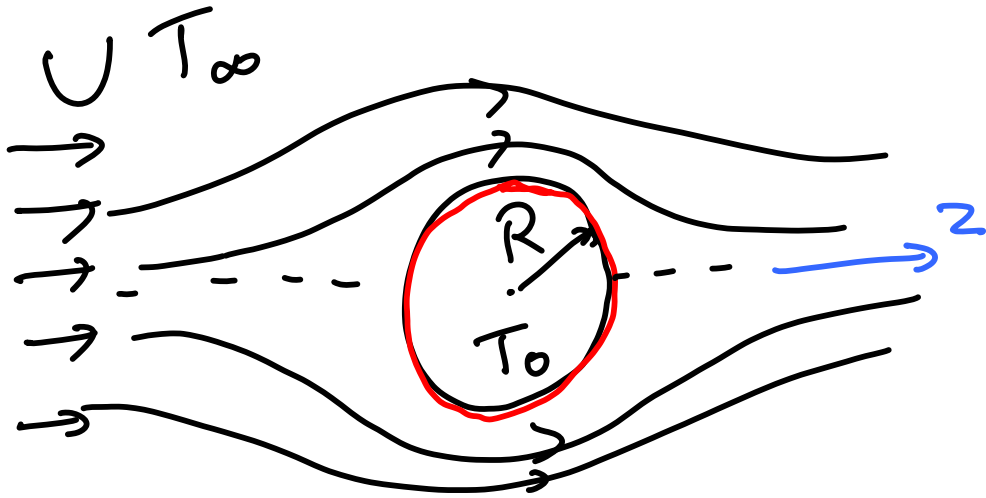
$$Q = \int_0^L dx q_y = \frac{k (T_1 - T_0)}{(\alpha / \delta)^{1/3}} \frac{3^{2/3}}{\Gamma(1/3)} \int_0^L \frac{dx}{x^{1/3}}$$

$$= \frac{k (T_1 - T_0)}{(\alpha / \delta)^{1/3}} \frac{3^{2/3}}{\Gamma(1/3)} \left[\frac{3}{2} L^{2/3} \right]$$

$$= \frac{3^{5/3}}{2 \Gamma(1/3)} \frac{k (T_1 - T_0)}{(\alpha / \delta L^2)^{1/3}}$$

$$Nu = \frac{2Q}{k (T_1 - T_0)} = \frac{3^{5/3}}{\Gamma(1/3)} Pe_L^{1/3} = \frac{3^{5/3}}{\Gamma(1/3)} Re^{1/3} Pr^{1/3}$$

Heat transfer from a spherical particle:



$$u_r = U \cos \theta \left(1 - \frac{3R}{2r} + \frac{R^3}{2r^3} \right)$$

$$u_\theta = -U \sin \theta \left(1 - \frac{3R}{4r} - \frac{R^3}{4r^3} \right)$$

$$T^* = \frac{T - T_\infty}{T_0 - T_\infty}$$

$$r^* = \frac{r}{R}$$

$$u_r^* = u_r / U$$

$$u_\theta^* = u_\theta / U$$

Boundary conditions:

At $r^* = 1$, $T^* = 1$

As $r^* \rightarrow \infty$, $T^* = 0$

$$u_r^* = \cos \theta \left(1 - \frac{3}{2r^*} + \frac{1}{2r^{*3}} \right)$$

$$u_\theta^* = -\sin \theta \left(1 - \frac{3}{4r^*} - \frac{1}{4r^{*3}} \right)$$

$$\nabla \cdot (\underline{u} T) = \alpha \nabla^2 T$$

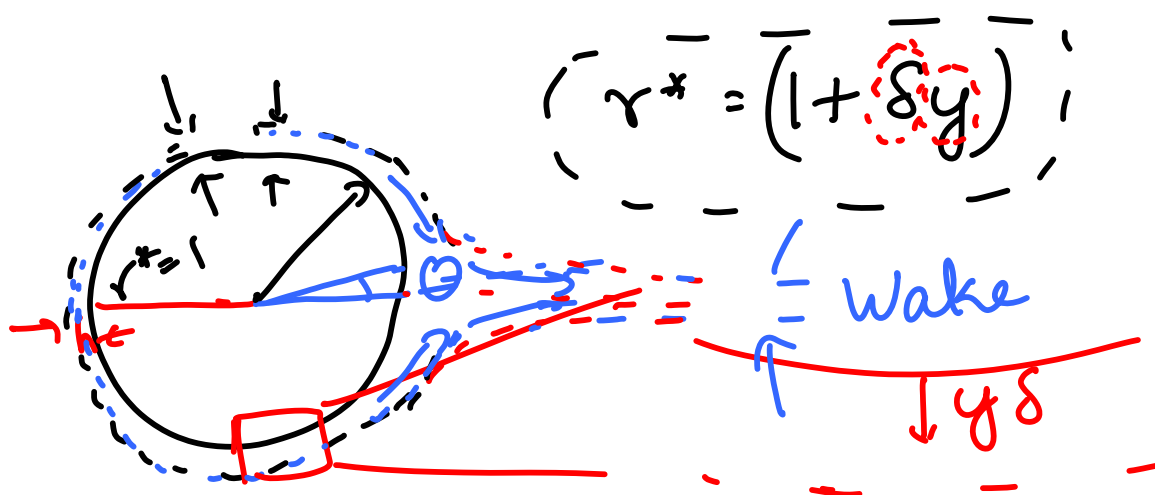
$$Pe \left(u_r^* \frac{\partial T^*}{\partial r^*} + \frac{u_\theta^*}{r^*} \frac{\partial T^*}{\partial \theta} \right) = \left(\frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial T^*}{\partial r^*} \right) \right) + \frac{1}{r^{*2} \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T^*}{\partial \theta} \right)$$

$$Pe = \left(\frac{UR}{\alpha} \right)$$

Limit $Pe \gg 1$

$$u_r^* \frac{\partial T^*}{\partial r^*} + \frac{u_\theta^*}{r^*} \frac{\partial T^*}{\partial \theta} = 0$$

$$\underline{u}^* \cdot \nabla^* T^* = 0$$



$$\begin{aligned}
 u_r^* &= \cos \theta \left(1 - \frac{3}{2r^*} + \frac{1}{2r^{*3}} \right) \\
 &= \cos \theta \left(1 - \frac{3}{2(1+\delta y)} + \frac{1}{2(1+\delta y)^3} \right) \\
 &= \cos \theta \left(1 - \frac{3}{2}(1+\delta y)^{-1} + \frac{1}{2}(1+\delta y)^{-3} \right) \\
 &= \cos \theta \left(1 - \frac{3}{2} + \frac{3}{2}\delta y - \frac{3}{2}(\delta y)^2 + \frac{1}{2} - \frac{3}{2}\delta y + 3(\delta y)^2 \right) \\
 &\approx \cos \theta \frac{3}{2} \delta^2 y^2
 \end{aligned}$$

