

Tutorial – 1

- Determine the y , y_{max} , the work/unit mass compressed, work/unit mass liquefied and FOM for the Simple and Precooled Linde – Hampson systems with Nitrogen as working fluid. The R134A is the refrigerant for the precooling system with ratio r as 0.08. The liquefaction system is operated between 1.013 bar (1 atm) and 101.3 bar (100 atm) at 300 K. The following is the data for R134a. Comment on the results.

	a	b	c
p (bar)	1.013	10.13	10.13
T (K)	300	373	300
h (J/g)	390	482	260

Tutorial – 1

Given

Cycle : Simple and Precooled L – H System

Working Fluid : Nitrogen

Pressure : 1 atm → 100 atm

Temperature : 300 K

Refrigerant : R134a, 1 atm → 10 atm

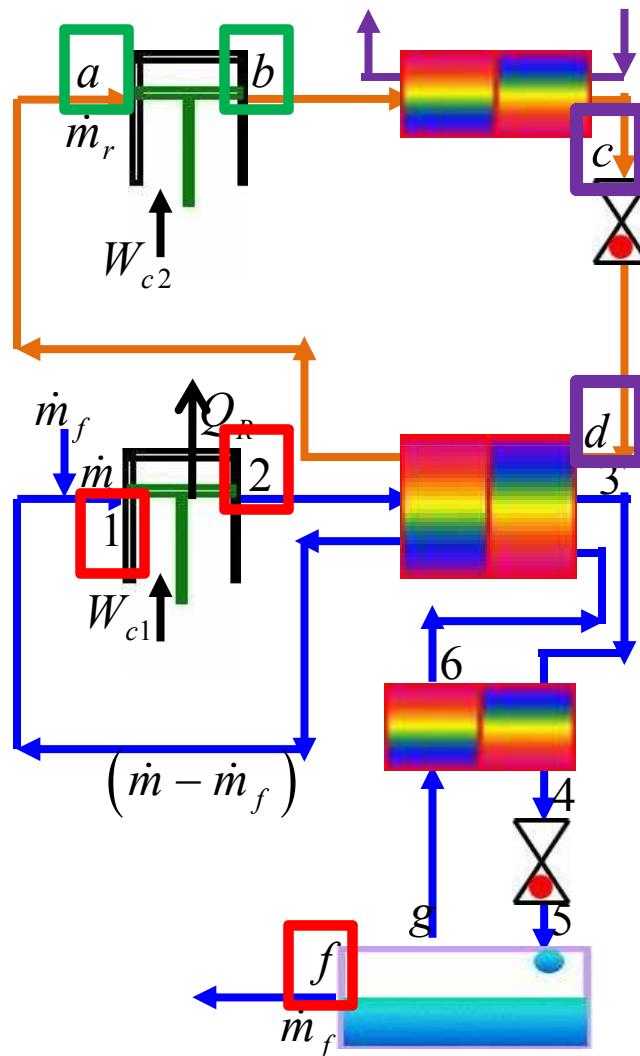
Mass ratio(r) : 0.08

For above cycles, Calculate and comment

- | | |
|---|----------------------------------|
| 1 | Liquid Yield y , y_{max} |
| 2 | Work/unit mass of gas compressed |
| 3 | Work/unit mass of gas liquefied |
| 4 | FOM |

CRYOGENIC ENGINEERING

Tutorial – 1



	1	2	f
p (bar)	1.013	101.3	1.013
T (K)	300	300	77
h (J/g)	462	445	29
s (J/gK)	4.42	3.1	0.42

	a	b	c
p (bar)	1.013	10.13	10.13
T (K)	300	373	300
h (J/g)	390	482	260
s (J/gK)			R134a

