

CRYOGENIC ENGINEERING



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Lecture No - **35**

Earlier Lecture

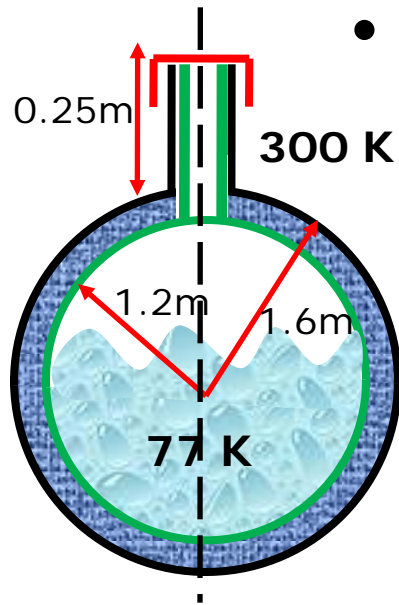
- In the earlier lecture, we have seen that radiation is dominant mode of heat transfer in vacuum.
- Evacuated powders are superior in performance than vacuum alone, in **300 K – 77 K**, as radiation heat transfer is comparatively less.
- In an opacified powder, radiation heat transfer is minimized by addition of reflective flakes.
- A tutorial problem is solved to compare the different types of insulations, so far discussed.

Outline of the Lecture

Topic : Cryogenic Insulation (contd)

- Multilayer Insulation
- Tutorial
- Conclusion

Introduction



- In the earlier lecture, we have solved the following tutorial.

A spherical **LN2** vessel ($e=0.8$) is as shown. The inner and outer radii are 1.2m and 1.6m respectively. Compare and comment on the heat in leak for the following cases.

- Perlite, Less Vacuum (1.5mPa), Vacuum alone, Vacuum + 10 shields, Evacuated Fine Perlite, 50/50 Cu – Santocel.

Introduction

Heat in leak (Q)

Perlite	349.7 W
Less Vacuum (1.5mPa)	$Q_r = 2648$ W $Q_{gc} = 0.356$ W
Vacuum alone	2648 W
Vacuum + 10 shields	11.02 W
Evacuated Fine Perlite	12.7 W
50/50 Cu – Santocel	4.41 W

- It is clear that opacified powder is the best insulation.
- A heat in leak of 4.41 W to **LN2** would vaporize 2.36 Lit/day as shown in the next slide.

Introduction

- Latent heat of LN2 = 200 kJ/Kg, Density of LN2 = 807 kg/m³.
- 1m³ = 1000 Lit and a day has 24 hours.
- 1 Lit/hr boil off of LN2 is equivalent to
$$\frac{(807)(200)(10^3)}{(10^3)(3600)}$$
$$= 44.83W$$
- Hence, 4.41 W of heat vaporizes 0.098 Lit/hr.
- Therefore, the total boil off in 1 day is 2.36 Lit.

Introduction

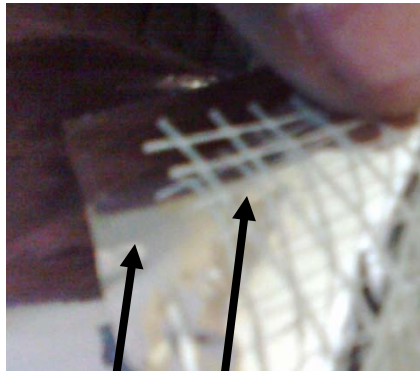
- Different types of insulations discussed in the earlier lectures are applicable only to **300 K** to **77 K** temperature range.
- Given that, latent heat of LHe = 20.2kJ/Kg and density of LHe = 124.8 kg/m³, 1 Lit/hr boil off of LHe is equivalent to 0.7 W.
- The same amount of heat in leak, that is 4.41 W, would vaporize 151.1 Lit of LHe in one day.
- Therefore, there is a need to develop better insulations for **77 K** to **4 K** temperature range.

Types of Insulation

- Expanded Foam – Mass
- Gas Filled Powders & Fibrous Materials – Mass
- Vacuum alone – Vacuum
- Evacuated Powders – Mass + Vacuum
- Opacified Powders – Mass + Vacuum + Reflective
- Multilayer Insulation – Vacuum + Reflective

Multilayer Insulation

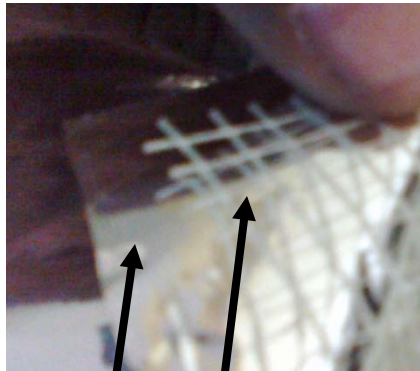
- Multilayer Insulation (MLI) was first developed by Petersen of Sweden in the year 1951.
- It consists of alternate layers of
 - High reflecting shields or foils
 - Separated by low conductivity spacers
 - And a very good vacuum.