$$u_{\theta}^* = -\sin \theta \left[1 - \frac{3}{4r^*} - \frac{1}{4r^{*3}} \right]$$

$$= -\sin \theta \left[1 - \frac{3}{4(1+\delta y)} - \frac{1}{4(1+\delta y)^3} \right]$$

$$= -\sin \theta \left[1 - \frac{3}{4} + \frac{3}{4}(\delta y) - \frac{1}{4} + \frac{3}{4}\delta y \right]$$

$$= -\sin \theta \frac{3}{2} \delta y$$

$$P_e \left[u_r^* \frac{\partial T^*}{\partial r^*} + \frac{u_{\theta}^*}{r^*} \frac{\partial T^*}{\partial \theta^*} \right] = \left[\frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial T^*}{\partial r^*} \right) + \frac{1}{r^{*2} \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T^*}{\partial \theta} \right) \right]$$

$$P_e \left[\frac{3}{2} \delta^2 y^2 \cos \theta \frac{1}{8} \frac{\partial T}{\partial y} - \frac{3}{2} \frac{\delta y \sin \theta}{(1+\delta y)} \frac{\partial T}{\partial \theta} \right]$$

$$= \left(\frac{1}{(1+\delta y)^2} \frac{1}{\delta} \frac{\partial}{\partial y} \left((1+\delta y)^2 \frac{1}{\delta} \frac{\partial T^*}{\partial y} \right) + \frac{1}{(1+\delta y)^2} \sin \theta \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T^*}{\partial \theta} \right) \right)$$

$$Pe \frac{3}{2} \left[\delta y^2 \cos \theta \frac{\partial T^*}{\partial y} - \delta y \sin \theta \frac{\partial T^*}{\partial \theta} \right] = \frac{1}{\delta^2} \frac{\partial^2 T^*}{\partial y^2} + \frac{1}{\sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T^*}{\partial \theta} \right)$$

$$Pe \delta^3 \frac{3}{2} \left[y^2 \cos \theta \frac{\partial T^*}{\partial y} - y \sin \theta \frac{\partial T^*}{\partial \theta} \right] = \frac{\partial^2 T^*}{\partial y^2}$$

$$\frac{3}{2} \left[y^2 \cos \theta \frac{\partial T^*}{\partial y} - y \sin \theta \frac{\partial T^*}{\partial \theta} \right] = \frac{\partial^2 T^*}{\partial y^2}$$

$$\delta = Pe^{-1/3}$$

$$\eta = \frac{y}{h(\theta)}$$

$$\frac{\partial T^*}{\partial y} = \frac{\partial T^*}{\partial \eta} \frac{\partial \eta}{\partial y} = \frac{1}{h(\theta)} \frac{\partial T^*}{\partial \eta}$$

$$\frac{\partial^2 T^*}{\partial y^2} = \frac{1}{h^2} \frac{\partial^2 T^*}{\partial \eta^2}$$

$$\begin{aligned} \frac{\partial T^*}{\partial \theta} &= \frac{\partial T^*}{\partial \eta} \frac{\partial \eta}{\partial \theta} = \left(\frac{\partial T^*}{\partial \eta} \right) \left(-\frac{y}{h^2} \frac{dh}{d\theta} \right) \\ &= \left(\frac{\partial T^*}{\partial \eta} \right) \left(-\frac{\eta}{h} \frac{dh}{d\theta} \right) \end{aligned}$$

$$\frac{3}{2} \left[y^2 \cos \theta \frac{1}{h(\theta)} \frac{dT^*}{d\eta} - y \sin \theta \left(\frac{-\eta}{h} \frac{dh}{d\theta} \right) \frac{dT^*}{d\eta} \right]$$

$$= \frac{1}{h^2} \frac{d^2 T^*}{d\eta^2}$$

$$\eta^2 \frac{dT^*}{d\eta} \left[\frac{3}{2} \left(h^3 \cos \theta + h^2 \sin \theta \frac{dh}{d\theta} \right) \right] = \frac{d^2 T^*}{d\eta^2}$$

$$h^3 \cot \theta + h^2 \sin \theta \frac{dh}{d\theta} = -2$$

$$\frac{dT^*}{d\eta^2} - 3\eta^2 \frac{dT^*}{d\eta} = 0$$

$$\frac{dT^*}{d\eta} = C_1 e^{-\eta^3}$$

$$T^* = C_1 \int_0^\eta dn' e^{-\eta'^3} + C_2$$

$$T^* = 0 \text{ as } y \rightarrow \infty \Rightarrow \eta \rightarrow \infty$$

$$T^* = 1 \text{ at } y = 0 \Rightarrow \eta = 0$$

$$T^* = \left[1 - \frac{\int_0^\eta dn' e^{-\eta'^3}}{\int_0^\infty dn' e^{-\eta'^3}} \right]$$

$$\frac{dT^*}{d\eta} =$$

$$\frac{1}{\int_0^\infty dn' e^{-\eta'^3}}$$

$$h^3 \cos \theta + h^2 \sin \theta \frac{dh}{d\theta} = -2$$

$$\frac{\sin \theta}{3} \frac{d(h^3)}{d\theta} + h^3 \cos \theta = -2$$

$$x = \cos \theta \quad dx = -\sin \theta d\theta$$

$$-\frac{\sin^2 \theta}{3} \frac{d(h^3)}{dx} + h^3 x = -2$$

$$-\frac{(1-x^2)}{3} \frac{d(h^3)}{dx} + h^3 x = -2$$

$$h^3 = g(x) + p(x)$$

$$\frac{(1-x^2)}{3} \frac{dg}{dx} - xg = 0$$

$$\frac{dg}{dx} = \frac{3xg}{1-x^2} \Rightarrow g = \frac{1}{(1-x^2)^{3/2}}$$

$$p(x) = g(x)q(x)$$

$$\frac{(1-x^2)}{3} \frac{d}{dx} (g(x)q(x)) - xg(x)q(x) = 2$$

$$\frac{(1-x^2)}{3} g(x) \frac{dq}{dx} = 2$$

$$\frac{dq}{dx} = \frac{6}{(1-x^2)g(x)}$$

$$q(x) = \int_{-1}^x dx' \frac{6}{(1-x'^2)g(x')} = \int_{-1}^x dx' 6(1-x'^2)^{1/2}$$