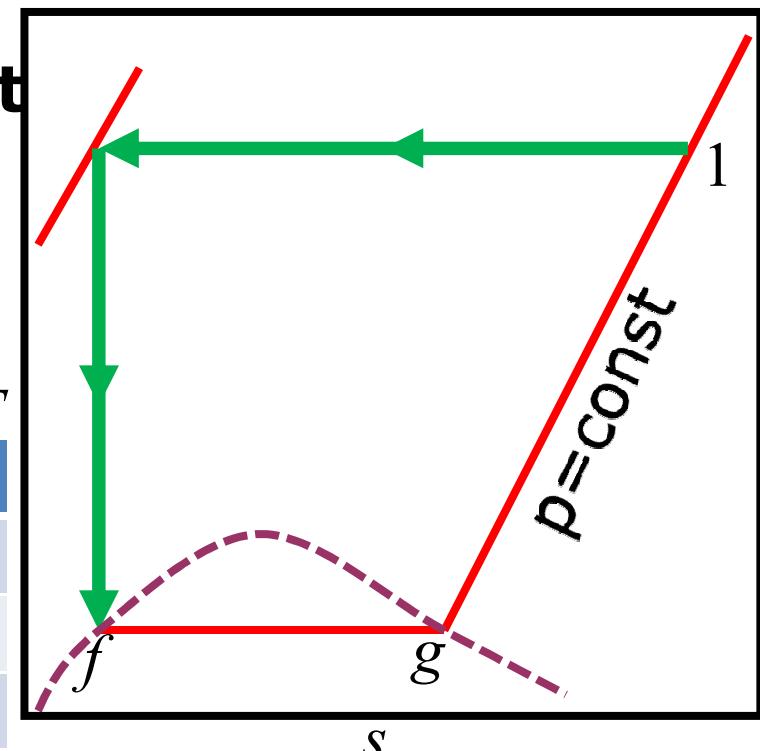
- $h_d = h_c$, since the expansion is isenthalpic.

Tutorial – 1

- Ideal Work Requirement**

$$-\frac{\dot{W}_i}{\dot{m}} = T_1 \left(s_1 - s_f \right) - \left(h_1 - h_f \right)$$

	1	2	f
p (bar)	1.013	101.3	1.013
T (K)	300	300	77
h (J/g)	462	445	29
s (J/gK)	4.42	3.1	0.42



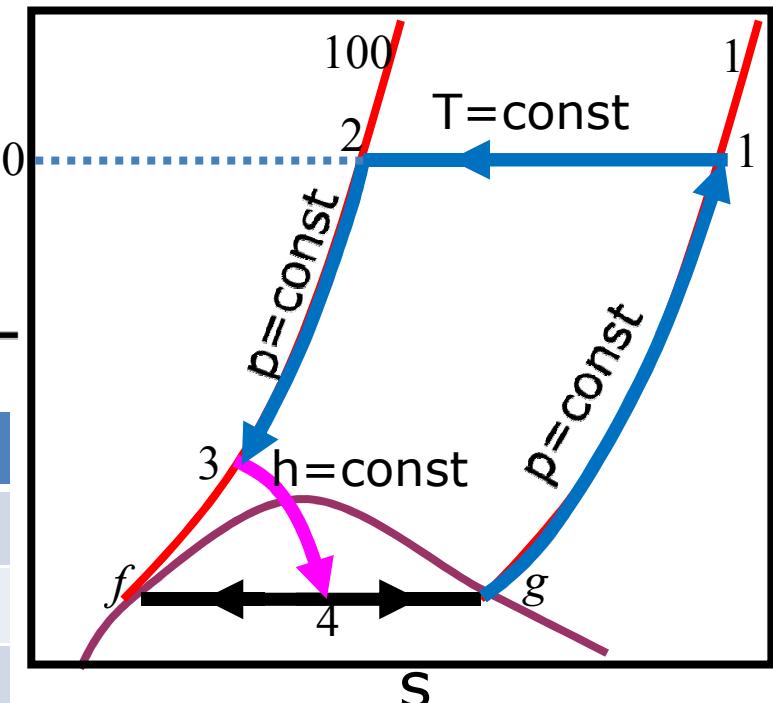
$$-\frac{W_c}{\dot{m}} = 300(4.42 - 0.42) - (462 - 29) = 767 \text{ J/g}$$

Tutorial – 1

- Liquid yield**

$$y = \left(\frac{h_1 - h_2}{h_1 - h_f} \right)$$

	1	2	f
p (bar)	1.013	101.3	1.013
T (K)	300	300	77
h (J/g)	462	445	29
s (J/gK)	4.42	3.1	0.42