Shield
Spacer

Multilayer Insulation

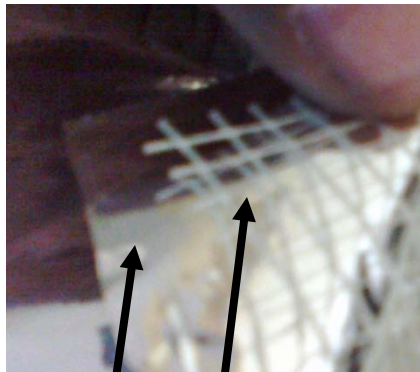
- The high reflecting shields are generally made of either Al, Cu or Aluminized Mylar.
- Aluminum sheet of $6\mu\text{m}$ thickness is commonly used at low temperatures.
- In order to improve mechanical strength and ease of application, plastic materials like Mylar and Kapton are coated with aluminum.



Shield
Spacer

Multilayer Insulation

- Low conductivity spacers are made of coarse silk or nylon net.
- Very often, substances like glass fiber, silica fiber, low density foam or fiber glass mat are also used.
- Most common materials among fibers are Dexiglas and Tissuglas.
- One layer of MLI is defined as one sheet of reflective shield + one sheet of spacer material.

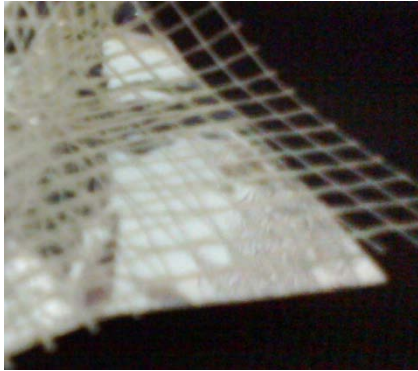


Shield

Spacer

Multilayer Insulation

- Each component of this insulation is designed for a particular function.



- Radiation shields – Foils with high reflectivity reduce radiant heat transfer.
- Spacers – Nylon spacers with very low thermal conductivity reduce conduction.
- Vacuum – Residual gas conduction, convection are minimized using vacuum.

Types of MLI

- MLIs are classified according to the type of spacers used.



- Multiple Resistance Spacers: Fibers are arranged in a parallel fashion to minimize contact area.
- Point Contact Spacers: A grid of nylon spheres is used to separate adjacent radiation shields.

Types of MLI

- Continuing further, we have



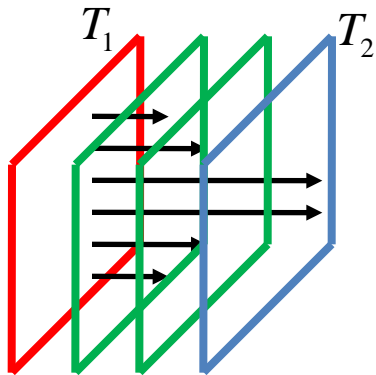
- Single Component MLI: Reflective shields are crinkled or embossed to minimize contact area. These MLI do not use any spacer material.
- Composite Spacers: Few spacers consist of two or more materials. Each material has a specific function to perform.

Multilayer Insulation

- Typically, thickness of each layer is 6 μm .
- Residual gas conduction inside an insulation depends on residual pressure of the gas.
- For an optimum performance, the usual levels of vacuum, that is maintained around an MLI, are in the range of **7.5×10^{-5}** torr.

Applications

- For an optimum performance, MLI is placed perpendicular to direction of heat flow.



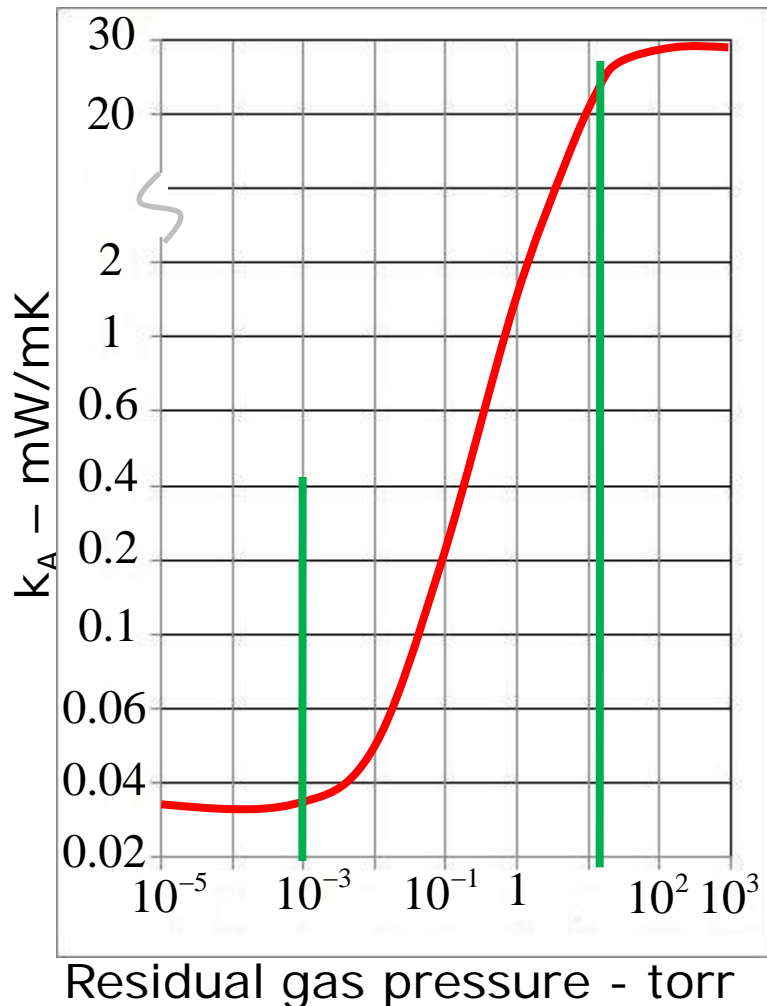
- The insulation performance is a function of following parameters.
 - Applied compressive load
 - Number of shields
 - Gas type and its pressure
 - Size and number of perforations
 - Operating temperature