$$h^3 = \frac{C}{(1-x^2)^{3/2}} + \frac{6}{(1-x^2)^{3/2}} \int_{-1}^x dx' (1-x'^2)^{1/2}$$

$$x = \cos \theta$$

$$h^3 = \left[\frac{6}{(1-x^2)^{3/2}} \int_{-1}^x dx' (1-x'^2)^{1/2} \right]$$

$$q_v|_{r=1} = -k \left. \frac{\partial T}{\partial r} \right|_{r=1}$$

$$= \frac{-k(T_0 - T_\infty)}{R} \left. \frac{\partial T^*}{\partial r^*} \right|_{r^*=1}$$

$$= \frac{-k(T_0 - T_\infty)}{R} \frac{1}{\delta} \left. \frac{\partial T^*}{\partial y} \right|_{y=0}$$

$$= \frac{-k(T_0 - T_\infty)}{R \delta h(\theta)} \left. \frac{\partial T^*}{\partial \eta} \right|_{\eta=0}$$

$$= \frac{-k(T_0 - T_\infty)}{R \delta h(\theta)} \left[\frac{1}{\int_0^\infty d\eta' e^{-\eta'^3}} \right]$$

$$\eta = \frac{y}{h(\theta)}$$

$$= \frac{k(T_0 - T_\infty)}{R \delta h(\theta)} \left[\frac{1}{\int_0^\infty d\eta' e^{-\eta'^3}} \right]$$

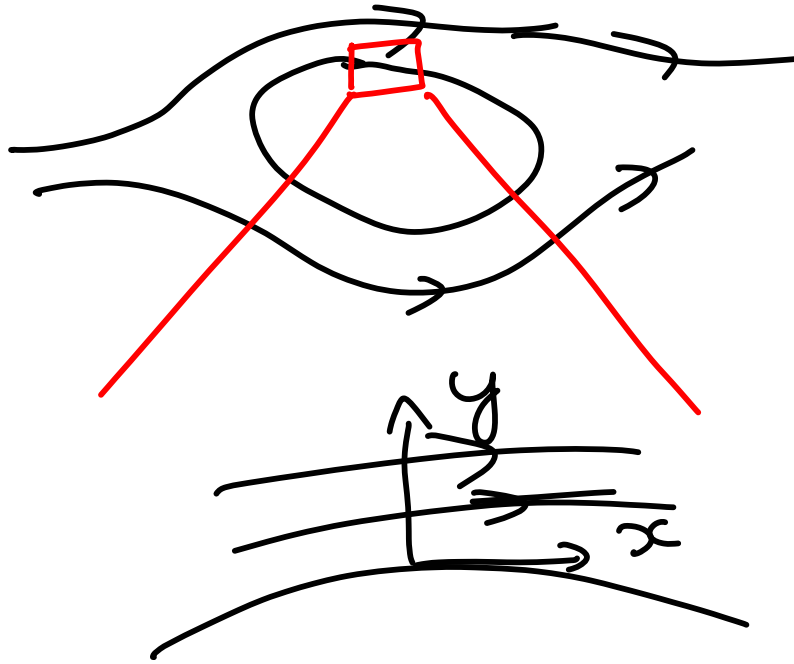
$$Q = \int_0^{2\pi} \int_0^\pi R^2 \sin\theta d\theta d\phi q_r(\theta, \phi)$$

$$= 2\pi R^2 \int_0^\pi \sin\theta d\theta q_r(\theta, \phi)$$

$$= (2\pi R^2) \frac{k(T_0 - T_\infty)}{R \delta \int_0^\infty d\eta' e^{-\eta'^3}} \int_0^\pi \sin\theta d\theta \left(\frac{1}{h(\theta)} \right)$$

$$= 1.2491 (2\pi R k (T_0 - T_\infty) Pe^{1/3})$$

$$Nu = \frac{2Q}{(4\pi R^2) k (T_0 - T_\infty) / R} = 1.2491 Pe^{1/3}$$



$u_x = 0$ at the surface
 $= y A(x)$ near the surface

Slip at surface

$$u_x = U$$

$$u_y \sim U \delta y$$

For an incompressible flow, velocity components satisfy

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0 \quad \nabla \cdot \underline{u} = 0$$

$$\frac{\partial u_y}{\partial y} = -\frac{\partial u_x}{\partial x} = -y \frac{dA}{dx}$$

$$u_y = -\frac{y^2}{2} \frac{dA}{dx}$$

$u_0 \sim \delta y$
 $u_x \sim (\delta y)^2$

$$u_x \frac{\partial T}{\partial x} + u_y \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2}$$

$$\frac{\partial T}{\partial x} (Ay) - \frac{y^2}{2} \frac{dA}{dx} \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2}$$

$$y^* = (y/\delta), \quad x^* = (x/L)$$

$$\frac{Ay^* \delta}{L} \frac{\partial T}{\partial x^*} - \frac{y^{*2} \delta}{2L} \frac{dA}{dx^*} \frac{\partial T}{\partial y^*} = \frac{\alpha}{\delta^2} \frac{\partial^2 T}{\partial y^{*2}}$$