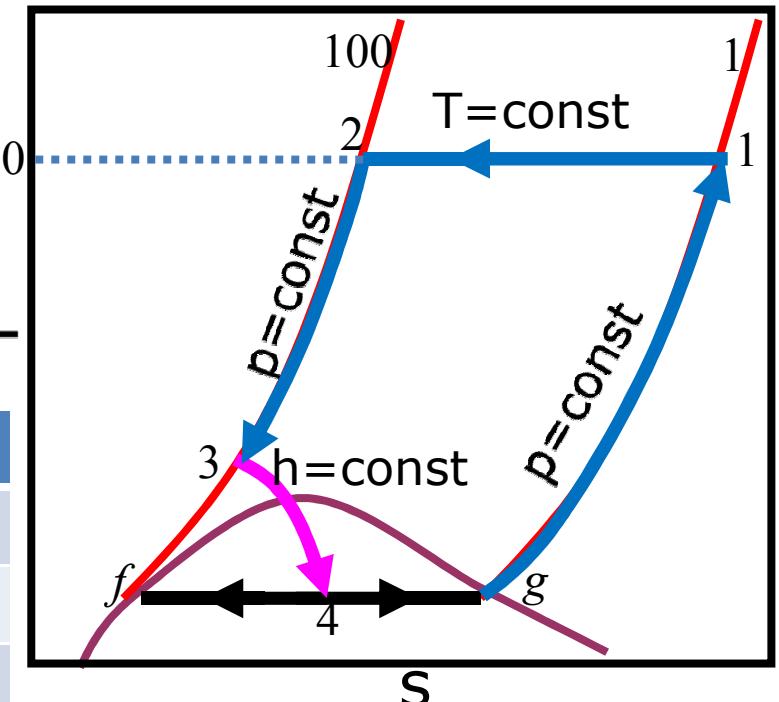
$$y = \left(\frac{h_1 - h_2}{h_1 - h_f} \right) = \left(\frac{462 - 445}{462 - 29} \right) = \left(\frac{17}{433} \right) = 0.04$$

Tutorial – 1

- Work/unit mass of gas compressed**

$$-\frac{W_c}{\dot{m}} = T_1(s_1 - s_2) - (h_1 - h_2)$$

	1	2	f
p (bar)	1.013	101.3	1.013
T (K)	300	300	77
h (J/g)	462	445	29
s (J/gK)	4.42	3.1	0.42



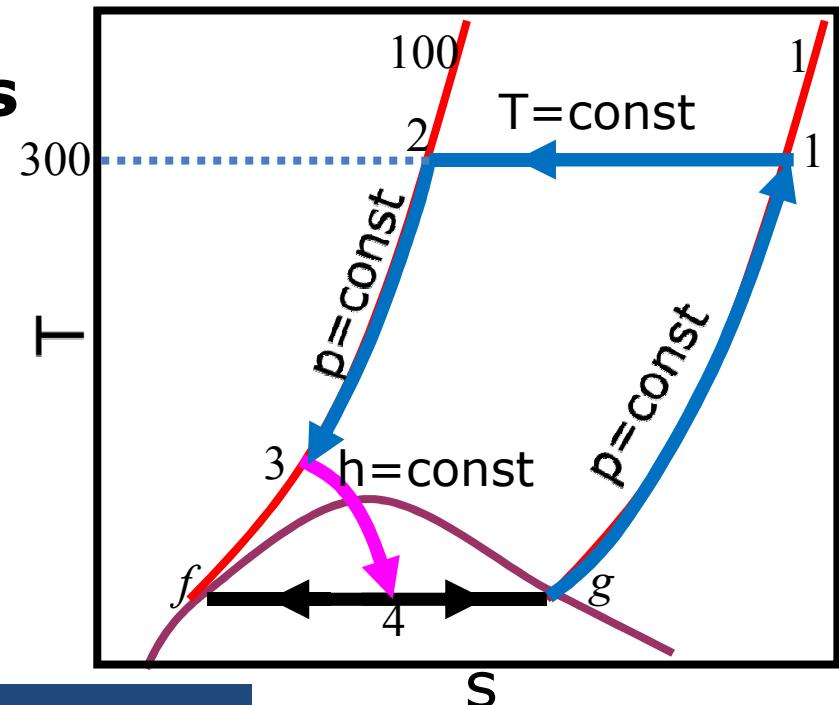
$$-\frac{W_c}{\dot{m}} = 300(4.42 - 3.1) - (462 - 445) = 379 \text{ J/g}$$