Applications



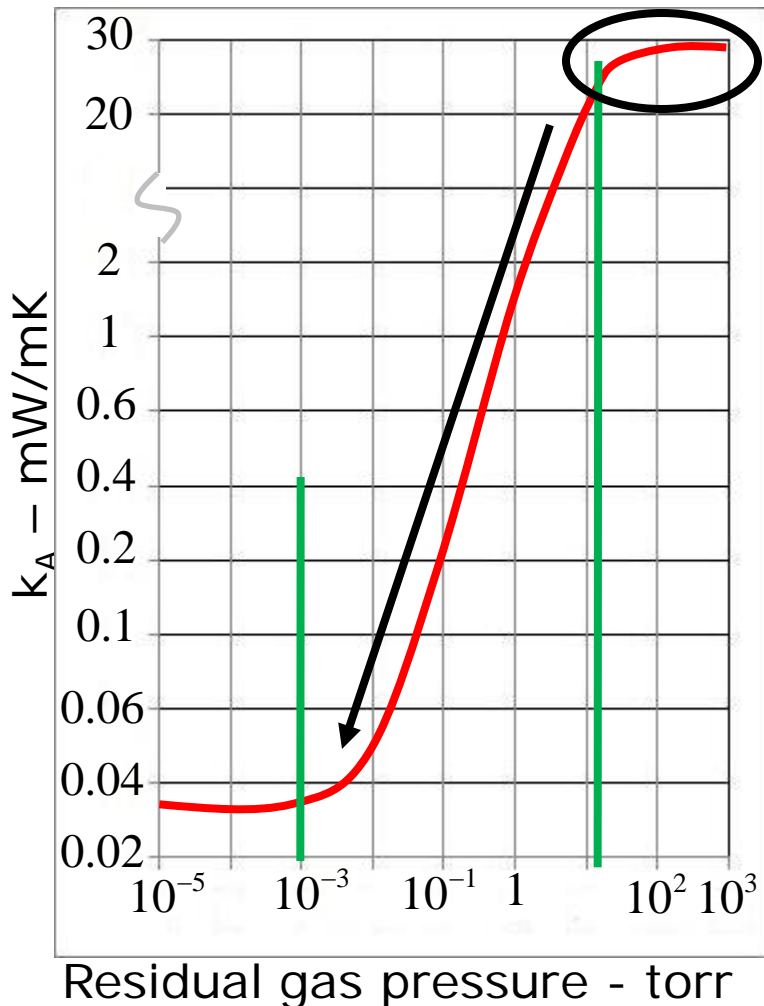
Courtesy: TIFR, Mumbai

Multilayer Insulation



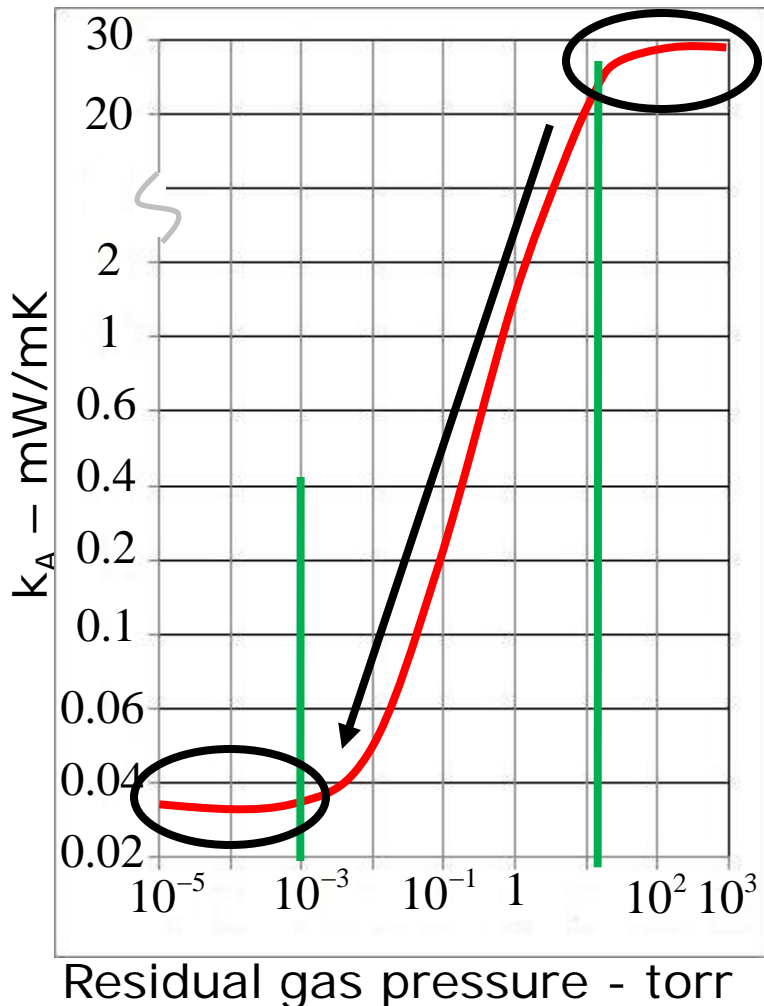
- The adjacent figure shows variation of k_A with residual gas pressure for a typical Multilayer Insulation.
- Insulation layer density is 24 layers/cm with boundary temperatures maintained at 300 K and 90 K.

Multilayer Insulation



- It is clear that, k_A is independent of residual gas pressure between atmospheric and 15 torr.
- With lowering of pressure, k_A is directly proportional to residual gas pressure.
- The variation is almost linear on a logarithmic chart as shown in the figure.

Multilayer Insulation



- The mode of heat transfer in this regime is mainly due to free molecular conduction or residual gas conduction.
- With further lowering of pressures, that is less than 10^{-3} torr, k_A remains fairly constant.

Multilayer Insulation

- MLI bulk density (ρ_a) is an important parameter of the insulation. It depends on
 - Thickness of each reflective shield – t_r
 - Density of each reflective shield – ρ_r
 - Mass per unit area of the spacer – S_s
 - Layer density per unit thickness – $N/\Delta x$