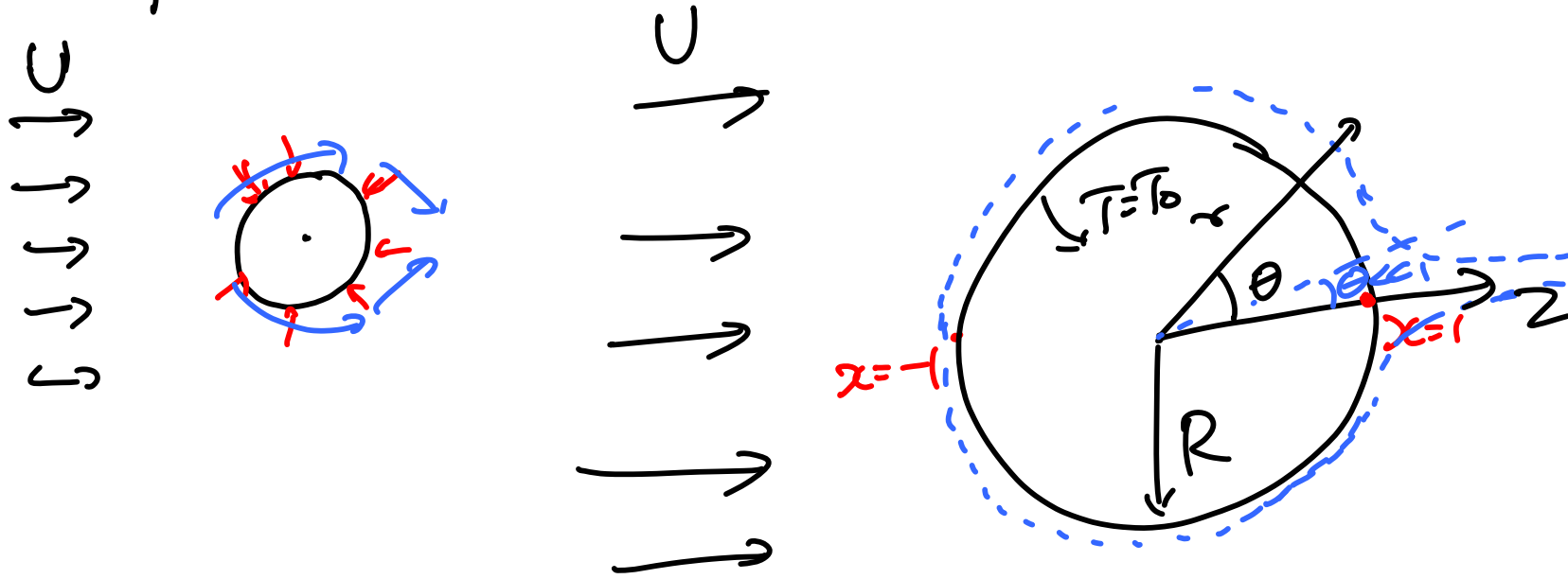
$$\left(\frac{\delta^3 A}{L \alpha} \right) \left(y^* \frac{\partial T}{\partial x^*} - \frac{y^{*2}}{2} \frac{1}{A} \frac{dA}{dx^*} \frac{\partial T}{\partial y^*} \right) = \frac{\partial^2 T}{\partial y^{*2}}$$

$$\frac{\delta}{L} \sim Pe^{-1/3} \sim \left(\frac{\alpha}{AL^2}\right)^{1/3} \quad \frac{\delta}{L} \sim Pe^{-1/2}$$

$$Nu \sim Pe^{1/3}$$

$$\eta = \left(\frac{\mu}{g(x)}\right)$$

Diffusion from a gas bubble: $T = T_\infty$ as $r \rightarrow \infty$



$$u_r = U \cos \theta \left(1 - \frac{R}{r}\right)$$

$$u_\theta = -U \sin \theta \left(1 - \frac{R}{2r}\right)$$

$$u_r \frac{\partial T}{\partial r} + \frac{u_\theta}{r} \frac{\partial T}{\partial \theta} = \alpha \left(\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T}{\partial \theta} \right) \right)$$

$$u_r^* = \frac{u_r}{U} \quad T^* = \frac{T - T_\infty}{T_0 - T_\infty} \quad r^* = \frac{r}{R}$$

$$Pe \left(u_r^* \frac{\partial T^*}{\partial r^*} + \frac{u_\theta^*}{r^*} \frac{\partial T^*}{\partial \theta} \right) = \frac{1}{r^{*2}} \frac{\partial}{\partial r^*} \left(r^{*2} \frac{\partial T^*}{\partial r^*} \right) + \frac{1}{r^{*2} \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T^*}{\partial \theta} \right)$$

$$\text{where } Pe = \left(\frac{UR}{\alpha} \right)$$

$$r^* = 1 + \delta y$$

$$u_r^* = \left(1 - \frac{1}{r^*} \right) \cos \theta = \left(1 - \frac{1}{1 + \delta y} \right) \cos \theta = \delta y \cos \theta$$

$$u_\theta^* = - \left(1 - \frac{1}{2r^*} \right) \sin \theta = - \left(1 - \frac{1}{2(1 + \delta y)} \right) \sin \theta = -\frac{1}{2} \sin \theta$$

$$Pe \left(\delta y \cos \theta \frac{1}{\delta} \frac{\partial T^*}{\partial y} + \frac{\left(-\frac{1}{2} \sin \theta\right)}{(1+\delta y)} \frac{\partial T^*}{\partial \theta} \right)$$

$$= \frac{1}{(1+\delta y)^2} \frac{1}{\delta} \frac{\partial}{\partial y} \left((1+\delta y)^2 \frac{1}{\delta} \frac{\partial T^*}{\partial y} \right) + \frac{1}{(1+\delta y)^2} \frac{1}{\sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T^*}{\partial \theta} \right)$$

$$Pe \left[y \cos \theta \frac{\partial T^*}{\partial y} - \frac{1}{2} \sin \theta \frac{\partial T^*}{\partial \theta} \right] = \left[\frac{1}{\delta^2} \frac{\partial^2 T^*}{\partial y^2} + \frac{1}{\sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T^*}{\partial \theta} \right) \right]$$

$$(Pe \delta^2) \left[y \cos \theta \frac{\partial T^*}{\partial y} - \frac{1}{2} \sin \theta \frac{\partial T^*}{\partial \theta} \right] = \frac{\partial^2 T^*}{\partial y^2}$$

$$Pe \delta^2 = 1 \implies \delta = Pe^{-1/2}$$

$$y \cos \theta \frac{\partial T^*}{\partial y} - \frac{1}{2} \sin \theta \frac{\partial T^*}{\partial \theta} = \frac{\partial^2 T}{\partial y^2}$$

$$\eta = \frac{y}{h(\theta)} \quad \frac{\partial T^*}{\partial y} = \frac{1}{h} \frac{\partial T^*}{\partial \eta}$$

$$\frac{\partial^2 T^*}{\partial y^2} = \frac{1}{h^2} \frac{\partial^2 T^*}{\partial \eta^2}$$

$$\begin{aligned} \frac{\partial T^*}{\partial \theta} &= -\frac{y}{h^2} \frac{dh}{d\theta} \frac{\partial T^*}{\partial \eta} \\ &= -\frac{\eta}{h} \frac{dh}{d\theta} \frac{\partial T^*}{\partial \eta} \end{aligned}$$

$$\frac{y \cos \theta}{h} \frac{\partial T^*}{\partial \eta} + \frac{1}{2} \sin \theta \frac{\eta}{h} \frac{dh}{d\theta} \frac{\partial T^*}{\partial \eta} = \frac{1}{h^2} \frac{\partial^2 T^*}{\partial \eta^2}$$

$$\eta \frac{\partial T^*}{\partial \eta} \left(h^2 \cos \theta + \frac{1}{2} h \frac{dh}{d\theta} \sin \theta \right) = \frac{\partial^2 T^*}{\partial \eta^2}$$

$$h^2 \cos \theta + \frac{1}{2} h \frac{dh}{d\theta} \sin \theta = -2$$

$$\frac{\partial^2 T^*}{\partial \eta^2} + 2\eta \frac{\partial T^*}{\partial \eta} = 0$$