Tutorial – 1

- Work/unit mass of gas liquefied**

$$-\frac{W_c}{\dot{m}} = 379$$

$$y = 0.04$$



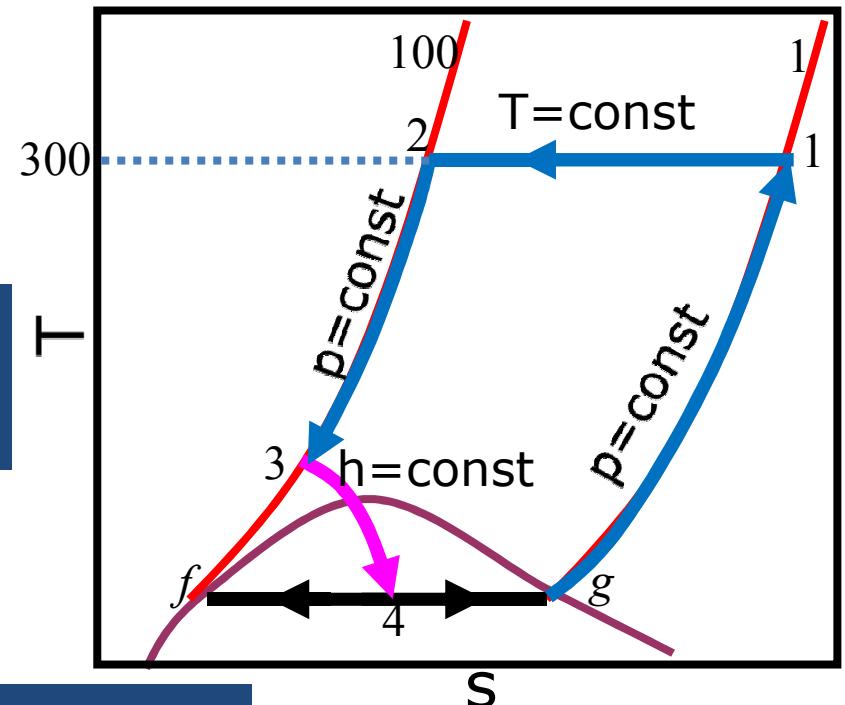
$$-\frac{W_c}{\dot{m}_f} = -\frac{W_c}{y \dot{m}} = \frac{379}{0.04} = 9475 \text{ J/g}$$

Tutorial – 1

- **Figure of Merit (FOM)**

$$-\frac{W_c}{\dot{m}_f} = 9475$$

$$-\frac{W_i}{\dot{m}_f} = 767$$

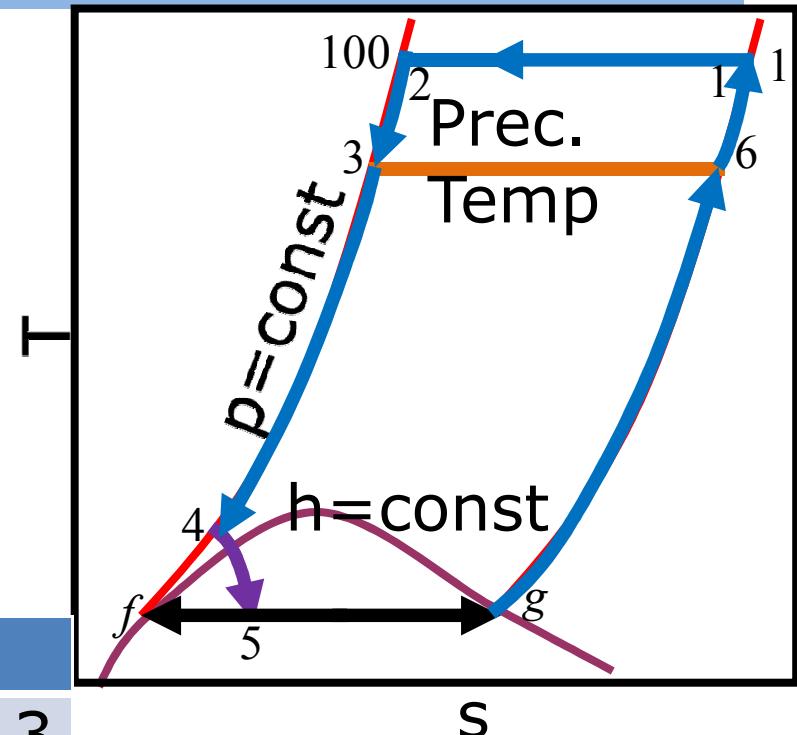


$$FOM = \frac{\frac{W_i}{\dot{m}_f}}{\frac{W_c}{\dot{m}_f}} = \frac{767}{9475} = 0.081$$

Tutorial – 1

- The T – s diagram for a Precooled Linde – Hampson system is as shown.
- The state properties are as tabulated below.