- The total mass per unit area is given by $(S_s + \rho_r t_r)$
- Density being mass per unit volume, for N layers, ρ_a is given by

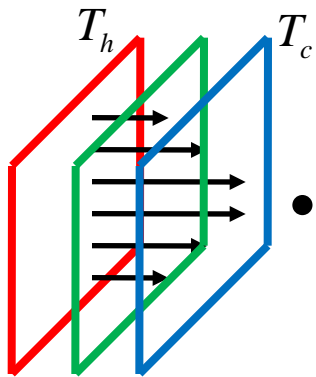
$$\rho_a = (S_s + \rho_r t_r) \frac{N}{\Delta x}$$

Multilayer Insulation

- The apparent thermal conductivity ($\mu\text{W}/\text{mK}$) and layer density (layer/cm) of few commonly used MLI are as shown. Residual gas pressure is 10^{-5} torr with end temperatures as **77 K** and **300 K**.

Insulation	$N/\Delta x$	k_A ($\mu\text{W}/\text{mK}$)
0.006mm Al foil+0.15mm Fiberglass	20	37
0.006mm Al foil+2mm mesh rayon net	10	78
0.006mm NRC-2 crinkled Al Mylar film	35	42

Apparent Thermal Cond.



- For an evacuated MLI, heat is transferred by radiation and solid conduction.

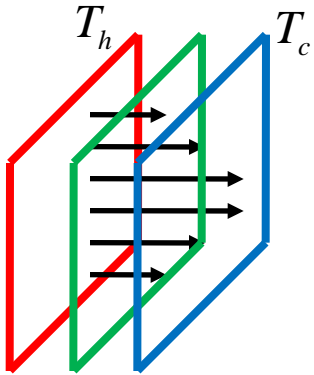
- For 1 layer, net heat transferred (Q_{net}) is

$$Q_{net} = Q_{Rad} + Q_{Solid Cond}$$

$$Q_{net} = F_e F_{1 \rightarrow 2} \sigma A (T_h^4 - T_c^4) + \frac{k_c A (T_h - T_c)}{\Delta x}$$

- F_e – Effective emissivity of the Shields
- $F_{1 \rightarrow 2}$ – Shape factor
- $A, \Delta x$ – Contact area and Width
- k_c – Effective thermal conductivity

Apparent Thermal Cond.