Boundary conditions:

$$\text{At } r^* = 1, \quad y = 0, \quad T^* = 1$$

$$\text{As } r^* \rightarrow \infty \quad (y \rightarrow \infty) \quad T^* = 0$$

$$T^* = \left[1 - \frac{\int_0^\eta dn' e^{-\eta'^2}}{\int_0^\infty dn' e^{-\eta'^2}} \right] \parallel \parallel$$

$$h^2 \cos \theta + \frac{1}{2} h \frac{dh}{d\theta} \sin \theta = -2$$

$$\cos \theta = x \Rightarrow dx = -\sin \theta d\theta$$

$$h^2 x - \frac{1}{4} (1-x^2) \frac{dh^2}{dx} = -2$$

$$\frac{(1-x^2)}{4} \frac{d(h^2)}{dx} - h^2 x = 2$$

$$h^2 = h_g^2 f$$

$$\frac{(1-x^2)}{4} \frac{d(h_g^2)}{dx} - h_g^2 x = 0$$

$$h_g^2 = \frac{C}{(1-x^2)^2} \quad f = 8x$$

$$h^2 = \frac{C}{(1-x^2)^2} + \frac{8x}{(1-x^2)^2}$$

$$h = \frac{8(1+x)}{(1-x^2)} = h(\alpha \theta)$$

$$q_r = -k \frac{\partial T}{\partial r} = -\frac{k(T_0 - T_\infty)}{R} \frac{\partial T^*}{\partial r^*}$$

$$= -\frac{k(T_0 - T_\infty)}{R \delta} \frac{\partial T}{\partial y} = -\frac{k(T_0 - T_\infty)}{R \delta h(\theta)} \frac{\partial T}{\partial \eta}$$

Heat flux at the surface:

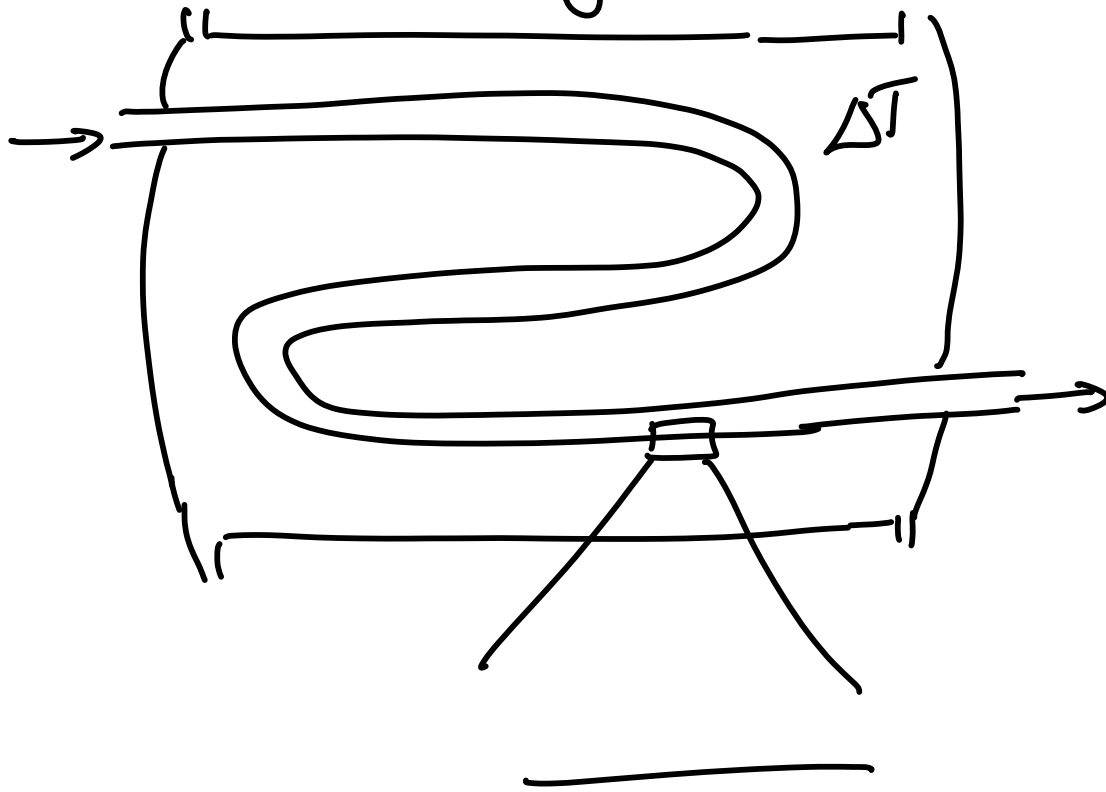
$$q_r|_{r=R} = \frac{-k(T_0 - T_\infty)}{R \delta h(\theta)} \left. \frac{\partial T^*}{\partial \eta} \right|_{\eta=0}$$

$$\rightarrow \frac{-k(T_0 - T_\infty)}{R \delta h(\theta)} \left(\frac{1}{\int_0^\infty d\eta' e^{-\eta'^2}} \right)$$

$$Q = 2\pi R^2 \int_0^\pi \sin \theta d\theta q_r(\theta)$$

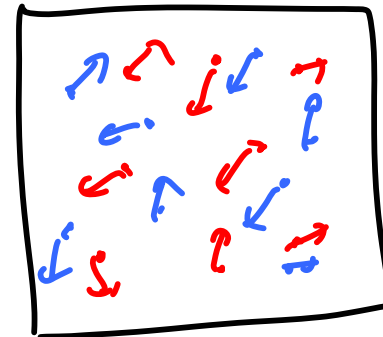
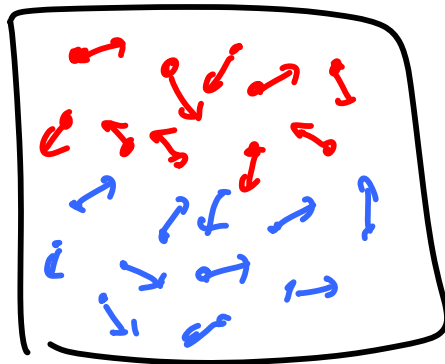
$$Nu = 0.9213 Pe^{1/2}$$