	1	2	f
p (bar)	1.013	101.3	1.013
T (K)	300	300	77
h (J/g)	462	445	29
s (J/gK)	4.42	3.1	0.42



Tutorial – 1

- Liquid yield

$$y = \frac{\dot{m}_f}{\dot{m}} = \frac{h_1 - h_2}{h_1 - h_f} + r \left(\frac{h_{a,r} - h_{d,r}}{h_1 - h_f} \right)$$

$$r = 0.08$$

	1	2	f	a	b	c	
p (bar)	1.013	101.3	1.013	1.013	10.13	10.13	
T (K)	300	300	77	300	373	300	
h (J/g)	462	445	29	390	482	260	
s (J/gK)	4.42	3.1	0.42	R134a			

$$y = \frac{(462 - 445)}{(462 - 29)} + 0.08 \frac{(390 - 260)}{(462 - 29)} = \frac{(17)}{(433)} + 0.08 \frac{(130)}{(433)} = 0.063$$

Tutorial – 1

- Work/unit mass of **N₂** compressed

$$-\frac{W_c}{\dot{m}} = T_1(s_1 - s_2) - (h_1 - h_2) + r(h_{b,r} - h_{a,r})$$

$$r = 0.08$$

	1	2	f	a	b	c
p (bar)	1.013	101.3	1.013	1.013	10.13	10.13
T (K)	300	300	77	300	373	300
h (J/g)	462	445	29	390	482	260
s (J/gK)	4.42	3.1	0.42	R134a		

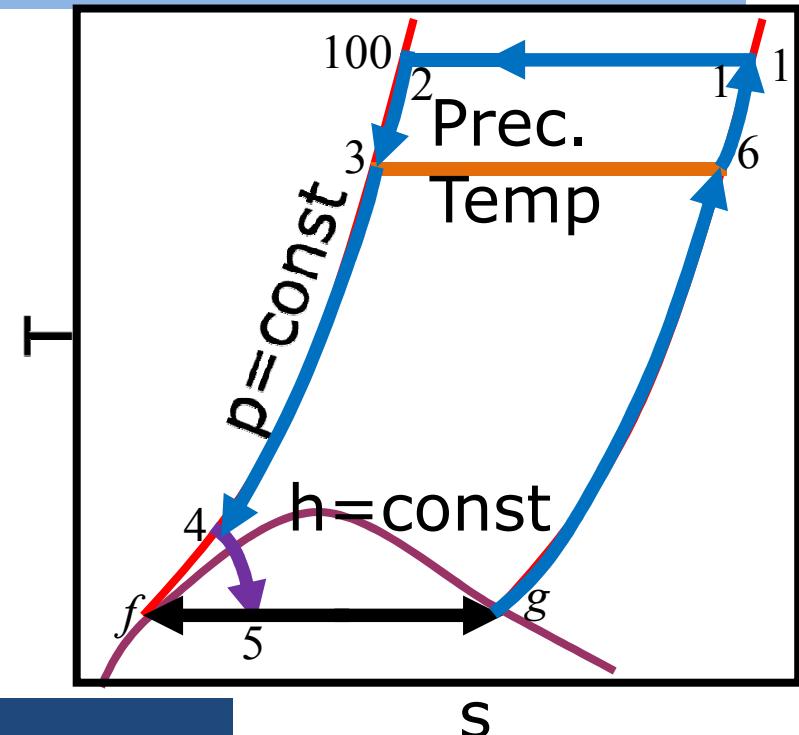
$$-\frac{W_c}{\dot{m}} = 300(4.42 - 3.1) - (462 - 445) + 0.08(482 - 390) = 386.3 \text{ J/g}$$