$$Q_{net} = F_e F_{1 \rightarrow 2} \sigma A (T_h^4 - T_c^4) + \frac{k_c A (T_h - T_c)}{\Delta x}$$

$$\frac{1}{F_e} = \left(\frac{2-e}{e} \right)$$

$$F_{1 \rightarrow 2} = 1$$

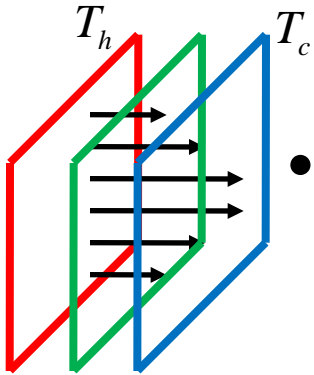
$$h_c = \frac{k_c}{\Delta x}$$

- Combining above equations, we have

$$Q_{net} = \sigma \left(\frac{e}{2-e} \right) A (T_h^4 - T_c^4) + h_c A (T_h - T_c)$$

- e** – Emissivity of the shield
- h_c** – Thermal conductance per unit area

Apparent Thermal Cond.



$$Q_{net} = \sigma \left(\frac{e}{2-e} \right) A (T_h^4 - T_c^4) + h_c A (T_h - T_c)$$

- Let k_A be apparent thermal conductivity of insulation. Therefore, Q_{net} is

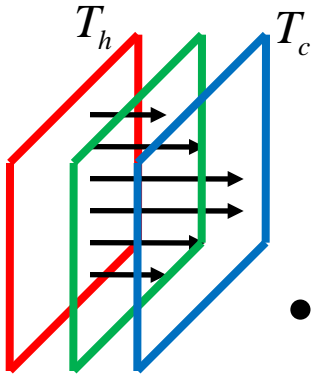
$$Q_{net} = \frac{k_A A (T_h - T_c)}{\Delta x}$$

- Equating above two equations and rearranging, we have

$$\frac{k_A A (T_h - T_c)}{\Delta x} = A (T_h - T_c) \left(\sigma (T_h^2 + T_c^2) (T_h + T_c) \left(\frac{e}{2-e} \right) + h_c \right)$$

Apparent Thermal Cond.

- The apparent thermal conductivity (k_A) is



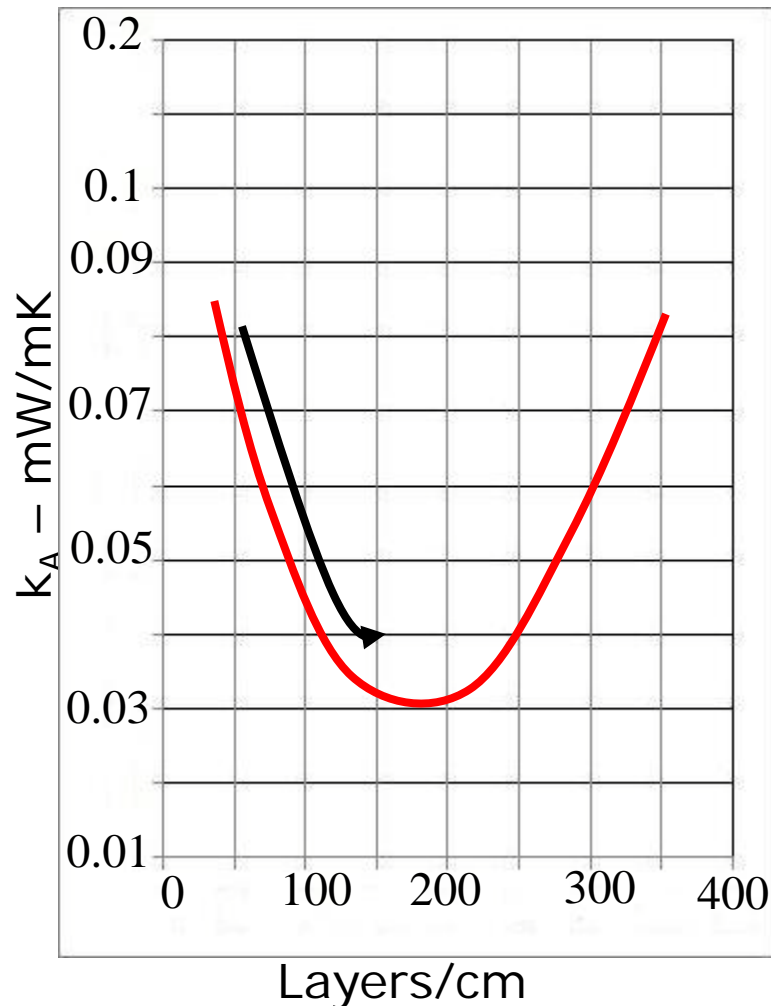
$$k_A = \Delta x \left(\sigma (T_h^2 + T_c^2) (T_h + T_c) \left(\frac{e}{2-e} \right) + h_c \right)$$

- For N layers, we have

$$k_A = \frac{\Delta x}{N} \left(\sigma (T_h^2 + T_c^2) (T_h + T_c) \left(\frac{e}{2-e} \right) + h_c \right)$$