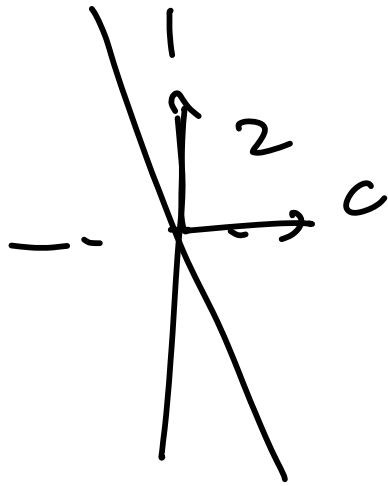
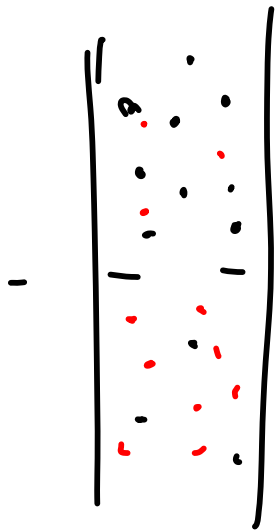
Summary:



Convection
Diffusion

Diffusion:

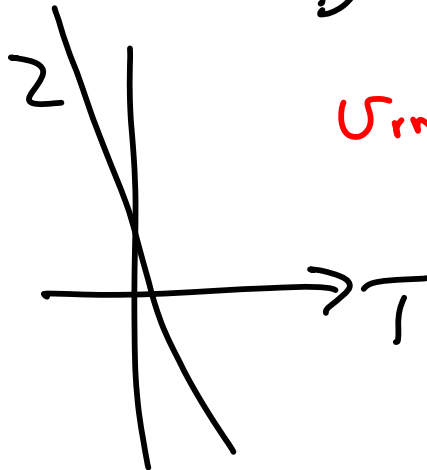
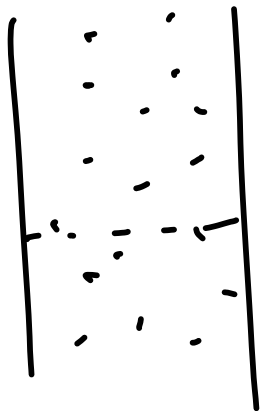