Tutorial – 1

- Work/unit mass of **N₂** liquefied

$$-\frac{W_c}{\dot{m}} = 386.3$$

$$y = 0.063$$



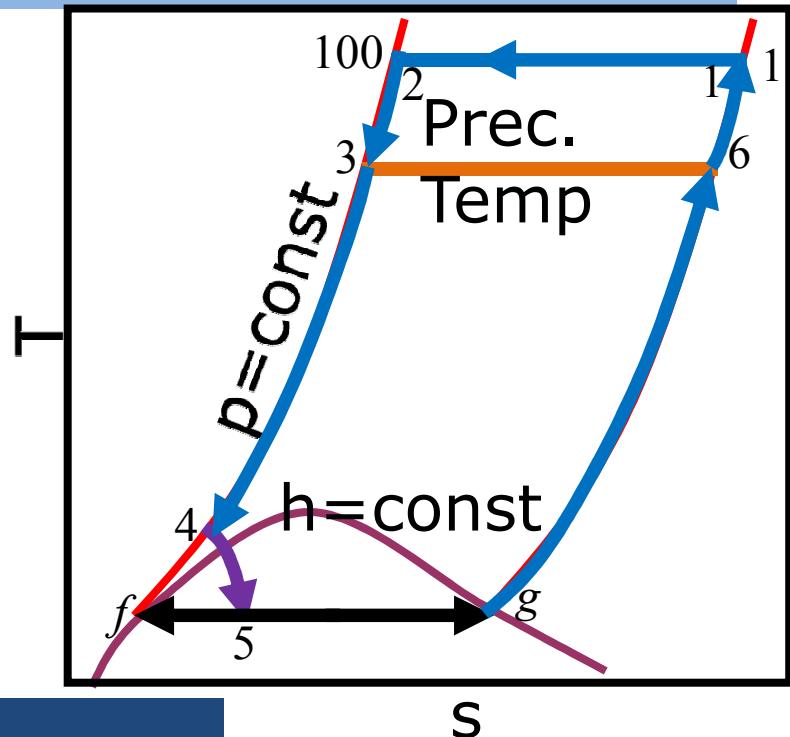
$$-\frac{W_c}{\dot{m}_f} = -\frac{W_c}{y \dot{m}} = \frac{386.3}{0.063} = 6131.7 \text{ J/g}$$

Tutorial – 1

- **Figure of Merit (FOM)**

$$-\frac{W_c}{\dot{m}_f} = 6131.7$$

$$-\frac{W_i}{\dot{m}_f} = 767$$



$$FOM = \frac{\frac{W_i}{\dot{m}_f}}{\frac{W_c}{\dot{m}_f}} = \frac{767}{6131.7} = 0.1251$$

Tutorial – 1

- Maximum Liquid yield**

$$y = y_{\max}$$

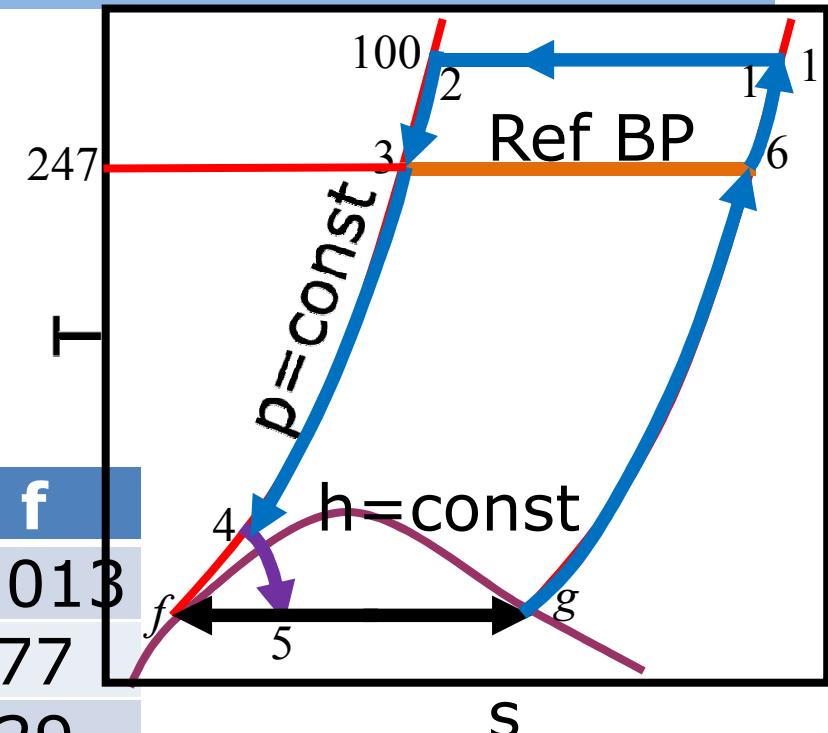
$$T_3 = T_6 = T_d = 247 \text{ K}$$

$$y_{\max} = \frac{h_6 - h_3}{h_6 - h_f}$$

$$r = 0.08$$

	3	6	f
p (bar)	101.3	1.013	1.013
T (K)	247	247	77
h (J/g)	380	408	29

$$y_{\max} = \frac{(408 - 380)}{(408 - 29)} = \frac{(28)}{(379)} = 0.074$$



Tutorial – 1

	Simple	Precooled	Max.
y	0.04	0.063	0.074
$-\frac{W_c}{\dot{m}}$	379	386.3	386.3
$-\frac{W_c}{\dot{m}_f}$	9475	6131.7	5220.2
FOM	0.081	0.1251	0.147

- Tabulating the results, we have the above comparison for Simple and Precooled Linde – Hampson System.