- where,
 - T_h, T_c – Boundary temperatures
 - $N/\Delta x$ – Layer density

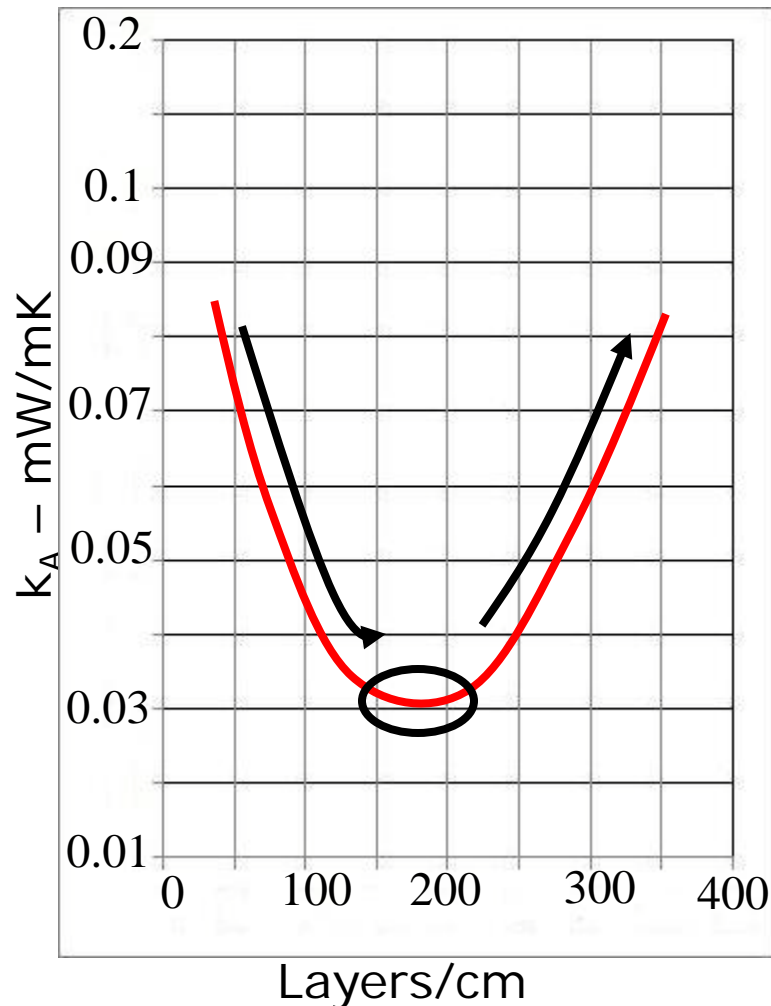
Apparent Thermal Cond.



$$Q_{net} = Q_{Rad} + Q_{Solid Cond}$$

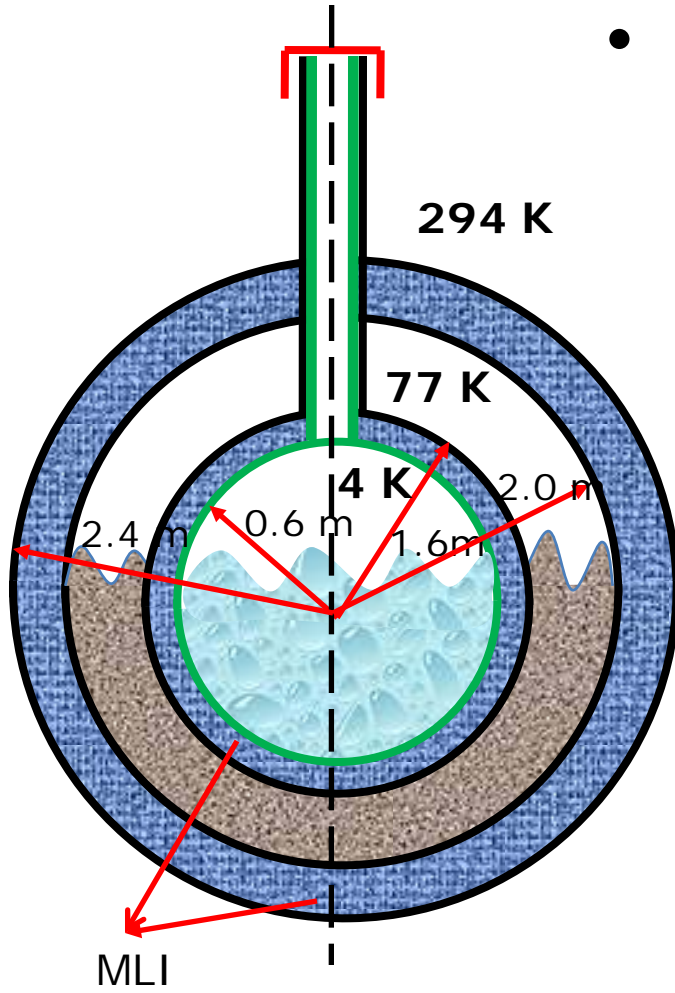
- With an initial increase in layer density, the decrease in radiation heat transfer is more than the increase in solid conduction.
- Hence, k_A of the insulation decreases.

Apparent Thermal Cond.