$$j_z = -D \frac{dc}{dz}$$

$$D = a \lambda v_{rms}$$

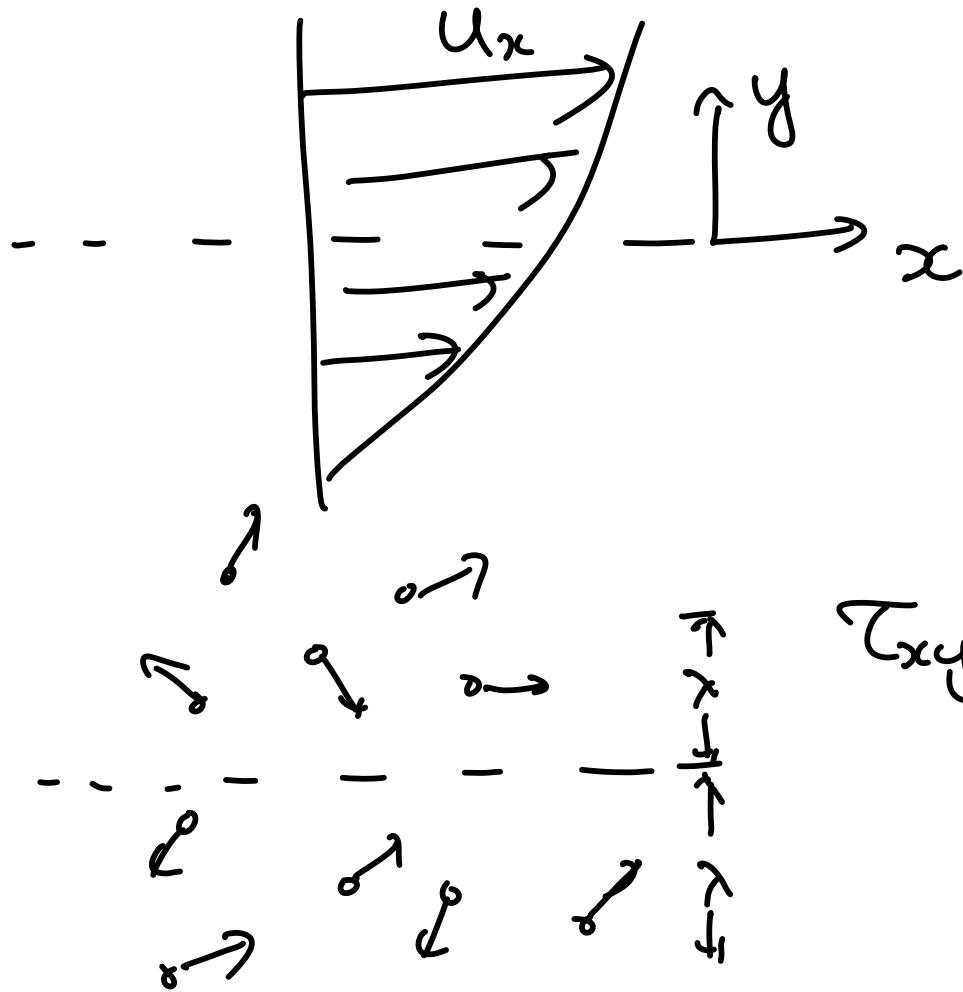
$$v_{rms} = \sqrt{\frac{3kT}{m}}$$



$$j_e = -k \frac{dT}{dz}$$

$$= -\alpha \frac{de}{dz}$$

$\alpha = \text{Thermal diffusivity} = (k / \rho C_p)$

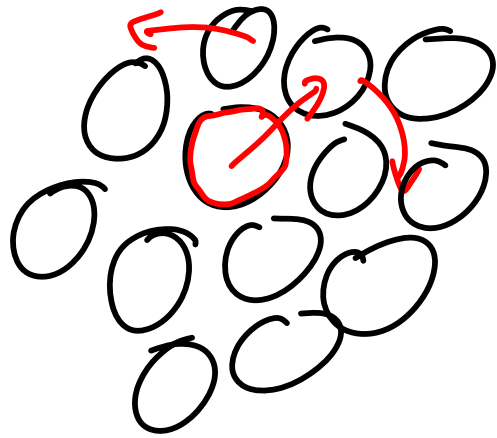


u_x is a function of y

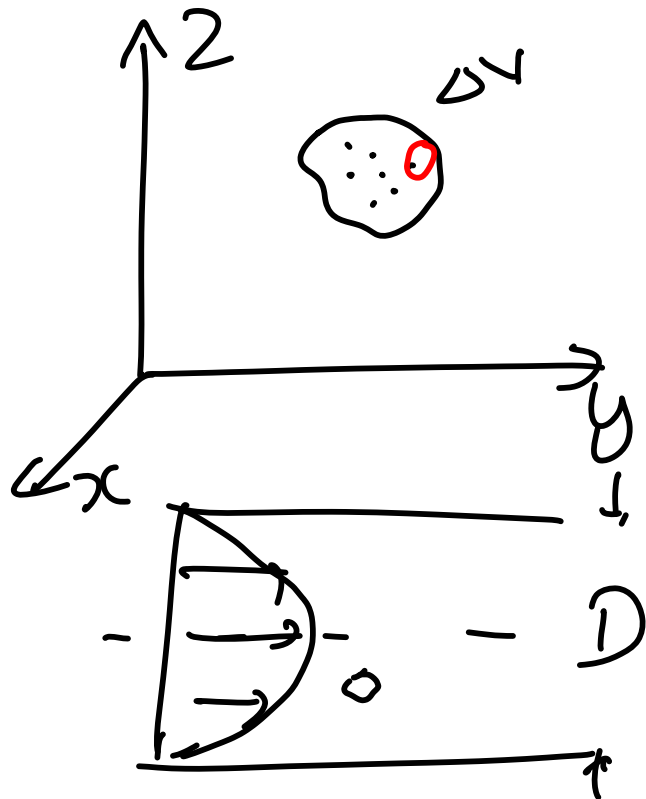
$\tau_{xy} = \text{Force/Area at the surface in } x \text{ direction at a surface with outward unit normal in } y \text{ direction}$

$$\tau_{xy} = \mu \frac{du_x}{dy} = \nu \frac{d(\rho u_x)}{dy}$$

$$\nu = (\mu / \rho)$$



Fields:



$$\rho(x, y, z) = \lim_{\Delta V \rightarrow 0} \frac{\sum m_i}{\Delta V}$$

Continuum approximation:

$$(\rho \underline{y}) = \lim_{\Delta V \rightarrow 0} \frac{\sum m_i \underline{y}_i}{\Delta V}$$

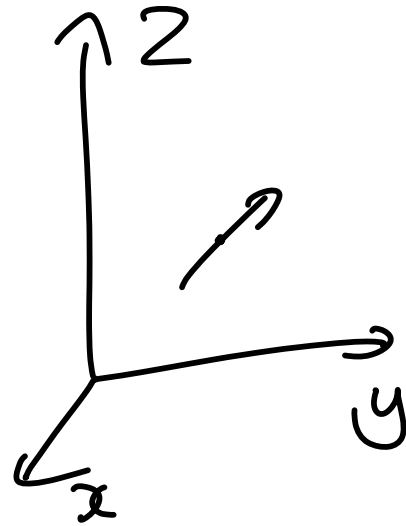
$$\underline{y} = \frac{(\rho \underline{y})}{\rho}$$

$$e = \lim_{\Delta V \rightarrow 0} \frac{\sum e_i}{\Delta V}$$

$$\delta C_b \Delta T = \Delta e$$

$$j_x = -D \frac{\partial C}{\partial x}$$

$$j_y = -D \frac{\partial C}{\partial y}$$

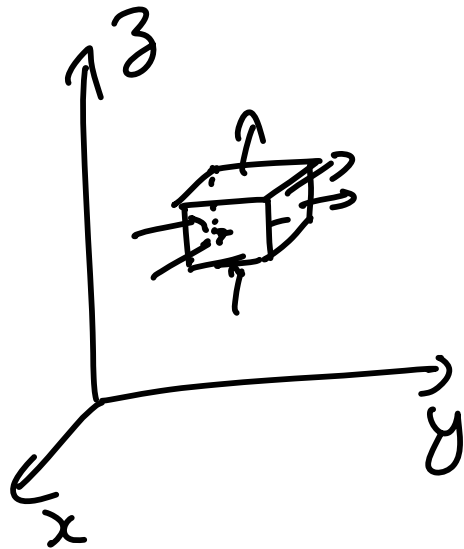


$$\underline{j} = j_x \underline{e}_x + j_y \underline{e}_y + j_z \underline{e}_z$$

$$= -D \left(\underline{e}_x \frac{\partial C}{\partial x} + \underline{e}_y \frac{\partial C}{\partial y} + \underline{e}_z \frac{\partial C}{\partial z} \right)$$

$$= -D \nabla C$$

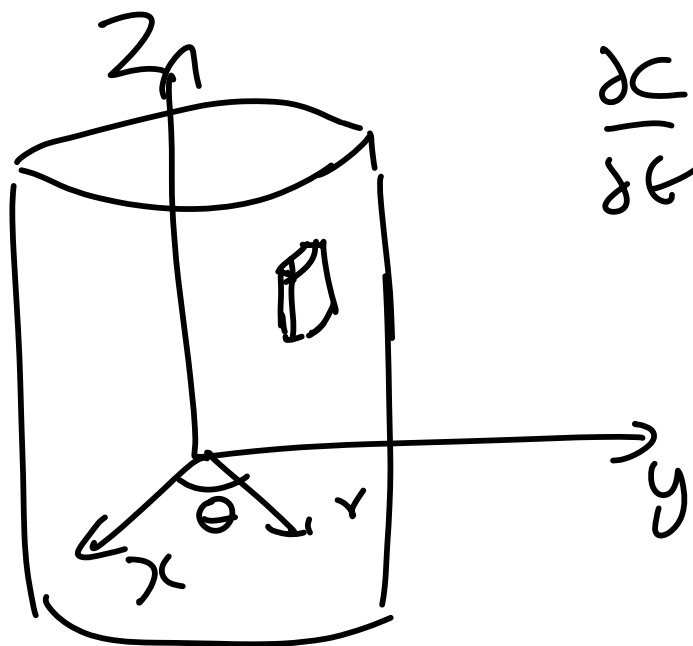
Shell balances:



$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x}(u_x C) + \frac{\partial}{\partial y}(u_y C) + \frac{\partial}{\partial z}(u_z C) =$$

$$D \left(\frac{\partial^2 C}{\partial x^2} + \frac{\partial^2 C}{\partial y^2} + \frac{\partial^2 C}{\partial z^2} \right) + S$$

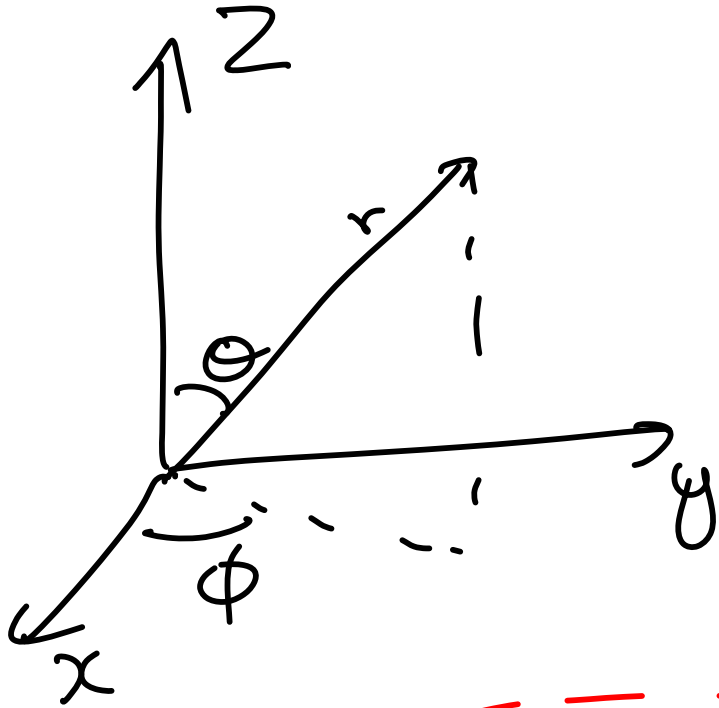
$$\frac{\partial C}{\partial t} + \nabla \cdot (\underline{u} C) = D \nabla^2 C + S$$



$$\frac{\partial C}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (r C u_r) + \frac{1}{r} \frac{\partial (C u_\theta)}{\partial \theta} + \frac{\partial (C u_z)}{\partial z}$$

$$= D \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial C}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 C}{\partial \theta^2} + \frac{\partial^2 C}{\partial z^2} \right)$$

Spherical co-ordinate system:



$$\frac{\partial C}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 C u_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta C u_\theta)$$

$$+ \frac{1}{r \sin \theta} \frac{\partial (C u_\phi)}{\partial \phi} =$$

$$\nabla \left(\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial C}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial C}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 C}{\partial \phi^2} \right)$$

$$\frac{\partial c}{\partial t} + \nabla \cdot (u c) = D \nabla^2 c + S$$

$$Pe \left(\frac{\partial c^*}{\partial t^*} + \nabla^* \cdot (u^* c^*) \right) = \nabla^{*2} c + S^*$$

$$Pe = \left(\frac{UL}{D} \right)$$

$$Pe \ll 1 \quad D \nabla^2 c + S = 0$$

$$\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} + \frac{\partial^2 c}{\partial z^2} = 0$$

$$c = X(x) Y(y) Z(z)$$

$$X(x) = \sin(n\pi x^*)$$

$$Y(y) = \sin(m\pi y^*)$$

$$c = \sum_n \sum_m A_{nm} \frac{\sin(n\pi x^*) \sin(m\pi y^*)}{e^{(m^2+n^2)\pi^2 z}}$$

$$\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial C}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial C}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 C}{\partial \phi^2} = 0$$

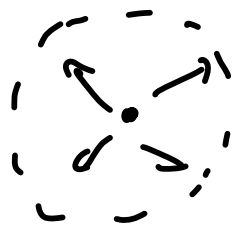
$$C = \sum_{nm} \left(A_n r^n + \frac{B_n}{r^{n+1}} \right) \boxed{Y_n^m(\theta, \phi)}$$

n, m are integers

$$Y_n^m(\theta, \phi) = P_n^m(\cos \theta) \begin{pmatrix} \cos \\ \sin \end{pmatrix} (m\phi)$$

$$\int_0^\pi \sin \theta d\theta \int_0^{2\pi} d\phi Y_n^m(\theta, \phi) Y_p^q(\theta, \phi) = \frac{2\pi}{2n+1} \frac{(n+m)!}{(n-m)!} \delta_{np} \delta_{mq}$$

$$n=0 \text{ \& } m=0$$

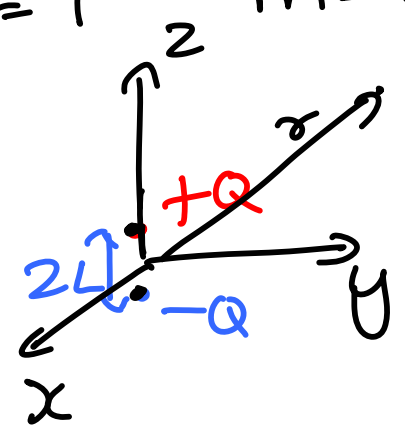


$$T = \frac{Q}{4\pi k r}$$

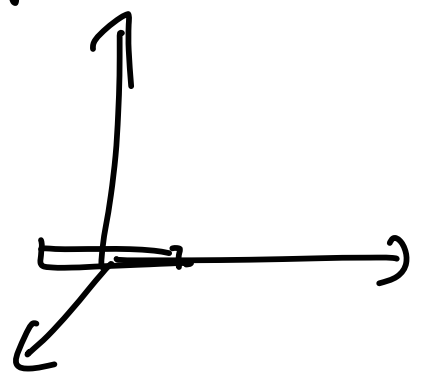
$$k \nabla^2 T + Q \delta(\mathbf{r}) = 0$$

$n=1$ $m=0$

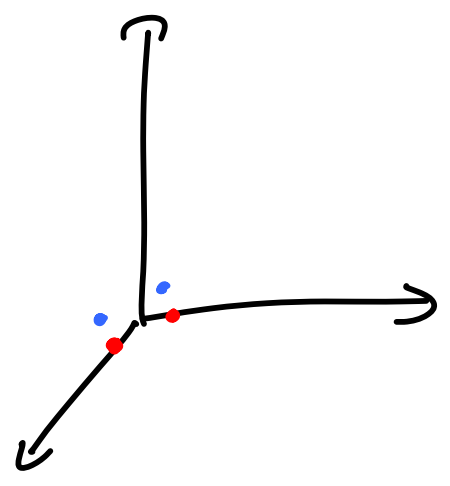
Dipole



$$T = \frac{1}{r^2} \cos\theta = \frac{1}{r^2} P_1^0(\cos\theta)$$



$n=1$ $m=\pm 1$



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High Peclet number limit:

$$Pe \left(\frac{\partial c^*}{\partial t^*} + \nabla^* \cdot (u^* c^*) \right) = \nabla^{*2} c^* + S$$

$$Pe \gg 1$$

$$l \sim Pe^{-1/3} \quad \text{for no-slip} \quad Nu \propto Pe^{1/3}$$

$$l \sim Pe^{-1/2} \quad \text{for finite velocity at surface.} \quad Nu \propto Pe^{1/2}$$