- With further increase in layer density, k_A increases due to an increase in solid conduction (h_c).
- Therefore, k_A goes through a minima and then rises as shown in the figure.

Tutorial



- Consider a spherical **LHe** vessel shielded with **LN2** bath. The radii of the spherical shells are as shown in the figure. MLI (24 layers/cm) is applied at each stage. Calculate the boil off/day of LN2 and LHe.

Given that emissivity of shield is 0.05. Solid conductance of spacer is $0.0851 \text{ W/m}^2\text{K}$ (assumed constant). Also, neglect neck conduction.

Tutorial

Given

Multi Layer Insulation

Operating LN2 boil off : 294 K to 77 K

Temperature LHe boil off : 77 K to 4 K

Emissivity of Shield : 0.05

Number of layers : 24/cm

Solid conductance : 0.0851 W/m²K

Calculate

Boil off of LN2 and LHe on per day basis.

Tutorial

Calculation of k_A for LN2 (294 K to 77 K)

- $\Delta x/N=(1/2400)$, $h_c=0.0851$, $e=0.05$, T_h , T_c .

$$k_A = \left(\frac{\Delta x}{N} \right) \left(h_c + \sigma e (T_h^2 + T_c^2) \left(\frac{T_h + T_c}{2 - e} \right) \right)$$

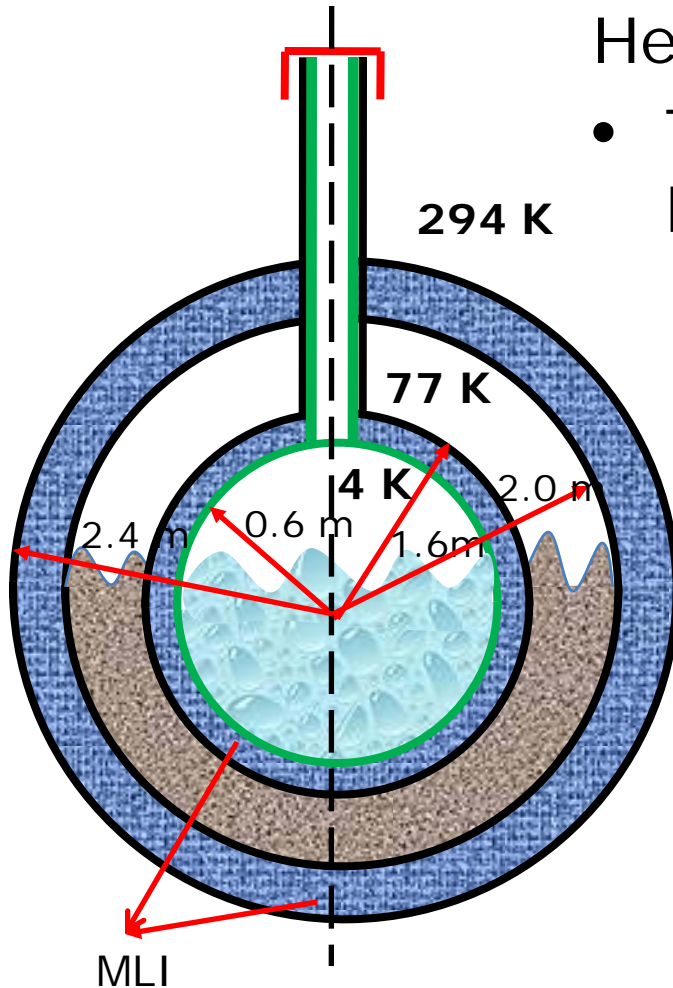
$$k_A = \left(\frac{1}{2400} \right) \left(0.0851 + \frac{(5.669)(10^{-8})(0.05)(92365)(371)}{(2 - 0.05)} \right)$$

$$k_A = 56.2 \mu W / mK$$

Tutorial

Heat in leak for LN2 (294 K to 77 K)

- $T_h, T_c, k_A = 56.2 \mu\text{W/mK}, R_1 = 2.4\text{m}, R_2 = 2.0\text{m}, \Delta T = (294 - 77) = 217.$



$$Q = \frac{4\pi k_A R_1 R_2 \Delta T}{(R_2 - R_1)}$$

$$Q = \frac{4\pi (56.2)(10^{-6})(2.4)(2.0)(217)}{(2.4 - 2.0)}$$

$$Q = 1.84\text{W}$$

Tutorial

Boil off of LN2 (294 K to 77 K)

- Latent heat of LN2 = 200 kJ/Kg, Density of LN2 = 807 kg/m³.
- 1 Lit/hr of LN2 is equivalent to 44.83 W.
- Hence, 1.84 W of heat vaporizes 0.041 Lit/hr.
- Therefore, the total boil off of LN2 in 1 day is 0.985 Lit.

Tutorial

Calculation of k_A for LHe (77 K to 4 K)

- $\Delta x/N=(1/2400)$, $h_c=0.0851$, $e=0.05$, T_h , T_c .

$$k_A = \left(\frac{\Delta x}{N} \right) \left(h_c + \sigma e (T_h^2 + T_c^2) \left(\frac{T_h + T_c}{2 - e} \right) \right)$$

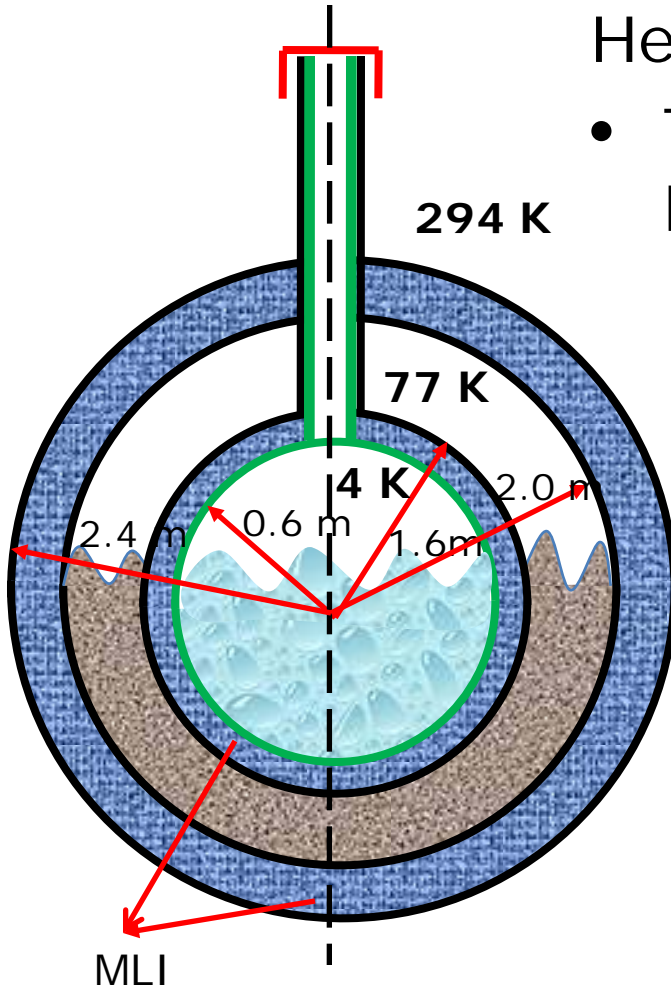
$$k_A = \left(\frac{1}{2400} \right) \left(0.0851 + \frac{(5.669)(10^{-8})(0.05)(5945)(81)}{(2 - 0.05)} \right)$$

$$k_A = 35.7 \mu W / mK$$

Tutorial

Heat in leak for LHe (77 K to 4 K)

- $T_h, T_c, k_A = 35.7 \mu\text{W/mK}, R_1 = 1.6\text{m}, R_2 = 0.6\text{m}, \Delta T = (77 - 4) = 73.$



$$Q = \frac{4\pi k_A R_1 R_2 \Delta T}{(R_2 - R_1)}$$

$$Q = \frac{4\pi (35.7)(10^{-6})(1.6)(0.6)(73)}{(1.6 - 0.6)}$$

$$Q = 0.031\text{W}$$

Tutorial

Boil off for LHe (77 K to 4 K)

- Latent heat of LHe = 20.2 kJ/Kg, Density of LHe = 124.8 kg/m³.
- 1 Lit/hr of LHe is equivalent to 0.7W.
- Hence, 0.031 W of heat vaporizes 0.044 Lit/hr.
- Therefore, the total boil off of LHe in 1 day is 1.062 Lit.

Tutorial

Results

LN2 boil off	LHe boil off
Working Fluid: LN2 between 294 K to 77 K	Working Fluid : LHe between 77 K to 4 K
$k_A = 56.2\mu\text{W/mk}$	$k_A = 35.7\mu\text{W/mk}$
$Q = 1.84 \text{ W}$	$Q = 0.03 \text{ W}$
Boil off : 0.985 Lit/day	Boil off : 1.062 Lit/day

Conclusion

- Cryogenic vessels need insulation to minimize all modes of heat transfer.
- k_A is calculated based on all the possible modes of heat transfer.
- In an expanded foam, heat is transferred only by solid conduction. With decrease in mean cell diameter, k_A decreases. With an increase in bulk density, k_A increases.
- In a gas filled powder or a fibrous insulation, heat is transferred by gas and solid conduction.

Conclusion

- In vacuum, radiation is the dominant mode of heat transfer. It is minimized by using radiation shields.
- In an evacuated powder, heat is transferred by free molecular conduction, solid conduction and radiation. At low pressures and temperatures, solid conduction dominates radiation.
- In an opacified powder, the radiation heat transfer is minimized by addition of reflective flakes.
- MLI consist of alternate layers of high reflecting shields and low conducting spacers.

Conclusion

- Multi Layer Insulations are more effective in **77 K** to **4 K** temperatures, when provided with a good vacuum.
- There is an optimum layer density, at which k_A of the insulation is minimum.

Thank You!